



Impact of Oil Phase Concentration on Physical and Oxidative Stability of Oil-In-Water Emulsions Stabilized by Sodium Caseinate and Ultra-High Pressure Homogenization

Journal:	<i>Journal of Dispersion Science and Technology</i>
Manuscript ID	LDIS-2019-0285.R1
Manuscript Type:	Original Article
Keywords:	Submicron emulsions, ultra-high pressure homogenization, conventional homogenization, sodium caseinate, oil concentration

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1 **Impact of Oil Phase Concentration on Physical and Oxidative Stability of** 2 **Oil-In-Water Emulsions Stabilized by Sodium Caseinate and Ultra-High** 3 **Pressure Homogenization**

4 **ABSTRACT**

5 In the present study, oil-in-water emulsions were formulated using 5.0% (w/v) of
6 sodium caseinate (SC) and different oil concentrations (10-30 %, v/v) by conventional
7 homogenization (CH) and ultra-high pressure homogenization (UHPH, 200-300 MPa).
8 The effect of oil concentration and pressure of treatment on emulsions characteristics
9 and stability was studied. Emulsions were characterized assessing their microstructure,
10 droplet size distribution, rheological properties, emulsifying activity index, creaming
11 stability by Turbiscan®, and photo-oxidation. UHPH emulsions, especially those
12 treated at 200 MPa, showed smaller droplet size and greater physical stability than CH
13 emulsions. In addition, emulsions containing higher oil volume fractions (20 and 30%)
14 exhibited greater physical and oxidative stability. UHPH emulsions treated at 200 MPa
15 and containing 20% oil content were the most stable emulsions against physical
16 separation and photo-oxidation. These results show that UHPH is a potential
17 technology to enhance the physical and oxidative stability of emulsions containing
18 sodium caseinate as emulsifier for several applications.

19 **Keywords:** Submicron emulsions, ultra-high pressure homogenization, conventional
20 homogenization, sodium caseinate, oil concentration.

1. Introduction

Emulsions form part of most commercial food products, including simple (e.g., milk) and sophisticated (e.g., mayonnaise) food systems. An emulsion is a mix of two non-miscible phases, which can be mixed by reducing droplet size using a proper emulsifier with the aid of a mechanical treatment such as homogenization.

In the last decade, there is a high interest in using emulsion-based systems for the delivery of bioactive compounds. Emulsions with large droplet size (i.e. conventional emulsions; $>1 \mu\text{m}$) have poor physical and oxidative stability when compared to submicron/nano emulsions [1]. Gravitational forces can be reduced when emulsion droplet size decreases, preventing flocculation, creaming or sedimentation [2].

The formation of sub-micron emulsions requires high-energy inputs. Current equipment used for emulsion preparation includes microfluidizers, sonicators or (ultra) high-pressure homogenizers [3] and conventional homogenizers [1]. Ultra-High Pressure Homogenization (UHPH) is a powerful technology that has been used to produce nano stable emulsions ($< 1 \mu\text{m}$) [1, 4-8]. In previous studies carried out in our laboratory [1, 6-8] using dairy proteins ingredients (sodium caseinate and whey protein isolate) and soy proteins, UHPH was capable of producing submicron emulsions with an improved physical and oxidative stability. Fernandez-Avila and Trujillo [9] applied UHPH (200 MPa) to obtain submicron emulsions enriched in conjugated linoleic acid (CLA, 6%, v/v) and stabilized by soy protein isolates (4%, w/v) to be incorporated into UHT milk. The authors reported that UHPH produced emulsions with low droplet size, high physical and oxidative stability during months and enhanced CLA delivery.

Subsequent to homogenization, the oil and water phases tend to separate. Proteins, when used as emulsifiers in the emulsion preparation, are adsorbed to the interface between oil

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3 46 and water during homogenization, which reduces the interfacial tension between oil and
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5 47 water phases and prevents coalescence [10]. Proteins also play an important role as
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8 48 inhibitors of lipid oxidation [2]. Sodium caseinate (SC), a milk protein product, can
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10 49 protect oil droplets against coalescence through electrostatic and steric repulsion [11].

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13 50 The choice of the oil concentration to be used in the emulsion formulation is critical as it
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15 51 has an eminent effect on emulsion structure and stability [12]. Different authors [4, 13,
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17 52 14] studied physical stability of concentrated emulsions produced by UHPH. However, to
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20 53 the best of our knowledge, the effect of different oil concentrations on oxidative stability
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22 54 of emulsions prepared by UHPH and milk proteins has been only reported in a recently
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24 55 published work using whey protein isolate [8].

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27 56 In a previous research [7], UHPH emulsions, in comparison to conventional
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29 57 homogenization, were screened (100-300 MPa) using SC at different protein levels (1 -
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31 58 5%, w/v) using a mixture of sunflower and olive oils (20%, v/v). It was concluded that
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34 59 UHPH treatment (200 and 300 MPa) was capable of producing sodium caseinate (5%,
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36 60 w/v) emulsions with improved physical and oxidative stability. The objective of the
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39 61 present study is to characterize UHPH emulsions with different oil concentrations (10, 20
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41 62 and 30%) emulsified by sodium caseinate (5%), in comparison to colloid mill and
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43 63 conventional homogenization.

44 45 46 47 64 **Materials and Methods**

48 49 50 65 *Materials*

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53 66 Sodium caseinate was obtained from Zeus Quimica (Sodium Caseinate 110, Barcelona,
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55 67 Spain). The physico-chemical characteristics, as indicated by the producer were: moisture =
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58 68 5.73%; granulometry (% < 300 μ m) = 99.99; pH = 6.7; sediment at 70 °C (%) = 0.05;

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3 69 minerals = 3.52%; MAT (N x 6.38) = 90%; fat = 1 %; density = 0.42. Refined sunflower and
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5 70 olive oils were purchased from Gustav Heess Company (Barcelona, Spain). The
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7 71 characteristics and composition of oils according to the producer are detailed in Hebishy et al.
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10 72 [8].
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13 73 **Preparation of Emulsions**

14 15 16 74 *Experimental Design*

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20 75 The effect of homogenization methods, pressure, and oil content on emulsion stability was
21
22 76 studied using a completely randomized factorial design. Twelve formulations were produced
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24 77 and stored in glass bottles (4 °C) for physical analyses Oxidative stability was examined
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26 78 during 10-days storage period at 10 °C in samples stored under light (2000 lux/m²).
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30 79 **Preparation of Protein Dispersions**

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33 80 Protein dispersions (5%, w/v; pH ≈ 6.5-7) were prepared in deionized water at 20 °C using a
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35 81 pilot-scale high speed (250 rpm) mechanical blender (Frigomat, Guardamiglio, Italy). The
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37 82 solutions were then placed at 4°C overnight to facilitate rehydration and equilibration of
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39 83 minerals.
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43 84 **Homogenization Treatments**

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47 85 After overnight rehydration, protein dispersions were equilibrated at 20 °C and mixed with
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49 86 the oil phase; sunflower and olive oil (3:1). Pre-emulsion (CM emulsion) was formed by
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51 87 mixing protein dispersion with oil using a colloid mill high-shear system (E. Bachiller B,
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53 88 S.A, Barcelona, Spain) during 5 min (5000 rpm).
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57 89 CM emulsions were homogenized using APV Rannie Copenhagen Series Conventional
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59 90 Homogenizer (Model 40.120 H, single-stage hydraulic valve assembly, Copenhagen,
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3 91 Denmark) at 15 MPa (CH emulsions).
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6 92 UHPH emulsions were formed by passing CM emulsions through a Stansted high-pressure
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8 93 homogenizer with a flow rate of 120 L/h (Model/DRG number FPG 11,300:400 Hygienic
9
10 94 Homogenizer, Stansted Fluid Power Ltd., Harlow, UK). Emulsions were cooled immediately
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12 95 after the HP-valve using two spiral-type heat exchangers (Garvía, Barcelona, Spain) in order
13
14 96 to minimize temperature retention. Emulsions were UHPH-treated for single-stage at two
15
16 97 different pressures (200 and 300 MPa) with an inlet temperature (T_{in}) of 25 °C. The inlet and
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18 98 outlet temperatures were monitored for the whole duration of the experiment.
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23 99 The experiment was repeated three times.
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26 27 100 **Emulsion Measurements and Analyses**

28 29 30 101 *Droplet Size Distribution*

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33 102 Emulsions droplet size distribution was measured the same day of preparation, as described
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35 103 by Hebishy et al. [1] using a Beckman Coulter laser diffraction particle size analyser (LS 13
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37 104 320 series, Beckman Coulter, Fullerton, CA, USA) by applying an optical model according to
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39 105 the Mie theory of light scattering. Emulsions were diluted in distilled water to get an
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41 106 appropriate obscuration. Samples were analysed at least four times and droplet size indices
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43 107 ($d_{4.3}$ and $d_{3.2}$, μm) and specific surface area (SSA, m^2/mL) were determined.
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48 108 *Rheological Measurements*

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51 109 Rheological measurements were performed in triplicate using a controlled stress rheometer
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53 110 (Haake Rheo Stress 1, Thermo Electron Corporation, Karlsruhe, Germany) with a parallel
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55 111 plate geometry [15] probe (1°, 60 mm diameter) at 25 °C. Before starting the experiment, the
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57 112 emulsion loaded to the rheometer was allowed to stand for 5 min in order to reach
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3 113 equilibrium and to avoid any structure destruction. Ostwald de Waele rheological model: $\tau =$
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5 114 $K\dot{\gamma}^n$ was used to fit the flow curves, and the consistency coefficient (K, mPa \times s) and flow
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7
8 115 behaviour index (n) were obtained.
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11 116 *Emulsifying properties*

