Advancing the Future of Energy

WITH CAPITAL DISCIPLINE, INNOVATION AND UNMATCHED EXECUTION

RELIABLE | AFFORDABLE | SUSTAINABLE ENERGY

Basics of Refining and Renewable Diesel



INVESTOR PRESENTATION | BASICS OF REFINING AND RENEWABLE DIESEL 2021

Gary Simmons

Executive Vice President Chief Commercial Officer

INVESTOR PRESENTATION | BASICS OF REFINING AND RENEWABLE DIESEL 2021



Agenda

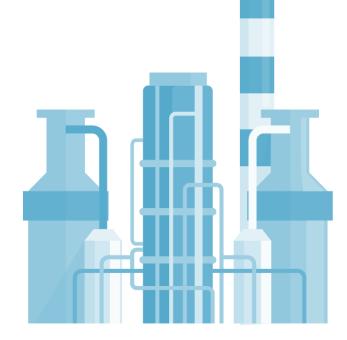
1	Crude Oil Overview
2	Refining Basics
3	Refinery Optimization and Economics
4	Renewable Diesel Basics



INVESTOR PRESENTATION | BASICS OF REFINING AND RENEWABLE DIESEL 2021

Crude Oil Characteristics

- Crude oils are blends of hydrocarbon molecules
 - Classified and priced by density, sulfur content and acidity
- **Density** is commonly measured in API gravity (relative density of crude oil to water)
 - API > 10: lighter, floats on water
 - API < 10: heavier, sinks in water
- Sulfur content is measured in weight percent
 - Less than 0.7% sulfur content = sweet
 - Greater than 0.7% sulfur content = sour
- Acidity is measured by Total Acid Number (TAN)
 - $_{\odot}$ $\,$ High acid crudes are those with TAN greater than 0.7 $\,$
 - Acidic crudes are corrosive to refinery equipment and require greater investment to process significant volumes

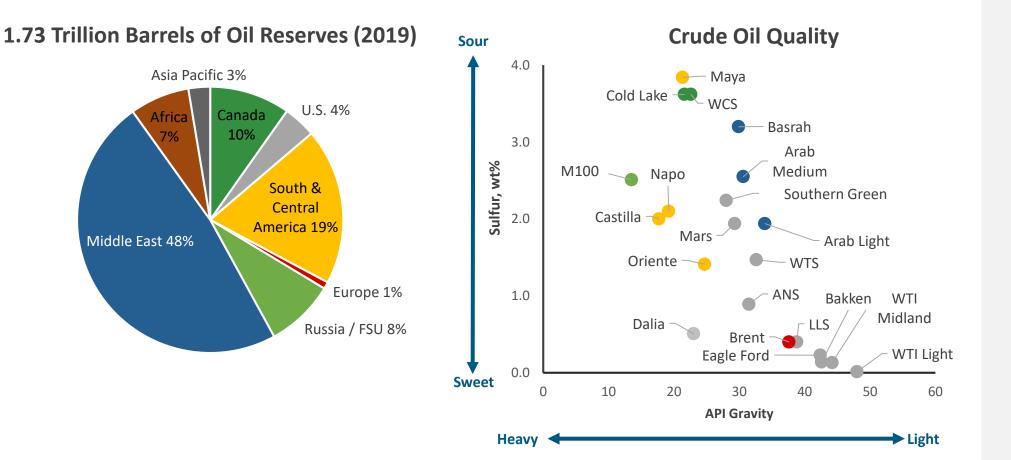




Heavy, sour, high acid crude oils are more difficult to process, but trade at a discount relative to light, sweet, low acid crudes oils



Crude Oil Reserves and Quality



 $\bullet \bullet \bullet \bullet$

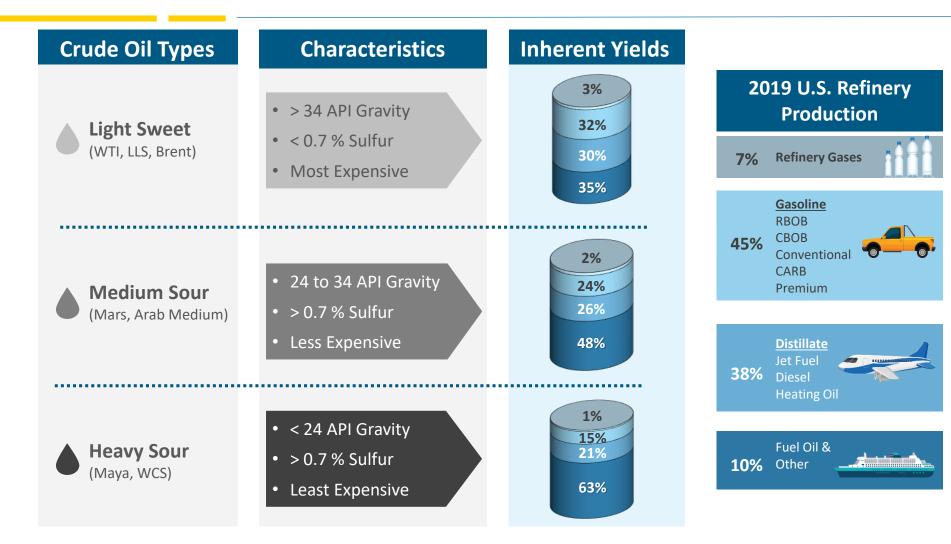
Majority of global reserves are **sour crude oils**

