#### Activated Sludge Design, Startup, Operation, Monitoring and Troubleshooting

- Ohio Water Environment Association
- Plant Operations Workshop
- Columbus, Ohio
- September 1, 2010

- Phil Anderson
- Operations Specialist





# Design - Activated Sludge

- Design Team
- Treatment Goals
- Activated Sludge Processes
- Engineering Standards
- Preliminary Treatment
- Tertiary Treatment

## Treatment Goals

#### BOD Removal

 Dissolved wastes are consumed as food by the activated sludge microbes and converted to biomass, water, carbon dioxide, and other gases

#### • Nitrification

- The process through which ammonia is oxidized to nitrite and nitrate
- Denitrification
  - A process by which nitrates and nitrites are converted to gaseous end products, primarily nitrogen gas.

## Activated Sludge Processes

Conventional – CBOD Removal Plug or Step Feed **Single-Stage Nitrification Oxidation Ditch - Vertical Loop** Reactor Extended Aeration MBR BNR

## **Additional Processes**

 Preliminary Treatment -Screening -Grit Removal Tertiary Treatment - Filters Solids Handling

Recycle Flows

# Design – Engineering Standards

 Design of Municipal Wastewater Treatment Plants WEF Manual of Practice No. 8

 Wastewater Engineering, Treatment, Disposal, Reuse
 Metcalf & Eddy

### Design – Engineering Standards

**Recommended Standards for Wastewater Facilities** 

Policies for the Design, Review, and Approval of Plans and Specifications for Wastewater Collection and Treatment Facilities

MEMBER STATES AND PROVINCE Illinois Indiana Iowa Michigan Minnesota Missouri New York Ohio Ontario Pennsylvania Wisconsin

**Ten States Standards** 

# Process Design

### Physical

–Aeration Tank Capacity - Ibs. CBOD/1000 CF of Aeration

Temperature – Summer/Winter
Final Settling – Circular Center Feed or Peripheral Feed

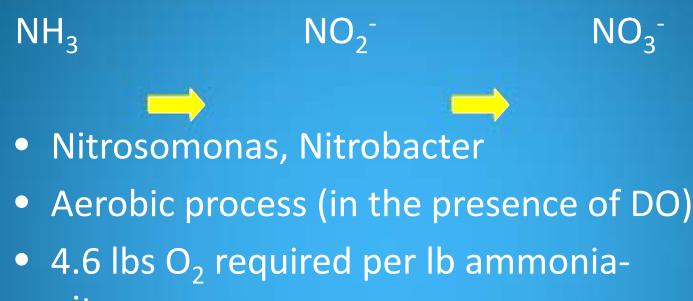
## Process Design

## Chemical —Ammonia Loading - Nitrification —Phosphorous Loading & Removal —pH & Alkalinity

## Process Design

 Biological -CBOD Loading - 15lbs - 40 lbs -D.O. in Aeration - 1.1 CBOD - 4.6 NH3 -MLSS, MLVSS, RAS -F/M Ratio - 0.5 - 1.0 - 2.0 -MCRT Days

### Nitrification



nitrogen

- 7.14 lb alkalinity is consumed per pound of ammonia nitrogen
- pH sensitive with optimal range between
   7.5 and 8.6

## Denitrification

 $NO_3^- \rightarrow NO_2^- \rightarrow NO \rightarrow N_2O \rightarrow N_2O$ 

- Anoxic process (not in the presence of DO)
- Nitrification can decrease pH
- Denitrification recovers 3.57 lb alkalinity per lb of nitrogen removed
- DO is consumed by nitrification and denitrification recovers 2.9 lb per lb of nitrogen removed

# Plant Startup

- Contractor Wants to push to startup
- What are Ohio EPA expectations?
- Manufacturer Checkout
- Operator Training Are You Ready
- What additional processes are available
- Do you and your Engineer have a Process Control Plan
- Are you seeding the aeration tanks?

# **Plant Operation**

- Summer/Winter
- Dry Weather/Wet Weather
- DO Control
- RAS Rate % Of Influent Flow
- Chemical Feed
- Wasting Sludge Biological & Chemical

#### Summer Verses Winter

Summer
MCRT - 22.17 days
F/M Ratio - 0.13
BOD Loading Rate - 16.5 lbs./1,000 cf

Required MCRT No.2 - 7.6 days
DT for BOD Oxidation - 13.20 hours
DT for NH3 Oxidation - 2.64 hours

•Aeration Tanks Required - 4.0

•MLSS - 3,000 mg/l •MLVSS - 2,100 mg/l Winter •MCRT - 35.47 days •F/M Ratio - 0.08 •BOD Loading Rate - 16.5 lbs./1,000 c.f.