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14 117 Emulsifying activity index (EAI) value was determined based on the method of Pearce and
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16 118 Kinsella. [16] with a minor modification. Briefly, aliquots (100 μ l) of samples were diluted
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18
19 119 by 0.1% (w/v) SDS solution to give appropriate absorbance after which the absorbance was
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21 120 measured using a UV-visible spectrophotometer (CECIL model 9000 series, Cambridge, UK)
22
23 121 at 500 nm. EAI value was calculated from the equation (Eq. 1) below as proposed by
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25
26 122 Cameron et al. [17].

$$29 \quad 123 \quad \quad \quad 2 \times 2.303 \times A \times DF$$

$$30 \quad 124 \quad \quad \quad \text{EAI (m}^2\text{/g)} = \frac{\quad}{\quad} \quad \quad \quad \text{Eq. (1)}$$

$$31 \quad 125 \quad \quad \quad C \times \emptyset \times (1-\emptyset) \times 1000$$

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34
35 126 where (DF) is the dilution factor (i.e. 250 times for CM emulsions and 2500 times for CH and
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37 127 UHPH emulsions), (A) is the spectrophotometric absorbance at 500 nm, (C) is the weight of
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39 128 protein per unit volume of aqueous phase before emulsion is formed (g/ml), (\emptyset) is the oil
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41
42 129 volume fraction (0.1, 0.2 and 0.3 for 10, 20 and 30% oil, respectively), and (\emptyset) is the optical
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45 130 path (0.01m). Measurements were performed in triplicate after the same day of preparation.
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48 131 *Physical Stability*

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51 132 Emulsion stability was measured with a vertical scan analyser Turbiscan MA 2000
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53 133 (Formulation, Toulouse, France) with an electro-luminescent diode in the near infrared (λ_{air}
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55 134 = 850 nm), as reported by Hebishy et al. [1]. Turbiscan is a powerful technique that allows
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58 135 the optical characterization of dispersions, detecting variations in droplet size (i.e.,
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3 136 flocculation, coalescence) or migration phenomena (i.e., creaming, sedimentation). Turbiscan
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5 137 measures the backscattered light at pre-set intervals (30 min for CM emulsions, 3 days for
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7 138 CH and UHPH emulsions) during the experiment (5 h for CM emulsions and 18 days for CH
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9 139 and UHPH emulsions). In order to follow the creaming kinetics, migration velocity (V ;
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12 140 $\mu\text{m}/\text{min}$) was also calculated by Turbisoft software.

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14
15 141 Creaming stability was also determined by measuring droplet size ($d_{4.3}$) at the top or at the
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17 142 bottom of the emulsions stored for 9 days at room temperature, as reported by Hebishy [18].

21 143 *Emulsion Microstructure*

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24 144 Microstructure of emulsions was performed using confocal laser scanning microscopy, as
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26 145 detailed by Hebishy [18]. The oil and protein were fluorescently stained with the fluorescent
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28 146 dyes, fluorescein isothiocyanate (FITC; Fluka, Steinheim, Germany) for protein, and Nile red
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30 147 (Sigma, Steinheim, Germany) for oil droplets. To assess changes in emulsion microstructure,
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32 148 micrographs were also obtained by using a transmission electron microscope with a Jeol 1400
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34 149 (Jeol Ltd., Tokyo, Japan) equipped with a Gatan Ultrascan ES1000 CCD Camera, preparing
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36 150 samples according to Hebishy et al. [1].

41 151 *Oxidative Stability of Emulsions*

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45 152 For the determination of primary oxidation products, lipid hydroperoxides were measured by
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47 153 mixing 0.3 mL of emulsion with 1.5 mL of isooctane/2-propanol (3:1, v/v) by vortexing (10
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49 154 s, three times) and isolating the organic solvent phase by centrifugation at $1000\times g$ for 2 min.
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51 155 The organic solvent phase (200 μL) was added to 2.8 mL of methanol/1-butanol (2:1, v/v),
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53 156 followed by 15 μL of 3.97 M ammonium thiocyanate and 15 μL of ferrous iron solution
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55 157 (prepared by mixing 0.132 M BaCl_2 and 0.144 M FeSO_4). The absorbance of the solution was
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57 158 measured at 510 nm, 20 min after the addition of the iron [19]. The hydroperoxide
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3 159 concentration was determined using a Fe^{+3} standard curve with an iron concentration varying
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5 160 from 1 to 20 μg , as described by Shantha and Decker [19]. The peroxide value, expressed as
6
7 161 milliequivalents of peroxide per kilogram of oil, was calculated using Eq. (2).
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$$10 \quad \text{Peroxide Value (PV)} = \frac{(A_s - A_b) \times m}{55.84 \times m_0 \times 2} \quad \text{Eq. (2)}$$

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17 165 where A_s = absorbance of the sample, A_b = absorbance of the blank, m = slope of the
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19 166 calibration curve, m_0 = mass (g) of the oil contained in mass of the emulsion used,
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22 167 55.84 = atomic weight of iron. The result was divided by a factor of 2 to express the peroxide
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24 168 value as milliequivalents of peroxide instead of milliequivalents of oxygen.
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28 169 For the determination of secondary oxidation products, thiobarbituric acid-reactive
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30 170 substances (TBARS) were determined according to an adapted method of McDonald and
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32 171 Hultin [20]. The emulsion (1.0 mL) was combined with 2.0 mL of TBA solution (prepared by
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34 172 mixing 15 g of trichloroacetic acid, 0.375 g of thiobarbituric acid, 1.76 mL of 12 N HCl, 0.1
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36 173 g of butylated hydroxy Toluene (BHT) and 82.8 mL of H_2O) in test tubes and placed in a
37
38 174 boiling water bath for 15 min. The tubes were allowed to cool to room temperature for 10
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40 175 min, and then, the coloured solution was separated by filtration through glass wool. The
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42 176 absorbance was measured at 532 nm. Concentrations of TBARS were calculated from a
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44 177 standard curve prepared using 1,1,3,3-tetraethoxypropane and presented as (μg
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46 178 malondialdehyde/mL).
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51 179 **Statistical Analyses**

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55 180 Statistical analyses were performed using SAS System® v9.2 (SAS Institute Inc., Cary, NC,
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57 181 USA) at 5% ($p < 0.05$) significance level and multiple comparisons of means using Tukey
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59 182 test. A general linear model with repeated measures was performed to compare between
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183 samples. The rheological consistency coefficient (K value) was compared separately for the
184 CH and UHPH treatments containing 30% oil content, due to the high variation in viscosity
185 between CH and UHPH emulsions comparing to other treatments, which made it hard to
186 detect statistical differences. A second comparison was needed for K value excluding the CH
187 and UHPH treatments containing 30% oil content. Due to the high variation of data, d3.2,
188 d4.3 and SSA values were compared only between CH and UHPH emulsions, excluding CM
189 emulsions. However, emulsifying activity index (EAI), hydroperoxides and TBARS values
190 were compared between the CM, CH and UHPH emulsions.

191 **Results and Discussion**

192 *Temperature elevation during UHPH treatment*

193 Temperatures of emulsions were monitored before (T1) and at the outlet (T2) of the high-
194 pressure valve (Table 1). Very little and non-significant variations in temperature (T1) were
195 noticed. On the other hand, results showed an increase in temperature (T2) of emulsions with
196 different oil concentrations (10, 20 and 30%) by the rate of 21.19, 21.5 and 23.7 °C per 100
197 MPa (as pressure increased from 200 to 300 MPa). Similar increase (12-18 °C per 100 MPa)
198 has been reported by previous studies [21-24] in high-pressure homogenized emulsions. This
199 increase in the temperature could be due to the high velocity, shear, turbulence and cavitation
200 forces at which the fluid exits the HP-valve, which may be turned into heat.

201 A marked increase in temperature (T2) was shown when the oil concentration increased. T2
202 increased by 0.459 and 0.585 °C per 1% oil content for emulsions treated at 200 and 300
203 MPa, respectively. However, this increase was only significant when oil concentration
204 increased to 30% and not to 20% ($P < 0.05$). Hayes and Kelly [22] reported that milk (0-10%
205 fat) outlet temperature increased (0.5 °C / 1% fat) as milk fat content increased in samples

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3 206 homogenized at 150 MPa. This could be a direct result of viscous dissipation or the increased
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5 207 number of oil droplets, which increases collision between droplets. Another explanation
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7 208 could be the high fluid compression in the intensifier during the pressure built up as the oil
8
9 209 content increased from 10 to 30%. This is due to higher heat of compression for oil
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11 210 comparing to water [4].
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15 211 *Droplet size distribution*

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19 212 Table 2 and Figure 1 (A-C) show the mean droplet sizes (d_{3.2} and d_{4.3}) and specific surface
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21 213 area (SSA, m²/ml) of SC emulsions containing different oil contents.
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23