WTI and Brent are the primary light sweet crude oil pricing benchmarks





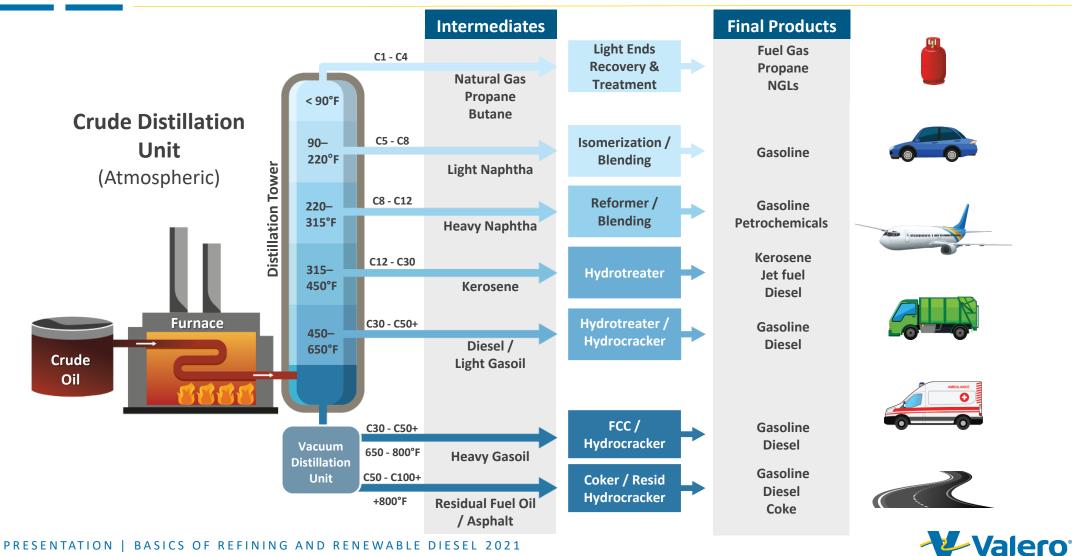
What is in a Barrel of Crude Oil?



Refineries upgrade crude oil into higher value gasoline and distillates

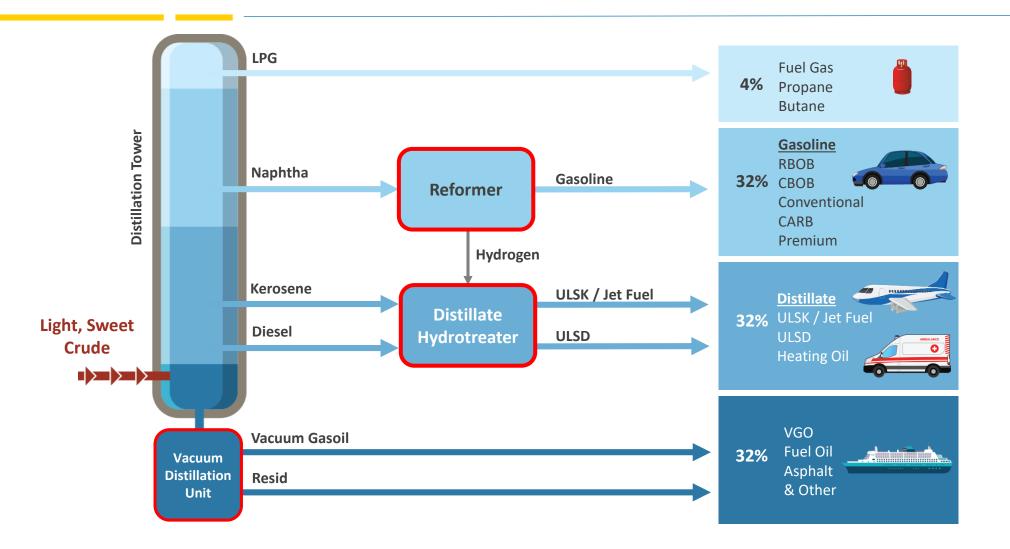


Basic Refining Concept



7

Low Conversion: Hydroskimming (Topping)



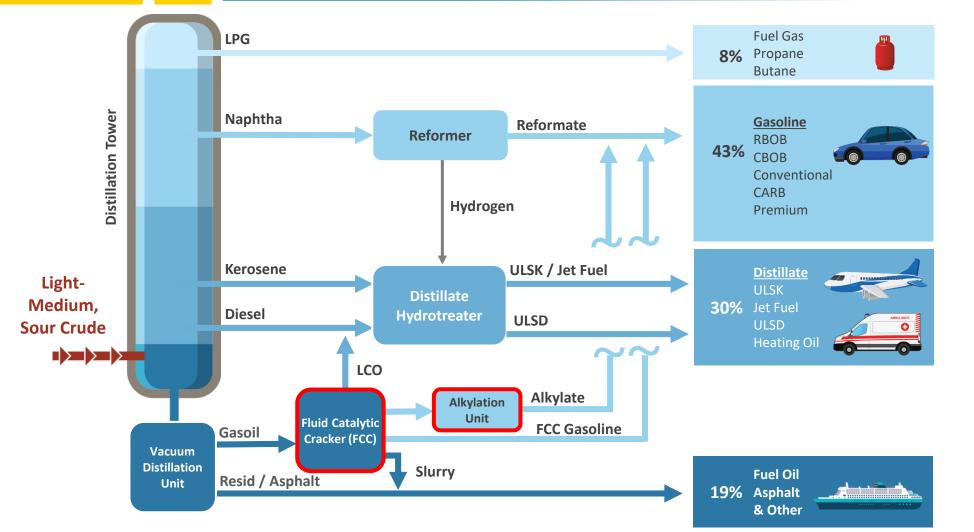
$\bullet \bullet \bullet \bullet$

Low complexity refineries process sweet crude oils





Medium Conversion: Catalytic Cracking



Moderate complexity refineries tend to run more **sour crudes,** yield more **high value products** and achieve **higher volume gain**



