## Introduction to Turbomachines

1. Define turbo machines. Briefly classify Turbomachines (1a, 06,Dec18/19, 1a, 08,Dec17/Jan18)
2. Define turbo machines. Briefly classify on the basis of work transfer (1a, 04,June/July14,)
3. Define turbomachine. Explain with neat sketch construction and working of turbomachine (1a, 06, June/July 18,1a,06,Dec15/Jan16, 1a,4, Dec13/Jan14)
4. Enumerate the difference between a turbomachine and a positive displacement pump (1b, 06, June/July 18,1a,08, Dec 18/jan19, 1a, 05, June/july 17,1a, 05, Dec16/Jan17,1a,06, June/July16, 1a, 06, June/July13)
5. Define with appropriate expressions i) flow mcoefficient ii) head coefficient iii) power coefficient iv) specific speed ( 1a, 08, June/July 18 15ME53,1b, 05,June/July 17)
6. Define specific speed of pumps. Derive an expression for specific speed of a pump 1b,08, Dec16/Jan17,1b, 06, Dec14/Jan15)
7. Define specific speed of a turbine. Obtain an expression for the same in terms of $P$ shaft power speed and head ( $1 \mathrm{c}, 06$, June/July13)
8. Define specific speed and specific power (1c, 04, June/July14)
9. Define specific speed of a pump and a turbine . Explain the significance of specific speed (1b, 06, Dec13/Jan14)
10. Define specific speed of pump. Show that specific speed of pump is given by $N_{s}=\frac{N \sqrt{Q}}{H^{\frac{3}{4}}}(1 \mathrm{~b}, 06$, Dec18/19, 1b, 06, Dec17/Jan 18)
11. What are Unit quantities.? Derive the expressions to each of them (1b, 06, June/July16)
12. With usual notations, derive expressions for unit Discharge coefficient, Head coefficient, and Power coefficient using Dimensional analysis (1c, 06, Dec15/Jan16)
13. Deducing an expression, expalain the significance of second law of thermodynamics applied to a turbo machine (1a, 06, Dec12)
14. Explain the significance of first and second law of thermodynamics applied to a turbomachine (1a, 06, Dec14/Jan15)
15. Define the following efficiencies of power obsorbine macines i) Total to total efficiency ii) static to static efficiency (1b, 06, June/July14)

Turbo Machine: It is a device in which energy transfer takes place between a flowing fluid and a rotating element due to dynamic action and results in change of pressure and momentum of fluid

Example: Turbine, centrifugal compressors, centrifugal pumps:
Principle components of turbomachines:

1. Rotor which carries a series of blades, rotating in the steams of fluid flow
2. A stationary element (fixed blade) which usually acts as a guide way for the proper control of proper direction during energy conversion process
3. An input shaft

## Classification of Turbo machine:

## i) Classification Based on Direction of Energy Conversion.

The device in which the kinetic, potential or intermolecular energy held by the fluid is converted in the form of mechanical energy of a rotating member is known as a turbine .

The machines, on the other hand, where the mechanical energy from moving parts is transferred to a fluid to increase its stored energy by increasing either its pressure or velocity are known as pumps, compressors, fans or blowers .
ii) Classification based on basic working principle
le Impulse and Reaction turbine----------
The machine for which the change in static head in the rotor is zero is known impulse machine. In these machines, the energy transfer in the rotor takes place only by the change in dynamic head of the fluid

In reaction turbine energy transfer in the rotor takes place by change in static and dynamic head of the fluid
iii) Classification based on the direction of fluid flow:

- $\quad$ Axial in which fluid enters and leaves parallel to the axis of rotor
- $\quad$ Radial in which fluid enters and leaves along the direction perpendicular to the axis of shaft
- Tangential in which fluid flow is tangent to the shaft
- Mixed flow: in which fluid entry is axial , exit is radial or vice versa

Difference between positive displacement machine and turbo machine:

| SI No | Positive Displacement machine | Turbomachine |
| :--- | :--- | :--- |
| 1 | Energy transfer takes place due to static <br> action and thermodynamic between <br> rotor and static fluid | Energy transfer takes place between <br> rotor and fluid due to dynamic action <br> and thermodynamics between rotor <br> and flowing fluid |
| 2 | Reciprocating in nature | Rotary in nature |
| 3 | Fluid flow is Unsteady | Fluid flow is Steady |
| 4 | Fluid containment is positive | Fluid containment is not positive |
| 5 | Low speed machine | High speed machine |
| 6 | Complex in design | Simple in design |
| 7 | Balancing of parts is difficult | Balancing of parts is easy |
| 8 | There is no problem of surging and <br> cavitation | There is problem of surging and <br> cavitiaon |
| 9 | Conversion efficiency is high | Conversion efficiency is low |
| 10 | Volumetric efficiency low | Volumetric efficiency is high |

## Dimension Analysis

| Force( N )/resistnace | mass x acceleration | $\mathrm{kg} \mathrm{m} / \mathrm{sec}^{2}$ | $\mathrm{MLT}^{-2}$ |
| :---: | :---: | :---: | :---: |
| work/Energy/Torque | Force x displacement | Nm | $\mathrm{MLT}{ }^{-2} \mathrm{xL}=\mathrm{ML}^{2} \mathrm{~T}^{-2}$ |
| Pressure/Change in Pressure | Force/Area | $\mathrm{N} / \mathrm{m}^{2}$ | $\mathrm{MLT}^{-2} / \mathrm{L}^{2}=\mathrm{ML}^{-1} \mathrm{~T}^{-2}$ |
| Power | workdone /sec | $\mathrm{Nm} / \mathrm{s}$ | $\mathrm{ML}^{2} \mathrm{~T}^{-2} \mathrm{x} T=\mathrm{ML}^{2} \mathrm{~T}^{-3}$ |
| Velocity | distance/sec | $\mathrm{m} / \mathrm{s}$ | $\mathrm{LT}^{-1}$ |
| Density | mass/Volume | $\mathrm{kg} / \mathrm{m}^{3}$ | $\mathrm{ML}^{-3}$ |
| Absolute viscosity |  | $\mathrm{Ns} / \mathrm{m}^{2}$ | $\mathrm{MLT}^{-2} \times \mathrm{T} / \mathrm{L}^{2}=\mathrm{ML}^{-1} \mathrm{~T}^{-1}$ |
| Kinematic viscosity | Absolute Viscosity/Density | $\mathrm{m}^{2} / \mathrm{s}$ | $\mathrm{ML}^{-1} \mathrm{~T}^{-1} / \mathrm{ML}^{-3}=\mathrm{L}^{2} \mathrm{~T}^{-1}$ |
| Surface tension |  | $\mathrm{N} / \mathrm{m}$ | $\mathrm{MLT}^{-2} / \mathrm{L}=\mathrm{MT}^{-2}$ |
| Discharge |  | $\mathrm{m}^{3} / \mathrm{s}$ | $\mathrm{L}^{3} \mathrm{~T}^{-1}$ |
| Energy per Unit mass | gH | $\mathrm{m}^{2} / \mathrm{s}$ | $\mathrm{ML}^{2} \mathrm{~T}^{-2} / \mathrm{M}=\mathrm{L}^{2} \mathrm{~T}^{-2}$ |
| Surface roughness |  | m | L |
| Length/Diameter/Height |  | m | L |
| Angular speed, speed of rotor |  | $\mathrm{rad} / \mathrm{sec}, \mathrm{rpm}$ | $\mathrm{T}^{-1}$ |
| Efficiency/pressure ratio |  | No dimension | Dimensionless number |

Performance of a turbomachine depends upon the following
Discharge Q , speed or rpm N , size of the rotor D , energy per unit mass gH , Power P , density $\rho$, dynamic viscosity $\mu$, Using dimensional analysis find the $\pi$ terms
$f(Q, N, D, g H, P, \rho, \mu)=0$
no of variables $n=7$
no of fundamental variables $\mathrm{m}=3$
no of $\pi$ terms $=n-m=7-3=4$

Let us select repeated variables, $\rho$ (fluid property) $N$ (dynamic property) D (Geometrical Property)
$\Pi_{1}=\rho^{\mathrm{a} 1}, \mathrm{~N}^{\mathrm{b} 1}, \mathrm{D}^{\mathrm{c} 1}, \mathrm{Q}$
$\Pi_{2}=\rho^{a 2}, N^{b 2}, D^{c 2}, g H$
$\Pi_{3}=\rho^{\mathrm{a} 3}, N^{\mathrm{b} 3}, \mathrm{D}^{\mathrm{c} 3}, \mathrm{P}$
$\Pi_{4}=\rho^{\mathrm{a} 4}, \mathrm{~N}^{\mathrm{b} 4}, \mathrm{D}^{\mathrm{c4}}, \mu$
$Q=L^{3} T^{-1}, N=T^{-1}, D=L, \rho=M L^{-3}, g H=L^{2} T^{-2}, \mu=M L^{-1} T^{-1}, P=M L^{2} T^{-3}$
$\Pi_{1}$
$M^{0} L^{0} T^{0}=\left(M L^{-3}\right)^{a 1}\left(T^{-1}\right)^{b 1} L^{c 1} L^{3} T^{-1}$

M ----- $0=a_{1}$

T------ $\quad 0=-b_{1}-1 \quad$ ie $b_{1}=-1$

L------- $0=-3 a_{1}+C_{1}+3$ ie $0=-3 x(0)+C_{1}+3$ ie $C_{1}=-3$
$\Pi_{1}=\rho^{0}, N^{-1}, D^{-3}, Q$
$=\frac{Q}{N D^{3}}$ Flow coefficient
$\Pi_{2}$
$M^{0} L^{0} T^{0}=\left(M L^{-3}\right)^{a 2}\left(T^{-1}\right)^{b 2} L^{c 2} L^{2} T^{-2}$
M ---- $0=a_{2}$

T------ $0=-b_{2}-2 \quad$ ie $b_{2}=-2$
$L-----\quad 0=-3 a_{2}+C_{2}+2$ ie $0=-3 x(0)+C_{2}+2$ ie $C_{2}=-2$
$\Pi_{2}=\rho^{0}, N^{-2}, D^{-2}, g H ; \quad \Pi_{2}==\frac{g H}{N^{2} D^{2}} \quad$ Head coefficient

## $\Pi_{3}$


$M$----- $0=a_{3}+1$ ie $a_{3}=-1$
T------ $\quad 0=-b_{3}-3 \quad$ ie $b_{3}=-3$
L------- $0=-3 a_{3}+C_{3}+2$ ie $0=-3 x(-1)+C_{3}+2$ ie $C_{3}=-5$
$\Pi_{3}=\rho^{-1}, N^{-3}, D^{-5}, \mathrm{P} ; \quad \Pi_{3}=\frac{\boldsymbol{P}}{\boldsymbol{\rho}^{1} N^{3} D^{5}} \quad$ Power coefficient
$\Pi_{4}$
$\mathrm{M}^{0} \mathrm{~L}^{0} \mathrm{~T}^{0}=\left(\mathrm{ML}^{-3}\right)^{\mathrm{a} 4}\left(\mathrm{~T}^{-1}\right)^{\mathrm{b4}} \mathrm{~L}^{\mathrm{c} 4} \mathrm{ML}^{-1} \mathrm{~T}^{-1}$
$M----\quad 0=a_{4}+1 \quad$ ie $a_{4}=-1$
T------ $\quad 0=-b_{4}-1 \quad$ ie $b_{4}=-1$
L------- $\quad 0=-3 a_{4}+C_{4}-1$ ie $0=-3 \times(-1)+C_{4}-1$ ie $C_{4}=-2$
$\Pi_{4}=\rho^{-1}, \mathrm{~N}^{-1}, \mathrm{D}^{-2}, \mu ; \quad \Pi_{4}==\frac{\mu}{\rho^{1} N^{1} D^{2}}$

## Significance of $\pi$ terms

$\Pi_{1}=\frac{Q}{N D^{3}}$ is called as flow coefficient / capacity coefficient
It is defined as the volume flow rate of the fluid through a turbomachine of unit diameter of runner operating at unit speed ie flow coefficient $=\mathrm{Q}$ when $\mathrm{N}=1$ and $\mathrm{H}=1$

From above $\pi_{1}$ term for a pump of certain diameter running at various speeds the discharge is proportional to the speed of the pump. This is called as First fan Law
$\Pi_{2}=\frac{g H}{N^{2} D^{2}}$ is called as Head coefficient
Since $U$ is directly proportional to $D N, N^{2} D^{2}$ can be replaced in $\pi$ term as $U^{2}$
Hence $\pi_{2}=\frac{H}{\frac{U^{2}}{g}}$
From the above expression, for a given impeller, head varies as the square of the tangential speed of the rotor. This is called second fan law
$\Pi_{3}=\frac{P}{\rho^{1} N^{3} D^{5}} \quad$ Power coefficient

From the above expression for the same runner of turbomachine and same fluid Power developed by the turbomachine is directly proportional to the cube power of speed. This is called $3^{\text {rd }}$ fan law

Specific speed for a pump: It is defined as the speed of the geometrically similar turbomachine (pump) which discharges $1 \mathrm{~m}^{3} / \mathrm{s}$ under unit head
$\mathrm{N}=\mathrm{N}_{\mathrm{s}}$ when $\mathrm{Q}=1 \mathrm{~m}^{3} / \mathrm{s}$ and $\mathrm{H}=1 \mathrm{~m}$
$\Pi_{2}=\frac{g H}{N^{2} D^{2}}$ is called as Head coefficient
From the above expression $H \alpha D^{2} N^{2}$

D $\alpha \frac{\sqrt{H}}{N}$ $\qquad$
From flow coefficient $\frac{Q}{N D^{3}}$; le $\mathrm{Q} \alpha \mathrm{ND}^{3}$
Substituting 1 in above eqution
$\mathrm{Q} \alpha \mathrm{N}\left(\frac{\sqrt{H}}{N}\right)^{3} ; \quad \mathrm{Q} \alpha \frac{H^{3 / 2}}{N^{2}} ; \quad \mathrm{Q}=\frac{k H^{3 / 2}}{N^{2}}$
From the definition of specific speed $N=N_{s}$ when $Q=1$ and $H=1$
Hence $1=\frac{k}{N_{S}^{2}}$ ie $\mathrm{k}=\mathrm{N}_{\mathrm{s}}{ }^{2}$; Hence $\mathrm{Q}=\frac{N_{S}^{2}}{N^{2}} H^{3 / 2} ; \mathrm{N}_{\mathrm{s}}=\frac{N \sqrt{Q}}{H^{3 / 4}}$
Specific speed for a Turbine: It is defined as the speed of the geometrically similar turbomachine (turbine) which develops unit power under unit head
$\mathrm{N}=\mathrm{N}_{\mathrm{s}}$ when $\mathrm{Q}=1 \mathrm{~m}^{3} / \mathrm{s}$ and $\mathrm{H}=1 \mathrm{~m}$
$\Pi_{2}=\frac{g H}{N^{2} D^{2}}$ is called as Head coefficient
From the above expression $H \alpha D^{2} N^{2}$
$\mathrm{D} \alpha \frac{\sqrt{H}}{N}$


From Power coefficient $\frac{P}{\rho^{1} N^{3} D^{5}}$
le $P \alpha N^{3} D^{5}$ for same fluid

Substituting 1 in above equation
$\mathrm{P} \alpha \mathrm{N}^{3}\left(\frac{\sqrt{H}}{N}\right)^{5} ; \quad \mathrm{P} \alpha \frac{H^{5 / 2}}{N^{2}} ; \quad \mathrm{P}=\frac{k H^{5 / 2}}{N^{2}}$
From the definition of specific speed $N=N_{s}$ when $\mathrm{P}=1$ and $\mathrm{H}=1$

Hence $1=\frac{k}{N_{S}^{2}}$ ie $k=N_{s}{ }^{2}$
Hence $\mathrm{P}=\frac{N_{S}^{2}}{N^{2}} H^{5 / 2} ; \mathrm{N}_{\mathrm{S}}=\frac{N \sqrt{P}}{H^{5 / 4}}$ where P is in kW
Unit quantities: (Applied to same machine)

Unit discharge $\mathbf{Q}_{\underline{u}}$ : is defined as the discharge of a pump under unit Head
$\mathrm{Q}=\mathrm{AV} ; \mathrm{Q} \alpha \sqrt{H}$ for a given pump as $\mathrm{V}=\sqrt{2 g H} ; \mathrm{Q}=\mathrm{k} \sqrt{H}-$ eqn 1
From definition of unit discharge $Q=Q_{u}$ when $H=1$
$Q_{u}=k x 1 ; k=Q_{u}$
Substituting k in eqn $1 ; \mathrm{Q}=\mathrm{Q}_{\mathrm{u}} \sqrt{H} ; \quad$ Therefore $\mathrm{Q}_{\mathrm{u}}=\frac{Q}{\sqrt{H}}$

## Unit Speed $N_{L}$

Unit Speed is defined as a speed of the turbomachine working under unit head From flow coefficient $\mathrm{gH} \alpha \mathrm{N}^{2} \mathrm{D}^{2}$

For the given turbomachine $\mathrm{H}_{\alpha} \mathrm{N}^{2} ; \mathrm{N} \alpha \sqrt{H} ; \mathrm{N}=\mathrm{k} \sqrt{H}-$ eqn 1
From definition of unit speed $\mathrm{N}=\mathrm{N}_{\mathrm{u}}$ when $\mathrm{H}=1$
$N_{u}=k x 1 ; \quad k=N_{u}$
Substituting k in eqn $1 ; \quad \mathrm{N}=\mathrm{N}_{\mathrm{u}} \sqrt{H} ; \quad \mathrm{N}_{\mathrm{u}}=\frac{N}{\sqrt{H}}$

## $\underline{\text { Unit } \text { Power } P_{U}}$

Unit Power defined as the power of turbomachine working under unit head
$P=\omega Q H$
$\mathrm{P} \alpha \sqrt{H} \mathrm{H}$ as $\mathrm{Q} \alpha \sqrt{H}$ for a given pump
$\mathrm{P} \alpha \mathrm{H}^{3 / 2} ; \quad \mathrm{P}=\mathrm{kH} \mathrm{H}^{3 / 2}-$ eqn 1
From the definition of unit power $P=P_{u}$ when $H=1 m$
$P_{u}=k x 1 ; k=P_{u}$
Substituting k in equation $1 ; \mathrm{P}=\mathrm{P}_{\mathrm{u}} \mathrm{H}^{3 / 2} ; \quad \mathrm{P}_{\mathrm{u}}=\frac{P}{H^{3 / 2}}$

Reynolds Number: is defined as a ratio of inertia force to viscous force
Reynold number $=\frac{\text { Inertia force }}{\text { Viscous force }}=\frac{\rho V D}{\mu}$
In a pipe flow if $\mathrm{R}_{\mathrm{e}}<2000-----$-Laminar flow
If $2000<R_{e}<3000$--------Transition
If $\mathrm{R}_{\mathrm{e}}>3000$-----------turbulent flow
In turbomachine Reynold mumber is not such an important parameter since machine losses are not determined by viscous force alone because various other losses such as losses due to shock at entry, turbulence, impact, friction, leakage and roughness

Most of the turbomachines use relatively low viscous fluid like air steam, water and lighoils. Therefore, the flow in a turbomachine is turbulent in nature

According to Moodys friction factor depends only on relative roughness and not on Reynold number which becomes constant for turbulent flow

For Hydraulic turbine, prototype will have low relative roughness due to its large size, even though model has a smooth surface. Due to this dissimilarties of surface roughness the model similarity loss must ve corrected for Reynolds number dependency. Moody has suffested an equation to determine efficiencies from experiment on a geometrically similar model

The equation I $s \eta_{\mathrm{p}}=1-\left(1-\eta_{\mathrm{m}}\right)\left(\frac{D_{m}}{D_{p}}\right)^{2}$

1. An output of 10 kW was recorded on a turbine, 0.5 m diameter, revolving at a speed of 800 rpm , under a head of 20 m . What is the diameter and output of another turbine which works under a head of 180 m at a speed of 200rpm when their efficiencies are same. Find the specific speed and name the turbine can be used.(1c, 10, June/July 17)

## Solution

$$
\begin{aligned}
& P_{1}=10 \mathrm{~kW} ; \mathrm{D}_{1}=0.5 \mathrm{~m} ; \mathrm{N}_{1}=800 \mathrm{rpm} ; \mathrm{H}_{1}=20 \mathrm{~m} \\
& \mathrm{D}_{1}=? ; P_{2}=? \mathrm{~N}_{2}=200 \mathrm{rpm} ; \mathrm{H}_{2}=180 \mathrm{~m} \\
& \eta_{1}=\eta_{2} ; \mathrm{N}_{\mathrm{s}}=? \\
& \frac{g H_{1}}{N_{1}^{2} D_{1}^{2}}=\frac{g H_{2}}{N_{2}^{2} D_{2}^{2}} ; D_{2}^{2}=\frac{H_{2}}{H_{1}}\left(\frac{N_{1}}{N_{2}}\right)^{2} D_{1}^{2} ; D_{2}^{2}=\frac{180}{20}\left(\frac{800}{200}\right)^{2} 0.5^{2} ; D_{2}^{2}=36 ; D_{2}=6 \mathrm{~m} \\
& \frac{P_{1}}{\rho N_{1}^{3} D_{1}^{5}}=\frac{P_{2}}{\rho N_{1}^{3} D_{1}^{5}} ; P_{2}=P_{1}\left(\frac{N_{2}}{N_{1}}\right)^{3}\left(\frac{D_{2}}{D_{1}}\right)^{5} ; P_{2}=10 *\left(\frac{200}{800}\right)^{3} *\left(\frac{6}{0.5}\right)^{5} ; P_{2}=38880 \mathrm{~kW}
\end{aligned}
$$

