## 9. Boundary layers

#### Flow around an arbitrarily-shaped bluff body



Outer flow (effectively potential, inviscid, irrotational)

## 9.1. Boundary layer thickness

- Outer flow solution (ideal): U
- Inner flow: *u*
- Arbitrary threshold to mark the viscous layer boundary:

$$y = \delta$$
 for  $u(x, \delta) = 0.99 U$ 

•  $\delta$ : BL thickess (or velocity BL thickness)



Displacement (stagnation) layer thickness

$$A_1 = A_2$$

$$\int_{0}^{\infty} \left( U - u \right) dy = U \delta^{*}$$
$$\delta^{*} = \int_{0}^{\infty} \left( 1 - \frac{u}{U} \right) dy$$

Momentum thickness  $\theta$ Similar to displacement thickness, but accounts for momentum transfer defect in BL:

$$\theta = \int_{0}^{\infty} \frac{u}{U} \left( 1 - \frac{u}{U} \right) dy$$

## 9.2. Boundary layer equations

- Start with full Navier-Stokes (2D steady) near a flat surface
- Main assumption: thin boundary layer ( $\delta/x \ll 1$ )
- Order of magnitude analysis for terms of Navier-Stokes equation
  - $u \sim U$
  - $\partial/\partial x \sim 1/x$
  - $\partial u/\partial x \sim U/x$
  - $\partial/\partial y \sim 1/\delta$

• From contunuity equation...

$$\frac{U}{x} \sim \frac{\partial u}{\partial x} \sim \frac{\partial v}{\partial y} \sim \frac{v}{\delta}$$
$$v \sim U \frac{\delta}{x}$$

Examine the orders of terms in momentum equations

 $U \frac{U}{x} \frac{U\delta}{x} \frac{U}{\delta}$  $u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial x}$  $\frac{U^{2}}{\rho}$ ' <u>&</u> <sup>1</sup>  $\mathcal{U}$ 2 x x



Much smaller than  $U^2/x$  terms we keep in first equation

What remains of the continuity and momentum equations



**Boundary layer equations** 

Notable scalings



Pressure – same as in outer (ideal) flow

Bernoulli equation for outer flow

$$\frac{p}{\rho} + \frac{U^2}{2} = const$$

#### Thus

$$-\frac{1}{\rho}\frac{d p}{dx} = U\frac{d U}{d x}$$

Plug this into momentum equation to get rid of pressure

**Boundary conditions** 

$$u(x,0) = 0$$
  

$$v(x,0) = 0$$
  

$$u(x,y) \rightarrow U \text{ as } y \rightarrow \infty$$

#### 9.3. Blasius solution

- Flat plate, U = const, p = const
- Boundary layer equations become



Reformulate for streamfunction  $\psi$ 

$$u = \frac{\partial \psi}{\partial y}, \quad v = -\frac{\partial \psi}{\partial x}$$

Continuity satisfied automatically, momentum equation is

$$\frac{\partial \psi}{\partial y} \frac{\partial^2 \psi}{\partial x \partial y} - \frac{\partial \psi}{\partial x} \frac{\partial^2 \psi}{\partial y^2} = v \frac{\partial^3 \psi}{\partial y^3}$$

No length scale!

Dimensional variables:  $x, y, v, U \rightarrow n = 4$ 

Dimensionally independent units: L, t  $\rightarrow k = 2$ For Buckingham's  $\pi$ -theorem, n - k = 2Look for

$$\psi/\nu = f(\pi_1, \pi_2)$$

Look for

$$\pi_1 = y^{a_{11}} U^{a_{21}} x^{a_{31}} v^{a_{41}}, \quad \pi_2 = y^{a_{12}} U^{a_{22}} x^{a_{32}} v^{a_{42}}$$

Construct a dimensional matrix

$$M = \begin{bmatrix} v & U & x & v \\ 1 & 1 & 1 & 2 \\ 0 & -1 & 0 & -1 \end{bmatrix} t$$

Find its kernel vectors  $a_i = (a_{1i}, a_{2i}, a_{3i}, a_{4i}), i = 1,2:$   $Ma_i^{T} = (0,0)$  $a_1 + a_2 + a_3 + 2 a_4 = 0$ 