Required MCRT No.2 - 13.7 days
DT for BOD Oxidation - 13.15 hours
DT for NH3 Oxidation = 2.71 hours

•Aeration Tanks Required - 4.0

•MLSS - 4,800 mg/l •MLVSS - 3,360 mg/l

# **Plant Operation**

- Summer/Winter
- Dry Weather/Wet Weather
- DO Control
- RAS Rate % Of Influent Flow
- Chemical Feed
- Wasting Sludge Biological & Chemical

# **Plant Monitoring**

- Regular Rounds Visual
- Aeration Tanks & FST
- Blowers/Aerators
- RAS Pumps
- Clarity of the Effluent

# Plant Monitoring

- SCADA Trending Flow, DO, ORP, pH
- Regular Rounds Visual
- Trending Instruments Flow, DO, ORP, pH
- Lab Data MLSS, RAS, Settling
- Microbiology

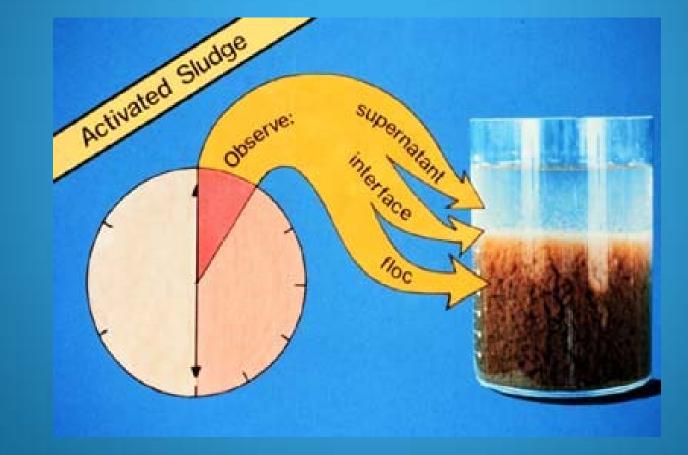
# Troubleshooting

- Foaming
- Bulking
- Solids Loss
- Turbid Effluent
- Odor
- No CBOD or Ammonia Removal

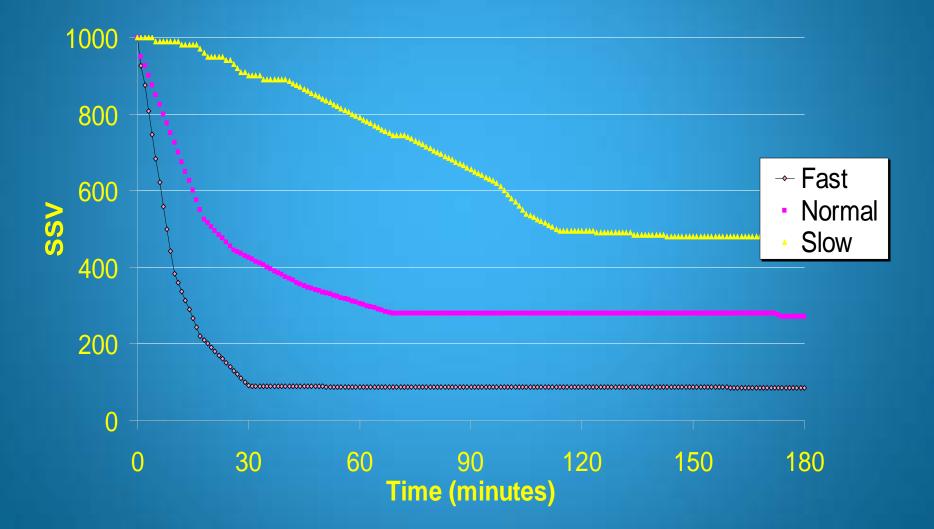
# Holy Crap!!



