Formula Sheet for all Wastewater Operator Exams Revised 8/15

F001

Surface area of a pond, acres = Length, ft x Width, ft 43560

F002

F004

BOD removal efficiency,
$$\% = \left(\frac{\text{Influent BOD, mg/L} - \text{Effluent BOD, mg/L}}{\text{Influent BOD, mg/L}}\right) \times 100\%$$

F008

Theoretical detention time of a pond, days = Volume of the pond, MG Flow rate. MGD

F011

Removal efficiency,
$$\% = \left(\frac{\text{Influent concentration} - \text{Effluent concentration}}{\text{Influent concentration}}\right) \times 100\%$$

F012

Solids, lbs= (Volume, MG) x (MLSS, mg/L) x (8.34)

F016

Average flow rate, MGD = (Final flow, MG) - (Initial flow, MG)
Time elapsed, days

F017

BOD loading, lbs/day = (Flow rate, MGD) x (BOD, mg/L) x 8.34

F018

TSS removal efficiency, % =
$$\left(\frac{Influent TSS - Effluent TSS}{Influent TSS}\right) \times 100\%$$

F020

Volume of sample needed for a BOD test bottle, $mL = \frac{1200}{EstimatedBOD of the sample,mg/L}$

F021

BOD,
$$mg/L = \frac{(Initial D.O., mg/L - Final D.O., mg/L) \times 300 mL}{Sample volume, mL}$$

Chlorine feed rate, lbs/day = (Flow, MGD) x (Dosage, mg/L) x (8.34)

F023

TSS test results, mg/L = $\left(\frac{\text{Net dry weight, mg}}{\text{Sample volume, mL}}\right) \times 1000 \text{ mL/L}$

F030

Pump capacity, $gpm = \underline{\text{(Width, ft)}} \times \underline{\text{(Length, ft)}} \times \underline{\text{(Draw-down, ft)}} \times 7.48$ Time of draw-down in minutes

F030B

Increased flow = $\frac{\text{(New pipe diameter, inch)}^2}{\text{(Old pipe diameter, inch)}^2}$

F030C

Flow rate in a pipe, gpd =

$$\left\lceil \frac{ (\text{Pipe diameter,inches})^2}{(12\,\text{in/ft})^2} \right\rceil \times 0.785 \times (\text{Velocity, ft/sec}) \times 60\,\text{sec/min} \times 1440\,\text{min/day} \times 7.48\,\text{gal/cf}$$

F032

Desired suspended solids, lbs = (Sludge age, days) x (Primary effluent solids, lb/day)

F033

Volume per stroke, gal/stroke =
$$\left[\frac{(0.785) \times (\text{Diameter,inches})^2}{12^2} \right] \times \left[\frac{(\text{Stroke,inches}) \times (7.48)}{12} \right]$$

F034

Total dry solids, lbs = $(Raw sludge, gal) \times (Total solids, %) \times (8.34)$ 100%

F035

MLSS, lbs = (Aeration volume, MG) x (MLSS conc, mg/L) x (8.34)

F037

Digestion time, days = <u>Digester volume, gal</u> Flow, gpd

F038

Phosphorus (P) removal, $\% = \left(\frac{\text{Influent P, mg/L} - \text{Effluent P, mg/L}}{\text{Influent P, mg/L}}\right) \times 100\%$

Sludge applied, gal = $(Area, sf) \times (Depth of application, in) \times (7.48)$ 12 in/ft

F040

Pollutant emission rate, lbs/day = $(Flow, gpd) \times (Pollutant conc., mg/L) \times (3.785 L/gal)$ 453,600 mg/lb

F043

Chemical application rate, lbs/day = (Flow, MGD) x (Chemical dosage, mg/L) x 8.34

F045

Flux, gpd/sf = $(Flow rate, gpm) \times (60 min/hr) \times (24 hr/day)$ Surface area of membrane, sf

F047

New, or actual, WAS flow rate, MGD = $(Calculated WAS flow, MGD) \times (24hr/day)$ Actual hours of sludge wasting, hr/day

F048

Solids produced, lbs/day = (BOD removed, lbs/day) x (Yield factor)

F050

Primary sludge, lbs/day = (Flow rate, MGD) x (Inflow SS, mg/L - Effluent SS, mg/L) x 8.34