 $a_{2}+a_{4}=0$ 

This simplifies to

L

$$a_1 + a_3 + a_4 = 0$$
  

$$a_2 = -a_4$$
  
Let  $a_{21} = 1/2$ , then  $a_{41} = -1/2$  and  

$$a_{11} + a_{31} = 1/2$$
  

$$a_{11} = 1, a_{31} = -1/2$$
 would fit, so

$$\pi_1 = y U^{1/2} x^{-1/2} v^{-1/2} = \frac{y}{\sqrt{\frac{v}{U}}} \sim \frac{y}{\delta}$$
  
Let  $a_{12} = 0$ ,  $a_{32} = 1$ , then  $a_{42} = -1$ ,  $a_{22} = 1$ :

$$\pi_2 = \frac{Ux}{v} = Re_x \sim \frac{x^2}{\delta^2}$$

#### Look for

 $\frac{\Psi}{V} = Re_x^n f\left(\frac{y}{\delta}\right)$ 

Not how Blasius did it though...

Blasius approach -

Similarity variable – clearly  $\eta = y/\delta$ How to nondimensionalize  $\psi$ ?

Let 
$$\psi \sim f(\eta)$$
, then  

$$u = \frac{\partial \psi}{\partial y} \sim \frac{d f}{d \eta} \frac{\partial \eta}{\partial y} = f' \frac{1}{\delta} = f' \sqrt{\frac{U}{vx}}$$

For  $\eta = const$ , u = const (otherwise velocity profiles would not be self-similar), thus  $\psi \sim x^{1/2} f(\eta)$ 

Rewrite this as  $\psi \sim Re_x^{1/2} f(\eta)$ 

dimensional dimensionless

Easy to fix that...  $\frac{\psi}{\mathbf{v}} = \sqrt{Re_x} f(\eta)$ 

So, look for

$$\psi = v \sqrt{\frac{Ux}{v}} f\left(\frac{y}{\sqrt{vx/U}}\right) = \sqrt{Uxv} f\left(\frac{y}{\sqrt{vx/U}}\right)$$

Plug this into momentum equation and BC to get...

$$f''' + \frac{1}{2}ff'' = 0 \quad \text{Blasius equation}$$
$$f(0) = f'(0) = 0$$
$$f'(\eta) \rightarrow 1, \ \eta \rightarrow \infty$$

Solve numerically to get some notable results For a plate of length *x*, drag coefficient



## 9.4. Falkner-Skan solutions

Look for solutions in the form (generalized from Blasius solution)

$$u(x, y) = U(x) f'(\eta), \quad \eta = \frac{y}{\xi(x)}$$
  
Outer flow solution

The corresponding streamfunction form is  $\psi(x, y) = U(x)\xi(x)f(\eta)$ 

Continuity satisfied, plug  $\psi$  into *x*-momentum equation...

$$\frac{\partial \psi}{\partial y} \frac{\partial^2 \psi}{\partial x \partial y} - \frac{\partial \psi}{\partial x} \frac{\partial^2 \psi}{\partial y^2} = U \frac{dU}{dx} + v \frac{\partial^3 \psi}{\partial y^3}$$

The momentum equation becomes...

$$f''' + \left[\frac{\xi}{\nu}\frac{d}{dx}(U\xi)\right]ff'' + \left[\frac{\xi^2}{\nu}\frac{dU}{dx}\right]\left(1 - (f')^2\right) = 0$$
*x*-dependent parts

For a similarity solution to exist, must have:

$$\alpha = \frac{\xi}{v} \frac{d}{dx} (U\xi) = const$$
$$\beta = \frac{\xi^2}{v} \frac{dU}{dx} = const$$

The Falkner-Skan approach (counterintuitive but neat)

- Choose  $\alpha$ ,  $\beta$
- Solve  $\alpha = ..., \beta = ...$  for *U*,  $\xi$ : does *U*(*x*) correspond to any useful outer flow?
- If yes, solve this system for f with chosen  $\alpha$ ,  $\beta$   $f''' + \alpha f f'' + \beta [1 - (f')^2] = 0$  f(0) = f'(0) = 0 $f'(\eta) \rightarrow 1, \eta \rightarrow \infty$
- Combine *U*, *y*, *f* to construct streamfunction:  $\psi(x, y) = U(x)\xi(x)f\left(\frac{y}{\xi(x)}\right)$