### **Observation of Settlometer Test**

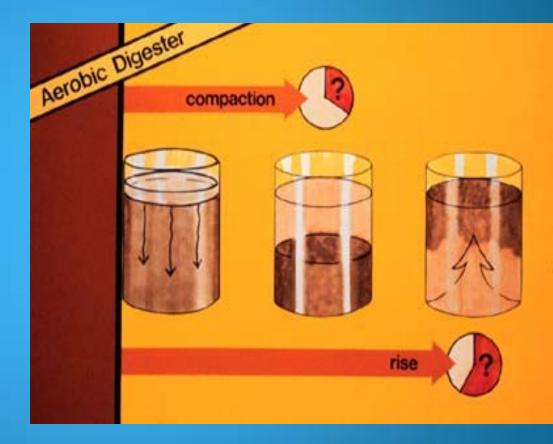


#### **Characteristic Sludge Settling**



### Length of Settleometer Test

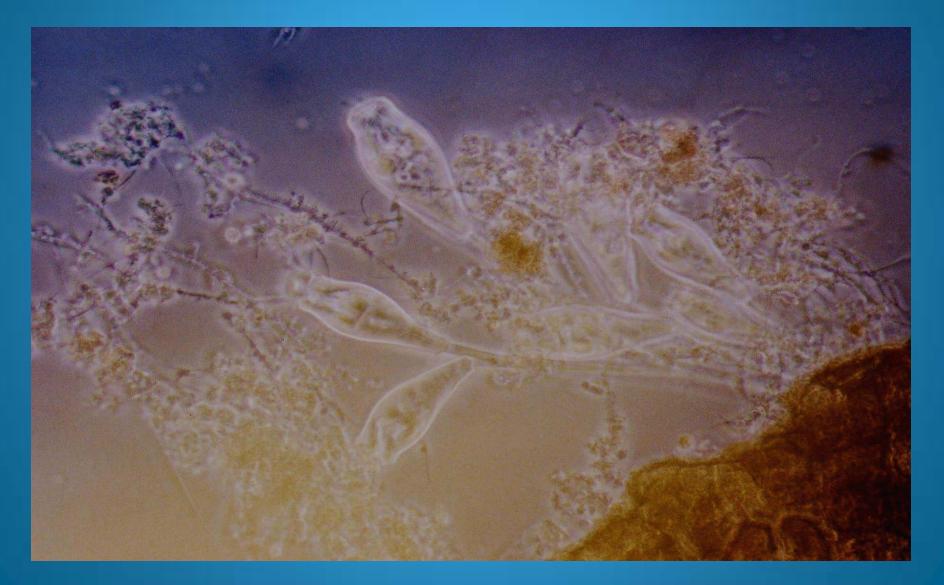
- Normal 30 minutes to 2 hours - until complete compaction
- Extended until the sludge begins to rise