Fluid Catalytic Cracker (FCC)



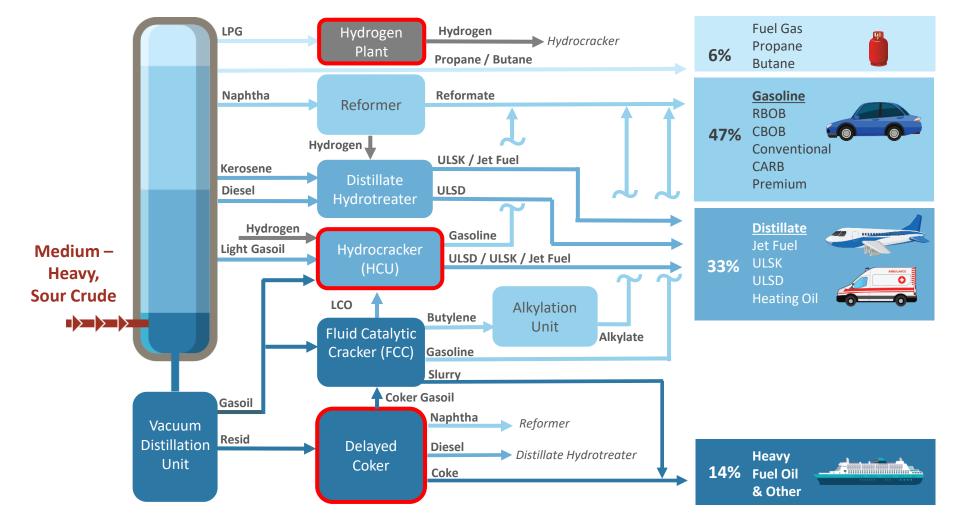
Fluid Catalytic Cracker Yields **Refinery Gases** Butylene Fractionato (Alky Feed) Gasoline Reactor **Light Cycle Oil** (Distillate) Spent Catalyst Regenerator Slurry Gasoil Regenerated Catalyst Total FCC liquid volume yield is approximately 110% of throughput Air

$\bullet \bullet \bullet \bullet$

FCC converts low-value gasoils into higher value light products



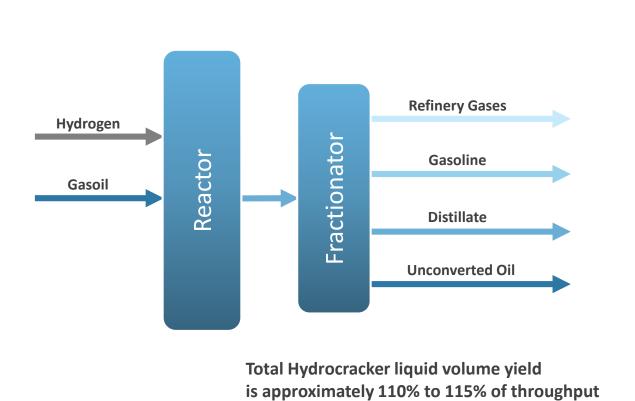
High Complexity: Coking / Resid Destruction



High complexity refineries can run heavier, more sour crudes oils while achieving the highest light product yields and volume gain



Hydrocracker Unit (HCU)