#### Example: $\alpha = 1/2$ , $\beta = 0$ : Blasius solution

#### 9.5. Flow over a wedge

• 
$$\alpha = 1, 0 < \beta < 1$$
:



## 9.6. Stagnation-point flow

•  $\alpha = 1, \beta = 1$ :



## 9.7. Flow in a convergent channel

- $\alpha = 0, \ \beta = 1$ :
- U(x) = -c/x,  $V = 0 \text{limit case } (Re \to \infty)$  for convergent wedge flow!
- No BL solution for divergent flow exists (which is physically correct!)

## 9.8. Approximate solution for a flat surface

 A demonstration of the widely applicable integral method developed by von Kármán (later refined by Ernst Pohlhausen)



Theodore von Kármán, 1881-1963

Flow over a flat plate, U = p = constBL equations for this case...

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$
$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = v \frac{\partial^2 u}{\partial y^2}$$

Rewrite first term in momentum equation...

$$u\frac{\partial u}{\partial x} = \frac{1}{2}\frac{\partial}{\partial x}\left(u^{2}\right) = \frac{\partial}{\partial x}\left(u^{2}\right) - u\frac{\partial u}{\partial x} =$$
$$= \frac{\partial}{\partial x}\left(u^{2}\right) + u\frac{\partial v}{\partial y}$$
From continuity equation

Momentum equation becomes

$$\frac{\partial}{\partial x} (u^2) + u \frac{\partial v}{\partial y} + v \frac{\partial u}{\partial y} = v \frac{\partial^2 u}{\partial y^2}$$
$$\frac{\partial}{\partial y} (uv)$$

Integrate this in *y* from surface to BL edge

$$\int_{y=0}^{\delta} \left[ \frac{\partial}{\partial x} \left( u^2 \right) + \frac{\partial}{\partial y} \left( u v \right) \right] dy = v \int_{y=0}^{\delta} \frac{\partial^2 u}{\partial y^2} dy$$

$$\int_{y=0}^{\delta} \frac{\partial}{\partial x} (u^2) dy + uv \Big|_{y=0}^{y=\delta} = v \frac{\partial u}{\partial y} \Big|_{y=0}^{y=\delta}$$

#### Note that

$$\begin{split} u \Big|_{y=0} &= v \Big|_{y=0} = 0 \quad \text{No slip on surface} \\ u \Big|_{y=\delta} &= U \quad \begin{array}{c} \text{Transition to outer flow} \\ \text{at BL edge is continuous} \\ \hline \frac{\partial u}{\partial y} \Big|_{y=\delta} &= 0 \quad \begin{array}{c} \text{Transition to outer flow} \\ \text{at BL edge is smooth} \\ \text{shear stress } \tau_0 \text{ as} \end{split}$$

**Define surface** 

$$\tau_0 = \mu \frac{\partial u}{\partial y} \bigg|_{y=0}$$

The integral becomes

$$\int_{y=0}^{\delta} \frac{\partial}{\partial x} (u^2) dy + U v(x, \delta) = -\frac{\tau_0}{\rho}$$

Integrate continuity equation to evaluate the Uv term in momentum equation

$$\int_{y=0}^{y=\delta} \left( \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} \right) dy = 0$$
  
$$\int_{y=0}^{y=\delta} \frac{\partial u}{\partial x} dy + v \Big|_{y=0}^{y=\delta} = 0$$
  
$$v(x, \delta) = -\int_{y=0}^{y=\delta} \frac{\partial u}{\partial x} dy$$

Substitute this into the momentum equation -

$$\int_{y=0}^{\delta(x)} \frac{\partial}{\partial x} (u^2) dy - U \int_{y=0}^{\delta(x)} \frac{\partial u}{\partial x} dy = -\frac{\tau_0}{\rho}$$