### Look Under the Microscope



### The Bugs - Good/Bad/Ugly

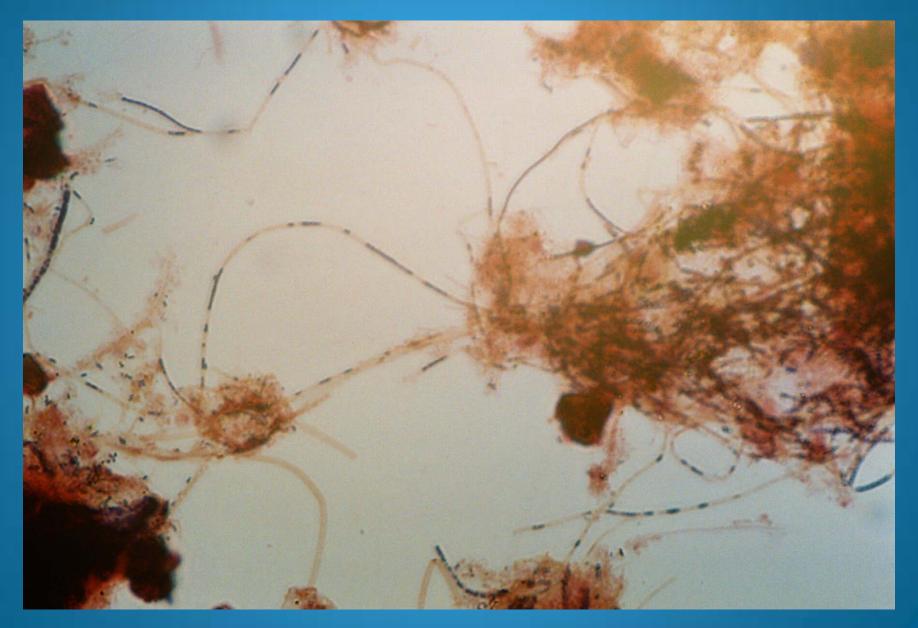




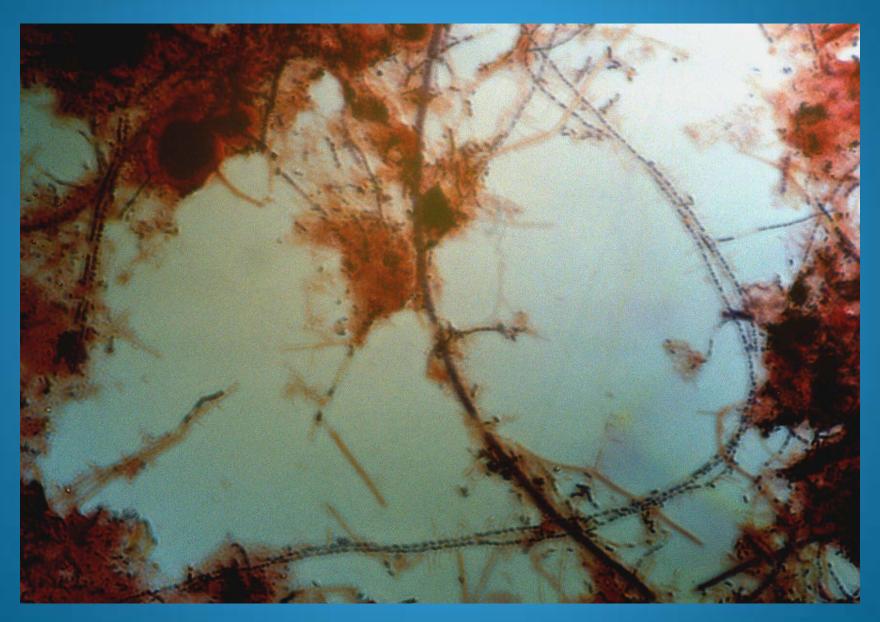
#### Nocardia



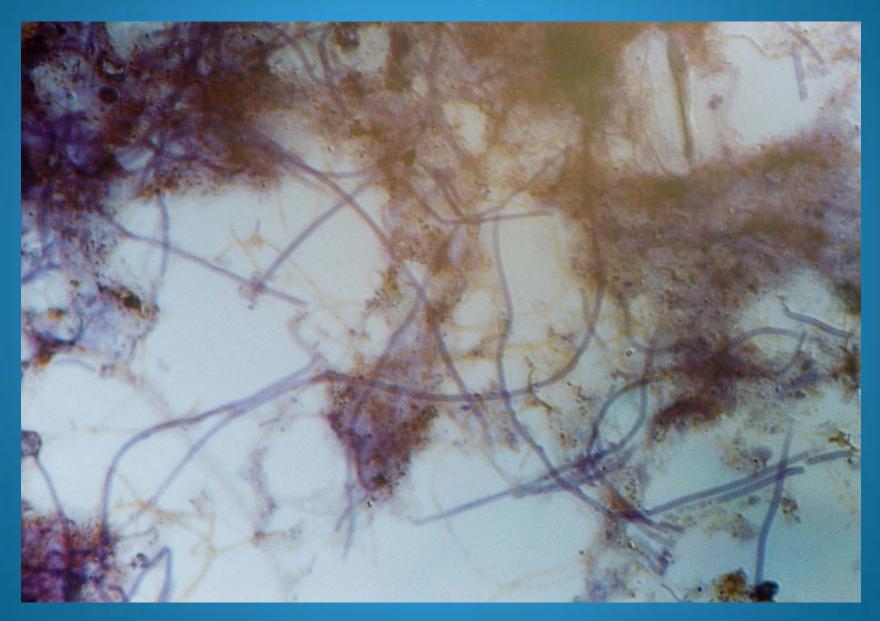
#### Microthrix parvicella



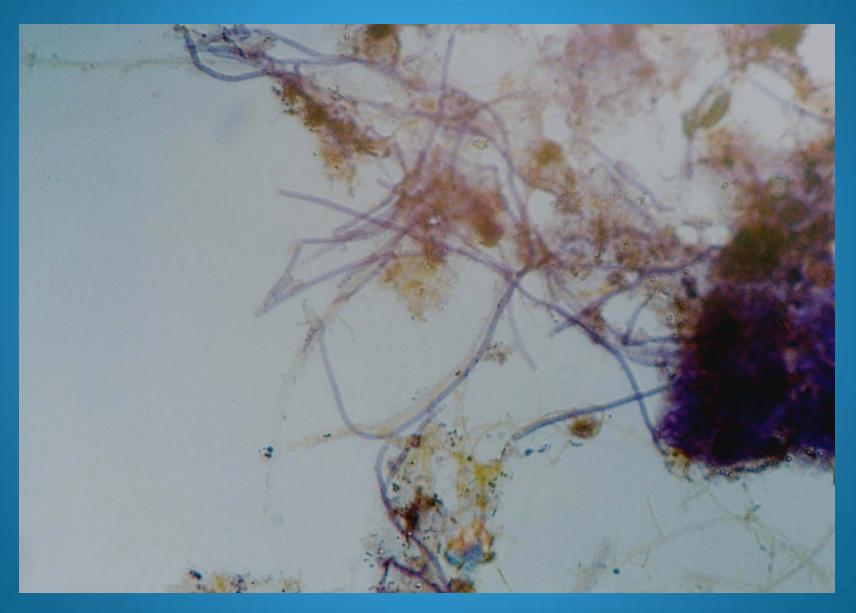
#### Filaments 1851 and 0041



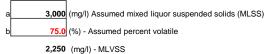
#### Filament Type 0092

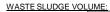


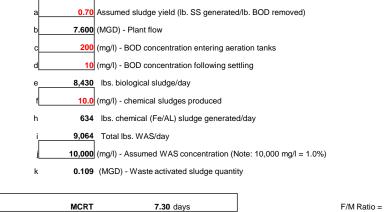
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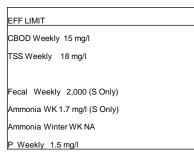


WWTP:	WWTP	Phil Anderson - ARCADIS panderson@arcadis- By:us.com			Summer Summar	
Operation:	Activated Sludge	Date: Summer 2009	3,000	MLSS, mg/l	MCRT	7.30 days
			20.0	Degrees C	F/M Ratio	0.24
	MEAN CELL RESIDENCE TIME (MCRT)		7.1	рН	BOD Loading Rate	33.54 lbs./1,000 c.f.
			5.0	D.O. Aeration	Required MCRT No.1	3.61 days
		20.0 Influent Ammonia	1.7	Effluent Ammonia	Required MCRT No.2	3.93 days
INPUT DATA:	· · · · · · · · · · · · · · · · · · ·		6	Aeration Tanks On Line	DT for BOD Oxidation	6.02 hours
	a 2.827 (MG) - Aeration tank volume (total)		0.471	Aeration Tank MG Each	DT for NH3 Oxidation	1.49 hours