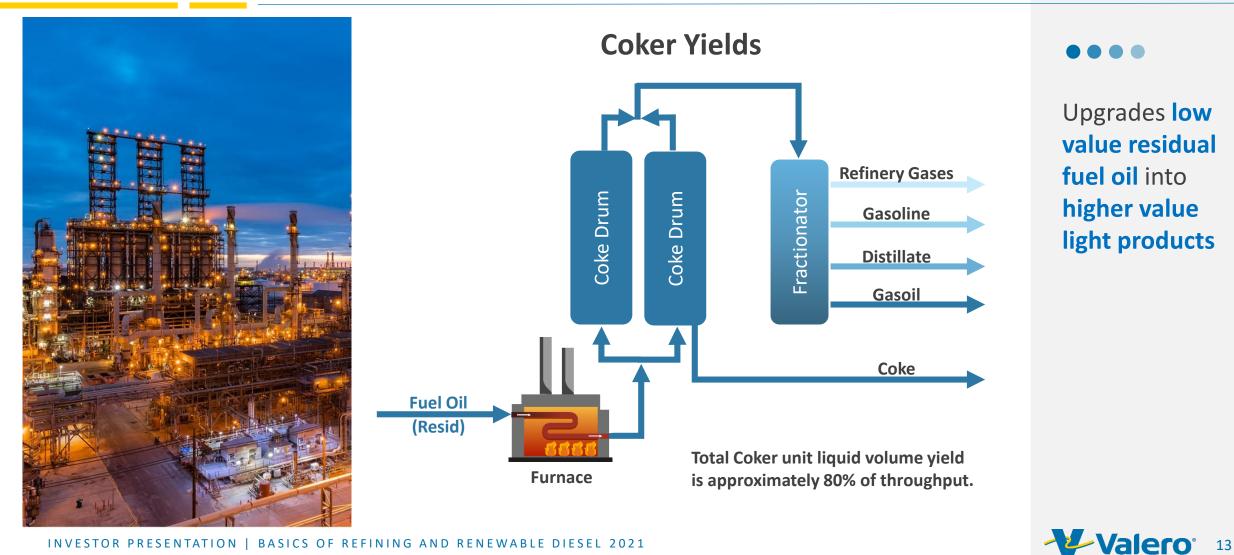
Hydrocracker Yields

 $\bullet \bullet \bullet \bullet$

Upgrades high sulfur gasoil into low sulfur gasoline, jet and diesel

Increases volumetric yield of products through hydrogen saturation

Delayed Coker



Greg Bram

Vice President Supply Chain Optimization

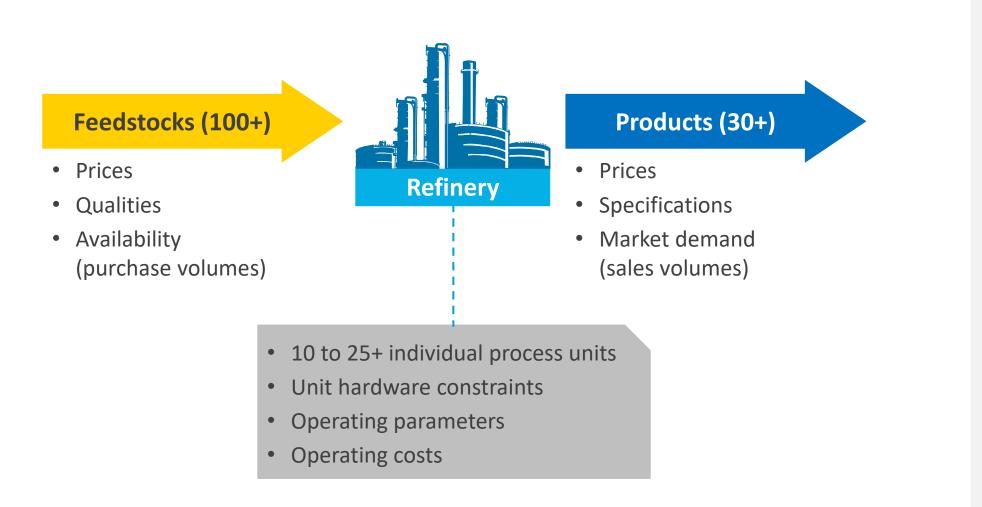
INVESTOR PRESENTATION | BASICS OF REFINING AND RENEWABLE DIESEL 2021



man farm

$\bullet \bullet \bullet \bullet$

Maximizing Refinery Profit Linear Programming (LP) Model

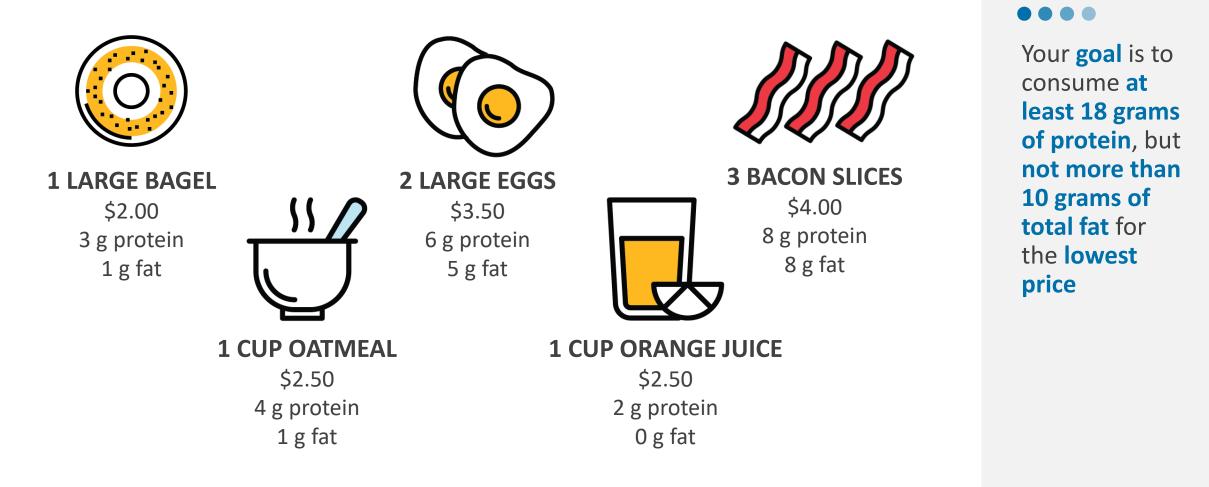


Relationship between variables are modeled in a series of linear equations

Linear program is used to find combination of feed slate, products, unit operating rates, and operating parameters that delivers highest profit