$\mathrm{N}_{\mathrm{s}}=\frac{N_{1} \sqrt{P_{1}}}{H_{1}^{\frac{5}{4}}} ; \mathrm{N}_{\mathrm{S}}=\frac{800 \sqrt{10}}{20^{\frac{5}{4}}} ; \mathrm{N}_{\mathrm{S}}=59.81$
2. Tests on a turbine runner 1.25 m in diameter at 30 m head gave the following results, power developed $=736 \mathrm{~kW}$, speed is 180 rpm and discharge $2.70 \mathrm{~m}^{3} / \mathrm{sec}$. Find the diameter speed and discharge of a runner to operate at 45 m head and give 1472 kW at the same efficiency. What is the specific speed of both the turbines? (1c, 08, Dec18/19,1b,08, Dec18?jan19 15ME53,1c, 08 Dec16/17,1c, 10, Dec13/Jan14)
$\mathrm{D}_{1}=1.25 \mathrm{~m} ; \mathrm{H}_{1}=30 \mathrm{~m} ; P_{1}=736 \mathrm{~kW} \mathrm{~N}_{1}=180 \mathrm{rpm} Q_{1}=2.70 \mathrm{~m}^{3} / \mathrm{s}$
$\mathrm{D}_{2}=$ ? ; $N_{2}=? Q_{2}=$ ? $\mathrm{H}_{2}=45 \mathrm{~m} ; P_{2}=1472 \mathrm{~kW}$;
Discharge:
$\eta_{1}=\eta_{2}$
$\frac{P_{1}}{\omega Q_{1} H_{1}}=\frac{P_{2}}{\omega Q_{2} H_{2}}$
$\frac{736}{2.7 * 30}=\frac{1472}{Q_{2} * 45} ; Q_{2}=3.6 \mathrm{~m}^{3} / \mathrm{s} ;$
Speed
$\mathrm{N}_{\mathrm{S}}=\frac{N_{1} \sqrt{P_{1}}}{H_{1}^{\frac{5}{4}}}=\frac{N_{2} \sqrt{P_{2}}}{H_{2}^{\frac{5}{4}}} ; \frac{180 \sqrt{736}}{30^{\frac{5}{4}}}=\frac{N_{2} \sqrt{1472}}{45^{\frac{5}{4}}} ; \quad N_{2}=211.28 \mathrm{rpm}$
Diameter
$\frac{Q_{1}}{N_{1} D_{1}^{3}}=\frac{Q_{2}}{N_{2} D_{2}^{3}} ; \frac{2.7}{180 * 1.25^{3}}=\frac{3.6}{211.28 * D_{2}^{3}} ; D_{2}^{3}=2.219 \quad D_{2}=1.303 m$
Specific Speed
$\mathrm{N}_{\mathrm{s}}=\frac{N_{1} \sqrt{P_{1}}}{H_{1}^{\frac{5}{4}}}=\frac{N_{2} \sqrt{P_{2}}}{H_{2}^{\frac{5}{4}}} ; \quad N_{S}=\frac{180 \sqrt{736}}{30^{\frac{5}{4}}}=69.55$
Type of turbine:
3. A model of turbine 1 m in diameter acting under a head of 2 m runs at 150 rpm .

Estimate the scale ratio of the prototype develops 20 MW under a head of 225 m with specific speed of 100 (1d, 06, June/July14)
$\mathrm{D}_{\mathrm{m}}=1 \mathrm{~m} ; \mathrm{H}_{\mathrm{m}}=2 \mathrm{~m} ; \mathrm{N}_{\mathrm{m}}=150 \mathrm{rpm} ;$ scale ratio $=\frac{D_{m}}{D_{p}}=$ ?
$P_{p}=20 \mathrm{MW}=20000 \mathrm{~kW} ; \mathrm{H}_{\mathrm{p}}=225 \mathrm{~m} ; N_{s}=100$
$\mathrm{N}_{\mathrm{s}}=\frac{N_{m} \sqrt{P_{m}}}{H_{m}^{\frac{5}{4}}} ; 100=\frac{150 * \sqrt{P_{m}}}{2^{\frac{5}{4}}} ; P_{m}=2.514 \mathrm{~kW}$
$\mathrm{N}_{\mathrm{s}}=\frac{N_{P} \sqrt{P_{P}}}{H_{P}^{\frac{5}{4}}} ; 100=\frac{N_{P} \sqrt{20000}}{225^{\frac{5}{4}}} ; N_{P}=616.188 \mathrm{rpm}$
$\frac{P_{m}}{\rho_{m} N_{m}^{3} D_{m}^{5}}=\frac{P_{P}}{\rho_{P} N_{p}^{3} D_{P}^{5}} ;\left(\frac{D_{m}}{D_{P}}\right)^{5}=\frac{2,514}{20000}\left(\frac{150}{616.188}\right)^{3} ;\left(\frac{D_{m}}{D_{P}}\right)^{5}=1.813 * 10^{-6} ; \quad \frac{D_{m}}{D_{P}}=\frac{1}{14.07}$
Scale ratio is 1: 14.07
4. A windmill model of $1: 10$ scale develops 2 kW under a head of 6 m at 500 rpm . A prototype work under a head of 40 m . Assuming that the efficiencies of model and prototype remains same Determine the power developed, speed of the prototype and its specific speed ( $1 \mathrm{c}, 08$, June/July18)
$\frac{D_{m}}{D_{P}}=\frac{1}{10^{\prime}} ; P_{m}=2 \mathrm{~kW} ; \mathrm{H}_{\mathrm{m}}=6 \mathrm{~m} ; \mathrm{N}_{\mathrm{m}}=500 \mathrm{rpm} ;$
$H_{P}=40 m ; \eta_{m}=\eta_{P} ; P_{P}=? ; \mathrm{N}_{\mathrm{p}}=$ ? $; \mathrm{N}_{\mathrm{s}}=$ ? $;$
Speed of the prototype
$\frac{g H_{m}}{N_{m}^{2} D_{m}^{2}}=\frac{g H_{p}}{N_{P}^{2} D_{P}^{2}} ; \quad N_{P}^{2}=N_{m}^{2} * \frac{H_{P}}{H_{m}} *\left(\frac{D_{m}}{D_{P}}\right)^{2} ; N_{P}^{2}=500^{2} * \frac{40}{6} *\left(\frac{1}{10}\right)^{2} N_{P}^{2}=16666.66$
$\mathrm{N}_{\mathrm{p}}=129.1 \mathrm{rpm}$
Power developed by prototype
$\frac{P_{m}}{\rho_{m} N_{m}^{3} D_{m}^{5}}=\frac{P_{P}}{\rho_{P} N_{p}^{3} D_{P}^{5}} ; \quad P_{P}=P_{m} *\left(\frac{N_{P}}{N_{m}}\right)^{3} *\left(\frac{D_{P}}{D_{m}}\right)^{5} ; P_{P}=2 *\left(\frac{129.1}{500}\right)^{3} * 10^{5} ;$
$P_{P}=3442.9 \mathrm{~kW}$
Specific speed
$\mathrm{N}_{\mathrm{s}}=\frac{N_{m} \sqrt{P_{m}}}{H_{m}^{\frac{5}{4}}} ; N_{S}=\frac{500 \sqrt{2}}{6^{\frac{5}{4}}} N_{S}=75.30$
5. A turbine model of $1: 10$ develops 2.0 kW under a head of 6 m at 500 rpm . Find the power developed by the prototype under a head of 40 m . Also find the speed of prototype and its specific speed. Assume the turbine efficiencies to remain same (1c, 06, Dec17/Jan18)
Solution is same as above problem
6. A one fourth scale turbine model is tested under a head of 10 meters. The prototype is required to work under a head of 30 meters and to run at 425 rpm . Estimate the speed of the model if it develops 125 kW and uses $1.1 \mathrm{~m}^{3} / \mathrm{s}$ of water at this speed. Also
calculate the power output of the prototype and suggest the type of turbine ( $1 \mathrm{c}, 08$, Dec14/Jan15)
$\frac{D_{m}}{D_{P}}=\frac{1}{4} ; H_{m}=10 \mathrm{~m} ; H_{P}=30 \mathrm{~m} \mathrm{~N}_{\mathrm{P}}=425 \mathrm{rpm} \quad P_{m}=125 \mathrm{~kW} ; \mathrm{Q}_{\mathrm{m}}=1.1 \mathrm{~m}^{3} / \mathrm{s} ; \mathrm{N}_{\mathrm{m}}=? ;$
$P_{P}=$ ?;
Speed of the model
$\frac{g H_{m}}{N_{m}^{2} D_{m}^{2}}=\frac{g H_{p}}{N_{P}^{2} D_{P}^{2}} ; \quad N_{m}^{2}=N_{P}^{2} * \frac{H_{m}}{H_{P}} *\left(\frac{D_{P}}{D_{m}}\right)^{2} ; N_{m}^{2}=425^{2} * \frac{10}{30} *(4)^{2}$
$\mathrm{N}_{\mathrm{m}}=981.49 \mathrm{rpm}$
Power developed by Prototype
$\frac{P_{m}}{\rho_{m} N_{m}^{3} D_{m}^{5}}=\frac{P_{P}}{\rho_{P} N_{P}^{3} D_{P}^{5}} ; \quad P_{P}=P_{m} *\left(\frac{N_{P}}{N_{m}}\right)^{3} *\left(\frac{D_{P}}{D_{m}}\right)^{5} ; P_{P}=125 *\left(\frac{425}{981.5}\right)^{3} * 4^{5} ;$
$P_{P}=10392.16 \mathrm{~kW}$
Specific speed
$N_{s}=\frac{N_{m} \sqrt{P_{m}}}{H_{m}^{\frac{5}{4}}} ; N_{S}=\frac{981.5 \sqrt{125}}{10^{\frac{5}{4}}} N_{S}=617.08$
Type of turbine suggested:
7. The quantity of water available for a hydroelectric power station is $260 \mathrm{~m}^{3} / \mathrm{sec}$. The head developed is 1.73 m . If the speed of the turbines is 50 rpm and efficiency $82.5 \%$, find the number of turbines. Assume specific speed to be 760.( 1c, 06, Dec25/Jan16, ,)*
$Q=260$ cumecs $=260 \mathrm{~m}^{3} / \mathrm{s} ; \mathrm{H}=1.73 \mathrm{~m} ; \mathrm{N}=50 \mathrm{rpm} ; \eta_{0}=82.5 \%$ number of turbine=?
$\eta_{0}=\frac{P}{\omega Q H} ; 0.85=\frac{P_{T}}{9810 * 260 * 173}$ ie $P_{T}=3640343 \mathrm{~W}=3640.343 \mathrm{~kW}$
$\mathrm{N}_{\text {seach }}=\frac{N \sqrt{P_{\text {each }}}}{H^{5 / 4}} ; 760=\frac{50 \sqrt{P_{\text {each }}}}{1.73^{5 / 4}} \quad \sqrt{P_{\text {each }}}=30.15 ; P_{\text {each }}=909.49 \mathrm{~kW}$
No of turbine required $=\frac{P_{T}}{P_{\text {each }}} ; n=\frac{3640.343}{909.49}=4$
8. A single stage centrifugal pump with impellor diameter of 30 cm rotates at 2000 rpm and with $3 \mathrm{~m}^{3}$ of water per second to a height of 30 m with an efficiency of $75 \%$. Find a) the number of stages and b) diameter of each impeller of a similar multistage pump to lift $5 \mathrm{~m}^{3}$ of water per sec to a height of 200 m , when rotating at 1500 rpm

A single stage centrifugal pump with impellor diameter of 30 cm rotates at 2000 rpm and with $3 \mathrm{~m}^{3}$ of water per second to a height of 30 m with an efficiency of $75 \%$.
$D_{1}=30 \mathrm{~cm} ; \mathrm{N}_{1}=2000 \mathrm{rpm} ; \mathrm{Q}_{1}=3 \mathrm{~m}^{3} / \mathrm{s} ; \mathrm{H}_{1}=30 \mathrm{~m} ;$
In multistage: find the number of stage required if similar single stage pumps (as above) are used to lift $5 \mathrm{~m}^{3} / \mathrm{s}$ to a height o 200 m when rotating at 1500 rpm
$\mathrm{Q}_{2}=5 \mathrm{~m}^{3} / \mathrm{s} ; \mathrm{N}_{2}=2000 \mathrm{rpm} \mathrm{H} \mathrm{H}_{\mathrm{T}}=200 \mathrm{~m}$
$\frac{N_{1} \sqrt{Q_{1}}}{H_{1}{ }^{3 / 4}}=\frac{N_{2} \sqrt{Q_{2}}}{H_{2}{ }^{3 / 4}} ; \quad \frac{2000 \sqrt{3}}{30^{3 / 4}}=\frac{1500 \sqrt{5}}{H_{2}{ }^{3 / 4}} ; \quad \mathrm{H}_{2}=28.73 \mathrm{~m}$

## No of stage required $=$

$H_{T}=n H_{2} ; 200=\mathrm{n} \times 28.73 ; \mathrm{n}=6.96$ ie 7
i) Diameter of the impellor
$\frac{g H_{1}}{N_{1}^{2} D_{1}^{2}}=\frac{g H_{2}}{N_{2}^{2} D_{2}^{2}} ; \frac{30}{2000^{2} \times 300^{2}}=\frac{28.73}{1500^{2} x D_{2}^{2}} ; D_{2}=39 \mathrm{~m}$
9. A quantity of water available for hydel station is 310 cumecs under a head of 1.8 m . Assuming speed of each turbine is 60rpm and efficiency of $85 \%$ find the no of turbines required and power produced by each turbine. Each turbine has a specific speed of 800(metric)

- A quantity of water available for hydel station is 310 cumecs under a head of 1.8 m . ie $\mathrm{Q}=310$ cumecs $=310 \mathrm{~m}^{3} / \mathrm{s} ; \mathrm{H}=1.8 \mathrm{~m}$
- Assuming speed of each turbine is 60 rpm and efficiency of $85 \% \mathrm{~N}=60 \mathrm{rpm} ; \eta_{0}=0.85$
- find the no of turbines required and power produced by each turbine. Each turbine has a specific speed of 800
ie no of turbines=? P each $=$ ?; $\mathrm{N}_{\text {seach }}=800 \mathrm{rpm}$ (metric)
$\eta_{0}=\frac{P}{\omega Q H} ; 0.85=\frac{P_{T}}{9810 \times 310 \times 1.8}$ ie $P_{T}=4652883 \mathrm{~W}=4652.9 \mathrm{~kW}$
$\mathrm{N}_{\text {s each }}=\frac{N \sqrt{P_{\text {each }}}}{H^{5 / 4}} ; 800=\frac{60 \sqrt{P_{\text {each }}}}{1.8^{5 / 4}}$ ie $P_{\text {each }}=772.8$ Metric HP since specific in turbine is metric power is in HP
$P_{\text {each }}=772.5 \times 0.7355 \mathrm{~kW} ; \mathrm{P}_{\text {each }}=\quad=566.25 \mathrm{~kW}$
No of turbine required $=\frac{P_{T}}{P_{\text {each }}} \quad$ No of turbine required $=\frac{4652.9}{566.25}=8.2$
Hence 9 turbine required

9. From the performance curves of the turbine it is seen that a turbine of 1 m diameter acting under a head of 1 m develops a speed of 25 rpm . What diameter should be prototyped if it is developed 1000 kW working under a head of 200 m with a specific speed of 150 (SI units)
10. A model of a centrifugal pump absorbs 5 kW at a speed of 1500 rpm , pumping water against a head of 6 m . The large prototype pump is required to pump water to a head of 30 m . The scale ratio of diameter is 4 . Assume same efficiency and similarities, find
(a) the speed (b) power of prototype and (c) the ratio of discharge of prototype and model (1b, 08, June/July 18, 15ME53)
A model of a centrifugal pump absorbs 5 kW at a speed of 1500 rpm , pumping water against a head of 6 m . ie $\mathrm{P}_{\mathrm{m}}=5 \mathrm{~kW} ; \mathrm{N}_{\mathrm{m}}=1500 \mathrm{rpm} ; \mathrm{H}_{\mathrm{m}}=6 \mathrm{~m}$
The large prototype pump is required to pump water to a head of 30 m ie $\mathrm{H}_{\mathrm{p}}=30 \mathrm{~m}$ The scale ratio of diameter is 4 . le $\frac{D_{P}}{D_{m}}=4$

## Speed of the model

$\frac{g H_{m}}{N_{m}^{2} D_{m}^{2}}=\frac{g H_{p}}{N_{P}^{2} D_{P}^{2}} ; \mathrm{N}^{2}=\frac{H_{P}}{H_{m}} x\left(\frac{D_{m}}{D_{p}}\right)^{2} x N_{m}^{2} ; \quad \mathrm{N}^{2}=\frac{30}{6} x\left(\frac{1}{4}\right)^{2} x 1500^{2} ; \mathrm{N}_{\mathrm{P}}=838.5 \mathrm{rpm}$

## Power of Prototype

$\frac{P_{m}}{\rho_{m} N_{m}^{3} D_{m}^{5}}=\frac{P_{P}}{\rho_{P} N_{p}^{3} D_{P}^{5}} ; \rho_{m}=\rho_{P}$ (same fluid) $; P_{P}=P_{m}\left(\frac{D_{p}}{D_{m}}\right)^{5}\left(\frac{N_{P}}{N_{m}}\right)^{3}$
$P_{P}=5(4)^{5}\left(\frac{838.5}{1500}\right)^{3} ; \mathrm{P}_{\mathrm{P}}=894.34 \mathrm{~kW}$

## Ratio of discharge of prototype and model

$\frac{Q_{m}}{N_{m} D_{m}^{3}}=\frac{Q_{P}}{N_{P} D_{P}^{3}} ; \quad \frac{Q_{P}}{Q_{m}}=\frac{N_{P}}{N_{m}} x\left(\frac{D_{p}}{D_{m}}\right)^{3} ; \quad \frac{Q_{P}}{Q_{m}}=\frac{838.5}{1500} x(4)^{3} ; \quad \frac{Q_{P}}{Q_{m}}=35.76$
11. Two geometrically similar pumps are running at same speed of 1000 rpm . One pump has an impeller diameter of 0.3 m and lifts water at the rate of 20 litres /sec against a head of 15 m Determine the head and impeller diameter of other pump to deliver half the discharge (1b, 08, June/July 13)
$N_{1}=N_{2}=1000 \mathrm{rpm} ; D_{1}=0.3 \mathrm{~m} ; Q_{1}=20 \mathrm{lit} / \mathrm{s}=20 * 10^{-3} \mathrm{~m}^{3} / \mathrm{s} ; H_{1}=15 \mathrm{~m} ; H_{2}=$ ? $D_{2}=$ ? $Q_{2}=\frac{Q_{1}}{2}$
$\frac{Q_{1}}{N_{1} D_{1}^{3}}=\frac{Q_{2}}{N_{2} D_{2}^{3}} ; \quad \frac{Q_{1}}{D_{1}^{3}}=\frac{Q_{2}}{D_{2}^{3}}$ as $N_{1}=N_{2}=1000 \mathrm{rpm}$
$\frac{Q_{1}}{D_{1}^{3}}=\frac{\frac{Q_{1}}{2}}{D_{2}^{3}} ; \quad \frac{1}{D_{1}^{3}}=\frac{1}{2 D_{2}^{3}} ; \frac{1}{0.3^{3}}=\frac{1}{2 D_{2}^{3}} ; D_{2}^{3}=\frac{0.3^{3}}{2} ; D_{2}=0.238 \mathrm{~m}$
$\frac{g H_{1}}{N_{1}^{2} D_{1}^{2}}=\frac{g H_{2}}{N_{2}^{2} D_{2}^{2}} ; \quad H_{2}=H_{1}\left(\frac{D_{1}}{D_{2}}\right)^{2}\left(\frac{N_{2}}{N_{1}}\right)^{2} ; H_{2}=15 *\left(\frac{0.3}{0.238}\right)^{2} *\left(\frac{1000}{1000}\right)^{2} ; H_{2}=9.48 m$
12. A model of Francis turbine of $1: 5$ scale ratio is tested under a head of 1.5 m . It develops 3 kW at 360 rpm . Determine the speed and power developed under a head of 6 m . Find its specific speed

- A model of Francis turbine of 1:5 scale ratio is tested under a head of 1.5 m ie $\frac{D_{m}}{D_{p}}=\frac{1}{5}$ and $\mathrm{H}_{\mathrm{m}}=1.5 \mathrm{~m}$
- It develops 3 kW at 360 rpm ie $\mathrm{P}_{\mathrm{m} 1}=3 \mathrm{~kW}$ and $\mathrm{N}_{\mathrm{m} 1}=360 \mathrm{rpm}$
- Determine the speed and power developed under a head of 6 m . Find its specific speed ie $N_{p}=$ ? $P_{p}=$ ? $H_{p}=6 m$