#### Leibniz integral rule

For an integral of f(x,y) with variable limits,

$$\int_{\alpha(x)}^{\beta(x)} \frac{\partial f}{\partial x} dy = \frac{d}{dx} \int_{\alpha(x)}^{\beta(x)} f dy - f(x, \beta) \frac{d\beta}{dx} + f(x, \alpha) \frac{d\alpha}{dx}$$



Step reckoner by G.W. Leibniz (1673) – mechanical computer for addition and multiplication



Gottfried Wilhelm Leibniz (1646-1716)

Apply Leibniz integral rule to momentum equation integral...

$$\int_{y=0}^{\delta(x)} \frac{\partial}{\partial x} (u^2) dy - U \int_{y=0}^{\delta(x)} \frac{\partial}{\partial x} u dy = -\frac{\tau_0}{\rho}$$
$$\frac{d}{dx} \int_{y=0}^{\delta(x)} u^2 dy - u^2 |_{y=\delta} \frac{d\delta}{dx} - U \left[ \frac{d}{dx} \int_{y=0}^{\delta(x)} u dy - u |_{y=\delta} \frac{d\delta}{dx} \right] = -\frac{\tau_0}{\rho}$$
$$\int_{y=0}^{\delta(x)} u^2 dy - U^2 \frac{d\delta}{dx} - U \frac{d}{dx} \int_{y=0}^{\delta(x)} u dy + U^2 \frac{d\delta}{dx} = -\frac{\tau_0}{\rho}$$

 $\frac{d}{dx}$ 

Momentum equation integral is...

$$\frac{d}{dx} \int_{y=0}^{\delta(x)} u^2 dy - U \frac{d}{dx} \int_{y=0}^{\delta(x)} u dy = -\frac{\tau_0}{\rho}$$

$$-\frac{d}{dx}\int_{y=0}^{\delta(x)} \left(u^2 - Uu\right) dy = \frac{d}{dx}\int_{y=0}^{\delta(x)} u\left(U - u\right) dy = \frac{\tau_0}{\rho}$$
  
Momentum integral for Blasius BL

**Physical meaning**: momentum change in BL is due to surface shear

#### General procedure for the von Kármán-Pohlhausen method

- Represent the unknown velocity profile with a polynomial (a general profile should have a polynomial series expansion?)
- Fit the polynomial constants to match known boundary conditions

$$u(x,0)=0$$

$$u(x,\delta) = U$$

$$\partial u/\partial y(x,\delta) = 0$$

 Can impose further boundary conditions (as needed to determine polynomial coefficients)

#### Additional boundary conditions



(For more BC, apply derivatives of momentum equation, etc.)

- Apply the BC to determine polynomial coefficients (as functions of  $\delta)$
- Plug the velocity profile polynomial into momentum integral, integrate, solve resulting ODE for  $\delta = \delta(x)$
- Find drag coefficient, etc.

Similar procedure can be applied to freesurface and other flows (replace unknown functions with polynomials, satisfy BC, satisfy conservation eqs.) For a flat-plate BL, look for

$$\begin{aligned} u &= a_0 + a_1 y + a_2 y^2 \\ u(0) &= 0 \\ u(\delta) &= U \\ \frac{\partial u}{\partial y} \bigg|_{y=\delta} = 0 \end{aligned}$$

This only works for zero pressure gradient!

From BC at 
$$y = 0$$
,  $a_0 = 0$   
 $\frac{\partial u}{\partial y} = a_1 + 2 a_2 y$ ,  $\frac{\partial u}{\partial y}\Big|_{y=\delta} = a_1 + 2 a_2 \delta = 0$ 

Thus from second BC at  $y = \delta$ ,

$$a_1 = -2a_2\delta$$

Now use first BC at  $y = \delta$ 

$$u(\delta) = a_0 + a_1 \delta + a_2 \delta^2 = U$$
  
$$a_2 \left(-2 \delta^2 + \delta^2\right) = U$$
  
$$a_2 = -\frac{U}{\delta^2}, \quad a_1 = 2\frac{U}{\delta}$$

Polynomial expression for *u* to plug into momentum integral

$$\frac{u}{U} = 2\frac{y}{\delta} - \left(\frac{y}{\delta}\right)^2 = 2\eta - \eta^2$$
$$\eta = \eta(x, y) = \frac{y}{\delta(x)} \quad \text{We've seen this one} \\ \text{before...}$$