24 214 CM treatment resulted in emulsions with largest droplet size (average of d_{4.3} value ~ 15 µm)
25
26 215 comparing with CH and UHPH treatments (average of d_{4.3} value ~ 1.12 and 0.123 µm,
27
28 216 respectively). In CM emulsions, droplets tend to coalesce after homogenization (Fig. 2 A
29
30 217 (A)), as a result of high droplet sizes obtained in this type of equipment, as the energy input is
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32 218 not as high as pressure homogenizers (the more the energy input, the more the interfacial area
33
34 219 that can be created) [3]. Droplets with larger sizes would cream more rapidly, coming close
35
36 220 to each other in the cream layer, thereby promoting membranes disruption [25]. Low protein
37
38 221 coverage (Fig. 2 A (B)) and high interfacial tension could be another reason for the high
39
40 222 coalescence rate in CM emulsions. Droplet size (d_{3.2}) of CM emulsions has been influenced
41
42 223 by varying the oil content, as can be seen in Table 1.
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48 224 CH emulsions containing 10% oil showed larger droplet size which was significantly
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50 225 decreased when oil concentration increased to 20% after which the decrease was not
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52 226 significant. Droplet size distribution curves (Fig. 1 A-C) show that CH emulsions with 10%
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54 227 oil had a bimodal distribution with a first population of droplets at ~ 0.5 µm and a second
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56 228 population of droplets at ~ 2 µm. On the other hand, in emulsions containing 30% oil, the
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3 229 first and second population of droplets were decreased to ~ 0.1 and $1 \mu\text{m}$, respectively.
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5 230 CLSM images (Fig. 3 (D-F)) have shown a high degree of flocculation in all CH emulsions.
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7 231 This could be attributed to poor protein coverage in these emulsions [26]. These results are
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9 232 not in agreement with other research studies that had been done in our lab under the same
10
11 233 conditions of pressure levels and oil concentrations, but using isolates of whey and soy
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13 234 proteins [5, 8] at a lower protein concentration (4%, w/v). This increment in biopolymer
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15 235 concentration in the aqueous phase to 5% (w/v) in the present study might have promoted
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17 236 depletion flocculation where droplet aggregation is promoted by the non-adsorbed protein
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19 237 remaining in the aqueous phase.
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25 238 UHPH emulsions slightly showed signs of flocculation and coalescence (Fig. 2 B (D-I)),
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27 239 which was more pronounced in emulsions containing 10% oil, which may explain the high
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29 240 creaming rate observed in these emulsions (Physical Stability section).
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241 *Rheological behavior*

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36 242 Rheological behavior of emulsions (consistency coefficient (K) value and the flow behavior
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38 243 index (n)) is presented in Table 3.
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42 244 CM emulsions showed low viscosities and Newtonian flow behavior due to low interaction
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44 245 between droplets. Increasing the oil concentration from 10 to 20 and 30% had a significant
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46 246 effect on viscosity of CM emulsions.
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50 247 CH emulsions exhibited a shear thinning behavior (viscosity decreases on shearing during the
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52 248 test due to deformation and breakdown of aggregates) with a flow behavior index below 1
53
54 249 which was accompanied by a significant increment in viscosity with increased oil
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56 250 concentration from 10 to 30%. Although no change was observed in the flow behavior index
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58 251 when the oil concentration increased from 10 to 20%, this change became significant when
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3 252 the oil concentration further increased to 30%. Increasing oil concentration increased
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5 253 emulsion viscosity as previously reported [27, 28]. Mewis and Wagner [29] attributed this
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7 254 viscosity increase to the strong inter-droplet interactions.
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11 255 Applying UHPH homogenization pressures (200 and 300 MPa) at 10 and 20% oil
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13 256 concentration resulted in emulsions with similar viscosities to the CH emulsions, however
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15 257 viscosity increased dramatically when the same pressure was applied to emulsions containing
16
17 258 30% oil with a complete change of the behavior to shear thinning. Flourey et al. [13] reported
18
19 259 a change in flow behavior of UHPH emulsions (1.5% whey protein) from highly fluid to
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21 260 highly thick with varying oil volume fractions (10-50%). Similar trend was found in our
22
23 261 recent published work [8] using whey protein isolate to produce emulsions with oil
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25 262 concentrations between 10-50% (v/v) under homogenization pressures (100-200 MPa). It was
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27 263 reported that viscosity had increased and flow behavior changed from Newtonian to shear-
28
29 264 thinning when oil content increased from 10 to 50% in emulsions treated at 200 MPa. This
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31 265 increase in viscosity was more pronounced in emulsions containing 50% oil than those
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33 266 containing 30% oil. What distinguishes the latterly mentioned study using whey proteins
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35 267 from the present study is that it was not possible to produce SC emulsions containing 50%
36
37 268 oil, as the emulsions completely gelled giving a mayonnaise-like structure (data not shown).
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39 269 Considerable increase in viscosity and change in flow behavior has been also reported in
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41 270 emulsions produced by the UHPH technology [4] using 4% whey protein isolate and 15-45%
42
43 271 oil content and [14] using micellar casein at 2-3.5% and oil content of 10-30%.

272 ***Emulsifying activity index (EAI)***

273 Emulsifying property refers to the stable interface area per unit weight of protein, which
274 represents the capability of proteins to adsorb at the oil-water interface. CM emulsions
275 presented low EAI values. Applying low-pressure (CH treatment) increased significantly the

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3 276 EAI; however, applying ultra high-pressures (200 and 300 MPa) resulted in lower EAI values
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5 277 (Table 3). Fernández-Ávila and Trujillo [6] also reported higher EAI values for emulsions
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7 278 treated by CH than UHPH treatment, which was attributed to the increase in surface area
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9 279 created during emulsification per unit mass in UHPH emulsions.

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13 280 In our previous study [8] under the same conditions of CM, CH and UHPH but using whey
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15 281 protein isolate as emulsifier, it was reported that protein load (mg/m^2) on the surface of the
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17 282 oil droplets was lower than CM and CH emulsions. However, the authors reported that when
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19 283 taking into account the SSA of droplets, which was significantly higher for UHPH compared
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21 284 with both CM and CH. The amount of surface protein per volume (millilitre) was much
22
23 285 higher in UHPH emulsions (41 and 53.51 mg/mL at 100 and 200 MPa, respectively) than in
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25 286 CM and CH emulsions (23.30 and 25.80 mg/mL , respectively). This was attributed to the
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27 287 increased spreading and rearrangement of adsorbed protein molecules at the interface. What
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29 288 can be concluded is that, taking into consideration the SSA, UHPH treatment improved the
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31 289 emulsifying activity of SC.

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36 290 Cha et al. [30] reported an increase in the EAI in emulsions produced using
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38 291 myofibrillar proteins and lecithin as emulsifiers and high pressure homogenization at
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40 292 pressures ranging between 40 and 120 MPa, using emulsions produced by ultraturrax as a
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42 293 control. The elevated EAI was attributed by the authors to exposed hydrophobic groups,
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44 294 which enhanced the interactions between proteins and lipids and increased solubility which
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46 295 promoted proteins to diffuse at oil–water interface, thus improving the emulsifying
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48 296 properties.

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53 297 CH emulsions presented higher EAI with an increase being significant when the oil
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55 298 concentration increased from 10 to 20% however; this increase was not statistically
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57 299 significant when oil concentration further increased to 30%. The EAI results correlated with
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3 300 the droplet size and SSA results, presenting same trend. The EAI results were also in line
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5 301 with the TEM (Fig. 2 A) images. In this sense, the emulsions containing 10% oil presented a
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7 302 poor surface coverage (Fig. 2 A (C)), while emulsions with 30% oil presented oil droplets
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9 303 with high surface protein covering the droplets (Fig. 2 A (D)).

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12
13 304 Table 3 shows a significant increase in EAI value in UHPH emulsions with increasing the oil
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15 305 concentration from 10 to 20% oil ($P < 0.05$). Fernández-Ávila and Trujillo [6] also reported
16
17 306 similar results when oil content increased from 10 to 20% in UHPH emulsions stabilized by
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19 307 soy proteins. However, in our study, no further significant effect on the EAI was observed
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21 308 when oil concentration increased to 30%. This may indicate that the amount of SC started to
22
23 309 become limited to cover the newly created O/W interface. Increasing the oil concentration,
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25 310 with a fixed protein amount, reduces the protein at the interface, thus suggesting the
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27 311 spreading of protein at an interface to form a thinner layer [31]. A similar trend was observed
28
29 312 in emulsions stabilized by bovine serum albumin [32] when the oil volume fraction increased
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31 313 from 25 to 56%.

314 *Physical stability of emulsions*

315 Figure 4 (A–F) shows the backscattering (BS) profiles for all emulsions containing 5% of SC
316 prepared with CM, CH and UHPH at 200 MPa. UHPH emulsions have shown longer stability
317 (Fig. 4 E,F) as compared to CM (Fig. 4 A,B) and CH emulsions (Fig. 4 C,D). For instance,
318 the same extent of creaming appears about 17 days after UHPH treatment at 200 MPa vs. 2
319 days after conventional homogenization (CH) and 5 hours after colloid mill (CM).
320 Backscattering results have shown a drop of BS at the bottom of all samples, due to
321 clarification of the mixture in the following order: CM > CH > UHPH emulsions. On the
322 other hand, there was an increase in BS at the top of samples, associated to creaming (particle
323 migration) with a creaming rate in the following order: CM > CH > UHPH emulsions.

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3 324 Physical stability was also assessed in the emulsions, measuring the $d_{4.3}$ value at the top or at
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5 325 the bottom of the emulsion tubes stored at room temperature for 9 days and under the same
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7 326 conditions for comparison. Physical stability was determined in the homogenized emulsions
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9 327 (conventional and UHPH), but not in the CM emulsions where oily or creamy phases were
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11 328 clearly separated from the aqueous phases 2 hours after preparation.