Solution
$\frac{g H_{m}}{N_{m}^{2} D_{m}^{2}}=\frac{g H_{p}}{N_{P}^{2} D_{P}^{2}} ; \quad \mathrm{N}_{P}{ }^{2}=\frac{H_{p}}{H_{m}} x\left(\frac{D_{m}}{D_{P}}\right)^{2} x N_{m}^{2} ; \quad N_{P}^{2}=\frac{6}{1.5} x\left(\frac{1}{5}\right)^{2} \times 360^{2} ; N_{P}^{2}=20736$
$\mathrm{N}_{\mathrm{p}}=144 \mathrm{rpm}$
$\mathrm{N}_{\mathrm{s}}=\frac{N_{m} \sqrt{P_{m}}}{H_{m}^{5 / 4}} ; \quad \mathrm{N}_{\mathrm{s}}=\frac{360 \sqrt{3}}{1.5^{5 / 4}}=375.62$
$\mathrm{N}_{\mathrm{s}}=\frac{N_{P} \sqrt{P_{P}}}{H_{P}^{5 / 4}} ; \quad 375.62=\frac{144 \sqrt{P_{P}}}{6^{5 / 4}} ; \quad P_{P}=600 \mathrm{~kW}$
13. A Pelton wheel produces 10000 kW while working under a head of 400 m and running at a speed of 300 rpm . Assuming an overall efficiency of $82 \%$, find the unit quantities, During the off season, the head over the turbine reduces to 350 m . Find the corresponding speed, discharge and power for the same efficiency
$P=10000 \times 10^{3} \mathrm{~W} ; \mathrm{H}=400 \mathrm{~m} ; \mathrm{N}=300 \mathrm{rpm} ; \eta_{\mathrm{o}}=0.82$
$\eta_{0}=\frac{P}{\omega Q H} ; \quad 0.82=\frac{10000 \times 10^{3}}{9810 \times Q \times 400} ; \quad \mathrm{Q}=3.1078 \mathrm{~m}^{3} / \mathrm{s}$

## Unit Discharge

$$
\mathrm{Q}_{\mathrm{u}}=\frac{Q}{\sqrt{H}} ; \quad \mathrm{Q}_{\mathrm{u}}=\frac{3.1078}{\sqrt{400}} ; \quad \mathrm{Q}_{\mathrm{u}}=0.1553 \mathrm{~m}^{3} / \mathrm{s}
$$

Unit speed:
$\mathrm{N}_{\mathrm{u}}=\frac{N}{\sqrt{H}} ; \quad \mathrm{N}_{\mathrm{u}}=\frac{300}{\sqrt{400}} ; \quad \mathrm{N}_{\mathrm{u}}=15 \mathrm{rpm}$

## Unit Power

$\mathrm{P}_{\mathrm{u}}=\frac{P}{H^{3 / 2}} ; \quad \mathrm{P}_{\mathrm{u}}=\frac{10000 \times 10^{3}}{400^{3 / 2}} ; \quad \mathrm{P}_{\mathrm{u}}=1250 \mathrm{~W}$
If head reduces to 350 m
$\frac{Q_{1}}{\sqrt{H_{1}}}=\frac{Q_{2}}{\sqrt{H_{2}}} ; \quad \frac{3.1078}{\sqrt{400}}=\frac{Q_{2}}{\sqrt{350}} ; \quad Q_{2}=2.907 \mathrm{~m}^{3} / \mathrm{s}$
$\frac{N_{1}}{\sqrt{H_{1}}}=\frac{N_{2}}{\sqrt{H_{2}}} ; \quad \frac{300}{\sqrt{400}}=\frac{N_{2}}{\sqrt{350}} ; \quad N_{2}=280.624 \mathrm{rpm}$
$\frac{P_{1}}{H_{1}^{3 / 2}}=\frac{P_{2}}{H_{2}^{3 / 2}} ; \quad \frac{10000 \times 10^{3}}{400^{3 / 2}}=\frac{P_{2}}{350^{3 / 2}} ; \quad \mathrm{P}_{2}=8184571.29 \mathrm{~W}$
14. The following data were obtained from the main characteristics of a Kaplan turbine of runner diameter $1 \mathrm{~m} \mathrm{P}_{\mathrm{u}}=30.695, \mathrm{Q}_{u}=108.6, \mathrm{~N}_{\mathrm{u}}=63.6$. Estimate a) the runner diameter b) the discharge c) the speed of a similar runner working under a head of 30 m and developing 2000kW. Also, d) determine the specific speed of the runner (1c, June/July16)
$D_{1}=1 m ; P_{u}=30.695 ; Q_{u}=108.6 ; N_{u}=63.6 ;$
$D_{2}=? ; Q_{2}=? ; N_{2}=? ; H_{2}=30 \mathrm{~m} ; P_{2}=2000 \mathrm{~kW} ; N_{s}=$ ?
$N_{s}=\frac{N \sqrt{P}}{H^{5 / 4}} ; N_{S}=\frac{N \sqrt{P}}{\sqrt{H} H^{3 / 4}} ; N_{S}=\frac{N}{\sqrt{H}} *\left(\frac{P}{H^{\frac{3}{2}}}\right)^{\frac{1}{2}} ; N_{S}=N_{u} \sqrt{P_{u}}$;
$N_{s}=63.6 \sqrt{30.695} ; N_{s}=352.36$
$N_{S}=\frac{N_{2} \sqrt{P_{2}}}{H_{2}^{5 / 4}} ; \quad 352.36=\frac{N_{2} \sqrt{2000}}{30^{5 / 4}} ; \quad N_{2}=553.18 \mathrm{rpm}$
$\frac{g H_{1}}{N_{1}^{2} D_{1}^{2}}=\frac{g H_{2}}{N_{2}^{2} D_{2}^{2}} ; \quad\left(\frac{\sqrt{H_{1}}}{N_{1}}\right)^{2} * \frac{1}{D_{1}^{2}}=\frac{H_{2}}{N_{2}^{2} D_{2}^{2}} ;\left(\frac{1}{N_{u 1}}\right)^{2} * \frac{1}{D_{1}^{2}}=\frac{H_{2}}{N_{2}^{2} D_{2}^{2}} ;$
$\frac{1}{63.6^{2}} * \frac{1}{1^{2}}=\frac{30}{553.18^{2} * D_{2}^{2}} ; D_{2}^{2}=0.3965 ; D_{2}=0.629 m$
$\frac{Q_{1}}{N_{1} D_{1}^{3}}=\frac{Q_{2}}{N_{2} D_{2}^{3}} ; \quad \frac{Q_{1}}{N_{1} D_{1} D_{1}^{2}}=\frac{Q_{2}}{N_{2} D_{2} D_{2}^{2}} ; \quad \frac{Q_{1}}{U_{1} D_{1}^{2}}=\frac{Q_{2}}{U_{2} D_{2}^{2}} ; \quad \frac{Q_{1}}{V_{1} D_{1}^{2}}=\frac{Q_{2}}{V_{2} D_{2}^{2}} ; \frac{Q_{1}}{\sqrt{H_{1} D_{1}^{2}}}=\frac{Q_{2}}{\sqrt{H_{2} D_{2}^{2}}}$
$\frac{Q_{u 1}}{D_{1}^{2}}=\frac{Q_{2}}{\sqrt{H_{2} D_{2}^{2}}} ; \frac{108.6}{1^{2}}=\frac{Q_{2}}{\sqrt{30} * 0.629^{2}} ; Q_{2}=235.33 \mathrm{~m}^{3} / \mathrm{s}$
15. A model of Kaplan turbine having scale ratio $1: 12$ tested under a head of 3 m . The prototype of Kaplan turbine is designed to produce a power of 8000 kW under a head of 8 m running at a speed of 150 rpm with a overall efficiency of $85 \%$. Find the speed, flow, power and specific speed of the model

- A model of Kaplan turbine having scale ratio 1:12 tested under a head of 3 m
le $\frac{D_{m}}{D_{p}}=\frac{1}{12}$ and $\quad H_{m}=3 m$
- The prototype of Kaplan turbine is designed to produce a power of 8000 kW under a head of 8 m running at a speed of 150 rpm with a overall efficiency of $85 \%$.
le $P_{P}=8000 \mathrm{~kW}, H_{P}=8 m N_{P}=150 \mathrm{rpm} \eta_{\mathrm{o}}=85 \%$
- Find the speed, flow, power and specific speed of the model
le $N_{m}=$ ? $Q_{m}=$ ? $Q_{P}=$ ? $N_{s}=$ ?
$\frac{g H_{m}}{N_{m}^{2} D_{m}^{2}}=\frac{g H_{p}}{N_{P}^{2} D_{P}^{2}} ; \mathrm{N}_{\mathrm{m}}{ }^{2}=\frac{H_{m}}{H_{P}} x\left(\frac{D_{P}}{D_{m}}\right)^{2} x N_{P}^{2} ; \quad \mathrm{N}_{\mathrm{m}}{ }^{2}=\frac{3}{8} x(12)^{2} x 150^{2} \quad \mathrm{~N}_{\mathrm{m}}{ }^{2}=12144999.15$ ie $\mathrm{N}_{\mathrm{m}}=1102.27 \mathrm{rpm}$
$\eta_{\mathrm{P}}=\frac{P_{P}}{\omega Q_{P} H_{p}} ; \quad 0.85=\frac{8000 \times 10^{3}}{9810 Q_{P} 8} ; \quad Q_{P}=119.92 \mathrm{~m}^{3} / \mathrm{s}$
$\frac{Q_{p}}{N_{p} D_{P}^{3}}=\frac{Q_{m}}{N_{m} D_{m}^{3}} ; \quad Q_{m}=\frac{N_{m}}{N_{P}} x\left(\frac{D_{m}}{D_{P}}\right)^{3} \times Q_{p} ; Q_{m}=\frac{1102.27}{150} x\left(\frac{1}{12}\right)^{3} \times 119.92$
$Q_{m}=0.509 \mathrm{~m}^{3} / \mathrm{s}$
$\frac{P_{P}}{P_{m}}=\frac{\eta_{P} \omega Q_{P} H_{P}}{\eta_{m} \omega Q_{m} H_{m}} ; \frac{8000}{P_{m}}=\frac{119.92 x 8}{0.509 \times 3} ; P_{m}=12.73 \mathrm{~kW}$

16. A model of a turbine built to a scale of $1: 4$ is tested under a head of 10 m . The prototype has to work under a head of 50 m at 450 rpm (a) what speed should the model run be if it develops 60 kW using 0.9 cumecs at this speed. (b) what power will be obtained from the prototype assuming that its efficiency is $3 \%$ better than that of model

- $\quad$ scale $=\frac{1}{4}=\frac{D_{m}}{D_{P}}$
- Model: $H_{m}=10 \mathrm{~m} ; N_{m}=? P_{m}=60 \mathrm{~kW} ; Q_{m}=0.9 \mathrm{~m}^{3} / \mathrm{s}$
- Prototype $H_{P}=50 \mathrm{~m} ; N_{P}=450 \mathrm{rpm} P_{P}=$ ?
- what power will be obtained from the prototype assuming that its efficiency is $3 \%$ better than that of model $P_{P}=$ ? if $\eta_{P}=1.03 \eta_{M}$
$\frac{g H_{m}}{N_{m}^{2} D_{m}^{2}}=\frac{g H_{p}}{N_{P}^{2} D_{P}^{2}}$


## Speed of the model

$\mathrm{N}_{\mathrm{m}}{ }^{2}=\frac{H_{m}}{H_{P}} x\left(\frac{D_{P}}{D_{m}}\right)^{2} x N_{P}^{2} ; \quad \mathrm{N}_{\mathrm{m}}{ }^{2}=\frac{10}{50} x(4)^{2} x 450^{2} ; \quad \mathrm{N}_{\mathrm{m}}=805 \mathrm{rpm}$

## Power of Prototype

$\eta=\frac{\omega Q H}{P} ; \quad P=\eta \omega Q H$
Hence $\frac{\eta_{P} Q_{P} H_{P}}{\eta_{m} Q_{m} H_{m}}=\frac{P_{P}}{P_{m}}$
But $\frac{Q_{p}}{N_{p} D_{P}^{3}}=\frac{Q_{m}}{N_{m} D_{m}^{3}} ; \quad \frac{Q_{p}}{Q_{m}}=\left(\frac{D_{P}}{D_{m}}\right)^{3} x \frac{N_{p}}{N_{m}}$
Hence,

$$
\begin{aligned}
& \frac{\eta_{P}}{\eta_{m}} x\left(\frac{D_{P}}{D_{m}}\right)^{3} x \frac{N_{p}}{N_{m}} \times \frac{H_{P}}{H_{m}}=\frac{P_{P}}{P_{m}} \\
& 1.03 x(4)^{3} \times \frac{450}{805} \times \frac{50}{10}=\frac{P_{P}}{60}
\end{aligned}
$$

$P_{P}=11055 \mathrm{~kW}$
17. A Francis turbine model of $1: 5$ scaleThe data for model is $\mathrm{P}=4 \mathrm{~kW}, \mathrm{~N}=3500 \mathrm{rpm}, \mathrm{H}=2 \mathrm{~m}$ and for prototype , $\mathrm{H}=6 \mathrm{~m}$ Assume that the overall efficiency is $70 \%$, Calculate i) speed of the prototype ii) Power of prototype Use Moodys equation (1c, 10, Dec 12)
$\frac{D_{m}}{D_{P}}=\frac{1}{5} ; P_{m}=4 \mathrm{~kW} ; N_{m}=3500 \mathrm{rpm} ; H_{m}=2 \mathrm{~m} ; H_{P}=6 \mathrm{~m} ; \eta_{m}=0.7 ; N_{P}=? P_{P}=$ ?
$\frac{g H_{m}}{N_{m}^{2} D_{m}^{2}}=\frac{g H_{p}}{N_{P}^{2} D_{P}^{2}} ; N_{P}^{2}=N_{m}^{2} * \frac{H_{m}}{H_{p}} *\left(\frac{D_{m}}{D_{P}}\right)^{2} ; N_{P}^{2}=3500^{2} * \frac{2}{6} *\left(\frac{1}{5}\right)^{2} ; N_{P}^{2}=163170 ;$
$N_{P}=403.94 \mathrm{rpm}$
$\eta_{p}=1-\left(1-\eta_{m}\right)\left(\frac{D_{m}}{D_{p}}\right)^{0.2} ; \quad \eta_{p}=1-(1-0.7)\left(\frac{1}{5}\right)^{0.2}=0.782$
$\eta_{m}=\frac{P_{m}}{\omega Q_{m} H_{m}}-$ eqn $1 ; \eta_{P}=\frac{P_{P}}{\omega Q_{P} H_{P}}-$ eqn 2
eqn 2/eqn 1; $\frac{\eta_{P}}{\eta_{m}}=\frac{P_{P}}{P_{m}} * \frac{Q_{m}}{Q_{P}} * \frac{H_{m}}{H_{P}} ; \quad \frac{\eta_{P}}{\eta_{m}}=\frac{P_{P}}{P_{m}} * \frac{D_{m}^{2} \sqrt{H_{m}}}{D_{P}^{2} \sqrt{H_{P}}} * \frac{H_{m}}{H_{P}} ; \quad \frac{\eta_{P}}{\eta_{m}}=\frac{P_{P}}{P_{m}} *\left(\frac{D_{m}}{D_{P}}\right)^{2} *$ $\left(\frac{H_{m}}{H_{P}}\right)^{3 / 2}$
$\frac{0.782}{0.7}=\frac{P_{P}}{4} *\left(\frac{1}{5}\right)^{2} *\left(\frac{2}{6}\right)^{3 / 2} ; \quad P_{P}=4 *(5)^{2} *\left(\frac{6}{2}\right)^{3 / 2} * \frac{0.782}{0.7} ; P_{P}=580.48 \mathrm{~kW}$
18. A small scale model of hydraulic turbine runs at a speed of 350 rpm , under a head of 20 m and produces 8 kW as output Find : a) Unit Discharge b) Unit speed and c) Unit Power assuming total to total efficiency of a turbine as 0.79 find the output power of the actual turbine which is 12 times the model size, assuming the model and prototype efficiencies are related by Moodys formula

Model: $H_{m}=20 \mathrm{~m} ; N_{m}=350 \mathrm{rpm} ; P_{m}=8 \mathrm{~kW} ; \eta_{\mathrm{tt}}=0.79 ; \frac{D_{p}}{D_{M}}=12$
$\eta_{t t}=\frac{P_{m}}{\omega Q_{m} H_{m}} ; \quad 0.79=\frac{8 \times 10^{3}}{9810 \times Q_{m} \times 20} ; Q_{m}=0.0516 \mathrm{~m}^{3} / \mathrm{s}$

## Unit Discharge

$Q_{u}=\frac{Q}{\sqrt{H}} \quad=\frac{0.056}{\sqrt{20}} ; \quad Q_{u}=0.0115 \mathrm{~m}^{3} / \mathrm{s}$

## Unit speed:

$N_{u}=\frac{N}{\sqrt{H^{\prime}}} ; N_{u}=\frac{350}{\sqrt{20}}=78.262 \mathrm{rpm}$

## Unit Power

$P_{u}=\frac{P}{H^{3 / 2}} ; \quad P_{u}=\frac{8 \times 10^{3}}{20^{3 / 2}}=89.442 \mathrm{~W}$
$\eta_{p}=1-\left(1-\eta_{m}\right)\left(\frac{D_{m}}{D_{p}}\right)^{0.2} ; \quad \eta_{p}=1-(1-0.79)\left(\frac{1}{12}\right)^{0.2}=0.8722$
For model; $\quad \eta_{m}=\frac{P_{m}}{\omega Q_{m} H_{m}}$
For Prototype; $\quad \eta_{P}=\frac{P_{P}}{\omega Q_{P} H_{p}}$
$\frac{\eta_{P}}{\eta_{m}}=\frac{P_{P}}{P_{m}} \frac{\omega Q_{m} H_{m}}{\omega Q_{P} H_{P}}-e q n 1$
Discharge $Q=A V$
$Q \alpha D^{2} \sqrt{H}$ as $A \alpha D^{2}$ and $V \alpha \sqrt{H}$
Hence $\frac{Q_{m}}{Q_{P}}=\frac{D_{m}^{2} \sqrt{H_{m}}}{D_{p}^{2} \sqrt{H_{p}}}$
Substituting $\frac{Q_{m}}{Q_{P}}$ in eqn 1
$\frac{\eta_{P}}{\eta_{m}}=\frac{P_{P}}{P_{m}} \frac{D_{m}^{2} \sqrt{H_{m}}}{D_{p}^{2} \sqrt{H_{p}}} \frac{H_{m}}{H_{P}} ; \quad \quad \frac{\eta_{P}}{\eta_{m}}=\frac{P_{P}}{P_{m}} *\left(\frac{D_{m}}{D_{p}}\right)^{2} *\left(\frac{H_{m}}{H_{P}}\right)^{3 / 2} ;$
Assuming $D \propto H ; \frac{D_{m}}{D_{p}}=\frac{H_{m}}{H_{P}} ; \frac{1}{12}=\frac{H_{m}}{H_{P}}$

$$
\frac{0.8722}{0.79}=\frac{P_{P}}{8} *\left(\frac{1}{12}\right)^{2} *\left(\frac{1}{12}\right)^{3 / 2} ; P_{P}=8 * \frac{0.8722}{0.79} *(12)^{2} *(12)^{3 / 2} ; P_{P}=52870.49 \mathrm{~kW}
$$

19. A centrifugal pump is required to handle water at a capacity $6.75 \mathrm{~m}^{3} / \mathrm{s}$, head of 125 m and a speed of 350 rpm . In designing a model of this pump the laboratory conditions impose a maximum capacity of $0.127 \mathrm{~m}^{3} / \mathrm{s}$ and a power consumption of 220 kW model and prototype efficiencies are assumed same, find the speed of model and scale ratio
20. An axial flow pump with a rotor diameter 30 cm handles water at the rate of $2.7 \mathrm{~m}^{3} / \mathrm{min}$, while operating at 1500 rpm . The corresponding energy input is $125 \mathrm{~J} / \mathrm{kg}$. The total to total efficiency is $75 \%$. If a second geometrically similar pump with a diameter of 20 cm operates at 3000 rpm , what is its flow rate? What is the change in total pressure

The total to total efficiency being $75 \%$.
le $D_{1}=30 \mathrm{~cm} ; N_{1}=1500 \mathrm{rpm} ; Q_{1}=2.7 \mathrm{~m}^{3} / \mathrm{s}$;
energy input is $125 \mathrm{~J} / \mathrm{kg}$ ie $\mathrm{gH}_{1}=125 \mathrm{~J} / \mathrm{kg}$; The total to total efficiency is $75 \%$.
If a second geometrically similar pump with a diameter of 20 cm operates at 3000 rpm ,
ie $D_{2}=20 \mathrm{~cm} ; \mathrm{N}_{1}=3000 \mathrm{rpm}$
what are a) its flow rate b) power input c) change in total pressure
$Q_{2}=$ ? ; $P_{2}=$ ? change in total pressure $=$ ?
$\frac{Q_{1}}{N_{1} D_{1}^{3}}=\frac{Q_{2}}{N_{2} D_{2}^{3}} ; \quad \frac{2.7}{1500 \times 30^{3}}=\frac{Q_{2}}{3000 \times 20^{3}} ; \quad Q_{2}=1.6 \mathrm{~m}^{3} / \mathrm{min}$
$\frac{g H_{1}}{N_{1}^{2} D_{1}^{2}}=\frac{g H_{2}}{N_{2}^{2} D_{2}^{2}} ; \quad \frac{125}{1500^{2} \times 0.30^{2}}=\frac{g H_{2}}{3000^{2} \times 0.20^{2}} ; \quad g H_{2}=222.22 \mathrm{~J} / \mathrm{kg}=\left(\frac{E}{m}\right)_{2}=\Delta h_{o 2}$
$\mathrm{P}=m * \frac{E}{m}$
$m_{2}=\rho Q_{2}$
Power input $=\mathrm{Q}_{2} g H_{2}$
$=1000 \times 1.6 \times 222.22=58.32 \times 10^{3} \mathrm{~W}$
Change in pressure
$\eta_{t t}=\frac{\Delta h_{o s}}{\Delta h_{o}} ; 0.75=\frac{\Delta h_{o s}}{222.22}$
$\Delta h_{o s}=0.75 * 222.22 ; \quad \Delta h_{o s}=166.65 \mathrm{~J} / \mathrm{kg}$
$\Delta h_{o s}=\frac{\Delta p_{o}}{\rho} ; \quad 166.65=\frac{\Delta p_{o}}{1000} ; \quad \Delta p_{o}=166.65 * 1000 \mathrm{~N} / \mathrm{m}^{2} ; \Delta p_{o}=1.66 \mathrm{bar}$