Rewrite the momentum integral a bit...

$$\frac{d}{dx} \int_{y=0}^{\delta(x)} u (U-u) dy = U^2 \frac{d}{dx} \int_{y=0}^{\delta(x)} \frac{u}{U} \left(1 - \frac{u}{U}\right) dy = \frac{\tau_0}{\rho}$$

Plug in expression for u/U

$$\frac{d}{dx} \int_{y=0}^{\delta(x)} \frac{u}{U} \left( 1 - \frac{u}{U} \right) dy = \frac{d}{dx} \int_{y=0}^{\delta(x)} \left( 2\eta - \eta^2 \right) \left( 1 - 2\eta + \eta^2 \right) dy$$

Evaluate the integral

$$\int_{y=0}^{\delta(x)} (2\eta - \eta^2) (1 - 2\eta + \eta^2) dy =$$
  
= 
$$\int_{y=0}^{\delta(x)} (2\eta - \eta^2 - 4\eta^2 + 2\eta^3 + 2\eta^3 - \eta^4) dy$$

Collect terms

$$= \int_{y=0}^{\delta(x)} \left( -\eta^4 + 4\eta^3 - 5\eta^2 + 2\eta \right) dy$$

Variable substitution  $y \rightarrow \eta$ ,  $y = \delta \eta$ ,  $dy = \delta d\eta$  and  $y = \delta \rightarrow \eta = 1$ 



Plug the evaluated integral back...

$$U^2 \frac{d}{dx} \left( \frac{2}{15} \delta \right) = \frac{\tau_0}{\rho}$$

Use the definition of surface shear stress

$$\tau_0 = \mu \frac{\partial u}{\partial y} \bigg|_{y=0}$$

Recall that  

$$u = U\left(2\frac{y}{\delta} - \left(\frac{y}{\delta}\right)^{2}\right)$$

$$\frac{\partial u}{\partial y} = U\left(\frac{2}{\delta} - 2\frac{y}{\delta^{2}}\right), \quad \frac{\partial u}{\partial y}\Big|_{y=0} = 2\frac{U}{\delta}$$

Plug that into the ODE for  $\delta$ 

$$U^{2} \frac{d}{dx} \left( \frac{2}{15} \delta \right) = \frac{\mu}{\rho} \frac{2U}{\delta}$$

A more compact form

$$\delta' \delta = 15 \frac{v}{U}$$
$$\frac{1}{2} \left( \delta^2 \right)' = 15 \frac{v}{U}$$

Integrate...

$$\delta^2 = 30 \frac{v x}{U} + C$$

Since at x = 0  $\delta = 0$ , C = 0 and

$$\delta = \sqrt{30 \frac{v x}{U}}$$

Note that



Compare with exact result:  $\frac{\delta}{x} \approx \frac{5}{\sqrt{Re_x}}$ 

Error < 10%, despite a very crude approximation

### 9.9. General momentum integral

Similar reasoning, but for an arbitrary BL with non-zero pressure gradient in the *x*-direction

Momentum equation (with pressure eliminated using Bernoulli equation for outer flow)...

$$u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y} = U\frac{dU}{dx} + v\frac{\partial^2 u}{\partial y^2}$$

...can be similarly rewritten as...

$$\frac{\partial}{\partial x} \left( u^2 \right) + \frac{\partial}{\partial y} \left( uv \right) = U \frac{d U}{d x} + v \frac{\partial^2 u}{\partial y^2}$$

Integrate this in *y* from 0 to  $\delta$  to obtain

$$\frac{d}{dx} \left( U^2(x) \theta \right) + U \delta^* \frac{dU}{dx} = \frac{\tau_0}{\rho}$$

where

$$\delta^* = \int_0^\infty \left( 1 - \frac{u}{U} \right) dy \quad \text{Displace}$$

cement thickness

$$\theta = \int_{0}^{\infty} \frac{u}{U} \left( 1 - \frac{u}{U} \right) dy$$

Momentum thickness

# 9.10. von Kármán – Pohlhausen approximation

- Consider velocity profile in the form of a 4<sup>th</sup> order polynomial (allows to account for nonuniform freestream velocity and nonzero pressure gradient)
- Apply five boundary conditions to find coefficients (two added conditions – second derivatives at y = 0 and y = δ)
- Plug resulting polynomial into expressions for  $\delta^{*},\,\theta,\,\tau_{_{0}}$
- Substitute results into general momentum integral, solve ODE for  $\delta(x)$