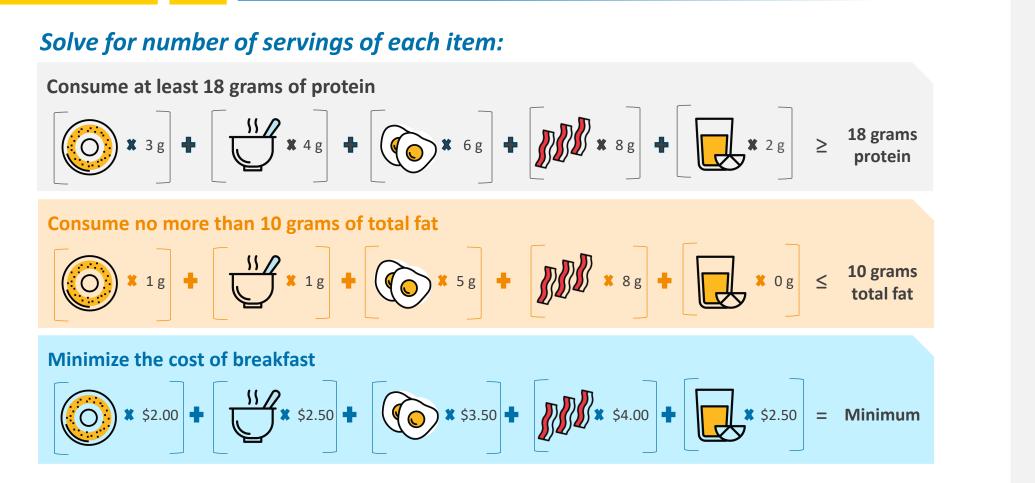


Linear Program (LP) Example: What's for Breakfast?





Optimizing Breakfast from an Engineer's Point of View



 $\bullet \bullet \bullet \bullet$

Even with only five food choices, there are so many possible combinations that using trial and error to find the one with the lowest cost is not efficient



What's the Optimal Breakfast?

\bigcirc	Servings 0	<u>Unit Cost</u>	<u>Protein (g)</u>	<u>Total Fat (g)</u>
Ű	2.7	≭ \$2.50 = \$6.75	₩ 4 = 10.8	₩ 1 = 2.7
	0			
	0.9	≍ \$4.00 = \$3.60	₩ 8 = 7.2	≈ 8 = 7.2
	0			
			<u>Meal</u>	
		\$10.35 GOAL = Lowest	18 g Min protein	10 g Max fat
				*

 $\bullet \bullet \bullet \bullet$

Linear programming is a branch of applied mathematics concerned with problems of constrained optimization

Price and "quality" of each variable drives the optimum solution



Crude Oil Break Even Values

Crude Product Yields and Prices (High and Low Crude Prices)

Products	Light Sweet ⁽¹⁾ Yields	Medium Sour ⁽²⁾ Yields	Heavy Sour ⁽²⁾ Yields	Light Sweet @ \$99/bbl Prices	Light Sweet @ \$51/bbl Prices
Refinery gases	3%	2%	1%	\$49	\$31
Gasoline ⁽³⁾	32%	24%	15%	\$108	\$60
Distillate ⁽⁴⁾	30%	26%	21%	\$117	\$69
Heavy fuel oil ⁽⁵⁾	35%	48%	63%	\$79	\$41

⁽¹⁾ Reference crude.

⁽²⁾ Alternate crudes.

⁽³⁾ Gasoline crack: \$9/bbl.

⁽⁴⁾ Distillate crack: \$18/bbl.

 $^{\rm (5)}$ Heavy fuel oil: 80% of reference crude value.

Crude Break Even Values (High and Low Crude Prices)

Crude	Light Sweet @ \$99/bbl BEV	Light Sweet @ \$51/bbl BEV	BEV @ \$99/bbl % of Light Sweet	BEV @ \$51/bbl % of Light Sweet
Medium sour	-\$3.55	-\$2.58	96%	95%
Heavy sour	-\$7.76	-\$5.65	92%	89%

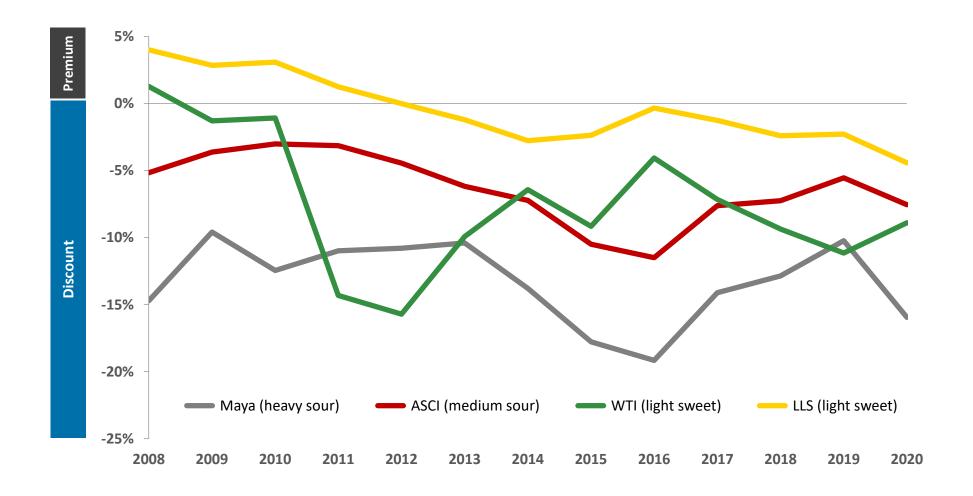
$\bullet \bullet \bullet \bullet$

Break Even Value (**BEV**) = Alternate Crude Total Product Value – Reference Crude Total Product Value

BEV for alternate crude as a percentage of reference crude value is relatively insensitive to flat price environment