## Module 1 : Thermodynamics of fluid flow in Turbomachines

## Important point:

Enthalpy $h=C_{p} T$ where $C_{p}$ is the specific heat in $\mathrm{kJ} / \mathrm{kgK}, \mathrm{T}$ is in temperature in K and h is in $\mathrm{kJ} / \mathrm{kg}$

If $C_{p}$ is in $\mathrm{J} / \mathrm{kgK}$ then h is in $\mathrm{J} / \mathrm{kg}$
$\frac{T_{2}}{T_{1}}=\left(\frac{P_{2}}{P_{1}}\right)^{\frac{\gamma-1}{\gamma}}$ if the process is isentropic
$\frac{T_{2}}{T_{1}}=\left(\frac{P_{2}}{P_{1}}\right)^{\frac{n-1}{n}}$ if the process is Polytropic
$\frac{T_{01}}{T_{1}}=\left(\frac{P_{01}}{P_{1}}\right)^{\frac{\gamma-1}{\gamma}}$ since static to stagnation is always isentropic
Efficiency of compressor or power absorbing machine
$\eta=\frac{\text { isentropic enthalpy increase }}{\text { Actual enthlpy drop }}$
$\eta=\frac{h_{02 s}-h_{01}}{h_{02}-h_{01}} ; \eta=\frac{T_{02 s}-T_{01}}{T_{02}-T_{01}}$

Efficiency of Turbine or power generating machine
$\eta=\frac{\text { Actual enthalpy drop }}{\text { isentropic enthlpy drop }}$
$\eta=\frac{h_{01}-h_{02}}{h_{01}-h_{02 s}} ; \eta=\frac{T_{01}-T_{02}}{T_{01}-T_{02 s}}$

## Static and stagnation states:

Static state: various properties such as pressure, temperature and volume may be determined at any given fluid particle

Static properties are those properties which are measured with instruments or devices which are at rest relative to the fluid. For example static temperature of any fluid particle moving with a given speed, the measuring thermometer or thermocouple should theoretically move with the same speed as the fluid particle itself while the measurements is being made

Example : measurements made by instrument fitted at the wall of the conduit in which fluid is flowing is static properties ( because fluid particles at the wall has zero velocity, measuring instrument fitted has zero velocity hence relative velocity between the fluid and measuring instrument is zero)

Stagnation state is defined as the terminal state of fictitious, isentropic and work free thermodynamic process, during which the macroscopic kinetic and potential energies of the fluid particle are reduced to zero in steady flow. Measurement made by the instrument in which sensing element is fixed at the centre of conduit represents stagnation property of fluid ( because Instrument has zero velocity and fluid at the centre of conduit is having stream velocity of the fluid)

Stagnation state , as defined above, does not represent the existing state of a fluid at any point;
From Ist law of thermodynamics applied to static to stagnation
$\dot{Q}+\dot{m}\left(h+\frac{V^{2}}{2}+Z g\right)=\dot{W}+\dot{m}\left(h_{0}+\frac{V_{0}^{2}}{2}+Z_{0} g\right)$
Note that $h, V, Z$ are static enthalpy, velocity, elevation at given point and $h_{0}$ is the stagnation enthalpy at same point, $\dot{Q}$ is the rate of heat transfer and $\dot{W}$ is the rate of work done

Also note that without suffix is the static properties at the given point and properties with suffix 0 represents stagnation properties

As stagnation point is the terminal state of fictitious, isentropic and work free; $\dot{Q}=0$;

$$
\begin{aligned}
& \dot{W}=0 ; V_{0}=0 ; \mathrm{Z}_{0}=0 \\
& \dot{m}\left(h+\frac{V^{2}}{2}+Z g\right)=\dot{m}\left(h_{0}\right) ; \quad h_{0}=h+\frac{V^{2}}{2}+Z g ; \\
& C_{p} T_{0}=C_{p} T+\frac{V^{2}}{2}+Z g ; \quad T_{0}=T+\frac{V^{2}}{2 c_{p}}+\frac{Z g}{C_{p}}
\end{aligned}
$$

If PE is neglected, stagntion enthalpy $h_{0}=h+\frac{V^{2}}{2}$;
$C_{p} T_{0}=C_{p} T+\frac{V^{2}}{2} ;$ Hence stagnation temperature, $T_{0}=T+\frac{V^{2}}{2 C_{p}}$

Stagnation pressure
Bernoulli's equation between static and stagnation prperties
$\frac{p}{\omega}+\frac{V^{2}}{2 g}+Z=\frac{p_{0}}{\omega}+\frac{V_{0}^{2}}{2 g}+Z_{0} ; \quad \frac{p_{0}}{\omega}=\frac{p}{\omega}+\frac{V^{2}}{2 g}+Z$ since at stagnation point velocity and potential energy become zero
$\frac{p_{0}}{\rho g}=\frac{p}{\rho g}+\frac{V^{2}}{2 g}+Z ; p_{0}=p+\frac{\rho V^{2}}{2}+Z \rho g$
If potential energy is neglected, ; $p_{0}=p+\frac{\rho V^{2}}{2}$
Note that
Static to stagnation property (relation between Temperature and pressure)
$\frac{T_{0}}{T}=\left(\frac{p_{0}}{p}\right)^{\frac{\gamma-1}{\gamma}}$ since static to stagnation process is isentropic Hence $\gamma$ is used

## Efficiency of turbomachine:

In turbomachines, losses occur in turbomachine is due to a) bearing friction, windage etc which is referred as Mechanical losses and b) Unsteady flow, friction between the blade and fluid losses referred to hydraulic losses

In Power generating machine;

## Referred to Mechanical losses

$\eta_{\text {mech }}=\frac{\text { Power developed at the shaft of runner }}{\text { Power developed at the runner }}$

## Referred to Hydraulic losses

$\eta_{\text {blade }}=\frac{\text { Power developed at the runner }}{\text { Fluid Power available at the inlet of turbine }}$
Overall efficiency:
$\eta_{0}=\frac{\text { Power developed at the shaft of runner }}{\text { Fluid Power available at the inlet of turbine }}=\eta_{\text {mech }} \eta_{\text {blade }}$
In Power absorbing machine;
Referred to Mechanical losses
$\eta_{\text {mech }}=\frac{\text { Power availabe at the impeller }}{\text { Input Power to the shaft }}$
Referred to Hydraulic losses
$\eta_{\text {manometric }}=\frac{\text { Fluid Power develped at outlet of the turbomachine }}{\text { Fluid Power available at the impeller }}$
Overall efficiency :
$\eta_{0}=\frac{\text { Fluid Power develped at outlet of the turbomachine }}{\text { Input Power to the shaft }}=\eta_{\text {mech }} \eta_{\text {manometric }}$

## Various efficiencies based on static and stagnation properties

## Power absorbing machine:


i) $\quad \mathrm{W}_{\mathrm{t}-\mathrm{t}}=\mathrm{h}_{02 \mathrm{~s}}-\mathrm{h}_{01} ; \quad \eta_{t-t}=\frac{h_{02 s}-h_{01}}{h_{02}-h_{01}}$
ii) $\quad \mathrm{W}_{\mathrm{t}-\mathrm{s}}=\mathrm{h}_{2 \mathrm{~s}}-\mathrm{h}_{01} ; \quad \eta_{t-s}=\frac{h_{2 s}-h_{01}}{h_{02}-h_{01}}$
iii) $\quad \mathrm{W}_{s-\mathrm{t}}=\mathrm{h}_{02 \mathrm{~s}}-\mathrm{h}_{1} ; \quad \eta_{s-t}=\frac{h_{02 s}-h_{1}}{h_{02}-h_{01}}$
iv) $\quad \mathrm{W}_{s-\mathrm{s}}=\mathrm{h}_{2 \mathrm{~s}}-\mathrm{h}_{1} ; \quad \eta_{s-s}=\frac{h_{2 s}-h_{1}}{h_{02}-h_{01}}$

## Power generating machine


i) $\quad \mathrm{W}_{\mathrm{t}-\mathrm{t}}=\mathrm{h}_{01}-\mathrm{h}_{02 \mathrm{~s}} ; \quad \eta_{t-t}=\frac{h_{01}-h_{02}}{h_{01}-h_{02 s}}$
ii) $\quad \mathrm{W}_{\mathrm{t}-\mathrm{s}}=\mathrm{h}_{01}-\mathrm{h}_{2 \mathrm{~s}} ; \quad \eta_{t-s}=\frac{h_{01}-h_{02}}{h_{01}-h_{2 s}}$
iii) $\quad W_{s-t}=h_{1}-h_{02 s} ; \quad \eta_{s-t}=\frac{h_{01}-h_{02}}{h_{1}-h_{02 s}}$
iv) $\quad \mathrm{W}_{\mathrm{s}-\mathrm{s}}=\mathrm{h}_{2 \mathrm{~s}}-\mathrm{h}_{1} ; \quad \eta_{s-s}=\frac{h_{01}-h_{02}}{h_{1}-h_{21}}$

## Application of First Law and Second Law of thermodynamics to Turbomachines

The fluid flow in any turbomachine is slightly varies with time (Steady flow) but unsteady flow near blade tips at entry and exit of cascades. But overall fluid flow is steady

Hence applying First law of thermodynamics for steady flow
$\dot{Q}+\dot{m}\left(h_{1}+\frac{V_{1}^{2}}{2}+Z_{1} g\right)=P+\dot{m}\left(h_{2}+\frac{V_{2}^{2}}{2}+Z_{2} g\right)$
But stagnation enthalpy: $\mathrm{h}_{0}=h+\frac{V^{2}}{2}+Z g$
Hence $\quad \dot{Q}+\dot{m} h_{01}=P+\dot{m} h_{02}$
$\dot{Q}-P=\dot{m}\left(h_{02}-h_{01}\right)$
$\frac{\dot{Q}}{\dot{m}}-\frac{\dot{P}}{\dot{m}}=h_{02}-h_{01}$
$q-w=\Delta h_{0}$
$\mathrm{q}=0$ as turbomachine is ideally assumed as adiabatic
Hence, $-w=\Delta h_{0}$
Hence energy transfer as work per unit mass flow is therefore numerically equal to change in stagnation enthalpy of the fluid between the turbomachine inlet and outlet

In power generating turbomachine, w is positive so that $\Delta h_{0}=h_{02}-h_{01}$ is negative In power absorbing turbomachine, w is negative so that $\Delta h_{0}=h_{02}-h_{01}$ is positive For incompressible fluid, internal energy changes are negligible, and density is constant
$H=u+p v$
$\Delta h=\left(u_{2}-u_{1}\right)+\left(p_{2} v_{2}-p_{1} v_{1}\right)$
$u_{2}-u_{1}=0$ as For incompressible fluid, internal energy changes are negligible
$\Delta h=\Delta p v ; \quad v=\frac{1}{\rho} ; \Delta h=\Delta \frac{p}{\rho}$
$\Delta h_{0}=\Delta h+\Delta K E+\Delta P$

## Application of II law of thermodynamics to turbomachine

From 2 law of thermaodynamics
$T_{0} d s_{0}=d h_{0}-v_{0} d p_{0}-A$
From Ist law of thermodynamics, $d h_{0}=-\delta w$
$T_{0} d s_{0}=-\delta w-v_{0} d p_{0}-1$
In ideal turbo machine , $T_{0} d s_{0}=0$; work done is $\delta w_{i}$
Hence equation A becomes $0=-\delta w_{i}-v_{0} d p_{0} ; \quad \delta w_{i}=-v_{0} d p_{0}$
Hence, substituting $\delta w_{i}=-v_{0} d p_{0}$, eq 1 becomes
$T_{0} d s_{0}=-\delta w+\delta w_{i} ; \quad \delta w_{i}-\delta w=T_{0} d s_{0}$

## Efficiencies of the compression process

## i) Total to total efficiency

It is defined as the ratio of ideal work to the actual work between the stagnation states.
$\eta_{\mathrm{tt}}=\frac{\text { Ideal work between the stagnation states }}{\text { Actual work }}$
$\eta_{\mathrm{tt}}=\frac{h_{o 2}^{\prime}-h_{01}}{h_{02}-h_{01}}=\frac{C_{p}\left(T_{o 2}^{\prime}-T_{01}\right)}{C_{p}\left(T_{02}-T_{01}\right)} ; \quad \eta_{\mathrm{tt}}=\frac{T_{o 2}^{\prime}-T_{01}}{T_{02}-T_{01}} ; \quad \eta_{\mathrm{tt}}=\frac{T_{01}\left(\frac{T_{o 2}^{\prime}}{T_{01}}-1\right)}{T_{02}-T_{01}}----------1$
But $\frac{T_{o 2}^{\prime}}{T_{01}}=\left(\frac{p_{02}}{p_{01}}\right)^{\frac{\gamma-1}{\gamma}} ; \frac{T_{o 2}^{\prime}}{T_{01}}=\left(p_{r o}\right)^{\gamma-1} ; \quad \eta_{\mathrm{tt}} \frac{T_{01}\left(p_{r o}^{\gamma-1}-1\right)}{T_{02}-T_{01}}$

## Actual Power required

Actual Power required, $\quad \mathrm{P}=\mathrm{m} C_{p}\left(T_{02}-T_{01}\right) ; \quad P=m C_{p}\left(\frac{T_{o 2}^{\prime}-T_{01}}{\eta_{\mathrm{tt}}}\right) ; \quad P=\frac{m C_{p}}{\eta_{\mathrm{tt}}} T_{01}\left(\frac{T_{o 2}^{\prime}}{T_{01}}-1\right)$
$P=\frac{m C_{p}}{\eta_{\mathrm{tt}}} T_{01}\left(p_{r o}^{\gamma-1}-1\right)$
If Mechanical Efficiency is given, $P=\frac{m c_{p}}{\eta_{\text {tt }} \eta_{\text {mech }}} T_{01}\left(p_{r o}^{\gamma-1}-1\right)$

## Efficiencies of the Expansion process

## Turbine

## i) Total to total efficiency

It is defined as the ratio of Actual work to the Ideal work between the stagnation states.
$\eta_{\mathrm{tt}}=\frac{\text { Actual work }}{\text { Ideal work between the stagnation states }} ; \quad \eta_{\mathrm{tt}}=\frac{h_{01}-h_{02}}{h_{01}-h_{o 2}^{\prime}} ; \quad \eta_{\mathrm{tt}}=\frac{C_{p}\left(T_{01}-T_{02}\right)}{C_{p}\left(T_{01}-T_{o 2}^{\prime}\right)}$
$\eta_{\mathrm{tt}}=\frac{T_{01}-T_{02}}{T_{01}-T_{02 s}} ; \quad \eta_{\mathrm{tt}}=\frac{T_{01}-T_{02}}{T_{01}\left(1-\frac{T_{02 s}}{T_{01}}\right)} ; \quad T_{01}-T_{02}=\eta_{\mathrm{tt}} T_{01}\left(1-\frac{T_{02 s}}{T_{01}}\right)$
But $\frac{T_{02 s}}{T_{01}}=\left(\frac{p_{02}}{p_{01}}\right)^{\frac{\gamma-1}{\gamma}} \frac{T_{02 s}}{T_{01}}=\left(\frac{p_{02}}{p_{01}}\right)^{\frac{\gamma-1}{\gamma}} ; \frac{T_{02 s}}{T_{01}}=\left(\frac{p_{01}}{p_{02}}\right)^{-\left(\frac{\gamma-1}{\gamma}\right)}$;
$\frac{T_{02 s}}{T_{01}}=p_{\text {ro }}^{-\left(\frac{\gamma-1}{\gamma}\right)}$ where $p_{r o}$ is the total pressure ratio $\frac{p_{01}}{p_{02}}$
$\eta_{\mathrm{tt}}=\frac{T_{01}-T_{02}}{T_{01}\left(1-p_{r o}^{-\left(\frac{\gamma-1}{\gamma}\right)}\right)}$ where $p_{r o}$ is the total pressure ratio $\frac{p_{01}}{p_{02}}$

## Actual Power required

Actual Power required, $P=\dot{m} C_{p}\left(T_{01}-T_{02}\right)$
$P=\eta_{\mathrm{tt}} m C_{p}\left(T_{01}-T_{02 s}\right)$
$=\eta_{\mathrm{tt}} m C_{p} T_{01}\left(1-\frac{T_{02 s}}{T_{01}}\right)$
$=\eta_{\mathrm{tt}} m C_{p} T_{01}\left(1-p_{\text {ro }}^{-\left(\frac{\gamma-1}{\gamma}\right)}\right)$
If Mechanical Efficiency is given
$\mathrm{P}=m \eta_{\mathrm{tt}} \eta_{\text {mech }} C_{p} T_{01}\left(1-p_{\text {ro }}^{-\left(\frac{\gamma-1}{\gamma}\right)}\right)$

1. A stream of combustion gases at the point of entry to a turbine has a static temperature of 1050 K , static pressure of 600 kPa and a velocity of $150 \mathrm{~m} / \mathrm{s}$. For the gases $\mathrm{C}_{\mathrm{p}}=1.004 \mathrm{~kJ} / \mathrm{kgK}$ and $\gamma=1.41$. Find total temperature and total pressure of the gases. Also find the difference between their static and total enthalpies. (2b. 08, Dec/Jan 19, 15ME19)
Solution:
$T_{1}=1050 \mathrm{~K} ; P_{1}=600 \mathrm{kPa} ; V_{1}=150 \mathrm{~m} / \mathrm{s}$
$T_{0}=T+\frac{V^{2}}{2 C_{p}}+\frac{Z g}{C_{p}}$; since elevation is not given $T_{0}=T+\frac{V^{2}}{2 C_{p}}$
$T_{01}=T_{1}+\frac{V_{1}^{2}}{2 C_{p}} ;$
$T_{01}=1050+\frac{150^{2}}{2 * 1004} ; \quad T_{01}=1061.21 \mathrm{~K}$
$p_{0}=p+\frac{\rho V^{2}}{2}+Z \rho g$; since elevation is not given $p_{0}=p+\frac{\rho V^{2}}{2}$
$P_{01}=P_{1}+\frac{\rho V^{2}}{2} ;$
$\rho=\frac{p}{R T} ; \quad \rho=\frac{600}{0.287 * 1050} ; \quad \rho=1.991 \mathrm{~kg} / \mathrm{m}^{3}$
$P_{01}=(600 * 1000)+\frac{1.991 * 150^{2}}{2} ; \quad P_{01}=622398.75 \mathrm{~Pa}=6.223 \mathrm{bar}$
Static enthalpy $\quad h_{1}=C_{p} T_{1} ; h_{1}=1.004 * 1050 ; h_{1}=1051.2 \mathrm{~kJ} / \mathrm{kgK}$
Stagnation enthalpy $\quad h_{01}=C_{p} T_{01} ; h_{01}=1.004 * 1061.21 ; h_{01}=1065.45 \mathrm{~kJ} / \mathrm{kgK}$
Difference between static enthalpy and total enthalpy $=h_{01}-h_{1}=1065.45-1051.2$
Difference between static enthalpy and total enthalpy $=14.25 \mathrm{~kJ} / \mathrm{kgK}$
2. Air enters a compressor at a static pressure of 15 bar , a static temperature of $15^{\circ} \mathrm{C}$ and a flow velocity of $50 \mathrm{~m} / \mathrm{s}$, At the exit the static pressure is 30 bar, the static temperature is $100^{\circ} \mathrm{C}$ and the flow velocity is $100 \mathrm{~m} / \mathrm{s}$. The outlet is 1 m above the inlet Evaluate i) the isentropic change in enthalpy ii) The actual change in enthalpy. Take $C_{p}$ for air as 1005J/kgK. Also draw the relevant T-S diagram (2b. 10 June/July 13)

$$
\begin{aligned}
& T_{1}=15^{\circ} \mathrm{C}=288 \mathrm{~K} ; P_{1}=15 \mathrm{bar}=15 * 10^{5} ; V_{1}=50 \mathrm{~m} / \mathrm{s} ; Z_{1}=0 \\
& T_{2}=100^{\circ} \mathrm{C}=373 \mathrm{~K} ; P_{2}=30 \mathrm{bar}=30 * 10^{5} ; V_{2}=100 \mathrm{~m} / \mathrm{s} ; Z_{2}=1 \mathrm{~m}
\end{aligned}
$$