F052

Hydraulic loading of a DAF unit, gpd/sf = (Inflow rate, gpm) x (1440) Liquid surface area, sf

F053

Solids loading to a centrifuge, lbs/hr = (Sludge flow rate, gal/hr) x (Sludge conc %) x 8.34 lbs/gal 100%

F054

Efficiency of solids removal, $\% = \left(\frac{\text{Influent SS}, \% - \text{Effluent SS}, \%}{\text{Influent SS}, \%}\right) \times 100\%$

Dry polymer, lbs = $(Volume of solution, gal) \times \left(\frac{Polymer concentration, \%}{100\%}\right) \times (8.34 lb/gal)$

F058

Pumping rate, gpm = $(Volume, cf) \times (7.48 \text{ gal/cf})$ Time, min

F061

Surface loading, $gpd/sf = \frac{Flow, gpd}{Surface area, sf}$

F062

Solids loading, lbs/day/sf = (Flow, MGD) x (TSS, mg/L) x (8.34) Surface area, sf

F063

Sludge age = $\frac{TSS \text{ in aerator, lbs}}{TSS \text{ in primary effluent, lbs/day}}$

F064

F/M = <u>lbs BOD/day to aeration tank</u> lbs of MLVSS under aeration

F065

Waste sludge pumping rate, MGD =

 $Current pump rate, MGD + \left[\frac{\left(Difference in aerator sludge inventory, lbs\right)}{\left(RAS \ concentration, mg/L\right) \times 8.34}\right]$

F066

MCRT, days = $\frac{\text{MLSS in aeration tion tank, lbs}}{(\text{TSS wasted, lbs/day}) + (\text{TSS in effluent, lbs/day})}$

F068

MLVSS, mg/L = $\frac{\text{BOD Loading from primary, lbs/day}}{(\text{F/M Ratio}) \times (\text{Aerator volume, MG}) \times (8.34)}$

F069

Return sludge rate, MGD = Settled solids, mL x (Flow, MGD) (1000 mL - Settled solids, mL)

F073

S0₂ feed, lbs/day =(Flow, MGD) x (Residual chlorine, mg/L + SO₂ overdose, mg/L) x (8.34)

Chlorine demand, mg/L = (Chlorine dose, mg/L) - (Chlorine residual, mg/L)

F076

Polymer dose, mg/L = (Polymer delivery rate, gpm) x (Polymer, Ibs/gal) x (1,000,000) (Flow, gpm) x (8.34)

F077

Polymer dose, mg/L = $\frac{\text{(Polymer feed rate, lbs/day)} \times (1,000,000)}{\text{(Flow, gpm)} \times (1440) \times (8.34)}$

F078

Volume of seed sludge, gal = (Volume of digester, gal) x (% seed)

F079

Solid loading, lbs/day = (Raw sludge volume, gal)x(Solid conc,%)x(Volatile fraction,%)x(8.34)

F081

Total settleable solids to pump to digester, $gpd = (Sludge removed, mL) \times (Flow, MGD) \times (1000)$

F082

% reduction of volatile matter, % = $\frac{(\ln - \text{Out}) \times (100)}{\ln - [(\ln) \times (\text{Out})]}$ ("in" and "out" in fraction, not in %)

F083

% reduction of volatile matter, % = $\left[\frac{\text{(Initial volatile matter, lbs)} - \text{(Final volatile matter, lbs)}}{\text{Initial volatile matter, lbs}} \right] \times 100\%$

F087

Seed correction per 1.0 mL of seed = <u>Initial D.O. – Final D.O.</u> mL of seed in bottle

and

 $BOD_{5}, \ mg/L \ = \ \left\{ \frac{\left[\left(Initial\,DO, mg/L\right) - \left(Final\,DO, mg/L\right)\right] - \left(Seed\,correction, mg/L\right)}{Sample\,volume, mL} \right\} \times 300\,mL$

F088

Volume diluted, mL = (<u>Target normality</u>) x (<u>Target volume, mL</u>) Stock acid normality

F091

Sludge flow, MGD = $\underline{\text{(Thickener loading, lbs/day/sf)} \times \text{(Surface area, sf)}}$ (8.34) x (10,000) x (% solids)