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15 329 CM emulsions containing the lowest oil concentration (10%) showed the highest creaming
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17 330 rate (Fig. 4 A). However, increasing the oil concentration improved creaming stability (Fig. 4
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19 331 B). The explanation for this low creaming stability of CM emulsions containing 10% oil
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21 332 could be the large droplet size (Table 2) and the high probability of coalescence, as discussed
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23 333 before in the Particle Size Distribution section.

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28 334 CH emulsions had higher creaming stability than CM emulsions; however, they were not as
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30 335 stable as UHPH emulsions (Table 3 and Fig. 4 C-F). Oil-phase concentration played an
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32 336 important role in the creaming stability of CH emulsions (higher oil concentration slowed
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34 337 down the creaming rate). Even $d_{4.3}$ value obtained at the top or the bottom of the CH
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36 338 emulsions (Table 3) showed significant differences after 9 days of storage during 9 days,
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38 339 regardless of the oil concentration, Figure (4 D) shows clearly the slow change of
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40 340 backscattering in CH emulsions containing 30% oil in comparison to their counterpart of
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42 341 emulsions containing 10% oil (Fig. 4 C). This could be due to the increase in packing fraction
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44 342 of oil droplets [33], which enhanced emulsion viscosity and lowered the creaming rate. High
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46 343 creaming stability with increasing oil content was also reported in CH emulsions stabilized
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48 344 by whey protein isolate [8] when oil content increased from 10 to 30 and 50%, and in non-
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50 345 heated soy protein isolate (SPI) [5] when soybean oil content increased from 10 to 20%,
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52 346 owing to high consistency. The later study reported that these emulsions also exhibited
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54 347 greater thickness of SPI at the droplets surface and the absence of clusters of protein
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3 348 aggregates. Higher oil content results in multiplied number of droplets [34], improving the
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5 349 resistance of emulsions to flow, and increasing the apparent viscosity [35].
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9 350 UHPH emulsions displayed better creaming stability; the emulsions remained turbid with no
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11 351 visual separation during 18 days (Fig. 4 E,F) comparing to CM (Fig. 4 A,B) and CH (Fig. 4
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13 352 C,D) emulsions. High-pressure homogenization reduces droplet size resulting in emulsions
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15 353 that are, according to Stokes law, higher stable towards creaming [36]. On the other hand,
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17 354 smaller size and the rigid interfacial layers, as a result strong interactions between adsorbed
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19 355 proteins at the interface due to the unfolding and exposure of hydrophobic sites of proteins,
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22 356 increase emulsion density, embedding droplets migration. San Martín-González et al. [14]
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24 357 observed that high-pressure homogenization (300 MPa), regardless of oil and casein
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26 358 concentration, reduced creaming index to zero during 10 days of storage. The authors
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28 359 attributed this high stability to increased availability of caseins due to extensive disruption.
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33 360 Although the changes in d4.3 value between top and bottom of emulsions with 10% oil
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35 361 showed no significant differences, Turbiscan was able to detect such slight creaming in
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37 362 emulsions with 10% oil (Fig. 4 E) comparing to no creaming in those containing 30% oil
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39 363 (Fig. 4 F). This may be attributed to large droplet size in these emulsions due the flocculation
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41 364 or coalescence observed, as explained in the Droplet Size Distribution section. These results
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43 365 are in line with what was reported in a previous study [5], UHPH emulsions showed no
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45 366 creaming after more than 5 months of cold storage.
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367 *Oxidative stability*

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53 368 Table 4 shows the hydroperoxide and TBARS ($\mu\text{g malondialdehyde/mL}$) contents of CM,
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55 369 CH and UHPH emulsions stabilized by SC using different oil concentrations.
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59 370 CM emulsions presented generally higher hydroperoxides and TBARS values than other
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3 371 emulsions especially those containing 10% and 30% oil content. There were no significant
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5 372 differences for hydroperoxides at day 1 between CM, CH and UHPH emulsions. The high
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7 373 hydroperoxide and TBARS indicates the progression to a secondary state of oxidation in
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9 374 these emulsions. This high sensitivity of CM emulsions to oxidation may be attributed to
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11 375 exposure of oil droplets to the oxidation factors due to poor protein coverage at the interface
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13 376 and the high coalescence rate between oil droplets (Fig. 2 A (A)). Similar trend was also
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15 377 observed in our previous study [8] using whey protein isolate. Oil concentration significantly
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17 378 affected the oxidative stability of CM emulsions. As can be seen from Table 4, all emulsions
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19 379 presented similar level of hydroperoxides and TBARS contents at day 1 of storage, except for
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21 380 significant amount in emulsions containing 10% oil. As the storage time progressed to 10
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23 381 days, emulsions containing 10% oil presented the highest hydroperoxide content. Emulsions
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25 382 containing 20% oil showed the lowest amount of TBARS after 10 days, contrary to
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27 383 emulsions containing 10 and 30 %.

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29 384 CH emulsions containing 10 and 20% oil presented lower amount of hydroperoxides which
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31 385 has significantly increased after 10 days of storage, being higher in hydroperoxides in
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33 386 emulsions containing 20% oil. On the other hand, the TBARS content has been decreased or
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35 387 maintained the same in these samples after 10 days of storage with no significant differences
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37 388 (day 10 – day 1). No significant changes were found in hydroperoxide content of CH
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39 389 emulsions at first or last day of storage. There was an increase in TBARS levels in emulsions
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41 390 containing 30% oil, unlike emulsions containing 10 and 20% oil, being significant when
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43 391 comparing to emulsions with 10% oil. Therefore, it can be concluded that increasing the oil
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45 392 content in CH emulsion systems more than 20% oil may facilitate lipid oxidation and bring it
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47 393 from primary to secondary oxidation.

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49 394 UHPH emulsions showed no differences in hydroperoxides neither at first nor last day of
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3 395 storage. Lower oxidative stability was observed in emulsions containing 10% oil; however,
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5 396 UHPH emulsions (20% oil) showed the best oxidative stability; the increase in TBARS
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7 397 content was not significant after 10 days of storage, it had even decreased significantly in
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9 398 emulsions containing 20% oil and treated at 200 MPa. This may indicate the sensitivity of
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11 399 emulsions containing 10% oil to oxidation. Results obtained by Fernández Ávila and Trujillo
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13 400 [6] indicated more protein coverage at the interface of CH and UHPH emulsions stabilized
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15 401 with non-heated SPI containing 20% (v/v) oil than those containing 10% (v/v) oil. The
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17 402 possible reasons for the high oxidation rate in emulsions with low oil content (10%),
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19 403 especially those treated at 300 MPa, could be the following: 1) the creaming observed in
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21 404 these emulsions, which makes the lipids closer to the ambient and favors oxidation [28]; 2)
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23 405 the increase in the amount of free radicals as a reason of the proportional increase in the
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25 406 aqueous phase fraction, as well as the water soluble prooxidants [37]; 3) the low viscosity of
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27 407 these emulsions, in comparison to emulsions with high oil content (30%). It has been
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29 408 proposed that elevated viscosity can affect oxidation by reducing the diffusion of potential
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31 409 pro-oxidative molecules, such as ferrous ions or lipid hydroperoxides [38-40].
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33 410 Improved oxidative stability was found by other researchers when oil volume fraction
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35 411 increased from 10 to 20% [5, 6] 5 to 40% [28], or from 5 to 30% [37]. In a recent study [8],
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37 412 we reported that increasing the oil content in UHPH emulsions stabilized by whey proteins
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39 413 from 10 to 30% oil resulted in improved oxidative stability, which is in line with what has
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41 414 been found in the present study. However, additional increase in oil concentration to 50%
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43 415 caused poor emulsion stability to oxidation.
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53 416 **Conclusion**

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56 417 Ultra high pressure homogenization technology is capable of producing submicron emulsions
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58 418 with up to 30% (v/v) oil content using SC (5%, w/v) as emulsifier with a high physical and
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oxidative stability compared to conventional treatments. Using high oil concentrations (20 and 30%) enhanced physical and creaming stability of all emulsions. Oxidative stability is oil concentration and homogenization treatment dependent. While increasing oil concentration, especially in emulsions containing 20% oil, produced the most stable emulsions in case of CM and UHPH emulsions, increasing oil concentration to 30% adversely affected lipid oxidation of CH emulsions during storage. To sum up, findings of the present study suggest the advantages of using UHPH technology to produce submicron emulsions with high physical and oxidative stability which might be used as carriers for bioactive ingredients with high sensitivity to oxidation.