	b       2,250       (mg/l) - Mixed liquor VOLATILE suspend         c       0.033       (MGD) - Daily flowrate of waste activated         d       10,000       (mg/l) - WAS suspended solids         e       7.600       (MGD) - Plant flow         f       10       (mg/l) - Effluent suspended solids				Aeration Tank Vol Required Aeration Tanks Required <u>Aeration Tanks On Line</u> MLSS MLVSS Nitrifiers (8% of MLVSS)	2.38 MG 5.05 6.00 3,000 mg/l 2,250 mg/l 180 mg/l
SUPPLEMENT/	TAL CALCULATIONS (MLVSS):					



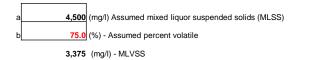




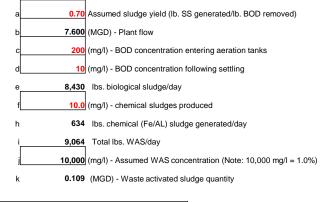


WWTP:     WWTP       By:panderson@arcadis-us.com				Winter Summary	
Operation: Activated Sludge	Date: Winter	4,500 11.0	MLSS, mg/l Degrees C	MCRT F/M Ratio	10.95 days 0.16
MEAN CELL RESIDENCE TIME (MCRT)		7.0 4.0	pH D.O. Aeration	BOD Loading Rate Required MCRT No.1	33.54lbs./1,000 c.f. 12.00 days
INPUT DATA:	20.0 Influent Ammonia	4.0 6	Effluent Ammonia Aeration Tanks On Line	Required MCRT No.2 DT for BOD Oxidation	8.66 days 10.96hours
a (MG) - Aeration tank volume (to	al)	0.471	Aeration Tank MG Each	DT for NH3 Oxidation	2.13hours
b 3,375 (mg/l) - Mixed liquor VOLATILE suspended solids (MLVSS) c 0.109 (MGD) - Daily flowrate of waste activated sludge (WAS) [See below]				Aeration Tank Vol Required Aeration Tanks Required	3.47MG 7.36
d 10,000 (mg/l) - WAS suspended solids e 7.600 (MGD) - Plant flow				Aeration Tanks On Line MLSS	6.00 4,500 mg/l
f <u>10</u> (mg/l) - Effluent suspended soli	ds			MLVSS Nitrifiers (8% of MLVSS)	3,375 mg/l 270 mg/l