Isentropic enthalpy drop

$$
\begin{aligned}
& \frac{T_{2 s}}{T_{1}}=\left(\frac{p_{2}}{p_{1}}\right)^{\frac{\gamma-1}{\gamma}} ; \quad \frac{T_{2 s}}{288}=\left(\frac{30}{15}\right)^{0.286} ; \quad T_{2 s}=351.14 \mathrm{~K} \\
& \quad h_{2 s}-h_{1}=C_{p}\left(T_{2 s}-T_{1}\right) ; \quad h_{2 s}-h_{1}=1.005(351.14-288) ; h_{2 s}-h_{1}=63.45 \mathrm{~kJ} / \mathrm{kg} \\
& h_{1}=C_{p} T_{1} ; \quad h_{1}=1005 * 288=289440 \mathrm{~J} / \mathrm{kg} \\
& h_{2 s}=C_{p} T_{2 s} ; \quad h_{2 s}=1005 * 351.14=352895.7 \mathrm{~J} / \mathrm{kg}
\end{aligned}
$$

$h_{01}=h_{1}+\frac{V_{1}^{2}}{2}+Z_{1} g ; h_{01}=C_{p} T_{1}+\frac{V_{1}^{2}}{2}+Z_{1} g ; h_{01}=289440+\frac{50^{2}}{2}+0 ;$
$h_{01}=290690 \mathrm{~J} / \mathrm{kgK}$

$$
\begin{array}{ll}
h_{02 s}=h_{2 s}+\frac{V_{2}^{2}}{2}+Z_{2} g ; & h_{02 s}=C_{p} T_{2}+\frac{V_{2}^{2}}{2}+Z_{2} g \\
h_{02 s}=352895.7+\frac{100^{2}}{2}+(1 * 9.81) ; & h_{02 s}=357904.81 \mathrm{~J} / \mathrm{kgK}
\end{array}
$$

Isentropic enthalpy drop
$h_{02 s}-h_{01}=357904.81-290690 ; \quad h_{02 s}-h_{01}=67214.81 \mathrm{~J} / \mathrm{kg}$

## Actual enthalpy drop

$h_{01}=h_{1}+\frac{V_{1}^{2}}{2}+Z_{1} g ; \quad h_{01}=289440+\frac{50^{2}}{2}+0 ; \quad h_{01}=290690 \mathrm{~J} / \mathrm{kgK}$
$h_{02}=h_{2}+\frac{V_{2}^{2}}{2}+Z_{2} g ; h_{01}=C_{p} T_{2}+\frac{V_{2}^{2}}{2}+Z_{2} g ; h_{02}=(1005 * 373)+\frac{100^{2}}{2}+(1 * 9.81) ;$
$h_{02}=379874.81 \mathrm{~J} / \mathrm{kgK}$
Change in total enthalpy $=h_{02}-h_{01}=379874.81-290690=89184.84 \mathrm{~J} / \mathrm{kg}=89.184 \mathrm{~kJ} / \mathrm{kg}$

## Efficiency of the compressor

$\eta_{t t}=\frac{h_{02 s}-h_{01}}{h_{02}-h_{01}} ; \quad \eta_{0}=\frac{67214.81}{89184.8} ; \quad \eta_{t t}=0.75365$
3. Air enters a compressor at a static pressure of 1.5 bar, a static temperature of $15^{\circ} \mathrm{C}$ and a flow velocity of $50 \mathrm{~m} / \mathrm{s}$, At the exit the static pressure is 3 bar , the static temperature is $100^{\circ} \mathrm{C}$ and the flow velocity is $100 \mathrm{~m} / \mathrm{s}$. The outlet is 1 m above the inlet Evaluate i) the isentropic change in enthalpy ii) The actual change in enthalpy iii) Efficiency of the compressor (2c. 10 June/July 17) (2b. O8 June/July 18, 15ME53)
$p_{1}=1.5 \mathrm{bar} ; T_{1}=15^{\circ} \mathrm{C} ; V_{1}=50 \mathrm{~m} / \mathrm{s}$
$p_{2}=3 \mathrm{bar} ; T_{2}=100^{\circ} \mathrm{C} ; V_{2}=1000 \mathrm{~m} / \mathrm{s}$
$\Delta h_{o^{\prime}}=? ; \quad \Delta h_{o}=? ; \eta_{o}=?$

## Isentropic enthalpy drop

$$
\begin{aligned}
& \frac{T_{2 s}}{T_{1}}=\left(\frac{p_{2}}{p_{1}}\right)^{\frac{\gamma-1}{\gamma}} ; \quad \frac{T_{2 s}}{288}=\left(\frac{3}{1.5}\right)^{0.286} ; \quad T_{2 s}=351.14 \mathrm{~K} \\
& h_{2 s}-h_{1}=C_{p}\left(T_{2,}-T_{1}\right) ; \quad h_{2 s}-h_{1}=1.005(351.14-288) ; h_{2 \prime}-h_{1}=63.45 \mathrm{~kJ} / \mathrm{kg} \\
& h_{02 s}-h_{01}=h_{2 s}-h_{1}+\frac{V_{2}^{2}-V_{1}^{2}}{2}+\left(Z_{2}-Z_{1}\right) g \\
& h_{02 s}-h_{01}=63.45 \times 10^{3}+\frac{100^{2}-50^{2}}{2}+1 x 9.81
\end{aligned}
$$

$$
h_{02 s}-h_{01}=67.20 \times 10^{3} \mathrm{~J} / \mathrm{kg}
$$

## Actual enthalpy drop

$$
\begin{aligned}
& h_{02}-h_{01}=h_{2}-h_{1}+\frac{V_{2}^{2}-V_{1}^{2}}{2}+\left(Z_{2}-Z_{1}\right) g \\
& h_{02}-h_{01}=C_{p}\left(T_{2}-T_{1}\right)+\frac{V_{2}^{2}-V_{1}^{2}}{2}+\left(Z_{2}-Z_{1}\right) g \\
& h_{02}-h_{01}=1005(100-15)+\frac{100^{2}-50^{2}}{2}+1 \times 9.81 \\
& h_{02}-h_{01}=89184.81 \mathrm{~J} / \mathrm{kg} \\
& \eta_{0}=\frac{h_{02 \prime}-h_{01}}{h_{02}-h_{01}} ; \eta_{0}=\frac{67.20 \times 10^{3}}{89184.8} \\
& \eta_{0}=0.7536
\end{aligned}
$$

## Effect of preheat in multistage compression or prove that preheat factor is always less than 1

The overall isentropic efficiency is useful as it indicates the overall performance of a turbomachine. But it is not always indicate the true efficiency from hydrodynamic point of view which is measure of fluid losses within the machine.

A compressor stage with a finite pressure stage is called as finite stage
In a multistage compressor, in each stage efficiency depends on inlet temperature of fluid to the stage and pressure ratio in each stage

Thus in multistage compressor for the same efficiency, each succeeding stage is suffered by the inefficiency of preceding stage which is handling the fluid at higher temperature


Here, a three stage compressor is considered between the inlet pressure $p_{1}$ and delivery pressure $p_{4}$
Assume that stage pressure ratio for all stage is same $\frac{p_{2}}{p_{1}}=\frac{p_{3}}{p_{2}}=\frac{p_{4}}{p_{3}}$
stage efficiency for all the stages are same $\eta_{s 1}=\eta_{s 2}=\eta_{s 3}=\eta_{s}$
Let 14 "and 14 are the total isentropic and actual compression process respectively.
$\eta_{o}$ is the overall efficiency, $\mathrm{W}_{\mathrm{a}}$ and $\mathrm{W}_{\mathrm{s}}$ are the total actual and total isentropic work absorbed
$\eta_{o}=\frac{W_{s}}{W_{a}} ; \quad W_{a}=\frac{W_{s}}{\eta_{o}}-$ eqn 1
For stage 1 , stage efficiency
$\eta_{s}=\frac{W_{s 1}}{W_{a 1}} ; \quad W_{a 1}=\frac{W_{s 1}}{\eta_{s}}$
Similarly for stage $2, W_{a 2}=\frac{W_{s 2}}{\eta_{s}} ;$ For stage $3, W_{a 3}=\frac{W_{s 3}}{\eta_{s}}$
Total Work absorbed $W_{a}=W_{a 1}+W_{a 2}+W_{a 3}$
Hence, $W_{a}=\frac{W_{s 1}+W_{s 2}+W_{s 3}+\cdots \ldots . .}{\eta_{s}} ; \quad W_{a}=\frac{\sum_{i=0}^{i=k} W_{s 1}}{\eta_{s}}-$ eqn 2
Eqn $1=$ Eqn 2; $\quad \frac{W_{s}}{\eta_{o}}=\frac{\sum_{i=0}^{i=k} W_{s i}}{\eta_{s}} ; \quad \eta_{o}=\eta_{s} \frac{W_{s}}{\sum_{i=0}^{i=k} W_{s 1}}$
As the constant pressure lines are diverging in nature towards the right hand side of temperature entropy diagram, the isentropic work per stage increases as the temperature difference increases for the same pressure ratio and stage efficiency, therefore,
$\frac{W_{s}}{\sum_{i=0}^{i=k} \Delta W_{s 1}}<1$ whch is called as pre - heat factor; $\quad \eta_{o}=\eta_{s} \times$ pre heat factor

## Effect of Reheat in multistage compression or prove that Rreheat factor is always greater than 1

Thus in multistage turbine for the same efficiency, each succeeding stage is suffered by the inefficiency of preceding stage which is handling the fluid at higher temperature


Here a three stage Turbine is considered between the inlet pressure $p_{1}$ and delivery pressure $p_{4}$ Assume that stage pressure ratio for all stage is same $\frac{p_{1}}{p_{2}}=\frac{p_{2}}{p_{3}}=\frac{p_{3}}{p_{4}}$ and stage efficiency for all the stages are same $\eta_{s 1}=\eta_{s 2}=\eta_{s 3}=\eta_{s}$

Let 14 " and 14 are the total isentropic and actual compression process respectively.
$\eta_{o}$ is the overall efficiency
$\mathrm{W}_{\mathrm{a}}$ and $\mathrm{W}_{\mathrm{s}}$ are the total actual and total isentropic work absorbed
$\eta_{o}=\frac{W_{a}}{W_{s}} ; \quad W_{a}=\eta_{o} W_{s}--$ eqn 1
For stage 1 , stage efficiency; $\eta_{s}=\frac{W_{a 1}}{W_{s 1}} ; \quad W_{a 1}=\eta_{s} W_{s 1}$
Similarly for stage 2, $W_{a 2}=\eta_{s} W_{s 2} ; \quad$ For stage $3, W_{a 3}=\eta_{s} W_{s 3}$
$W_{a}=W_{a 1}+W_{a 2}+W_{a 3} ; W_{a}=\eta_{s}\left(W_{s 1}+W_{s 2}+W_{s 3}+\cdots \ldots\right) ; \quad W_{a}=\eta_{s} \sum_{i=0}^{i=k} W_{s i}-$ eqn 2
$\eta_{o} W_{s}=\eta_{s} \sum_{i=0}^{i=k} W_{s i} ; \quad \eta_{o}=\eta_{s} \frac{\sum_{i=0}^{i=k} \Delta W_{s 1}}{W_{s}}$
As the constant pressure lines are diverging in nature towards the right hand side of temperature entropy diagram, the isentropic work per stage increases as the temperature difference increases for the same pressure ratio and stage efficiency, therefore ,
$\frac{\sum_{i=0}^{i=k} W_{s 1}}{W_{s}}>1$ whch is called as Re-heat factor;
$\eta_{o}=\eta_{s} \times$ Re heat factor $=\eta_{0}=R F \times \eta_{s}$

## Infinitesimal stage efficiency or Polytropic efficiency in compression Process(compressor)

A finite compressor stage can be viewed as it made up of infinitesimal number of small stages. Each of these small stages has an efficiency, $\eta_{p}$, is called polytropic or infinitesimal stage efficiency

Consider a single stage compressor having stage efficiency $\eta_{s}$ operates between $p_{1}$ and $p_{2}$ divided into infinitesimal stages.

Considering one intermediate stage operating between pressures p and $\mathrm{p}+\mathrm{dp}$ and temperatures T and T+dT ( efficiency of such stage is called Polytropic efficiency)


ENTROPY
$\eta_{\mathrm{p}}=\frac{\text { Isentripic temp rise }}{\text { Actual temperature rise }}=\frac{d T_{S}}{d T} ; \quad d T=\frac{d T_{s}}{\eta_{P}} ; \quad d T=\frac{T^{\prime}-T}{\eta_{P}} ; d T=\frac{T\left(\frac{T^{\prime}}{T}-1\right)}{\eta_{P}}$
$\frac{d T}{T}=\frac{T\left(\left(\frac{p+d p}{P}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\eta_{P}} ; \quad \frac{d T}{T}=\frac{\left(\left(1+\frac{d p}{P}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\eta_{P}}$
Using series of expansion $(1+x)^{n}=1+n x+\frac{n(n-1)}{2} \pm--$; Neglecting higher order $1+n x$

$$
\frac{d T}{T}=\frac{1}{\eta_{P}}\left(1+\frac{\gamma-1}{\gamma}\left(\frac{d p}{P}\right)-1\right) ; \quad \frac{d T}{T}=\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)\left(\frac{d p}{P}\right)
$$

Integrating above equation pressure from $p_{1}$ to $p_{2}$ and temperature from $T_{1}$ to $T_{2}$
$\ln \frac{T_{2}}{T_{1}}=\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right) \ln \frac{p_{2}}{p_{1}} ; \quad \eta_{P}=\frac{\left(\frac{\gamma-1}{\gamma}\right) \ln \frac{p_{2}}{p_{1}}}{\ln \frac{T_{2}}{T_{1}}}$
Also, $\ln \frac{T_{2}}{T_{1}}=\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right) \ln \frac{p_{2}}{p_{1}} ; \quad \ln \frac{T_{2}}{T_{1}}=\ln \left(\frac{p_{2}}{p_{1}}\right)^{\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)} ; \quad \frac{T_{2}}{T_{1}}=\left(\frac{p_{2}}{p_{1}}\right)^{\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)}$ $\qquad$

Assuming the irreversible adiabatic compression process 1-2 as equivalent process with an index of compression $n$
$\frac{T_{2}}{T_{1}}=\left(\frac{p_{2}}{p_{1}}\right)^{\left(\frac{n-1}{n}\right)}$ $\qquad$
Comparing 1 and 2
$\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)=\left(\frac{n-1}{n}\right) ; \quad \eta_{P}=\left(\frac{\gamma-1}{\gamma}\right)\left(\frac{n}{n-1}\right)$
Hence there are two formulae to find polytropic efficiency

1. $\eta_{P}=\frac{\left(\frac{\gamma-1}{\gamma}\right) \ln \frac{p_{2}}{p_{1}}}{\ln \frac{T_{2}}{T_{1}}}$
2. $\eta_{P}=\left(\frac{\gamma-1}{\gamma}\right)\left(\frac{n}{n-1}\right)$

## Infinitesimal stage efficiency or Polytropic efficiency in expansion process (Turbine)

A finite turbine stage can be viewed as it made up of infinitesimal number of small stages. Each of these small stages has an efficiency, $\eta_{p}$, is called polytropic or infinitesimal stage efficiency

Consider a single stage turbine having stage efficiency $\eta_{s}$ operates between $p_{1}$ and $p_{2}$ divided into infinitesimal stages.

Considering one intermediate stage operating between pressures p and $\mathrm{p}+\mathrm{dp}$ and temperatures T and $\mathrm{T}+\mathrm{dp}$ ( efficiency of such stage is called Polytropic efficiency)


ENTROPY
$\eta_{\mathrm{p}}=\frac{\text { Actual temperature rise }}{\text { Isentripic temp rise }}=\frac{d T}{d T_{s}} ; d T=\eta_{P} d T_{S} ; d T=\eta_{P}\left(T-T_{S}\right) ; d T=\eta_{P} T\left(1-\frac{T_{s}}{T}\right)$
$\frac{d T}{T}=\eta_{P}\left(1-\left(\frac{p-d p}{p}\right)^{\frac{\gamma-1}{\gamma}}\right) ; \quad \frac{d T}{T}=\eta_{P}\left(1-\left(1-\frac{d p}{P}\right)^{\frac{\gamma-1}{\gamma}}\right) ;$
Using series of expansion $(1-x)^{n}=1-n x+\frac{n(n-1)}{2!} x^{2}-\frac{n(n-1)(n-2)}{3!}$
Neglecting higher order $1-n x ; \quad \frac{d T}{T}=\eta_{P}\left(1-\left(1-\frac{\gamma-1}{\gamma}\left(\frac{d p}{P}\right)\right)\right) ; \quad \frac{d T}{T}=\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)\left(\frac{d p}{P}\right)$

Integrating above equation pressure from $p_{1}$ to $p_{2}$ and temperature from $T_{1}$ to $T_{2}$
$\ln \frac{T_{2}}{T_{1}}=\eta_{P}\left(\frac{\gamma-1}{\gamma}\right) \ln \frac{p_{2}}{p_{1}} ; \quad \eta_{P}=\frac{\ln \frac{T_{2}}{T_{1}}}{\left(\frac{\gamma-1}{\gamma}\right) \ln \frac{p_{2}}{p_{1}}} ;$
$\ln \frac{T_{2}}{T_{1}}=\eta_{P}\left(\frac{\gamma-1}{\gamma}\right) \ln \frac{p_{2}}{p_{1}} ; \quad \ln \frac{T_{2}}{T_{1}}=\ln \left(\frac{p_{2}}{p_{1}}\right)^{\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)} ; \quad \frac{T_{2}}{T_{1}}=\left(\frac{p_{2}}{p_{1}}\right)^{\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}$ $\qquad$

Assuming the irreversible adiabatic compression process 1-2 as equivalent process with an index of compression n
$\frac{T_{2}}{T_{1}}=\left(\frac{p_{2}}{p_{1}}\right)^{\left(\frac{n-1}{n}\right)}$ $\qquad$

Comparing 1 and 2
$\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)=\left(\frac{n-1}{n}\right) ; \quad \eta_{P}=\left(\frac{\gamma}{\gamma-1}\right)\left(\frac{n-1}{n}\right)$ this is another formulae for polytropic efficiency

There are two formulae to determine polytropic efficiency for turbine

1. $\quad \eta_{P}=\frac{\ln \frac{T_{2}}{T_{1}}}{\left(\frac{\gamma-1}{\gamma}\right) \ln \frac{p_{2}}{p_{1}}} ; \quad$ 2. $\quad \eta_{P}=\frac{\ln \frac{T_{2}}{T_{1}}}{\left(\frac{\gamma-1}{\gamma}\right) \ln \frac{p_{2}}{p_{1}}}$

## Multistage compressors (Equal Pressure ratio case)



ENTROPY

Consider multistage compression of $k$ stages between the pressures $p_{1}$ and $p_{k+1}$ with overall pressure ratio $\frac{p_{k+1}}{p_{1}}$ and having equal stage efficiencies $\eta_{s t}$ or $\eta_{p}$ then the pressure ratio in each stage is given by
$p_{r}=\frac{p_{2}}{p_{1}}=\frac{p_{3}}{p_{2}}=\frac{p_{4}}{p_{3}}=\cdots \ldots \ldots=\frac{p_{k+1}}{p_{k}}$
$p_{\text {ro }}=\frac{p_{k+1}}{p_{1}}=\frac{p_{2}}{p_{1}} \times \frac{p_{3}}{p_{2}} \times \frac{p_{4}}{p_{3}} \times \ldots \ldots \ldots \times \frac{p_{k+1}}{p_{k}}$
$p_{\text {ro }}=\frac{p_{k+1}}{p_{1}}=p_{r} \times p_{r} \times p_{r} x \ldots \ldots \ldots \times p_{r}$
$p_{r o}=\frac{p_{k+1}}{p_{1}}=p_{r}^{k}$

Efficiency of stage in multi stage compressor is called stage efficiency

## a. Compressor

$\eta_{s t}=\frac{T_{2}^{\prime}-T_{1}}{T_{2}-T_{1}} ; \quad \eta_{s t}=\frac{T_{1}\left(\frac{T_{2}^{\prime}}{T_{1}}-1\right)}{T_{1}\left(\frac{T_{2}}{T_{1}}-1\right)} ; \quad \eta_{s t}=\frac{\left(\frac{p_{2}}{p_{1}}\right)^{\left(\frac{\gamma-1}{\gamma}\right)}-1}{\left(\frac{p_{2}}{p_{1}}\right)^{\left(\frac{n-1}{n}\right)}-1}$
But, $\left(\frac{n-1}{n}\right)=\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)$; Hence $\eta_{s t}=\frac{\left(\frac{p_{2}}{p_{1}}\right)^{\left(\frac{\gamma-1}{\gamma}\right)}-1}{\left(\frac{p_{2}}{p_{1}}\right)^{\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)}-1}$
$\eta_{s t}=\frac{p_{r}{ }^{\left(\frac{\gamma-1}{\gamma}\right)}-1}{p_{r}{ }^{\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)}-1}$

## Overall efficiency of multistage compressor

For multistage compressor the stage efficiency $\eta_{s t}$ is replaced by the overall efficiency $\eta_{o}$ and the stage pressure ratio $p_{r}$ by the overall pressure ratio $p_{\mathrm{r}}$ then the above equation becomes