References

- [1] Hebishy, E.; Buffa, M.; Guamis, B.; Blasco-Moreno, A.; Trujillo, A. J. Physical and oxidative stability of whey protein oil-in-water emulsions produced by conventional and ultra high-pressure homogenization: Effects of pressure and protein concentration on emulsion characteristics. *Innov Food Sci Emerg* **2015**, 32, 79-90.
- [2] McClements, D.J.; Decker, E.A. Lipid Oxidation in Oil-in-Water Emulsions: Impact of Molecular Environment on Chemical Reactions in Heterogeneous Food Systems. *J Food Sci* **2000**, 65, 1270-1282.
- [3] Stang, M.; Schuchmann, H.; Schubert, H. Emulsification in High-Pressure Homogenizers. *Eng Life Sci* **2001**, 1, 151-157.
- [4] Cortés-Muñoz, M.; Chevalier-Lucia, D.; Dumay, E. Characteristics of submicron emulsions prepared by ultra-high pressure homogenisation: Effect of chilled or frozen storage. *Food Hydrocolloid* **2009**, 23, 640-654.
- [5] Fernández-Ávila, C.; Escriu, R.; Trujillo, A.J. Ultra-High Pressure Homogenization enhances physicochemical properties of soy protein isolate-stabilized emulsions. *Food Res Int* **2015**, 75, 357-366.
- [6] Fernandez-Avila, C.; Trujillo, A.J. Ultra-High Pressure Homogenization improves oxidative stability and interfacial properties of soy protein isolate-stabilized emulsions. *Food Chem* **2016**, 209, 104-113.
- [7] Hebishy, E.; Buffa, M.; Juan, B.; Blasco-Moreno, A.; Trujillo, A.-J. Ultra high-pressure homogenized emulsions stabilized by sodium caseinate: Effects of protein concentration and pressure on emulsions structure and stability. *LWT - Food Sci Tech* **2017**, 76, 57-66.
- [8] Hebishy, E.; Zamora, A.; Buffa, M.; Blasco-Moreno, A.; Trujillo, A.-J. Characterization of Whey Protein Oil-In-Water Emulsions with Different Oil Concentrations Stabilized by Ultra-High Pressure Homogenization. *Processes* **2017**, 5.
- [9] Fernandez-Avila, C.; Trujillo, A.J. Enhanced stability of emulsions treated by Ultra-High Pressure Homogenization for delivering conjugated linoleic acid in Caco-2 cells. *Food Hydrocolloid* **2017**, 71, 271-281.

- 1
2
3 458 [10] Dickinson, E. Milk protein interfacial layers and the relationship to emulsion
4 459 stability and rheology. *Colloid Surface B* **2001**, 20, 197-210.
- 5 460 [11] Dickinson, E. Caseins in emulsions: interfacial properties and interactions. *Int*
6 461 *Dairy J* **1999**, 9, 305-312.
- 7 462 [12] Soleimanpour, M.; Koocheki, A.; Kadkhodae, R. Influence of main emulsion
8 463 components on the physical properties of corn oil in water emulsion: Effect of oil
9 464 volume fraction, whey protein concentrate and *Lepidium perfoliatum* seed gum. *Food*
10 465 *Res Int* **2013**, 50, 457-466.
- 11 466 [13] Flourey, J.; Desrumaux, A.; Lardières, J. Effect of high-pressure
12 467 homogenization on droplet size distributions and rheological properties of model oil-
13 468 in-water emulsions. *Innov Food Sci Emerg Technologies* **2000**, 1, 127-134.
- 14 469 [14] San Martin-González, M.F.; Roach, A.; Harte, F. Rheological properties of
15 470 corn oil emulsions stabilized by commercial micellar casein and high pressure
16 471 homogenization. *LWT - Food Sci Tech* **2009**, 42, 307-311.
- 17 472 [15] Saeidy, S.; Nasirpour, A.; Djelveh, G.; Ursu, A.-V.; Delattre, C.; Pierre, G.;
18 473 Michaud, P. Emulsion properties of Asafoetida gum: Effect of oil concentration on
19 474 stability and rheological properties. *Colloid Surface A* **2019**, 560, 114-121.
- 20 475 [16] Pearce, K.N.; Kinsella, J.E. Emulsifying properties of proteins: evaluation of a
21 476 turbidimetric technique. *J Agric Food Chem* **1978**, 26, 716-723.
- 22 477 [17] Cameron, D.R.; Weber, M.E.; Idziak, E.S.; Neufeld, R.J.; Cooper, D.G.
23 478 Determination of Interfacial Areas in Emulsions Using Turbidimetric and Droplet
24 479 Size Data: Correction of the Formula for Emulsifying Activity Index. *J. Agric. Food*
25 480 *Chem.* 1991, 39, 655-659.
- 26 481 [18] Hebshy, E. Application of ultra high-pressure homogenization (UHPH) in the
27 482 production of submicron/nano-oil-in-water emulsions using vegetable oils and milk
28 483 proteins as emulsifiers. *Universitat Autònoma de Barcelona* **2013**, Doctoral degree,
29 484 ISBN 9788449040344. <http://hdl.handle.net/10803/126517>.
- 30 485 [19] Shantha, N.C.; Decker, E.A. Rapid, sensitive, iron-based spectrophotometric
31 486 methods for determination of peroxide values of food lipids. *J AOAC Int* **1994**, 77,
32 487 421-424.
- 33 488 [20] McDonald, R.E.; Hultin, H.O. Some Characteristics of the Enzymic Lipid
34 489 Peroxidation System in the Microsomal Fraction of Flounder Skeletal Muscle. *J Food*
35 490 *Sci* **1987**, 52, 15-21.
- 36 491 [21] Thiebaud, M.; Dumay, E.; Picart, L.; Guiraud, J.P.; Cheftel, J.C. High-
37 492 pressure homogenisation of raw bovine milk. Effects on fat globule size distribution
38 493 and microbial inactivation. *Int Dairy J* **2003**, 13, 427-439.
- 39 494 [22] Hayes, M.G.; Kelly, A.L. High pressure homogenisation of raw whole bovine
40 495 milk (a) effects on fat globule size and other properties. *J Dairy Res* **2003**, 70, 297-
41 496 305.
- 42 497 [23] Desrumaux, A.; Marcand, J. Formation of sunflower oil emulsions stabilized
43 498 by whey proteins with high-pressure homogenization (up to 350 MPa): effect of
44 499 pressure on emulsion characteristics. *Int J Food Sci Tech* **2002**, 37, 263-269.
- 45 500 [24] Flourey, J.; Desrumaux, A.; Axelos, M.A.V.; Legrand, J. Effect of high
46 501 pressure homogenisation on methylcellulose as food emulsifier. *J Food Eng* **2003**, 58,
47 502 227-238.
- 48 503 [25] McClements, D. J. (2005). *Food emulsions: Principles, practices, and*
49 504 *techniques*, 2nd Ed., CRC Press, Boca Raton, Florida, USA.

- 1
2
3 505 [26] Tomas, A.; Paquet, D.; Courthaudon, J.L.; Lorient, D. Effect of Fat and
4 506 Protein Contents on Droplet Size and Surface Protein Coverage in Dairy Emulsions. *J*
5 507 *Dairy Sci* **1994**, *77*, 413-417.
- 6 508 [27] Wang, B.; Li, D.; Wang, L.-J.; Özkan, N. Effect of concentrated flaxseed
7 509 protein on the stability and rheological properties of soybean oil-in-water emulsions. *J*
8 510 *Food Eng* **2010**, *96*, 555-561.
- 9 511 [28] Sun, C.; Gunasekaran, S. Effects of protein concentration and oil-phase
10 512 volume fraction on the stability and rheology of menhaden oil-in-water emulsions
11 513 stabilized by whey protein isolate with xanthan gum. *Food Hydrocolloid* **2009**, *23*,
12 514 165-174.
- 13 515 [29] Mewis, J.; Wagner, N.J. Thixotropy. *Adv Colloid Interfac* **2009**, 147-148,
14 516 214-227.
- 15 517 [30] Cha, Y., Xiaojie, S., Fan, W., Henan, Z., Chuting, C., Yingnan, G., Meng, Y.,
16 518 Cuiping, Y. Improving the stability of oil-in-water emulsions by using mussel
17 519 myofibrillar proteins and lecithin as emulsifiers and high-pressure homogenization. *J*
18 520 *Food Eng.* **2019**, *258*: 1-8.
- 19 521 [31] Srinivasan, M.; Singh, H.; Munro, P.A. Sodium Caseinate-Stabilized
20 522 Emulsions: Factors Affecting Coverage and Composition of Surface Proteins. *J Agric*
21 523 *Food Chem* **1996**, *44*, 3807-3811.
- 22 524 [32] Al-Malah, K.I.; Azzam, M.O.J.; Omari, R.M. Emulsifying properties of BSA
23 525 in different vegetable oil emulsions using conductivity technique. *Food Hydrocolloid*
24 526 **2000**, *14*, 485-490.
- 25 527 [33] Dickinson, E.; Golding, M. Rheology of Sodium Caseinate Stabilized Oil-in-
26 528 Water Emulsions. *J Colloid Interfac* **1997**, *191*, 166-176.
- 27 529 [34] Rezvani, E.; Schleining, G.; Taherian, A.R. Assessment of physical and
28 530 mechanical properties of orange oil-in-water beverage emulsions using response
29 531 surface methodology. *LWT - Food Sci Tech* **2012**, *48*, 82-88.
- 30 532 [35] Mirhosseini, H.; Tan, C.P.; Hamid, N.S.A.; Yusof, S. Optimization of the
31 533 contents of Arabic gum, xanthan gum and orange oil affecting turbidity, average
32 534 particle size, polydispersity index and density in orange beverage emulsion. *Food*
33 535 *Hydrocolloid* **2008**, *22*, 1212-1223.
- 34 536 [36] Lee, S.-H.; Lefèvre, T.; Subirade, M.; Paquin, P. Effects of ultra-high pressure
35 537 homogenization on the properties and structure of interfacial protein layer in whey
36 538 protein-stabilized emulsion. *Food Chem* **2009**, *113*, 191-195.
- 37 539 [37] Kargar, M.; Spyropoulos, F.; Norton, I.T. The effect of interfacial
38 540 microstructure on the lipid oxidation stability of oil-in-water emulsions. *J Colloid*
39 541 *Interfac* **2011**, *357*, 527-533.
- 40 542 [38] Ponginebbi, L.; Nawar, W.W.; Chinachoti, P. Oxidation of linoleic acid in
41 543 emulsions: Effect of substrate, emulsifier, and sugar concentration. *J Am Oil Chem*
42 544 *Soc* **1999**, *76*, 131.
- 43 545 [39] Sims, R. J. Oxidation of fats in food products. *Inform* **1994**, *5*, 1020-1027.
- 44 546 [40] Hsieh, Y.P.; Harris, N.D. Oxidation of Ascorbic Acid in Copper-Catalyzed
45 547 Sucrose Solutions. *J Food Sci* **1987**, *52*, 1384-1386.
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Table 1. Mean \pm SD values of temperature measured before (T1) and at the outlet (T2) of the high-pressure valve for emulsions containing different oil concentrations (10, 20 and 30%) treated by ultra high-pressure homogenization at 200 and 300 MPa ($T_{in} = 25^{\circ}\text{C}$).