#### SUPPLEMENTAL CALCULATIONS (MLVSS):



#### WASTE SLUDGE VOLUME:

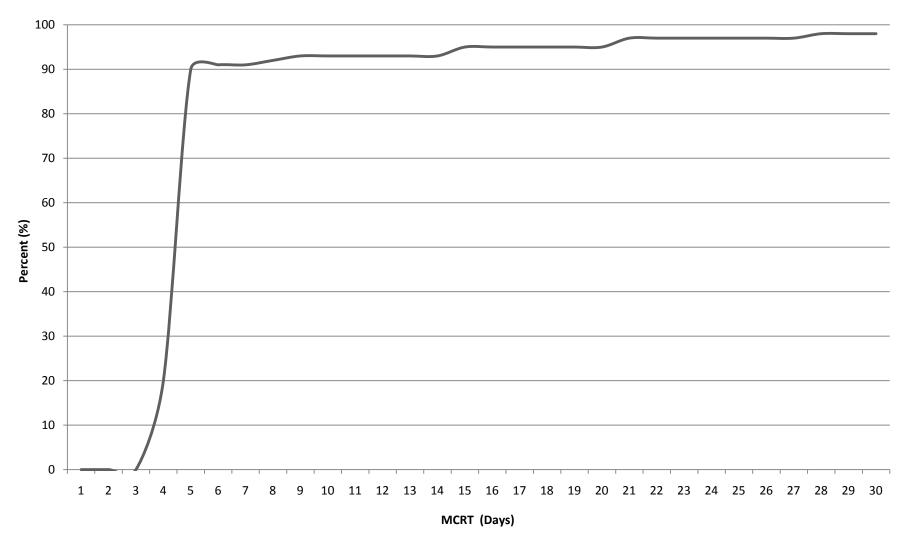


EFFLUENT LIMITS		
CBOD Weekly 15 mg/l		
TSS Weekly 18 mg/l		
Fecal Weekly 2,000 (S Only)		
Ammonia WK 1.7 mg/l (S Only)		
Ammonia Winter WK NA		
P Weekly 1.5 mg/l		

BOD Loading Rate =

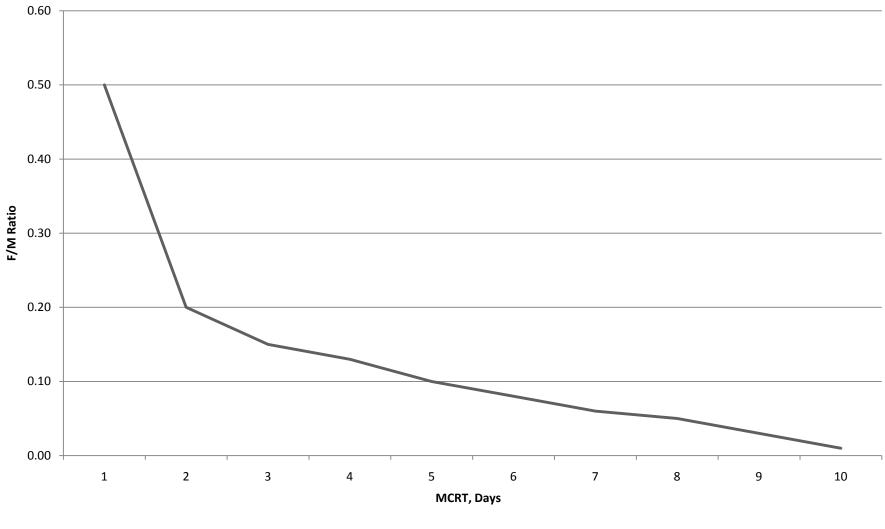


33.5 lbs./1,000 c.f.