## Multi stage turbine (Equal Pressure ratio case)

For multistage turbine the stage efficiency $\eta_{s t}$ is replaced by the overall efficiency $\eta_{o}$ and the stage pressure ratio $p_{\mathrm{r}}$ by the overall pressure ratio $p_{\mathrm{ro}}$ then the above equation becomes
$\eta_{0}=\frac{1-\left(p_{r 0}\right)^{-\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}}{1-\left(p_{r_{0}}\right)^{-\left(\frac{\gamma-1}{\gamma}\right)}}$ Multistage turbine
Consider multistage expansion of $k$ stages between the pressures $p_{1}$ and $p_{k+1}$ with overall pressure ratio $\frac{p_{1}}{p_{k+1}}$ and having equal stage efficiencies $\eta_{s t}$ or $\eta_{\mathrm{p}}$ then the pressure ratio in each stage is given by
$p_{r}=\frac{p_{1}}{p_{2}}=\frac{p_{2}}{p_{3}}=\frac{p_{3}}{p_{4}}=\ldots \ldots \ldots=\frac{p_{k}}{p_{k+1}}$
$p_{r o}=\frac{p_{1}}{p_{k+1}}=\frac{p_{1}}{p_{2}} x \frac{p_{2}}{p_{3}} x \frac{p_{3}}{p_{4}} \times \ldots \ldots \ldots \times \frac{p_{k}}{p_{k+1}}$
$p_{r o}=\frac{p_{1}}{p_{k+1}}=p_{r} \times p_{r} \times p_{r} \times \ldots \ldots \ldots \times p_{r}$
$p_{r o}=\frac{p_{1}}{p_{k+1}}=p_{r}^{k}$

## Stage Efficiency (Expansion Process - Turbine)

Stage efficiency
$\eta_{s t}=\frac{T_{1}-T_{2}}{T_{1}-T_{2}^{\prime}} ; \quad \eta_{s t}=\frac{T_{1}\left(1-\frac{T_{2}}{T_{1}}\right)}{T_{1}\left(1-\frac{T_{2}^{\prime}}{T_{1}}\right)^{\prime}} ; \quad \eta_{s t}=\frac{1-\left(\frac{p_{2}}{p_{1}}\right)^{\left(\frac{n-1}{n}\right)}}{1-\left(\frac{p_{2}}{p_{1}}\right)^{\left(\frac{\gamma-1}{\gamma}\right)}} ;$
But
$\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)=\left(\frac{n-1}{n}\right)$
$\eta_{s t}=\frac{1-\left(\frac{p_{2}}{p_{1}}\right)^{\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}}{1-\left(\frac{p_{2}}{p_{1}}\right)^{\left(\frac{\gamma-1}{\gamma}\right)}} ; \quad \eta_{s t}=\frac{1-\left(\frac{p_{1}}{p_{2}}\right)^{-\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}}{1-\left(\frac{p_{1}}{p_{2}}\right)^{-\left(\frac{\gamma-1}{\gamma}\right)}} ; \quad \eta_{s t}=\frac{1-\left(p_{r}\right)^{-\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}}{1-\left(p_{r}\right)^{-\left(\frac{\gamma-1}{\gamma}\right)}}$ where $p_{r}=\frac{p_{1}}{p_{2}}$

## Overall efficiency of multistage Turbine

For multistage expansion the stage efficiency $\eta_{s t}$ is replaced by the overall efficiency $\eta_{o}$ and the stage pressure ratio $p_{r}$ by the overall pressure ratio $p_{r o}$ then the above equation becomes
$\eta_{0}=\frac{1-\left(p_{r 0}\right)^{-\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}}{1-\left(p_{r 0}\right)^{-\left(\frac{\gamma-1}{\gamma}\right)}} ; \quad \eta_{0}=\frac{1-\left(p_{r}\right)^{-K \eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}}{1-\left(p_{r}\right)^{-K\left(\frac{\gamma-1}{\gamma}\right)}}$

## Overall efficiency for a finite number compressor stages in terms of stage efficiency for a Compressor

$T_{i}$ is the initial temperature at which the fluid enters the turbine, $K$ is the number of stages having equal pressure ratio, $p_{r}$ is the pressure ratio in each stage, then the actual temperature rise in each stage can be calculated as follows

For First stage
$\eta_{s}=\frac{T_{i+1}^{\prime}-T_{i}}{T_{i+1}-T_{i}} ; \quad \eta_{s}=\frac{T_{i}\left(\frac{T_{i+1}^{\prime}}{T_{i}}-1\right)}{T_{i+1}-T_{i}} ; \quad \eta_{s}=\frac{T_{i}\left(\left(\frac{p_{i+1}}{p_{i}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{T_{i+1}-T_{i}} ;$
$T_{i+1}-T_{i}=\frac{T_{i}\left(\left(\frac{p_{i+1}}{p_{i}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\eta_{s}} ; \Delta T_{i}=\frac{T_{i}}{\eta_{s}}\left(\left(\frac{p_{i+1}}{p_{i}}\right)^{\frac{\gamma-1}{\gamma}}-1\right) ; \Delta T_{i}=\frac{T_{i}}{\eta_{s}}\left(\left(p_{r}\right)^{\frac{\gamma-1}{\gamma}}-1\right)$
$\Delta T_{i}=A T_{i}$ where $A=\frac{1}{\eta_{s}}\left(\left(p_{r}\right)^{\frac{\gamma-1}{\gamma}}-1\right)$
For First stage $\quad \Delta T_{1}=A T_{1} ;$
$T_{2}-T_{1}=A T_{1} ; \quad T_{2}=T_{1}+A T_{1} ; \quad T_{2}=T_{1}(1+A)$

For Second stage $\Delta T_{2}=A T_{2} ;$
Substituting $T_{2}$ in terms of $T_{1}, \quad \Delta T_{2}=A T_{1}(1+A)$

$$
T_{3}-T_{2}=A T_{2} ; T_{3}=T_{2}+A T_{2} ; \quad T_{3}=T_{2}(1+A) ; T_{3}=T_{1}(1+A)(1+A) ; T_{3}=T_{1}(1+A)^{2}
$$

For Third stage $\Delta T_{3}=A T_{3} ;$
Substituting $T_{2}$ in terms of $T_{1} ; \Delta T_{3}=A T_{1}(1+A)^{2}$
For Kth stage
$\Delta T_{4}=A T_{1}(1+A)^{K-1}$
$\sum_{i=1}^{i=K} \Delta T_{i}=\Delta T_{1}+\Delta T_{2}+\Delta T_{3}+\cdots \ldots \ldots+\Delta T_{k}$
$\sum_{i=1}^{i=K} \Delta T_{i}=A T_{1}+T_{1} A(1+A)+A T_{1}(1+A)^{2}+A T_{1}(1+A)^{3}+\cdots \ldots \ldots .+A T_{1}(1+A)^{K-1} ;$
$\sum_{i=1}^{i=K} \Delta T_{i}=A T_{1}\left(1+(1+A)+(1+A)^{2}+(1+A)^{3}+\cdots \ldots \ldots \ldots+(1+A)^{K-1}\right) ; ;$
$\sum_{i=1}^{i=K} \Delta T_{i}=T_{1}\left[(1+A)^{K}-1\right]$
$\Delta T_{o}=T_{1}\left[\left(1+\frac{\left(p_{r}\right)^{\frac{\gamma-1}{\gamma}}-1}{\eta_{s}}\right)^{K}-1\right]$
$\eta_{o}=\frac{T_{k+1}^{\prime}-T_{1}}{T_{K}-T_{1}} ; \quad \eta_{o}=\frac{T_{1}\left(\frac{T_{k+1}^{\prime}}{T_{1}}-1\right)}{\Delta T_{o}} ; \quad \eta_{o}=\frac{T_{1}\left[\left(p_{r 0}\right)^{\frac{\gamma-1}{\gamma}}-1\right]}{T_{1}\left[\left(1+\frac{\left(p_{r}\right)^{\frac{\gamma-1}{\gamma}}-1}{\eta_{s}}\right)^{K}-1\right]} ;$
$\eta_{o}=\frac{\left[\left(p_{r 0}\right)^{\frac{\gamma-1}{\gamma}}-1\right]}{\left[\left(1+\frac{\left(p_{r}\right)^{\frac{\gamma-1}{\gamma}-1}}{\eta_{s}}\right)^{K}-1\right]^{K}} ;$

$$
\eta_{o}=\frac{\left[\left(p_{r}\right)^{\frac{\gamma-1}{\gamma}}-1\right]}{\left[\left(1+\frac{\left(p_{r}\right)^{\frac{\gamma-1}{\gamma}}-1}{\eta_{S}}\right)^{K}-1\right]} \quad \text { as } p_{r 0}=\left(p_{r}\right)^{K}
$$

Let $S=1+(1+A)+(1+A)^{2}+(1+A)^{3}+\cdots \ldots \ldots \ldots+(1+A)^{K-1}$
$S=1+(1+A)\left(1+(1+A)+(1+A)^{2}+(1+A)^{3}+\cdots \ldots \ldots+(1+A)^{K-2}\right)$
$S=1+(1+A)\left(S-(1+A)^{K-1}\right)$
$S-1=(1+A) S-(1+A)(1+A)^{K-1}$
$S-1=S+A S-(1+A)^{K}$
$(1+A)^{K}-1=A S$

$$
\begin{aligned}
\Delta T_{o}=\sum_{i=1}^{i=K} \Delta T_{i} & =A T_{1} S \\
& =T_{1}\left[(1+A)^{K}-1\right]
\end{aligned}
$$

## Overall efficiency for a finite number of turbine stages in terms of stage

 efficiency for a Turbine$T_{i}$ is the initial temperature at which the fluid enters the compressor, $K$ is the number of stages having equal pressure ratio, $\mathrm{p}_{\mathrm{r}}$ is the pressure ratio in each stage, then the actual temperature rise in each stage can be calculated as follows

For First stage
$\eta_{s}=\frac{T_{i}-T_{i+1}}{T_{i}-T_{i+1}^{\prime}} ; \quad \eta_{s}=\frac{T_{i}-T_{i+1}}{T_{i}\left(1-\frac{T_{i+1}^{\prime}}{T_{i}}\right)} ; \quad \eta_{s}=\frac{T_{i}-T_{i+1}}{T_{i}\left(1-\left(\frac{p_{i+1}}{p_{i}}\right)^{\frac{\gamma-1}{\gamma}}\right)} ; T_{i}-T_{i+1}=\eta_{s} T_{i}\left(1-\left(\frac{p_{i+1}}{p_{i}}\right)^{\frac{\gamma-1}{\gamma}}\right)$
$\Delta T_{i}=\eta_{s} T_{i}\left(1-\left(\frac{p_{i+1}}{p_{i}}\right)^{\frac{\gamma-1}{\gamma}}\right) ; \Delta T_{i}=\eta_{S} T_{i}\left(1-\left(\frac{p_{i+1}}{p_{i}}\right)^{\frac{\gamma-1}{\gamma}}\right) ; \Delta T_{i}=\eta_{s} T_{i}\left(1-\left(\frac{p_{i}}{p_{i+1}}\right)^{-\frac{\gamma-1}{\gamma}}\right)$
$\Delta T_{i}=\eta_{s} T_{i}\left(1-\left(p_{r}\right)^{-\frac{\gamma-1}{\gamma}}\right)$
$\Delta T_{i}=A T_{i}$ where $A=\eta_{s}\left(1-\left(p_{r}\right)^{-\frac{\gamma-1}{\gamma}}\right)$
For First stage
$\Delta T_{1}=A T_{1} ;$
$T_{1}-T_{2}=A T_{1} ; \quad T_{2}=T_{1}-A T_{1} ; \quad T_{2}=T_{1}(1-A)$
For Second stage, $\Delta T_{2}=A T_{2}$
Substituting $T_{2}$ in terms of $T_{1}, \Delta T_{2}=A T_{1}(1-A)$
$T_{2}-T_{3}=A T_{2} ; \quad T_{3}=T_{2}-A T_{2} ; \quad T_{3}=T_{2}(1-A) ; \quad T_{3}=T_{2}(1-A) ; T_{3}=T_{1}(1-A)(1-A)$
$T_{3}=T_{1}(1-A)^{2}$
For third stage, $\Delta T_{3}=A T_{3}$;
Substituting $T_{2}$ in terms of $T_{1}, \Delta T_{3}=A T_{1}(1-A)^{2}$
Similarly for $4^{\text {th }}$ stage, $\Delta T_{4}=A T_{1}(1-A)^{3}$
For Kth stage, $\Delta T_{4}=A T_{1}(1-A)^{K-1}$

$$
\begin{aligned}
& \sum_{i=1}^{i=K} \Delta T_{i}=\Delta T_{1}+\Delta T_{2}+\Delta T_{3}+\cdots \ldots \ldots+\Delta T_{k} \\
& \sum_{i=1}^{i=K} \Delta T_{i}=A T_{1}+T_{1} A(1-A)+A T_{1}(1-A)^{2}+A T_{1}(1-A)^{3}+\cdots \ldots \ldots . .+A T_{1}(1-A)^{K-1} ; \\
& \sum_{i=1}^{i=K} \Delta T_{i}=A T_{1}\left(1+(1-A)+(1-A)^{2}+(1-A)^{3}+\cdots \ldots \ldots \ldots+(1-A)^{K-1}\right) ; \\
& =T_{1}\left[1-(1-A)^{K}\right] \\
& \Delta T_{o}=T_{1}\left[1-(1-A)^{K}\right] \\
& \eta_{o}=\frac{T_{1}-T_{K}}{T_{1}-T_{k+1}^{\prime}} ; \eta_{o}=\frac{\Delta T_{o}}{T_{1}\left(1-\frac{T_{k+1}^{\prime}}{T_{1}}\right)} ; \eta_{o}=\frac{T_{1}\left[1-(1-A)^{K}\right]}{T_{1}\left(1-\frac{T_{k+1}^{\prime}}{T_{1}}\right)} ; \quad \eta_{o}=\frac{\left[1-(1-A)^{K}\right]}{1-\left(\frac{p_{k+1}^{\prime}}{p_{1}}\right)^{\frac{\gamma-1}{\gamma}} ;} \eta_{o}=\frac{\left[1-(1-A)^{K}\right]}{1-\left(\frac{p_{1}}{p_{k+1}^{\prime}}\right)^{-\frac{\gamma-1}{\gamma}}} \\
& \eta_{o}=\frac{\left[1-\left(1-\eta_{s}\left(1-\left(p_{r}\right)^{-\frac{\gamma-1}{\gamma}}\right)\right)^{K}\right]}{1-\left(p_{r 0}\right)^{-\frac{\gamma-1}{\gamma}}} ; \quad \eta_{0}=\frac{\left[1-\left(1-\eta_{s}\left(1-\left(p_{r}\right)^{-\frac{\gamma-1}{\gamma}}\right)\right)^{K}\right]}{1-\left(p_{r}\right)^{-K \frac{\gamma-1}{\gamma}}} \\
& \text { Let } S=1+(1-A)+(1-A)^{2}+(1-A)^{3}+\cdots \ldots \ldots \ldots+(1-A)^{K-1} \\
& S=1+(1-A)\left(1+(1-A)+(1-A)^{2}+(1-A)^{3}+\cdots \ldots \ldots \ldots+(1-A)^{K-2}\right) \\
& S=1+(1-A)\left(S-(1-A)^{K-1}\right) \\
& S-1=(1-A) S-(1-A)(1-A)^{K-1} \\
& S-1=S-A S-(1-A)^{K} \\
& A S=1-(1-A)^{K}
\end{aligned}
$$

## Mutli Stage Compressor (Constant temperature rise for compressor)

For constant stage work in a multistage compressor, the temperature rise in each stage is same, but the temperature at entry of each stage will be different. For given values of overall pressure ratio $p_{r o}$ and polytropic efficiency $\eta_{p}$, the total temperature rise per stage is given by
$\Delta T_{s t}=\frac{\Delta T_{0}}{K} ; \quad \Delta T_{0}=T_{0 k+1}-T_{01} ; \quad \Delta T_{0}=T_{01}\left(\frac{T_{0 k+1}}{T_{01}}-1\right) ; \Delta T_{0}=T_{01}\left(\left(\frac{p_{k+1}}{p_{1}}\right)^{\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)}-1\right)$
$\Delta T_{0}=T_{01}\left(\left(p_{r o}\right)^{\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)}-1\right) ; \Delta T_{s t}=\frac{T_{01}\left(\left(p_{r o}\right)^{\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)}-1\right)}{K}$
Knowing the temperature rise in each stage, the pressure ratio and hence the efficiency for each stages can now be calculated.

For $i^{\text {th }}$ stage, it is given by
$\Delta T_{i}=T_{i+1}-T_{i}$

$$
\begin{gathered}
=T_{i}\left(\frac{T_{i+1}}{T_{i}}-1\right) \\
=T_{i}\left(\left(p_{r i}\right)^{\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)}-1\right) \\
\frac{\Delta T_{i}}{T_{i}}=\left(p_{r i}\right)^{\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)}-1 \\
1+\frac{\Delta T_{i}}{T_{i}}=\left(p_{r i}\right)^{\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)}
\end{gathered}
$$

Hence the pressure rise in each stage is
$p_{r i}=\left(1+\frac{\Delta T_{i}}{T_{i}}\right)^{\eta_{P}\left(\frac{\gamma}{\gamma-1}\right)}$

From the above equation it can be seen that the pressure ratio in each stage decreases as $T_{i}$ increases (as $\Delta T_{i}$ is constant for all stages

Hence stage efficiency is not constant and it varies for each stage, Hence

It can be calculated for each stage as
$\eta_{s t i}=\frac{p_{r i}{ }^{\left(\frac{\gamma-1}{\gamma}\right)}-1}{p_{r i}{ }^{\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)}-1}$

## Constant temperature rise for Expansion stages (Turbine stage)

For constant stage work in a multistage turbine, the temperature rise in each stage is same, but the temperature at entry of each stage will be different. For given values of overall pressure ratio $p_{r o}$ and polytropic efficiency $\eta_{p}$, the total temperature rise per stage is given by
$\Delta T_{s t}=\frac{\Delta T_{0}}{K} ;$
$\Delta T_{0}=T_{01}-T_{0 k+1} ; \quad \Delta T_{0}=T_{01}\left(1-\frac{T_{0 k+1}}{T_{01}}\right) ; \Delta T_{0}=T_{01}\left(1-\left(\frac{p_{k+1}}{p_{1}}\right)^{\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}\right)$
$\Delta T_{0}=T_{01}\left(1-\left(\frac{p_{1}}{p_{k+1}}\right)^{-\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}\right) ; \quad \Delta T_{0}=T_{01}\left(1-\left(p_{r o}\right)^{-\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}\right)$
$\Delta T_{s t}=\frac{T_{01}\left(1-\left(p_{r o}\right)^{-\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}\right)}{K}$
Knowing the temperature rise in each stage, the pressure ratio and hence the efficiency for each stages can now be calculated.