Oil content (%)	Pressure (MPa)	T1 ($^{\circ}\text{C}$)	T2 ($^{\circ}\text{C}$)
10	200	41.00 ± 2.29^{ab}	84.31 ± 3.01^d
	300	43.70 ± 2.52^a	105.5 ± 3.28^b
20	200	42.70 ± 0.58^a	86.00 ± 3.00^d
	300	40.50 ± 5.50^{ab}	107.5 ± 0.50^b
30	200	44.00 ± 3.60^a	93.50 ± 3.77^c
	300	47.82 ± 3.82^a	117.2 ± 5.80^a

553

554 **Table 2.** Mean \pm SD of particle size distribution indices (d3.2 and d4.3) and specific surface area
 555 (SSA, m²/ml) of emulsions containing sunflower and olive oils (10, 20 and 30%) and prepared by
 556 colloidal mill (CM), conventional homogenization (CH, 15 MPa) and ultra high-pressure
 557 homogenization (UHPH) at 200 and 300 MPa with 5% of sodium caseinate.

Pressure (MPa)	Oil content (%)	Particle size distribution		
		d3.2 (μm)	d4.3 (μm)	Specific surface area SSA (m ² /ml)
CM	10	6.358 \pm 0.643 ^a	18.06 \pm 4.194 ^a	0.915 \pm 0.154 ^a
	20	5.410 \pm 0.303 ^{ab}	13.40 \pm 2.776 ^a	1.117 \pm 0.068 ^a
	30	5.232 \pm 0.417 ^b	12.73 \pm 2.693 ^a	1.152 \pm 0.091 ^a
CH	10	0.614 \pm 0.042 ^c	1.315 \pm 0.234 ^b	9.841 \pm 0.617 ^a
	20	0.521 \pm 0.036 ^c	0.961 \pm 0.122 ^c	11.56 \pm 0.825 ^b
	30	0.547 \pm 0.106 ^c	1.076 \pm 0.104 ^b	11.40 \pm 2.376 ^b
UHPH (200MPa)	10	0.110 \pm 0.007 ^d	0.131 \pm 0.009 ^d	54.91 \pm 3.15 ^c
	20	0.102 \pm 0.004 ^d	0.126 \pm 0.005 ^d	59.21 \pm 1.80 ^c
	30	0.108 \pm 0.008 ^d	0.130 \pm 0.010 ^d	55.70 \pm 4.060 ^c
UHPH (300MPa)	10	0.093 \pm 0.007 ^d	0.111 \pm 0.006 ^d	65.16 \pm 4.10 ^c
	20	0.105 \pm 0.014 ^d	0.119 \pm 0.007 ^d	57.06 \pm 6.991 ^c
	30	0.103 \pm 0.014 ^d	0.121 \pm 0.017 ^d	59.48 \pm 7.992 ^c

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 559 ^{a-d} Different letters in the same column indicate significant differences ($P < 0.05$)
 560 between treatments.

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562 **Table 3.** Mean \pm SD of rheological characteristics (flow and consistency indices), emulsifying activity index (EAI, m^2/g) and creaming stability
 563 (d_{4,3} values at the top or at the bottom of samples stored at room temperature for 9 days under the same conditions for comparison) of emulsions
 564 containing sunflower and olive oils (10, 20 and 30%) and prepared by colloidal mill (CM), conventional homogenization (CH, 15 MPa) and
 565 ultra high-pressure homogenization at 200 and 300 MPa with 5% of sodium caseinate.

Treatment	Oil content (%)	Rheological behavior & emulsifying activity			Emulsions creaming stability after 9 days		
		Consistency coefficient (K, mPa \times s)	Flow behavior index (n)	Emulsifying activity index (EAI, m^2/g)	D4.3 (μm) (TOP)	D4.3 (μm) (BOTTOM)	<i>P value</i>
CM	10	0.005 \pm 0.001 ^h	0.988 \pm 0.009 ^a	6.76 \pm 0.37 ^f			
	20	0.012 \pm 0.001 ^g	0.986 \pm 0.025 ^a	15.50 \pm 4.00 ^e	ND	ND	ND
	30	0.024 \pm 0.002 ^f	1.003 \pm 0.008 ^a	28.20 \pm 6.18 ^{cd}			
CH	10	0.010 \pm 0.002 ^g	0.858 \pm 0.019 ^{ab}	55.00 \pm 4.36 ^b	1.07 \pm 0.10 ^a	0.41 \pm 0.26 ^a	0.0022**
	20	0.044 \pm 0.012 ^{de}	0.754 \pm 0.038 ^{bc}	133.14 \pm 17.81 ^a	1.11 \pm 0.27 ^a	0.27 \pm 0.12 ^a	0.0022**
	30	0.209 \pm 0.104 ^{C*}	0.608 \pm 0.068 ^c	217.41 \pm 10.00 ^a	1.14 \pm 0.23 ^a	0.38 \pm 0.19 ^a	0.0022**
UHPH (200MPa)	10	0.005 \pm 0.001 ^h	0.998 \pm 0.017 ^a	8.93 \pm 1.40 ^f	0.12 \pm 0.01 ^b	0.12 \pm 0.01 ^a	0.9654
	20	0.038 \pm 0.009 ^e	0.885 \pm 0.089 ^{ab}	26.90 \pm 1.61 ^{cd}	0.14 \pm 0.02 ^b	0.14 \pm 0.02 ^a	0.9740
	30	1.937 \pm 0.148 ^{B*}	0.339 \pm 0.052 ^d	38.76 \pm 4.41 ^{bc}	0.12 \pm 0.01 ^b	0.12 \pm 0.01 ^a	0.8442
UHPH (300MPa)	10	0.005 \pm 0.001 ^h	1.011 \pm 0.008 ^a	6.49 \pm 0.98 ^f	0.10 \pm 0.01 ^b	0.11 \pm 0.01 ^a	0.3745
	20	0.049 \pm 0.009 ^d	0.850 \pm 0.044 ^{ab}	20.55 \pm 3.47 ^{de}	0.12 \pm 0.02 ^b	0.12 \pm 0.02 ^a	0.7338
	30	4.283 \pm 1.022 ^{A*}	0.252 \pm 0.039 ^d	27.31 \pm 5.42 ^{cd}	0.11 \pm 0.01 ^b	0.11 \pm 0.01 ^a	0.8593

566 a-f Different small letters in the same column indicate significant differences ($P < 0.05$) between treatments.

567 *A-C Different capital letters in the same column indicate significant differences ($P < 0.05$) between CH and UHPH emulsions with 30% oil content. This group of samples were compared
 568 separately from rest of the samples due to the high variation in viscosity.

569 **Sign and bold font size indicate that the differences between the d_{4,3} at the top or at the bottom of emulsions are significant (Wilcoxon statistic test $P < 0.05$) per level of pressure and protein
 570 concentration.

571 * ND means not determined

572 **Table 4.** Mean \pm SD of hydroperoxides (milliequivalents /kg) and TBA reactive substances ($\mu\text{g malondialdehyde/mL}$) of O/W emulsions
 573 containing sunflower and olive oils (10, 20 and 30%) and prepared by colloidal mill (CM), conventional homogenization (CH, 15 MPa) and
 574 ultra high-pressure homogenization (UHPH) at 200 and 300 MPa with 5% of sodium caseinate.