Crude Oil Differentials Versus ICE Brent





Martin Parrish

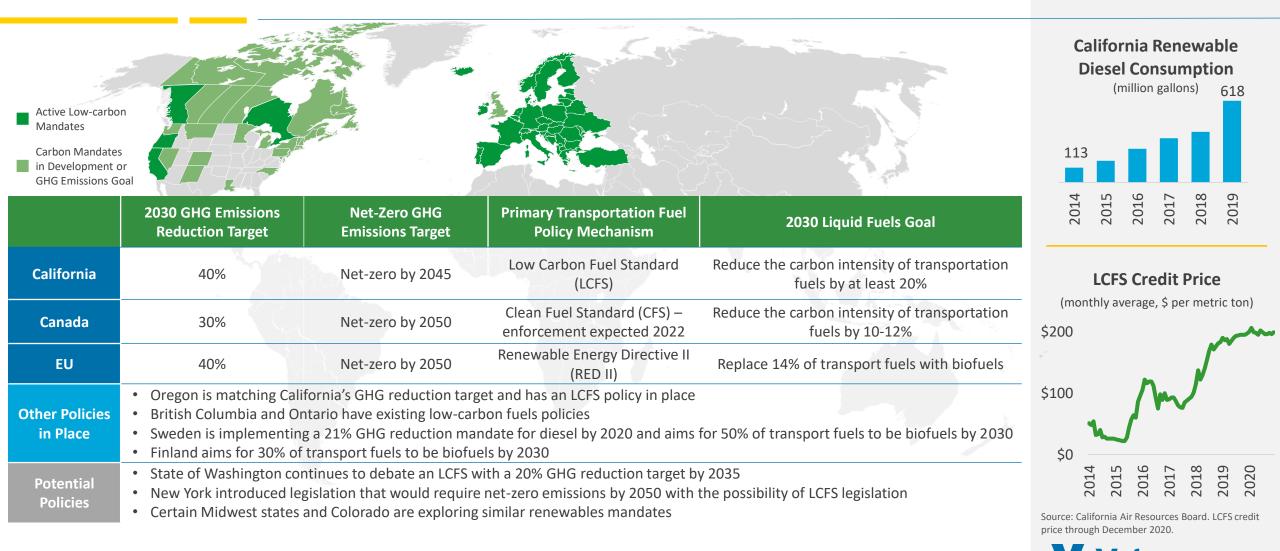
Senior Vice President Alternative Energy and Project Development





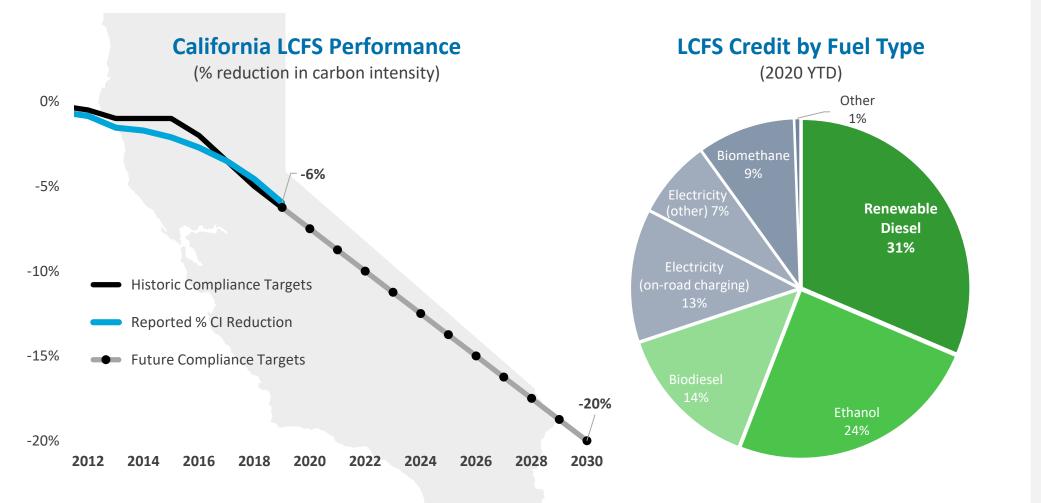
$\bullet \bullet \bullet \bullet$

Global Low-carbon Fuel Policies Driving Demand Growth for Renewable Diesel



22

Renewable Diesel Driving Low Carbon Results in California





Cost-effective fuel that can be used with existing vehicles

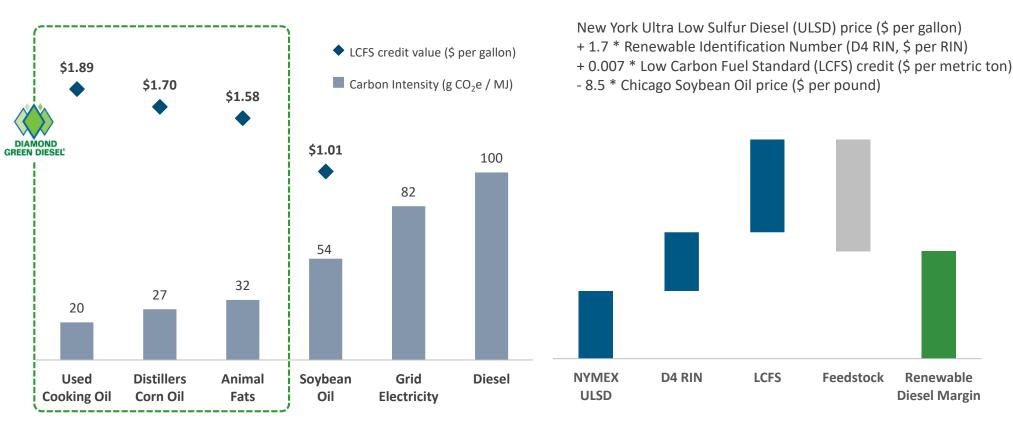
Does not require infrastructure investments