F092

Desired lbs of solids in aeration tank = (Daily solids addition, lbs/day) x (Sludge age, days)

New digestion time, days = (Digester volume, gal)x(Increase in sludge conc,%-Initial sludge conc,%) (Initial sludge flow, qpd) x (Initial sludge conc, %)

F096

Volume of working solution, $mL = (Beaker volume, mL) \times (Dosage, mg/L)$ (Stock solution conc, %) x (10,000)

F097

Chemical feed rate, gph = $(Flow, MGD) \times (Dosage, mg/L) \times 100\%$ (Solution strength, %) x (24 hr/day)

F098

Surface loading rate, $gpd/sf = \underline{(Flow\ rate,\ MGD)\ x\ (1,000,000\ gal/MG)}$ (Diameter, ft)² x (0.785)

F099

Polymer dosage, mg/L = (Polymer pumping rate, gpm) x (Polymer conc. lbs/gal) x (1,000,000) (Sludge flow rate, gpm) x (8.34 lbs/gal)

F100

Retention % = $\frac{(Retentate conc., mg/L) - (Permeate conc., mg/L)}{Retentate conc., mg/L} \times 100\%$

F101

Average transmembrane pressure, psi = (Inlet pressure, psi + Outlet pressure, psi) - Permeate pressure, psi

F103

RAS, MGD = (Settled volume, mL/L) x (Influent flow rate, MGD) (1000 mL/L) - (Settled volume, mL/L)

F105

 $Sludge \ age, \ days = \frac{\left(Tank \ volume, MG\right) \times \left(MLSS, mg/L\right)}{\left(Inflowrate, MGD\right) \times \left(Primary \ effluent \ SS, mg/L\right)}$

F106

F/M, lb COD/day per lb MLVSS = $\frac{(Flow, MGD) \times (COD, mg/L) \times (8.34 \, lbs/gal)}{(Solids under aeration, lbs) \times (Volatile fraction)}$

F108

Phosphorus to be added, lbs/day = [BOD lbs/day x P/BOD (desired ratio)] - (P in wastewater, lbs)

Desired COD loading, lbs/day = (COD loading rate, lbs COD/lbs VS) x (VS, lbs)

F111

Sludge produced, lbs/day = (Flow, MGD) x (Influent BOD, mg/L - Effluent BOD, mg/L) x (8.34 x yield factor)

F112

Thickened sludge volume, gal/day = $\left(\frac{\text{Sludge,lbs/day}}{8.34\,\text{lbs/gal}}\right) \times \left(\frac{100\%}{\text{Sludge solids concentration, \%}}\right)$

F114

Solids loading, lbs/hr/sf = $(Flow, gpm) \times (60) \times (8.34 lbs/gal) \times (SS\%)$ (Liquid surface area, sf) x (100%)

F115

Air to solids ratio = $\frac{\text{(Air supplyrate, cfm)} \times (0.075 \,\text{lb/cf}) \times (100\%)}{\text{(Solids feed rate, gpm)} \times \text{(Sludge conc, \%)} \times (8.34 \,\text{lbs/gal})}$

F116

Feed time to a centrifuge, min = $(Storage volume, cf) \times (Basket sludge conc, %) \times (62.4 lbs/cu ft)$ (Flow, gpm) x (Influent solids, %) x (8.34 lbs/gal)

F117

Increase of detention time, days = $\frac{(\text{Aerobic digester volume, gal}) \times (\text{Increase in sludgeconc., \%})}{(\text{Initial sludgeflow, gpd}) \times (\text{Initial sludgeconc., \%})}$

F122

Polymer dosage, lbs/ton = (Polymer solution conc, %) x (Polymer added, gpm) x (2,000 lbs/ton) (Sludge conc, %) x (Sludge flow rate, gpm)

F123

 $Vacuum \ filter \ yield, \ lbs/hr/sq \ ft = \frac{Sludgeloading,lbs/day \times \left(\frac{Recovery, \%}{100\%}\right)}{\left(Duration of \ filter \ operation,hr/day\right) \times \left(Filter \ area,sf\right)}$

F124

Required filter run time, hr/day = Sludge solids loading, lbs/day x Solids recovery, % (Filter yield, lbs/hr/sf) x (Filter area, sf) x (100%)