Pressure (MPa)	Oil content (%)	Hydroperoxides (Milliequivalents /kg)			TBARS ($\mu\text{g Malondialdehyde/mL}$)		
		Day 1	Day 10	Diference (Day 10 – Day 1)	Day 1	Day 10	Diference (Day 10 – Day 1)
CM	10	0.482 \pm 0.297 ^a	2.322 \pm 0.218 ^a	1.840 \pm 0.079 ^a	0.217 \pm 0.054 ^a	0.239 \pm 0.055 ^a	0.022 \pm 0.017 ^c
	20	0.421 \pm 0.305 ^a	0.833 \pm 0.417 ^b	0.412 \pm 0.112 ^{bc}	0.107 \pm 0.008 ^{cd}	0.146 \pm 0.008 ^{bcde}	0.039 \pm 0.014 ^{bc}
	30	0.197 \pm 0.087 ^a	0.578 \pm 0.112 ^{bc}	0.381 \pm 0.025 ^{bc}	0.155 \pm 0.010 ^{abc}	0.218 \pm 0.019 ^{ab}	0.062 \pm 0.013 ^{ab}
CH	10	0.320 \pm 0.033 ^a	0.542 \pm 0.189 ^{bc}	0.222 \pm 0.156 ^{bc}	0.174 \pm 0.006 ^{abc}	0.144 \pm 0.003 ^{bcde}	- 0.030 \pm 0.005 ^e
	20	0.198 \pm 0.062 ^a	0.703 \pm 0.077 ^b	0.505 \pm 0.016 ^b	0.065 \pm 0.003 ^d	0.070 \pm 0.002 ^e	0.005 \pm 0.004 ^{cde}
	30	0.603 \pm 0.399 ^a	0.493 \pm 0.334 ^{bc}	- 0.109 \pm 0.099 ^{bc}	0.154 \pm 0.012 ^{abc}	0.172 \pm 0.008 ^{abc}	0.017 \pm 0.008 ^{cd}
UHPH 200MPa	10	0.655 \pm 0.514 ^a	0.248 \pm 0.065 ^{bc}	- 0.406 \pm 0.449 ^c	0.141 \pm 0.005 ^{bc}	0.182 \pm 0.009 ^{abc}	0.040 \pm 0.012 ^{bc}
	20	0.280 \pm 0.212 ^a	0.181 \pm 0.037 ^{bc}	- 0.099 \pm 0.175 ^{bc}	0.107 \pm 0.004 ^{cd}	0.091 \pm 0.004 ^{de}	- 0.015 \pm 0.008 ^{de}
	30	0.237 \pm 0.075 ^a	0.106 \pm 0.073 ^{bc}	- 0.131 \pm 0.013 ^{bc}	0.187 \pm 0.008 ^{ab}	0.200 \pm 0.011 ^{ab}	0.013 \pm 0.016 ^{cd}
UHPH 300MPa	10	0.602 \pm 0.108 ^a	0.225 \pm 0.099 ^{bc}	- 0.377 \pm 0.062 ^{bc}	0.148 \pm 0.008 ^{abc}	0.239 \pm 0.014 ^a	0.091 \pm 0.020 ^a
	20	0.032 \pm 0.003 ^a	0.023 \pm 0.004 ^c	- 0.008 \pm 0.001 ^{bc}	0.108 \pm 0.013 ^{cd}	0.114 \pm 0.011 ^{cde}	0.005 \pm 0.013 ^{cde}
	30	0.108 \pm 0.025 ^a	0.097 \pm 0.031 ^{bc}	- 0.011 \pm 0.040 ^{bc}	0.132 \pm 0.011 ^{bcd}	0.155 \pm 0.010 ^{bcd}	0.023 \pm 0.005 ^c

a-h Different letters in the same column indicate significant differences ($P < 0.05$) between treatments.

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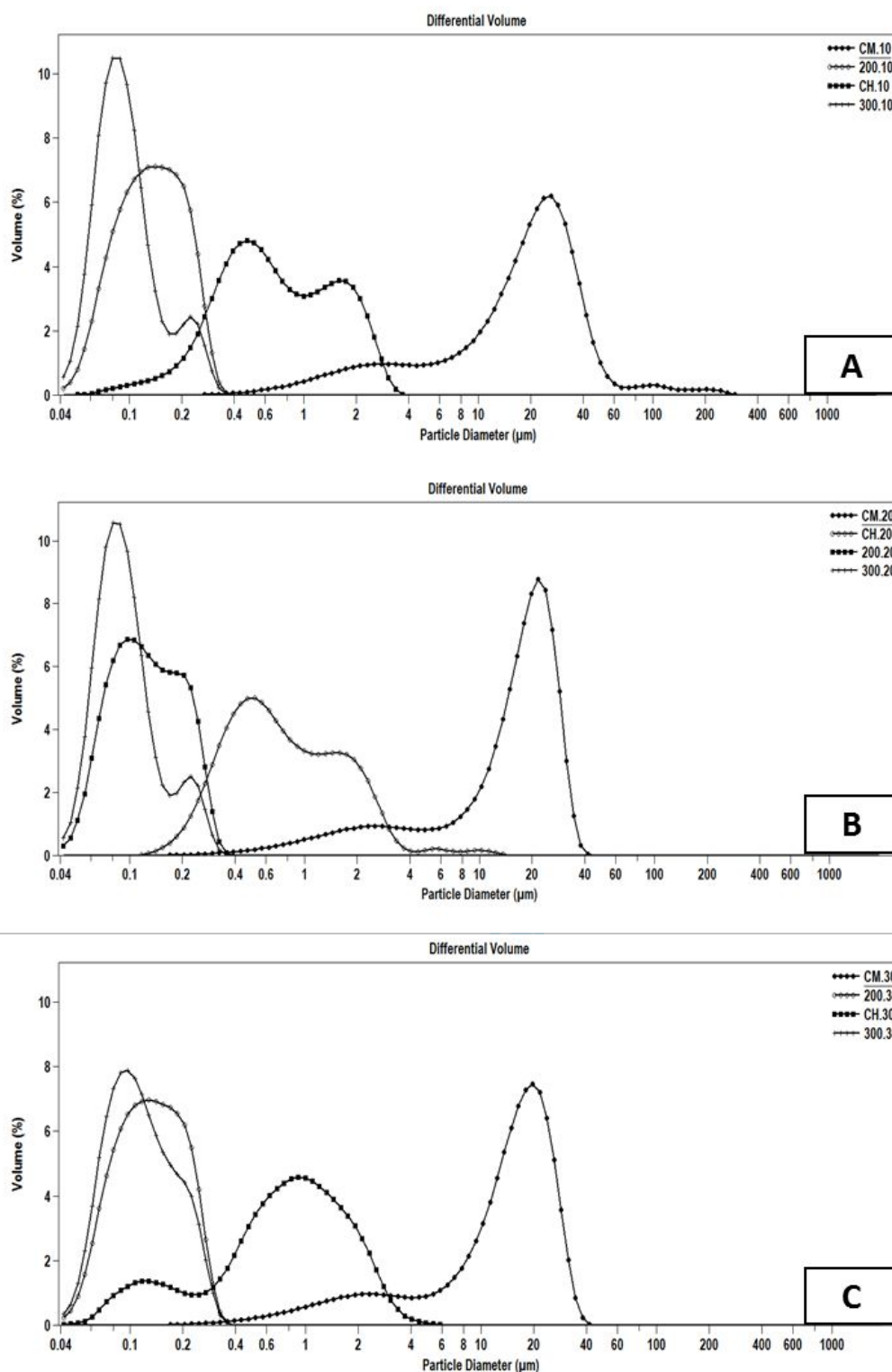
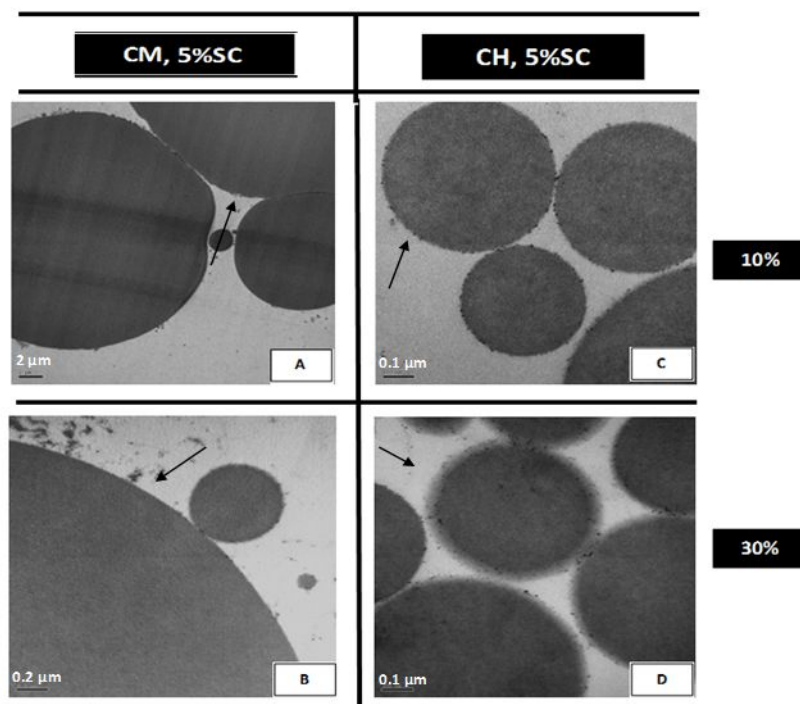


Figure 1.

Droplet size distribution curves measured by light scattering of O/W emulsions containing 5% of sodium caseinate and sunflower and olive oils at (a) 10, (b) 20 and (c) 30%, and prepared by colloidal mill (CM), conventional homogenization (15 MPa) and ultra high-pressure homogenization at 200 and 300 MPa.