Over 2 billion gallons consumed since 2011



Diamond Green Diesel (DGD) Feedstock and Margin Indicator

DGD Feedstock Carbon Intensity and Product Value



DGD Margin Indicator \$ per gallon

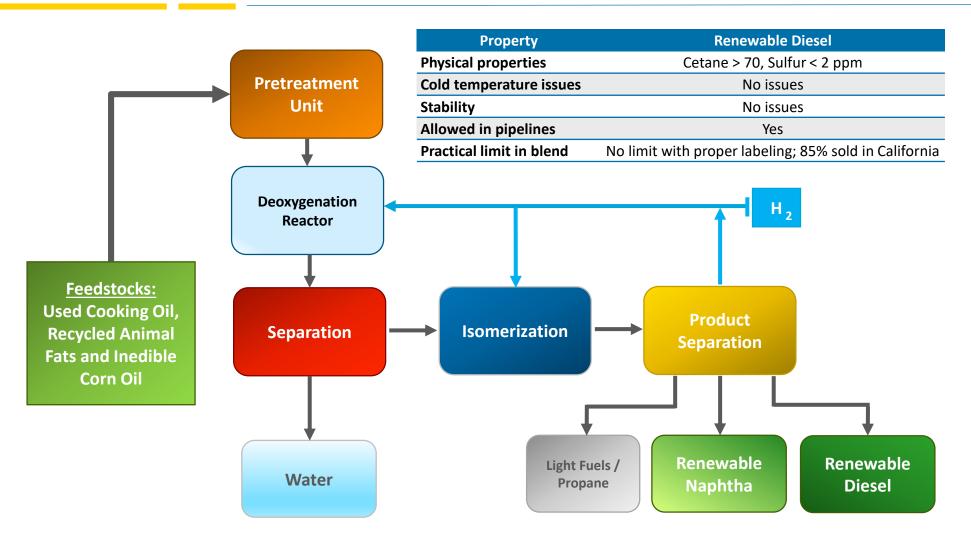
DGD is designed to process low carbon feedstocks for higher product value

Source: California Low Carbon Fuel Standard (LCFS) 2020 values, assuming \$200 per metric ton carbon price.



Renewable

Renewable Diesel Process and Properties



A Pretreatment Unit allows the plant to process advantaged, low carbon intensity feedstocks

Questions and Answers





Appendix Contents

Торіс	Pages
Major Refining Processes – Crude Processing	28
Major Refining Processes – Cracking	29
Major Refining Processes – Combination	30
Major Refining Processes – Treating	31
Refining and Renewable Diesel Acronyms	32



Major Refining Processes – Crude Processing

• Definition

- Separating crude oil into different hydrocarbon groups.
- The most common means is through distillation.

• Process

- **Desalting** Prior to distillation, crude oil is often desalted to remove corrosive salts as well as metals and other suspended solids.
- Atmospheric distillation Used to separate the desalted crude into specific hydrocarbon groups (straight run gasoline, naphtha, light gas oil, etc.) or fractions.
- Vacuum distillation Heavy crude residue ("bottoms") from the atmospheric column is further separated using a lowerpressure distillation process. Means to lower the boiling points of the fractions and permit separation at lower temperatures, without decomposition and excessive coke formation.



Major Refining Processes – Cracking

• Definition

 Breaking down large, heavy hydrocarbon molecules into smaller hydrocarbon molecules through application of heat (thermal) or the use of catalysts.

• Process

- **Coking** Thermal non-catalytic cracking process that converts low value oils to higher value gasoline, gas oils and marketable coke. Residual fuel oil from vacuum distillation column is typical feedstock.
- Visbreaking Thermal non-catalytic process used to convert large hydrocarbon molecules in heavy feedstocks to lighter
 products such as fuel gas, gasoline, naphtha, and gas oil. Produces sufficient middle distillates to reduce the viscosity of the
 heavy feed.
- **Catalytic cracking** A central process in refining where heavy gas oil range feeds are subjected to heat in the presence of catalyst, whereby large molecules crack into smaller molecules in the gasoline and lighter boiling ranges.
- Catalytic hydrocracking Like cracking, used to produce blending stocks for gasoline and other fuels from heavy feedstocks. Introduction of hydrogen in addition to a catalyst allows the cracking reaction to proceed at lower temperatures than in catalytic cracking, although pressures are much higher.



Major Refining Processes – Combination

• Definition

• Linking two or more hydrocarbon molecules together to form a large molecule (e.g. converting gases to liquids) or rearranging to improve the quality of the molecule.

• Process

- Alkylation Important process to upgrade light olefins to high-value gasoline components. Used to combine small molecules into large molecules to produce a higher octane product for blending into gasoline.
- Catalytic reforming The process whereby naphthas are changed chemically to increase their octane number. Octane number is
 a measure of whether a gasoline will knock in an engine. The higher the octane number, the more resistance to pre or self–
 ignition.
- **Polymerization** Process that combines smaller molecules to produce high octane blendstock.
- **Isomerization** Process used to produce compounds with high octane for blending into the gasoline pool. Also used to produce isobutene, an important feedstock for alkylation.