For $\mathrm{i}^{\text {th }}$ stage, it is given by
$\Delta T_{i}=T_{i}-T_{i+1} ; \quad \Delta T_{i}=T_{i}\left(1-\frac{T_{i+1}}{T_{i}}\right) ; \quad \Delta T_{i}=T_{i}\left(1-\left(\frac{p_{i+1}}{p_{i}}\right)^{\frac{n-1}{n}}\right) ; \Delta T_{i}=T_{i}\left(1-\left(\frac{p_{i}}{p_{i+1}}\right)^{-\frac{n-1}{n}}\right)$
$\Delta T_{i}=T_{i}\left(1-\left(\frac{p_{i}}{p_{i+1}}\right)^{-\eta_{P}\left(\frac{\gamma-1}{r}\right)}\right) ; \frac{\Delta T_{i}}{T_{i}}=1-\left(p_{r i}\right)^{-\eta_{P}\left(\frac{\gamma-1}{r}\right)}$
$1-\frac{\Delta T_{i}}{T_{i}}=\left(p_{r i}\right)^{-\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}$
Hence the pressure rise in each stage is
$p_{r i}=\left(1-\frac{\Delta T_{i}}{T_{i}}\right)^{-\frac{1}{\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}}$
From the above equation it can be seen that the pressure ratio in each stage decreases as $T_{i}$ increases (as $\Delta T_{i}$ is constant for all stages

Various formulae

| Efficiency | Compressor | Turbine |
| :---: | :---: | :---: |
| Infinitesimal or Polytropic | $\begin{gathered} \eta_{P}=\frac{\left(\frac{\gamma-1}{\gamma}\right) \ln \frac{p_{2}}{p_{1}}}{\ln \frac{T_{2}}{T_{1}}} \\ \eta_{P}=\left(\frac{\gamma-1}{\gamma}\right)\left(\frac{n}{n-1}\right) \end{gathered}$ | $\begin{aligned} \eta_{P} & =\frac{\ln \frac{T_{2}}{T_{1}}}{\left(\frac{\gamma-1}{\gamma}\right) \ln \frac{p_{2}}{p_{1}}} \\ \eta_{P} & =\left(\frac{\gamma}{\gamma-1}\right)\left(\frac{n-1}{n}\right) \end{aligned}$ |
| Stage | $\begin{aligned} & \eta_{s t}=\frac{\left(\frac{p_{2}}{p_{1}}\right)^{\left(\frac{\gamma-1}{\gamma}\right)}-1}{\left(\frac{p_{2}}{p_{1}}\right)^{\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)}-1} \\ & \eta_{s t}=\frac{\left(p_{r}\right)^{\left(\frac{\gamma-1}{\gamma}\right)}-1}{\left(p_{r}\right)^{\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)}-1} \end{aligned}$ | $\begin{aligned} & \eta_{s t}=\frac{1-\left(\frac{p_{1}}{p_{2}}\right)^{-\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}}{1-\left(\frac{p_{1}}{p_{2}}\right)^{-\left(\frac{\gamma-1}{\gamma}\right)}} \\ & \eta_{s t}=\frac{1-\left(p_{r}\right)^{-\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}}{1-\left(p_{r}\right)^{-\left(\frac{\gamma-1}{\gamma}\right)}} \end{aligned}$ |
| Overall | $\begin{aligned} & \eta_{s t}=\frac{\left(\frac{p_{k+1}}{p_{1}}\right)^{\left(\frac{\gamma-1}{\gamma}\right)}-1}{\left(\frac{p_{k+1}}{p_{1}}\right)^{\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)}-1} \\ & \eta_{s t}=\frac{\left(p_{r 0}\right)^{\left(\frac{\gamma-1}{\gamma}\right)}-1}{\left(p_{r 0}\right)^{\frac{1}{\eta_{P}}\left(\frac{\gamma-1}{\gamma}\right)}-1} \end{aligned}$ | $\begin{aligned} \eta_{s t} & =\frac{1-\left(\frac{p_{1}}{p_{k+1}}\right)^{-\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}}{1-\left(\frac{p_{1}}{p_{k+1}}\right)^{-\left(\frac{\gamma-1}{\gamma}\right)}} \\ \eta_{s t} & =\frac{1-\left(p_{r 0}\right)^{-\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}}{1-\left(p_{r o}\right)^{-\left(\frac{\gamma-1}{\gamma}\right)}} \end{aligned}$ |
| Efficiency | Compressor | Turbine |
| Overall efficiency in terms of stage efficiency | $\begin{aligned} & \eta_{o}=\frac{\left[\left(p_{r 0}\right)^{\frac{\gamma-1}{\gamma}}-1\right]}{\left[\left(1+\frac{\left(p_{r}\right)^{\frac{\gamma-1}{\gamma}}-1}{\eta_{S}}\right)^{K}-1\right]} \\ & \eta_{o}=\frac{\left[\left(p_{r}\right)^{K \frac{\gamma-1}{\gamma}}-1\right]}{\left[\left(1+\frac{\left(p_{r}\right)^{\frac{\gamma-1}{\gamma}}-1}{\eta_{S}}\right)^{K}-1\right]} \\ & p_{r 0}=\left(p_{r}\right)^{K} \end{aligned}$ | $\begin{aligned} & \eta_{o}=\frac{\left[1-\left(1-\eta_{s}\left(1-\left(p_{r}\right)^{-\frac{\gamma-1}{\gamma}}\right)\right)^{K}\right]}{1-\left(p_{r 0}\right)^{-\frac{\gamma-1}{\gamma}}} \\ & \eta_{0}=\frac{\left[1-\left(1-\eta_{s}\left(1-\left(p_{r}\right)^{-\frac{\gamma-1}{\gamma}}\right)\right)^{K}\right]}{1-\left(p_{r}\right)^{-K \frac{\gamma-1}{\gamma}}} \\ & p_{r 0}=\left(p_{r}\right)^{K} \end{aligned}$ |

## Numericals

4. A 16 stage axial flow compressor is to have a pressure ratio of 6.3 and tests have shown that a stage efficiency of $89.5 \%$ can be obtained. The intake conditions are 288 K and 1 bar pressure Find i) Overall efficiency ii) Polytropic efficiency iii) Preheat factor(2c. 08 Dec/Jan 17)
$\mathrm{K}=16 ; p_{r 0}=6.3 ; \eta_{s}=0.895 ; T_{1}=288 \mathrm{~K} ; p_{1}=1 \mathrm{bar}$
$\eta_{0}=? ; \eta_{p}=? ;$ PHF=?
$p_{r 0}=\left(p_{r}\right)^{K} ; 6.3=\left(p_{r}\right)^{16} ; \quad p_{r}=1.1219$
$\eta_{0}=\frac{\left[\left(p_{r 0}\right)^{\frac{\gamma-1}{\gamma}}-1\right]}{\left[\left(1+\frac{\left(p_{r}\right)^{\frac{\gamma-1}{\gamma}}-1}{\eta_{S}}\right)^{K}-1\right]} \quad$ as $p_{r 0}=\left(p_{r}\right)^{K}$
$\eta_{0}=\frac{\left[(6.3)^{0.286}-1\right]}{\left[\left(1+\frac{(1.1219)^{0.286-1}}{0.895}\right)^{K}-1\right]}=0.8674$
Also, Overall efficiency

$\eta_{0}=\eta_{s} x P H F ; \quad 0.8674=0.895 \times$ PHF ie $\mathrm{PHF}=0.9691$
5. In a three stage turbine the pressure ratio of each stage is 2 and the stage efficiency is $75 \%$.

Calculate the overall efficiency and reheat factor (2c. 08, June/July 14)

$$
\begin{aligned}
& p_{r}=2 ; \eta_{s}=0.75 ; \\
& \eta_{0}=\frac{\left[1-\left(1-\eta_{s}\left(1-\left(p_{r}\right)^{-\frac{\gamma-1}{\gamma}}\right)\right)^{K}\right]}{1-\left(p_{r}\right)^{-K \frac{\gamma-1}{\gamma}}} ; \quad \eta_{0}=\frac{\left[1-\left(1-0.75\left(1-(2)^{-0.286}\right)\right)^{3}\right]}{1-(2)^{-3 \times 0.286}} ; \quad \eta_{0}=\frac{0.3525}{0.4483} ; \quad \eta_{0}=0.7863 \\
& \eta_{0}=\eta_{s} x P H F ; \quad 0.7863=0.75 * R H F ; \quad R H F=1.048
\end{aligned}
$$

6. An air compressor has eight stages of equal pressure ratio 1:3.5. The flow rate through the compressor and its overall efficiency are $50 \mathrm{~kg} / \mathrm{s}$ and $82 \%$ respectively. If the conditions of air at the entry are 1 bar and 300 K determine
i) The state of air at compressor exit
ii) Polytropic efficiency
iii) Stage efficiency
$p_{\text {ro }}=3.5 ; \quad \dot{m}=50 \mathrm{~kg} / \mathrm{s} ; \eta_{0}=0.82 ; p_{1}=1$ bar $; T_{1}=300 \mathrm{~K}$
i) The state of air at compressor exit
$\eta_{0}=\frac{T_{095}-T_{01}}{T_{09}-T_{01}} ; \quad \eta_{0}=\frac{T_{095}-T_{01}}{T_{09}-T_{01}} ; \quad \eta_{0}=\frac{T_{01}\left(\frac{T_{095}}{T_{01}}-1\right)}{T_{09}-T_{01}}$
$\eta_{0}=\frac{T_{01}\left(p_{r 0}^{k\left(\frac{\gamma-1}{\gamma}\right)}-1\right)}{T_{09}-T_{01}}$;
$0.82=\frac{300\left(3.5^{8(0.286)}-1\right)}{T_{09}-300} ; \quad T_{09}=6363.02 \mathrm{~K}$
ii) Polytropic efficiency

$$
\begin{aligned}
& \eta_{0}=\frac{p_{r}{ }^{K\left(\frac{\gamma-1}{\gamma}\right)_{-1}}}{p_{r} \frac{1}{\eta_{P} K\left(\frac{\gamma-1}{\gamma}\right)}} ;-1 \quad 0.82=\frac{3.5^{(18 * 0.286)}-1}{3.5^{\left(\frac{18 * 0.286}{\eta_{P}}\right)}-1} ; \quad 3.5^{\left(\frac{18 * 0.286}{\eta_{P}}\right)}-1=769.76+1 ; \\
& \frac{18 * 0.286}{\eta_{P}} \ln 3.5=\ln 770.76 ; \quad \eta_{P}=0.970
\end{aligned}
$$

## iii) Stage efficiency

$$
\begin{aligned}
& \eta_{s}=\frac{T_{02 s}-T_{01}}{T_{02}-T_{01}} ; \quad \eta_{s}=\frac{T_{01}\left(p_{r}^{\frac{\gamma-1}{\gamma}}-1\right)}{T_{01}\left(p_{r}^{\frac{n-1}{n}}-1\right)} ; \quad \eta_{s}=\frac{\left(p_{r}^{\frac{\gamma-1}{\gamma}}-1\right)}{\left(p_{r}^{\frac{\gamma-1}{\eta_{p} \gamma}}-1\right)} \\
& \eta_{s}=\frac{\left(3.5^{0.286}-1\right)}{\left(3.5^{0.286}-1\right)} ; \quad \eta_{s}=\frac{0.431}{0.447} ; \quad \eta_{s}=0.9642
\end{aligned}
$$

7. Air flows through an air turbine where its stagnation pressure is reduced in the ratio 5:1, the total to total efficiency is $80 \%$. The air flow rate is $5 \mathrm{~kg} / \mathrm{s}$ If the total power output is 500 kW , find i) inlet total temperature ii) actual exit temperature iii) actual exit static temperature if the flow velocity is $100 \mathrm{~m} / \mathrm{s}$ iv) total to static efficiency (2b. 10 June/July 16) (2c. 10 Dec17/Jan 18)
$p_{r 0}=\frac{p_{1}}{p_{k+1}}=5 ; \eta_{t t}=80 \% ; \mathrm{m}=5 \mathrm{~kg} / \mathrm{s} ; \mathrm{P}=500 \mathrm{~kW} ; T_{01}=? ; T_{02}=? ; T_{2}=?$

## i) inlet total temperature

$P=m\left(h_{01}-h_{02}\right) ; \quad 500=5\left(\dot{h}_{01}-h_{02}\right) ; \quad\left(h_{01} \dot{-} h_{02}\right)=100 \mathrm{~kJ} / \mathrm{kg}$
$C_{p}\left(T_{01}-T_{02}\right)=100 ; \quad 1.005\left(T_{01}-T_{02}\right)=100 ;\left(T_{01}-T_{02}\right)=99.52 \mathrm{~K}$
$\eta_{\mathrm{tt}}=\frac{T_{01}-T_{02}}{T_{01}\left(1-\left(p_{r 0}\right)^{-\frac{\gamma-1}{\gamma}}\right)} ; \quad 0.8=\frac{99.52}{T_{01}\left(1-(5)^{-0.286}\right)} ; \quad T_{01}=337.12 \mathrm{~K}$

## ii) Actual exit temperature

$\left(T_{01}-T_{02}\right)=99.52 K ; \quad\left(337.12-T_{02}\right)=99.52 K ; T_{02}=237.6 \mathrm{~K}$

## iii) Actual exit static temperature

$T_{02}=T_{2}+\frac{V_{2}^{2}}{2 C_{p}} ; \quad 237.6=T_{2}+\frac{100^{2}}{2 \times 1005} ; \quad T_{2}=232.62 K$

## v) Total to static efficiency

$\eta_{t-s}=\frac{h_{01}-h_{02}}{h_{01}-h_{2 s}}$
$\frac{T_{01}}{T_{02 s}}=\left(\frac{p_{01}}{p_{02}}\right)^{\frac{\gamma-1}{\gamma}} ; \quad \frac{337.2}{T_{02 s}}=(5)^{0.286} ; \quad T_{02 s}=212.80 \mathrm{~K}$
$T_{02 s}=T_{2 s}+\frac{V_{2}^{2}}{2 C_{p}} ; \quad 212.8=T_{2 s}+\frac{100^{2}}{2 \times 1005}$
$T_{2 s}=207.82 \mathrm{~K}$
$\eta_{t-s}=\frac{T_{01}-T_{02}}{T_{01}-T_{2 s}} ; \quad \eta_{t-s}=\frac{99.52}{337.12-207.82} ; \quad \eta_{t-s}=0.769$
8. A gas turbine has 2 stages and develops 20MW power. The inlet temperature is 1450 K . The overall pressure ratio is 7.5 . Assume that pressure ratio of each stage is same and the expansion isentropic efficiency is 0.88 . Claculate i) Pressure ratio at each stage i) Pressure ratio at each stage ii) Polytropic Efficiency iii) Mass flow rate iv) Stage efficnecy and power of each stage (2b. 10 Dec/Jan 12)
9. The output of three stage gas turbine is 30 MW at the shaft coupling at an entry temperature of 1500 K . The overall pressure ratio across the turbine is 11.0 and efficiency is $88 \%$. If the pressure ratio of each stage is the same. Determine i) Pressure ratio of each stage ii) Polytropic effiency iii) The mass flow rate iv) The efficiency and power of each stage. Assume $\gamma_{\text {air }}=$ $1.4, C_{p}=1.005 \mathrm{~kJ} / \mathrm{kgK}, \eta_{\text {mech }}=91 \%$ (2b. $\left.10 \mathrm{Dec} / \mathrm{Jan} 19\right)$
$\mathrm{P}=30 \mathrm{MW}=30000 \mathrm{~kW} ; T_{01}=1500 K p_{r 0}=11 ; \eta_{0}=88 \% ; p_{r}=? ; \eta_{p}=? ; \dot{m}=? \eta_{s}=$ ?
i) Pressure ratio in each stage

$$
p_{r 0}=\left(p_{r}\right)^{K} ; 11=\left(p_{r}\right)^{3} ; p_{r}=2.22
$$

ii) Polytropic effieciency

$$
\begin{aligned}
& \eta_{0}=\frac{1-\left(p_{r 0}\right)^{-\eta_{p}\left(\frac{\gamma-1}{\gamma}\right)}}{1-\left(p_{r 0}\right)^{-\left(\frac{\gamma-1}{\gamma}\right)}} ; \\
& 0.88=\frac{1-(11)^{-\eta_{p}(0.286)}}{1-(11)^{-(0.286)}} ; 0.436=1-(11)^{-\eta_{p}(0.286)} ;(11)^{-\eta_{p}(0.286)}=0.564 \\
& -\eta_{p}(0.286) \ln 11=\ln 0.564 ; \quad-\eta_{p} * 0.686=-0.5727 ; \quad \eta_{p}=0.8348
\end{aligned}
$$

$$
\text { Polytropic effeiciency }=83.48 \%
$$

## iii) Total mass flow rate

$$
\begin{aligned}
& P=\frac{P_{S}}{\eta_{\text {mech }}} ; P=\frac{30000}{0.91} ; P=32967 \mathrm{~kW} \\
& \eta_{0}=\frac{T_{01}-T_{04}}{T_{01}-T_{04 s}} ; \quad \eta_{0}=\frac{T_{01}-T_{04}}{T_{01}\left(1-\frac{T_{04 s}}{T_{01}}\right)} ; \quad ; \quad \eta_{0}=\frac{T_{01}-T_{04}}{T_{01}\left(1-\left(\frac{p_{4}}{p_{1}}\right)^{\frac{\gamma-1}{\gamma}}\right)^{\prime}} ; \\
& \eta_{0}=\frac{T_{01}-T_{04}}{T_{01}\left(1-\left(p_{r o}\right)^{-\left(\frac{\gamma-1}{\gamma}\right)}\right)} ; \quad 0.88=\frac{T_{01}-T_{04}}{1500\left(1-(11)^{-0.286}\right)^{2}} ; T_{01}-T_{04}=655.13 \mathrm{~K}
\end{aligned}
$$

$$
P=\dot{m} C_{P}\left(T_{4}-T_{1}\right) ; 32967=\dot{m} * 1.005 * 655.13 ; \quad \dot{m}=50.07 \mathrm{~kg} / \mathrm{s}
$$

## iv) The efficiency and power of each stage

$$
\eta_{s t}=\frac{1-\left(p_{r}\right)^{-\eta_{P}\left(\frac{\gamma-1}{\gamma}\right)}}{1-\left(p_{r}\right)^{-\left(\frac{\gamma-1}{\gamma}\right)}} \text { where } p_{r}=\frac{p_{1}}{p_{2}}
$$

$$
\begin{aligned}
& \eta_{s t}=\frac{1-2.33^{-(0.8348 * 0.286)}}{1-2.33^{-0.286}} \\
& \eta_{s t}=\frac{0.1828}{0.2148} ; \quad \eta_{s t}=0.851 \\
& \left.\eta_{s t}=\frac{W_{a}}{C_{p}\left(T_{1}-T_{2 s}\right)} ; \quad \eta_{s t}=\frac{W_{a}}{C_{p} T_{1}\left(1-\frac{T_{2 s}}{T_{1}}\right)} ; \quad \eta_{s t}=\frac{W_{a}}{C_{p} T_{1}\left(1-p_{r}-\left(\frac{\gamma-1}{\gamma}\right)\right.}\right) \\
& 0.851=\frac{W_{a}}{1.005 * 1500\left(1-2.33^{-0.286}\right)} ; \\
& W_{a}=275.67 \mathrm{~kJ} / \mathrm{kg} \\
& P_{s}=\dot{m} W_{s a} ; P_{s}=50.07 * 275.66 ; P_{s}=13802.79 \mathrm{~kW}
\end{aligned}
$$

10. A multi stage axial flow compressor, the air is taken at 1 bar and $15^{\circ} \mathrm{C}$ and compressed to a pressure of 6.4 bar . The final true temperature is $300^{\circ} \mathrm{C}$ due to the compression process. Determine the overall compression efficiency and also the polytropic efficiency. Determine the number of stages required if the true temperature rise is limited to $13^{\circ} \mathrm{K}$ for each stage. Assume polytropic efficiency is equal to stage efficiency. (2c. $10 \mathrm{Dec} / \mathrm{Jan}$ 15)
$p_{1}=1 \mathrm{bar}=100 \mathrm{kPa} ; T_{1}=15^{\circ} \mathrm{C}=288 \mathrm{~K} ; p_{k+1}=6.4 \mathrm{bar}=640 \mathrm{kPa}$
$T_{k+1}=300^{\circ} \mathrm{C}=573 \mathrm{~K}$
$\frac{T_{k+1 s}}{T_{1}}=\left(\frac{p_{k+1}}{p_{1}}\right)^{\frac{\gamma-1}{\gamma}} ; \frac{T_{k+1 s}}{288}=\left(\frac{6.4}{1}\right)^{0.286} ; T_{k+1 s}=489.73 \mathrm{~K}$
$\eta_{0}=\frac{T_{k+1 s}-T_{01}}{T_{k+1}-T_{01}} ; \eta_{0}=\frac{489.73-288}{573-288} ; \quad \eta_{0}=0.7078$

$\eta_{P}=0.7717$
11. Air enters a compressor at a static pressure of 1.5 bar, a static temperature of $15^{\circ} \mathrm{C}$ and a flow velocity of $50 \mathrm{~m} / \mathrm{s}$, At the exit the static pressure is 3 bar , the static temperature is $100^{\circ} \mathrm{C}$ and the flow velocity is $100 \mathrm{~m} / \mathrm{s}$. The outlet is 1 m above the inlet Evaluate i) the isentropic change in enthalpy ii) The actual change in enthalpy iii) Efficiency of the compressor (2c. 10 June/July 17) (2b. O8 June/July 18, 15ME53)
12. A 16 stage axial flow compressor is to have a pressure ratio of 6.3 with a stage efficiency of $89.5 \%$ can be obtained. The intake conditions are $15^{\circ} \mathrm{C}$ and 1 bar pressure Determine i) Expected Overall efficiency ii) Polytropic efficiency Take $\gamma=\frac{C_{p}}{C_{v}}=1.4 \quad$ (2c. 08 June/July 18)
13. A 9 stage centrifugal compressor has overall stage pressure ratio 2.82 . Air enters the compressor at 1 bar and $15^{\circ} \mathrm{C}$. The efficiency of the compressor is $88 \%$. Determine the following : i) Pressure ratio of each stage ii) Polytropic efficiency iii) Preheat factor (2b. 10 Dec/Jan 16

## ENERGY TRANSFER IN TURBOMACHINES

1. With neat sketch derive an expression for Eulers turbine equation (3a. 10 June/July 17)
2. Derive an alternate form of Euler's turbine equation and explain the significance of each energy equations (3a. 10, June/July14)( 3a,10, Dec17/Jan18) ( 3a,10, Dec18/Jan19,08scheme)
3. Show that the alternate form of Eulers Turbine equation can be expressed as

$$
W=\frac{\left(V_{1}^{2}-V_{2}^{2}\right)+\left(U_{1}^{2}-U_{2}^{2}\right)-\left(V_{r 1}^{2}-V_{r 2}^{2}\right)}{2} \text { (3a. } 10 \text { June/July 13) }
$$

Draw the velocity triangles
4. Define degree of reaction ( R ) . Derive an expression relating utilization factor with degree of reaction (2b. 10, Dec16/Jan 17)
5. Define utilization factor for a turbine. Derive an expression relating utilization factor with degree of reaction for an axial flow turbine (3a. 10, Dec14/Jan 15) (3a. 10, June/July18) (3a. 08, June/July18, 15 scheme)
6. Why the discharge blade angles has considerable effect in the analysis of turbomachine. Give reasons (3a,04, Dec18/Jan 19,10scheme)
7. Draw the velocity triangles at inlet and outlet of an axial flow turbine when i) $R$ is $-v e$,ii) $R=0$, iii) $\mathrm{R}=0.5$ iv) $\mathrm{R}=1$ v) $R>1$. Discuss the energy in each case (3b,10, Dec18/Jan 19,10scheme)
8. Explain why turbine with reaction $R>1$ and $R<0$ are not in practical use (4a, 4, June/July18)