(A)



(B)

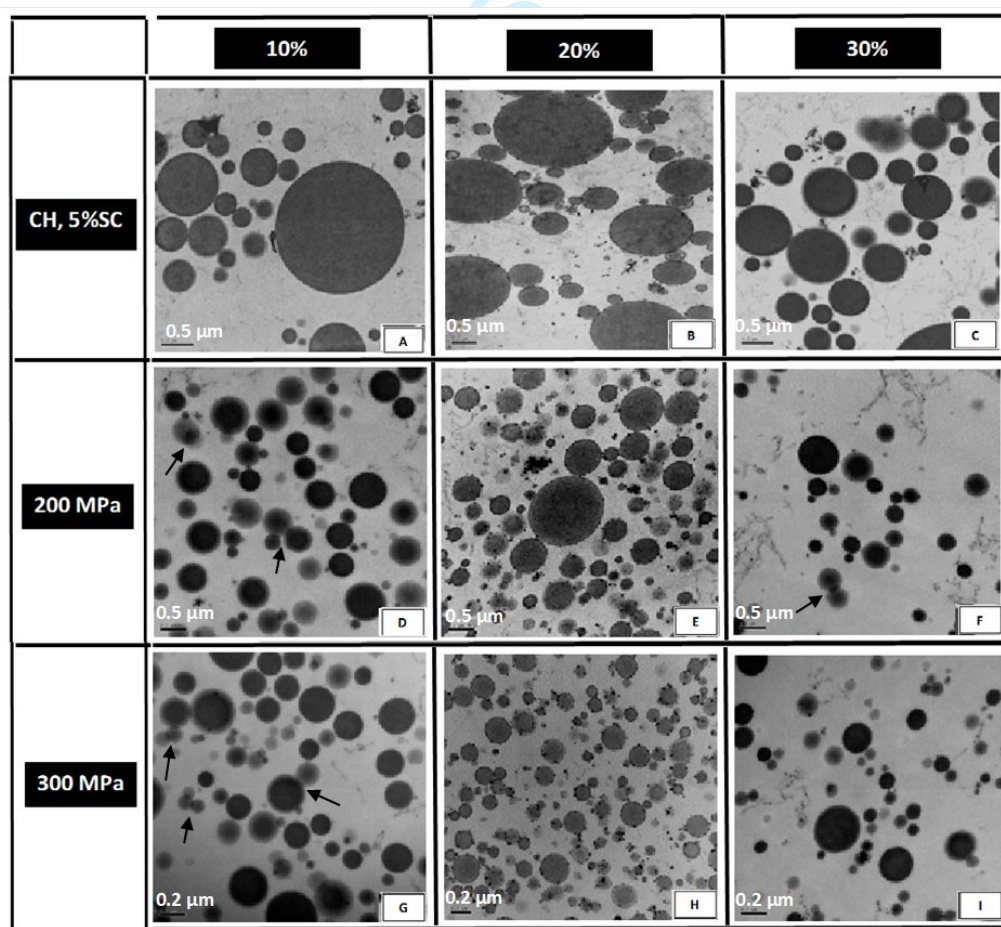


Figure 2.

(A) TEM images of O/W emulsions containing sunflower and olive oils at 10% (A,C) and 30% (B,D) and prepared by (A,B; $\times 4000$ and $\times 50000$, respectively) colloidal mill (CM), and by (C,D; $\times 100000$) conventional homogenization (15 MPa) with 5% of sodium caseinate. Arrows indicate the coalescence between droplets in image (A) and difference in the protein amounts on the interface of oil droplets in images (B, C and D).

(B) TEM images ($\times 50000$) of O/W emulsions containing sunflower and olive oils (10, 20 and 30%) and 5% of sodium caseinate, prepared by (A-C) conventional homogenization (15 MPa) and (D-I) by ultra high-pressure homogenization at 200 MPa (D-F) and 300 MPa (G-I). Arrows indicate flocculation and coalescence between oil droplets.

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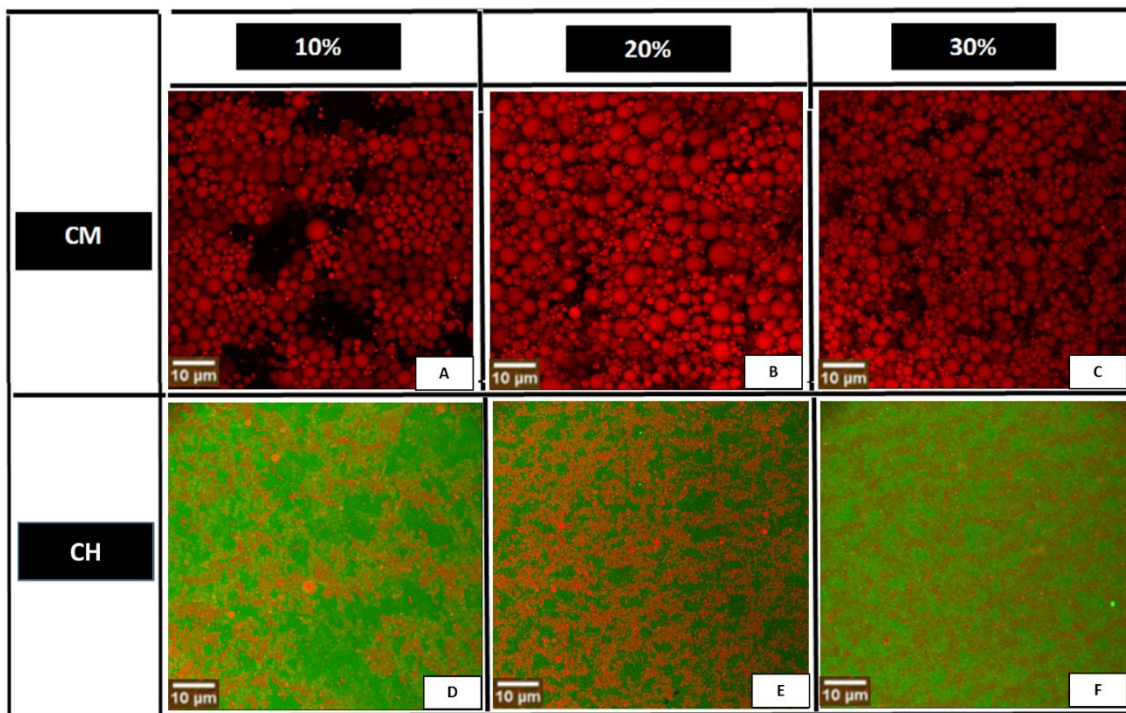


Figure 3. Confocal laser scanning microscope images of O/W emulsions containing sunflower and olive oils (10, 20 and 30%) and 5% of sodium caseinate, and prepared by (A-C) colloidal mill (CM) and (D-F) conventional homogenization (15 MPa).

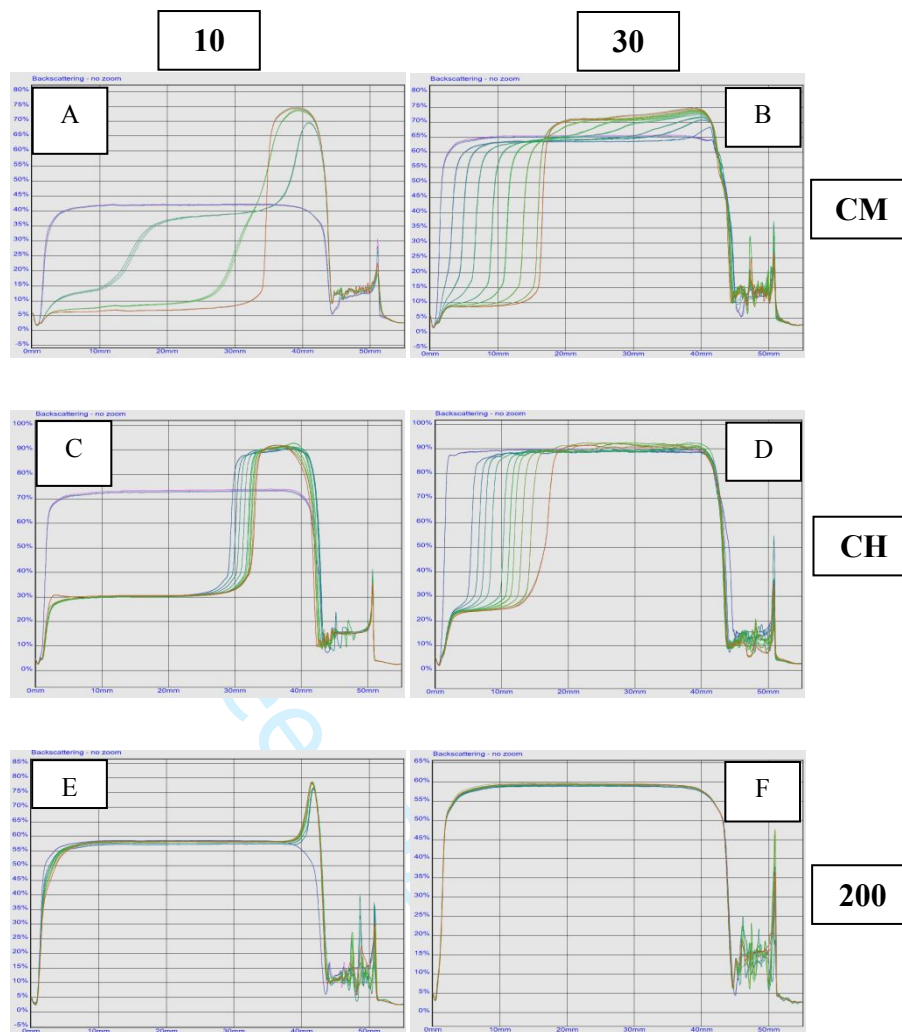


Figure 4. Changes in backscattering profiles of O/W emulsions containing sunflower and olive oils (10 and 30%) and 5% of sodium caseinate and prepared by (A,B) colloidal mill (CM), conventional homogenization (15 MPa) (C,D), and by ultra high-pressure homogenization (UHPH) at 200 (E,F), as a function of sample height with storage time (5 h for CM emulsions and 18 days for both CH and UHPH emulsions).