Major Refining Processes – Treating

• Definition

• Processing of petroleum products to remove some of the sulfur, nitrogen, heavy metals, and other impurities

• Process

Catalytic hydrotreating and hydroprocessing – Used to remove impurities (e.g. sulfur, nitrogen, oxygen, and halides) from
petroleum fractions. Hydrotreating further upgrades heavy feeds by converting olefins and diolefins to paraffins, which reduces
gum formation in fuels. Hydroprocessing also cracks heavier products to lighter, more saleable products.

Refining and Renewable Diesel Acronyms

- AGO Atmospheric Gasoil
- API American Petroleum Institute
- **ATB** Atmospheric Tower Bottoms
- **B–B** Butane-Butylene Fraction
- **BBLS** Barrels
- **BPD** Barrels Per Day
- BTC Blenders Tax Credit
- BTX Benzene, Toluene, Xylene
- **CARB** California Air Resource Board
- CCR Continuous Catalytic Regenerator
- **CI** Carbon Intensity
- DAO De–Asphalted Oil
- **DCS** Distributed Control Systems
- **DHT** Diesel Hydrotreater
- **DSU** Desulfurization Unit
- EPA Environmental Protection Agency
- **ESP** Electrostatic Precipitator
- FCC Fluid Catalytic Cracker
- **GDU** Gasoline Desulfurization Unit
- **GHT** Gasoline Hydrotreater
- GOHT Gasoil Hydrotreater
- **GPM** Gallon Per Minute

- HAGO Heavy Atmospheric Gasoil
- HCU Hydrocracker Unit
- **HDS** Hydrodesulfurization
- HDT Hydrotreating
- HGO Heavy Gasoil
- HOC Heavy Oil Cracker (FCC)
- H2 Hydrogen
- H2S Hydrogen Sulfide
- **HF** Hydroflouric (acid)
- HVGO Heavy Vacuum Gasoil
- **kV** Kilovolt
- **kVA** Kilovolt Amp
- LCFS Low Carbon Fuel Standard
- LCO Light Cycle Oil
- LGO Light Gasoil
- LPG Liquefied Petroleum Gas
- LSD Low Sulfur Diesel
- LSR Light Straight Run (Gasoline)
- MON Motor Octane Number
- MTBE Methyl Tertiary–Butyl Ether
- **MW** Megawatt
- **NGL** Natural Gas Liquids
- NOX Nitrogen Oxides

- **P–P** Propane–Propylene
- **PSI** Pounds per Square Inch
- RBOB Reformulated Blendstock for Oxygenate Blending
- **RDS** Resid Desulfurization
- **RFG** Reformulated Gasoline
- **RFS** Renewable Fuel Standard
- **RIN** Renewable Identification Number
- RON Research Octane Number
- **RVP** Reid Vapor Pressure
- SMR Steam Methane Reformer (Hydrogen Plant)
- **SOX** Sulfur Oxides
- **SRU** Sulfur Recovery Unit
- TAME Tertiary Amyl Methyl Ether
- TAN Total Acid Number
- UCO Used Cooking Oil
- ULSD Ultra Low Sulfur Diesel
- ULSK Ultra Low Sulfur Kerosene
- VGO Vacuum Gasoil
- VOC Volatile Organic Compound
- VPP Voluntary Protection Program
- VTB Vacuum Tower Bottoms
- WTI West Texas Intermediate
- WWTP Waste Water Treatment Plant

Cautionary Statement



This presentation contains forward-looking statements made by Valero Energy Corporation ("VLO" or "Valero") within the meaning of federal securities laws. These statements discuss future expectations, contain projections of results of operations or of financial condition or state other forward-looking information. You can identify forwardlooking statements by words such as "believe," "estimate," "expect," "forecast," "could," "may," "will," "targeting," or other similar expressions that convey the uncertainty of future events or outcomes. These forward-looking statements are not guarantees of future performance and are subject to risks, uncertainties and other factors, some of which are beyond the control of Valero and are difficult to predict including, but not limited to, the effect, impact, potential duration or other implications of the COVID-19 pandemic. These statements are often based upon various assumptions, many of which are based, in turn, upon further assumptions, including examination of historical operating trends made by the management of Valero. Although Valero believes that the assumptions were reasonable when made, because assumptions are inherently subject to significant uncertainties and contingencies, which are difficult or impossible to predict and are beyond its control, Valero cannot give assurance that it will achieve or accomplish its expectations, beliefs or intentions. When considering these forward-looking statements, you should keep in mind the risk factors and other cautionary statements contained in Valero's filings with the Securities and Exchange Commission, including Valero's annual reports on Form 10-K, quarterly reports on Form 10-Q, and other reports available on Valero's website at www.valero.com. These risks could cause the actual results of Valero to differ materially from those contained in any forward-looking statement.



Investor Relations Contacts

Our products fuel modern life and make a better future possible

-

Homer Bhullar

Vice President, Investor Relations 210.345.1982 Homer.Bhullar@Valero.com

Eric Herbort

Senior Manager, Investor Relations 210.345.3331 Eric.Herbort@Valero.com

Gautam Srivastava

Senior Manager, Investor Relations 210.345.3992 Gautam.Srivastava@Valero.com