## **Boundary-layer separation**

**BL** momentum equation

$$u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y} = -\frac{1}{\rho}\frac{d p}{d x} + v\frac{\partial^2 u}{\partial y^2}$$

Apply this equation at y = 0

$$0 = -\frac{1}{\rho} \frac{d p}{d x} + v \frac{\partial^2 u}{\partial y^2} \bigg|_{y=0}$$

Pressure gradient of the outer flow determines velocity profile curvature on the surface!

## Non-negative dp/dx: non-positive curvature of velocity profile throughout BL



Now suppose we have negative dp/dx:

curvature of velocity profile near the boundary will be positive  $\mathbf{A}^{y}$ 

same curvature near the BL edge must approach zero from the negative direction (otherwise – no smooth transition to outer flow!)



A point of inflection must exist in velocity profile (where curvature changes sign)



## Velocity profiles for increasing adverse pressure gradient



#### Separated boundary layers



Roshko, early 1950s



Vorobieff & Ecke, XIIth century



Flometrics.com, 2011

### 9.12. Boundary layer stability

Consider a narrow strip of a boundary layer and a small perturbation to steady-state velocity and pressure:

$$\begin{aligned} u(x, y, t) &= u(y) + u'(x, y, t) \\ v(x, y, t) &= v'(x, y, t) \\ p(x, y, t) &= p(x) + p'(x, y, t) \end{aligned}$$
$$\begin{aligned} \left| \frac{u'}{u} \right| \ll 1, \quad \left| \frac{v'}{u} \right| \ll 1, \quad \left| \frac{p'}{p} \right| \ll 1 \end{aligned}$$

Perturbation – same scale as v (which is small), so consider entire v as perturbation (no loss of generality) Plug these *u*, *v*, *p* into Navier-Stokes (not BL) equations

Linearize

Introduce a perturbation streamfunction

$$u' = \frac{\partial \psi}{\partial y}, \quad v' = -\frac{\partial \psi}{\partial x}$$

Continuity eliminated, rewrite the momentum equations in terms of  $\boldsymbol{\psi}$ 

Cross-differentiate *x*-momentum equation in *y*, *y*-momentum equation in x

Get rid of the pressure term...

Result:  $4^{th}$  order linear PDE for  $\psi$ Consider the streamfunction in the form

$$\psi = \psi(y) e^{i\alpha(x-ct)}$$

- c speed of perturbation propagation
- $\alpha$  perturbation wavenumber ( $\alpha = 2\pi/\lambda$ )
- If c is real (Im c = 0), perturbation is *neutrally* stable (propagates but does not grow)
- If Im c < 0, perturbation is decaying

If Im c > 0, perturbation grows and the **boundary** layer is unstable

Plugging the variable-separated form of y into the momentum equation reduces it to a 4<sup>th</sup> order ODE

$$(u-c)(\psi''-\alpha^2\psi)-u''\psi=\frac{\nu}{i\alpha}(\psi^{(4)}-2\alpha^2\psi''+\alpha^4\psi)$$

The Orr-Somerfeld equation

#### **Boundary conditions**

 $\psi(0) = \psi'(0) = 0$  (perturbations go to zero on body surface)

 $\psi(y) \rightarrow 0, \psi'(y) \rightarrow 0, y \rightarrow \infty$  (perturbations decay away from the boundary layer)

For every wavelength  $\alpha$ , solve for c, determine stability

#### Results of stability analysis



**Note.** We look for a 2D perturbation... but what if the flow first becomes unstable in zdirection? Such instability exists, but luckily, the flow is less stable to xy perturbations

#### Effects of local pressure gradient on stability







Favorable pressure gradient expands stability region, adverse pressure gradient shrinks it