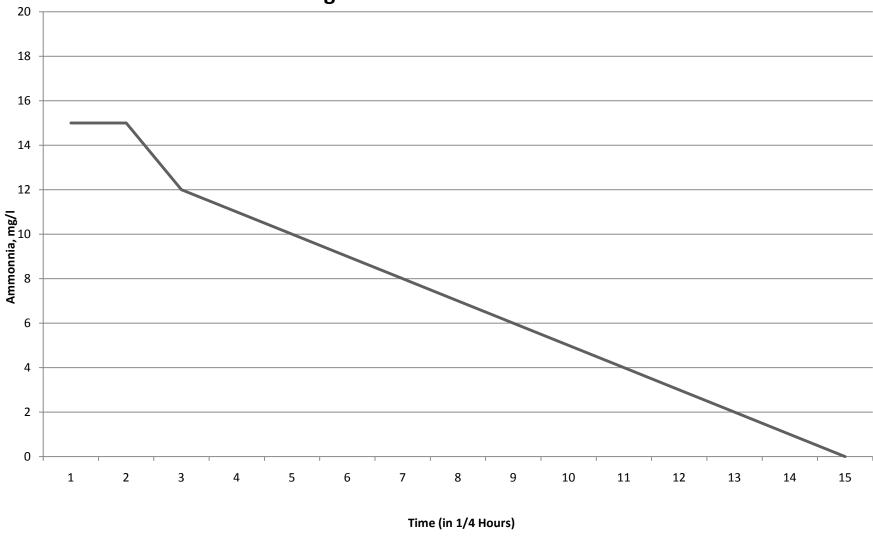


#### Figure 1 Effect of MCRT On Nitrification

——Nitrification Efficiency %

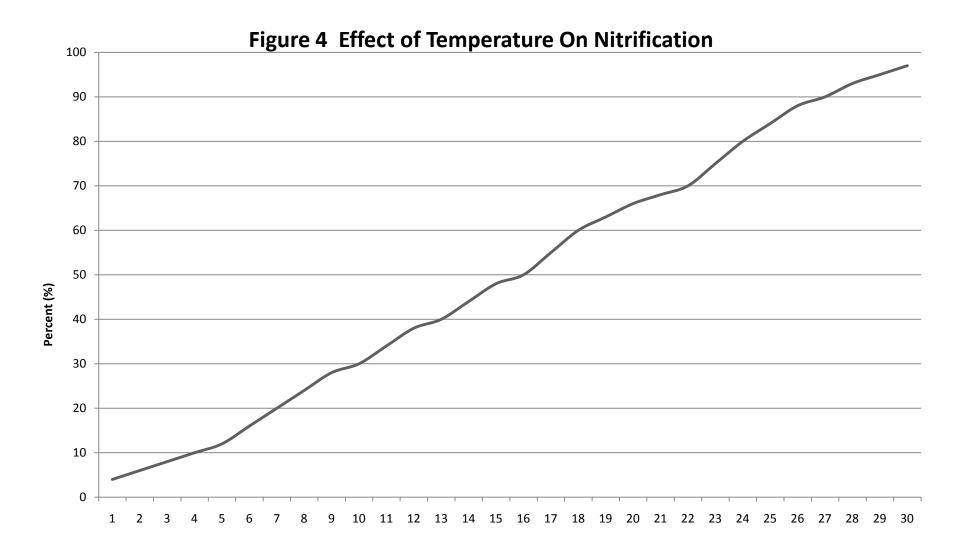


#### Figure 2 Relationship Between MCRT and F/M Ratio



#### Figure 3 Ammonia Removal vs Time

------Ammonia



Temperature (C)

-

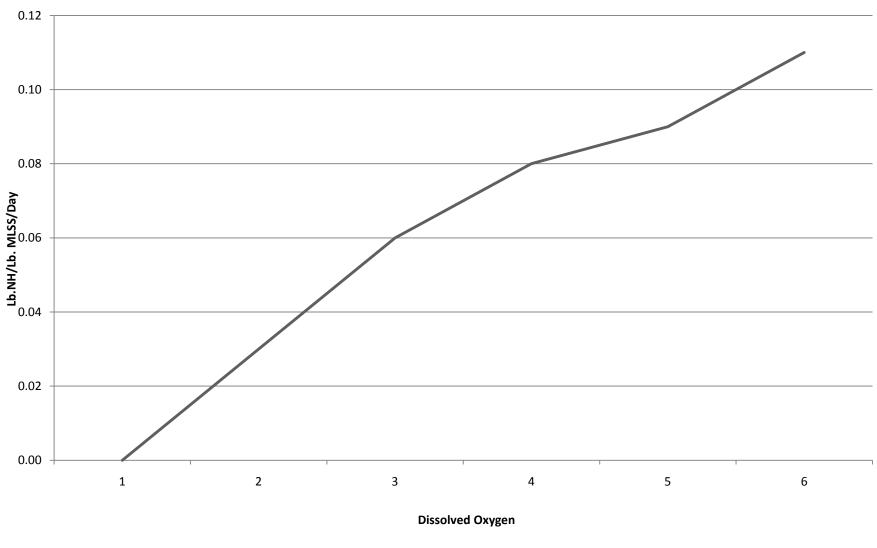
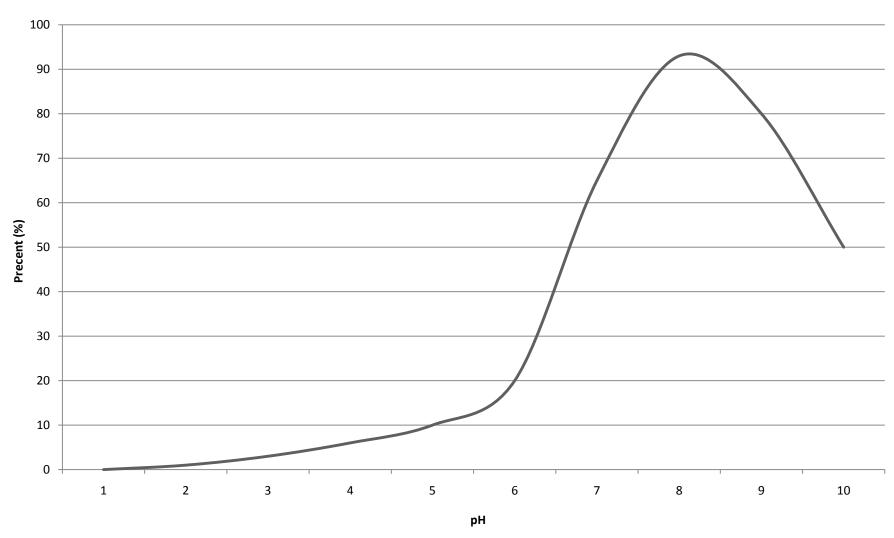
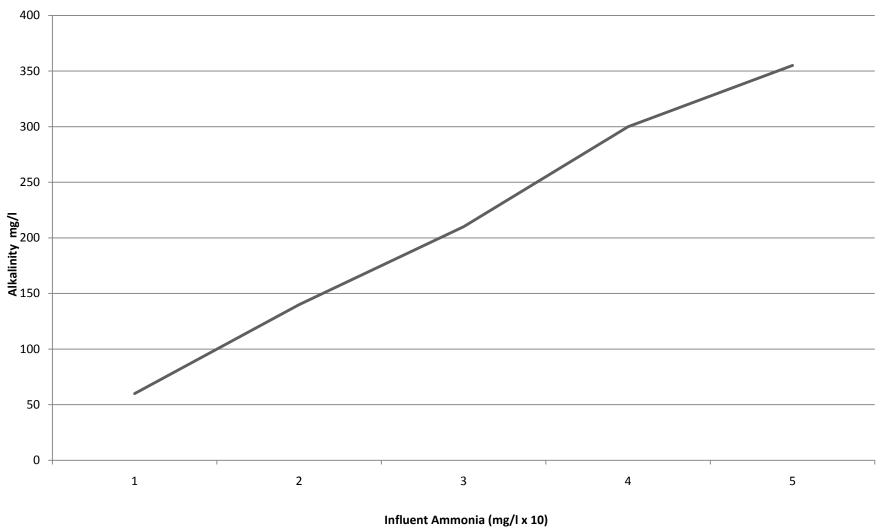


Figure 5 Effect of D.O. on Nitrification



#### Figure 6 Effect of pH on Nitrification

— Maximum Nitrification Rate (%)



#### Figure 7 Alkalinity Used in Nitrification

### Maumee River WWTP





## DO Probe



# Single Stage Blower



## Center Feed FST



#### Center Feed FST



# Peripheral Feed FST



# Peripheral Feed FST



#### Center Feed FST





## QUESTIONS???

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### Imagine the result