## Energy Transfer in Turbo machines

Rotor Speed- tangential speed -peripheral speed of the shaft $-U=\frac{\pi D N}{60}$
In velocity triangle is always horizontal


Velocity of fluid (steam, water, air,jet)----- Absolute velocity of fluid----- $V$
Fluid Angle at inlet , nozzle exit angle (Impulse turbine), exit angle of guide (fixed) blade $\alpha_{1}$ with the direction of $U$


[^0]1) along tangential direction and is called as tangential component velocity of fluid $\mathrm{V}_{\mathrm{u} 1}$ (whirl velocity $\mathrm{V}_{\mathrm{w} 1}$ ) ---- along horizontal direction (along U ) ie the image of $\mathrm{V}_{1}$ along the direction of $U$

$$
V_{u} \text { or } V_{w}
$$

2) Along axial direction in axial turbomachine $\mathrm{V}_{\mathrm{ax1}}$ (called as axial component), along radial direction in radial flow turbomachine $\mathrm{V}_{\text {rd1 }}$ (called as radial component). Axial and radial direction represented in velocity triangle in $Y$ direction

$$
V_{\mathrm{ax} 1} \text { or } V_{\mathrm{rd} 1} \text { or } V_{m 1} \text { or } V_{f 1}
$$

Axial component in axial flow turbomachine and radial component in radial flow turbine is called as velocity of flow

Symbol used in y direction is $\mathbf{V a x}_{\mathrm{ax}}$ or $\mathbf{V}_{\mathrm{rd} 1}$ or $\mathrm{V}_{\mathrm{m} 1}$ or $\mathbf{V}_{\mathrm{f} 1}$
In drawing velocity triangle $\mathrm{U}_{1}$ and $\mathrm{V}_{1}$ should lead from common point

$\mathrm{U}_{1}$

Vector difference between absolute velocity of the fluid and tangential speed of rotor is called as relative velocity and in velocity diagram this is the line connecting tip of U and V as given below and arrow opposes V and $\mathrm{V}_{\mathrm{r}}$ follows U


Above triangle is the general velocity triangle at inlet of the turbine
Direction of $\mathrm{V}_{\mathrm{r}}$ is the moving vane angle ( vane (blade)angle, runner vane (blade) angle, moving vane (blade) angle) and it is denoted by $\beta$

Hence $\alpha$ is always associated with V and $\beta$ is always associated with $V_{r}$

$$
V_{u 1}=V_{1} \cos \alpha_{1} ; \quad V_{m 1} \text { or } V_{f 1}=V_{1} \sin \alpha_{1} ; \quad \tan \beta_{1}=\frac{V_{m 1}}{V_{u 1}-U_{1}} ; \quad V_{r 1}=V_{m 1} \sin \beta_{1}
$$

General outlet triangle as given below

$U_{2}$ and $V_{2}$ are emerging from single point and line joining tip of $V_{2}$ and $U_{2}$ is relative velocity at outlet

$\overleftarrow{V_{u 2}}=V_{r 2} \cos \beta_{2}-U_{2} ; \quad V_{m 2}$ or $V_{f 2}=V_{r 2} \sin \beta_{2}$
Note down the difference between inlet velocity triangle for turbine (general) :

1) Direction of $V_{1}$ is towards right in the inlet velocity triangle where as Direction of $V_{2}$ in the outlet velocity triangle is towards right
2) Direction of $V_{1}$ is towards right in the inlet velocity triangle where as Direction of $V_{2}$ in the outlet velocity triangle is towards right

Inlet triangle for given condition:
If the vane angle at inlet is Axial/radial ie $\beta_{1}=90^{\circ}$


$$
\overrightarrow{V_{u 1}}=U_{1} ; \quad V_{r 1}=V_{m 1} ; \quad \tan \alpha_{1}=\frac{V_{m 1}}{u_{1}}
$$

## If $\mathrm{U}_{1}$ is greater than $\mathrm{V}_{\mathrm{u} 1}$



## Outlet velocity triangle for turbine

If fluid exit is Axial/Radial or utilization factor is maximum $\alpha_{2}=90$ (whirl velocity at outlet or tangential component at outlet $=0$ )

$\overrightarrow{V_{u 2}}=0$;
$V_{2}=V_{m 2} ;$
$\tan \beta_{2}=\frac{v_{m 2}}{U_{2}}$

## If blade angle at outlet $=90^{\circ}$ ie $\boldsymbol{\beta}_{2}=90^{0+}$



If $U_{2}$ is greater than $\overrightarrow{V_{u 2}}$ or tangential component of absolute velocity (Whirl velocity) at outlet is in the opposite direction of tangential component at inlet


General velocity triangle for power absorbing turbomachine:

Direction of $\overrightarrow{V_{u 1}}$ and $\overrightarrow{V_{u 2}}$ are in the same direction
$U_{1}$ is greater than $\overrightarrow{V_{u 1}}$
$U_{2}$ is greater than $\overrightarrow{V_{u 2}}$

Outlet velocity triangle:


Here $\overrightarrow{V_{u 2}}$ is greater than $\overrightarrow{V_{u 1}}$

## Eulers turbine equation:

Force $=$ Rate change of momentum $=$ mass $(\mathrm{kg} / \mathrm{s}) \mathrm{x}$ change in velocity
Force along tangential direction $=$ mass $(\mathrm{kg} / \mathrm{s}) \times$ change in velocity along tangential direction
$F_{u}=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right)$ (tangential thrust (force)
Force along a axial/radial direction= mass $(\mathrm{kg} / \mathrm{s}) \mathrm{x}$ change in velocity along axial/radial direction (Axial/radial thrust)
$F_{a}=\frac{\dot{m}}{g_{c}}\left(V_{m 1}-V_{m 2}\right)$
Torque $=$ force $*$ radius
Torque along tangential direction $=T=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}} r_{1}-\overrightarrow{V_{u 2}} r_{2}\right)$
Power $=$ Torque $*$ angular velocity
$E=T * \omega$
$E=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}} r_{1}-\overrightarrow{V_{u 2}} r_{2}\right) \omega ; E=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}} r_{1} \omega-\overrightarrow{V_{u 2}} r_{2} \omega\right) ; E=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}} r_{1} \frac{2 \pi N}{60}-\overrightarrow{V_{u 2}} r_{2} \frac{2 \pi N}{60}\right)$
$E=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}} \frac{\pi D_{1} N}{60}-\overrightarrow{V_{u 2}} \frac{\pi D_{2} N}{60}\right) ; E=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right)$
$\frac{E}{\dot{m}}=\frac{\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}}{g_{c}}---$ called as Eulers turbine equation
$\frac{E}{\dot{m}}$ is also equal to change in stagnation enthalpy $\left(\Delta h_{o}\right)=C_{p}\left(T_{01}-T_{02}\right)=C_{p} \Delta T_{\text {o }}$
$\frac{E}{\dot{m}}=\frac{\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}}{g_{c}}$
If $V_{u 1}$ and $V_{u 2}$ are in the opposite direction ie
Hence $\frac{E}{\dot{m}}=\frac{1}{g_{c}}\left(\overrightarrow{V_{u 1}} U_{1}+\overleftarrow{V_{u 2}} U_{2}\right)$

## Inlet Velocity triangle



Outlet velocity triangle:


Inlet and outlet velocity triangle if $\mathrm{V}_{\mathrm{u} 1}$ and $\mathrm{V}_{\mathrm{u} 2}$ are in the opposite direction Inlet Velocity triangle


[^1]Outlet velocity triangle

$\frac{E}{\dot{m}}=\frac{\left(\overline{{V_{11}}_{1}} U_{1}+\overline{u_{u 2}} U_{2}\right)}{g_{c}}$
In axial flow turbo machines $U_{1}=U_{2}=U$ since $D_{1}=D_{2}$
And generally (unless stated) $V_{m 1}=V_{m 2}=V_{m}$ (ie flow velocity is constant)
In radial flow turbomachine $U_{1} \neq\left(\right.$ not equal) $U_{2}$ since $D_{1} \neq D_{2}$ ( centrifugal compressor, Francis turbine)

All impulse turbine are axial flow machines ie $U_{1}=U_{2}=U$
In an Impulse turbine generally (unless stated) $V_{r 1}=V_{r 2}$;
If blade friction coefficient K is given in the problem $V_{r 2}=K V_{r 1}$
In reaction turbine $V_{r 2}>V_{r 1}$ and generally $V_{m 1}=V_{m 2}$ (ie flow velocity is constant)
If blades are equiangular means $\beta_{1}=\beta_{2}$
If outlet velocity triangle is $3^{\circ}$ is less than inlet blade angle then $\beta_{2}=\beta_{1}-3$
Other Important point is

- For the power developing turbomachine ie turbine $\frac{E}{\dot{m}}$ is + ve (ie $\overrightarrow{V_{u 1}} U_{1}>\overrightarrow{V_{u 2}} U_{2}$ )
- For the power absorbing turbomachine ie pump or compressor

$$
\left.\frac{E}{\dot{m}} \text { is }- \text { ve (ie } \overrightarrow{V_{u 2}} U_{2}>\overrightarrow{V_{u 1}} U_{1}\right)
$$

## Alternative form of Eulers turbine equation:

## Inlet Velocity triangle



## Outlet Velocity triangle


$\frac{E}{\dot{m}}=\frac{\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right)}{g_{c}}$ $\qquad$

From Inlet Velocity triangle
$V_{1}^{2}=V_{u 1}^{2}+V_{m 1}^{2} ; \quad V_{m 1}^{2}=V_{1}^{2}-V_{u 1}^{2}$ 1
$V_{r 1}^{2}=\left(U_{1}-V_{u 1}\right)^{2}+V_{m 1}^{2} ; \quad V_{m 1}^{2}=V_{r 1}^{2}-\left(U_{1}-V_{u 1}\right)^{2} ; \quad V_{m 1}^{2}=V_{r 1}^{2}-\left(U_{1}^{2}+V_{u 1}^{2}-2 U_{1} V_{u 1}\right)$
eqn-2
Eqn 1 =Eqn2; $\quad V_{1}^{2}-V_{u 1}^{2}=V_{r 1}^{2}-\left(U_{1}^{2}+V_{u 1}^{2}-2 U_{1} V_{u 1}\right) ; \quad V_{1}^{2}=V_{r 1}^{2}-\left(U_{1}^{2}-2 U_{1} V_{u 1}\right)$
$2 U_{1} \overrightarrow{V_{u 1}}=V_{1}^{2}+U_{1}^{2}-V_{r 1}^{2} ; \quad U_{1} V_{u 1}=\frac{V_{1}^{2}+U_{1}^{2}-V_{r 1}^{2}}{2}$
Similarly from outlet velcocity triangle
$U_{2} \overrightarrow{V_{u 2}}=\frac{V_{2}^{2}+U_{2}^{2}-V_{r 2}^{2}}{2}$
----------------4 --4

Substituting 3 and 4 in equation $A$
$\frac{E}{\dot{m}}=\frac{V_{1}^{2}+U_{1}^{2}-V_{r 1}^{2}}{2 g_{c}}-\frac{V_{2}^{2}+U_{2}^{2}-V_{r 2}^{2}}{2 g_{c}}$
$\frac{E}{\dot{m}}=\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}$
${ }^{\text {st }}$ term is the change in KE of the fluid due to change in absolute velocity of the fluid $2^{\text {nd }}$ term is the change in KE of the fluid due to change in tangential speed of the rotor $3^{\text {nd }}$ term is the change in KE of the fluid due to change in relative velocity of the rotor Hence
$\frac{E}{\dot{m}}=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right)=\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}=\mathrm{C}_{\mathrm{p}} \Delta \mathrm{T}_{\mathrm{o}}$

- Tangential force $=F_{u}=\frac{\dot{\boldsymbol{m}}}{g_{c}}\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right)$ Newton
- Torque $=\mathrm{T}=\frac{\dot{\boldsymbol{m}}}{g_{c}}\left(\overrightarrow{V_{u 1}} \mathrm{r}_{1}-\overrightarrow{V_{u 2}} \mathrm{r}_{2}\right)$ Newton meter
- Power $E=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}} \mathrm{U}_{1}-\overrightarrow{V_{u 2}} \mathrm{U}_{2}\right)$ Watts Power $E=\frac{\dot{\boldsymbol{m}}}{\boldsymbol{g}_{\boldsymbol{c}}}\left(\overrightarrow{\boldsymbol{V}_{u 1}} \boldsymbol{U}_{1}+\overleftarrow{\boldsymbol{V}_{u 2}} \boldsymbol{U}_{2}\right)$ watts
- Force along a axial/radial direction= mass $(\mathrm{kg} / \mathrm{s}) \times$ change in velocity along axial/radial direction (Axial/radial thrust)

$$
\mathrm{F}_{\mathrm{a}}=\frac{\dot{m}}{g_{c}}\left(V_{m 1}-V_{m 2}\right) \text { Newton }
$$

Degree of Reaction: It is defined as the ratio of static enthalpy drop of the fluid to stagnation enthalpy drop of fluid when it passes through the rotor of the turbomachine

Degree of Reaction $=\frac{\text { static enthalpy drop of the fluid }}{\text { stagnation enthalpy drop of fluid }}$
$R=\frac{h_{1}-h_{2}}{h_{01}-h_{02}} \cdots---\mathrm{A}$

$$
h_{01}-h_{02}=\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}
$$

$$
\left(h_{01}-\frac{V_{1}^{2}}{2 g_{c}}\right)-\left(h_{02}-\frac{V_{2}^{2}}{2 g_{c}}\right)=\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}
$$

But $\quad h_{1}=\left(h_{01}-\frac{V_{1}^{2}}{2}\right) ; h_{2}=\left(h_{02}-\frac{V_{2}^{2}}{2 g_{c}}\right)$

Hence, $\quad h_{1}-h_{2}=\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}$
Substituting, $\quad h_{1}-h_{2}$ and $h_{01}-h_{02}$
$R=\frac{\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}}{\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}}$
$R=\frac{\left(\boldsymbol{U}_{\mathbf{1}}^{2}-\boldsymbol{U}_{\mathbf{2}}^{2}\right)+\left(\boldsymbol{V}_{\boldsymbol{r} \mathbf{1}}^{2}-\boldsymbol{V}_{\boldsymbol{r} 2}^{2}\right)}{\left(\boldsymbol{V}_{\mathbf{1}}^{2}-\boldsymbol{V}_{\mathbf{2}}^{2}\right)+\left(\boldsymbol{U}_{\mathbf{1}}^{2}-\boldsymbol{U}_{\mathbf{2}}^{2}\right)+\left(\boldsymbol{V}_{\boldsymbol{r} \mathbf{1}}^{2}-\boldsymbol{V}_{\boldsymbol{r} 2}^{2}\right)}$
Another form of Degree of Reaction
$R=\frac{\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}-\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}}{\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}}$
$R=\frac{\frac{E}{\dot{m}}-\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}}{\frac{E}{\dot{m}}} ; \quad \quad R=1-\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c} \frac{E}{\dot{m}}}$
Hence Degree of Reaction can be written in two forms

1. $R=\frac{\left(\boldsymbol{U}_{\mathbf{1}}^{2}-\boldsymbol{U}_{\mathbf{2}}^{2}\right)+\left(\boldsymbol{V}_{\boldsymbol{r} 1}^{2}-V_{\boldsymbol{r} 2}^{2}\right)}{\left(\boldsymbol{V}_{\mathbf{1}}^{2}-\boldsymbol{V}_{\mathbf{2}}^{2}\right)+\left(\boldsymbol{U}_{\mathbf{1}}^{2}-\boldsymbol{U}_{\mathbf{2}}^{2}\right)+\left(\boldsymbol{V}_{\boldsymbol{r}}^{2}-\boldsymbol{V}_{\boldsymbol{r} 2}^{2}\right)}$
2. $R=1-\frac{\boldsymbol{V}_{\mathbf{1}}^{\mathbf{2}}-\boldsymbol{V}_{\mathbf{2}}^{\mathbf{2}}}{\mathbf{2} g_{c} \frac{E}{\underline{\boldsymbol{m}}}}$

Utilization factor: is defined as the ratio of ideal work done by the turbomachine to the energy supplied at the inlet of turbine


$$
\text { Output }=\frac{E}{\dot{m}}=\quad \frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}
$$

Input = Output + exit fluid KE
Input $=\frac{E}{\dot{m}}+\frac{V_{2}^{2}}{2 g_{c}}$
Hence utilization factor, $\epsilon=\frac{\frac{E}{\dot{m}}}{\frac{E}{\dot{m}}+\frac{V_{2}^{2}}{2 g_{C}}}$
$\epsilon=\frac{\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}}{\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}+\frac{V_{2}^{2}}{2 g_{c}}}$
Hence, $\epsilon=\frac{\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}}{\frac{V_{1}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}}$
After simplifying ,

$$
\epsilon=\frac{\left(V_{1}^{2}-V_{2}^{2}\right)+\left(U_{1}^{2}-U_{2}^{2}\right)+\left(V_{r 1}^{2}-V_{r 2}^{2}\right)}{V_{1^{+}}^{2}\left(U_{1}^{2}-U_{2}^{2}\right)+\left(V_{r 1}^{2}-V_{r 2}^{2}\right)}
$$

Establish the relation between utilization factor and degree of reaction (or prove that $\epsilon=\frac{V_{1}^{2}-V_{2}^{2}}{V_{1}^{2}-R V_{2}^{2}}$

$$
\begin{aligned}
& \mathrm{R}=\frac{\left(U_{1}^{2}-U_{2}^{2}\right)+\left(V_{r 1}^{2}-V_{r 2}^{2}\right)}{\left(V_{1}^{2}-V_{2}^{2}\right)+\left(U_{1}^{2}-U_{2}^{2}\right)+\left(V_{r 1}^{2}-V_{r 2}^{2}\right)} \\
& \mathrm{R}\left[\left(V_{1}^{2}-V_{2}^{2}\right)+\left(U_{1}^{2}-U_{2}^{2}\right)+\left(V_{r 1}^{2}-V_{r 2}^{2}\right)\right]=\left(U_{1}^{2}-U_{2}^{2}\right)+\left(V_{r 1}^{2}-V_{r 2}^{2}\right) \\
& \mathrm{R}\left(V_{1}^{2}-V_{2}^{2}\right)+\mathrm{R}\left[\left(U_{1}^{2}-U_{2}^{2}\right)+\left(V_{r 1}^{2}-V_{r 2}^{2}\right)\right]=\left(U_{1}^{2}-U_{2}^{2}\right)+\left(V_{r 1}^{2}-V_{r 2}^{2}\right) \\
& \mathrm{R}\left(V_{1}^{2}-V_{2}^{2}\right)=\left[\left(U_{1}^{2}-U_{2}^{2}\right)+\left(V_{r 1}^{2}-V_{r 2}^{2}\right)\right](1-R) \\
& \left(U_{1}^{2}-U_{2}^{2}\right)+\left(V_{r 1}^{2}-V_{r 2}^{2}\right)=\frac{R}{1-R}\left(V_{1}^{2}-V_{2}^{2}\right)-\cdots--------1
\end{aligned}
$$

$\epsilon=\frac{\left(V_{1}^{2}-V_{\mathbf{2}}^{2}\right)+\left(U_{1}^{2}-U_{\mathbf{2}}^{2}\right)+\left(\boldsymbol{V}_{r \mathbf{1}}^{2}-V_{r 2}^{2}\right)}{\boldsymbol{V}_{1^{+}}^{2}\left(\boldsymbol{U}_{1}^{2}-\boldsymbol{U}_{\mathbf{2}}^{2}\right)+\left(V_{r 1}^{2}-V_{r 2}^{2}\right)}$
substituting 1 in above equation
$\epsilon=\frac{\left(V_{1}^{2}-V_{2}^{2}\right)+\frac{R}{1-R}\left(V_{1}^{2}-V_{2}^{2}\right)}{V_{1}^{2}+\frac{R}{1-R}\left(V_{1}^{2}-V_{2}^{2}\right)}$
$\epsilon=\frac{\frac{(1-R)\left(V_{1}^{2}-V_{2}^{2}\right)+R\left(V_{1}^{2}-V_{2}^{2}\right)}{(1-R)}}{\frac{(1-R)\left(V_{\mathbf{1}}^{2}\right)+R\left(V_{\mathbf{1}}^{2}-V_{\mathbf{2}}^{2}\right)}{(1-R)}}$
after simplification
$\epsilon=\frac{V_{1}^{2}-V_{2}^{2}}{V_{1}^{2}-R V_{2}^{2}} \quad$ Hence proved

For Maximum utilization,
From the expression $\epsilon=\frac{\boldsymbol{V}_{\mathbf{1}}^{2}-\boldsymbol{V}_{\mathbf{2}}^{2}}{\boldsymbol{V}_{\mathbf{1}}^{2}-\boldsymbol{R} \boldsymbol{V}_{\mathbf{2}}^{2}}$ it can be understand $\mathrm{V}_{2}$ is to be minimum
For $\mathrm{V}_{2}$ to be minimum, $\mathrm{V}_{2}$ to be in the axial / radial direction ie $\alpha_{2}=90^{\circ}$ and $\mathrm{V}_{\mathrm{u} 2}=0$

1. Air enters in an axial flow turbine with a tangential component of the absolute velocity $600 \mathrm{~m} / \mathrm{s}$ in the direction of rotation. At the rotor exit, the tangential component of the absolute velocity is $100 \mathrm{~m} / \mathrm{s}$ in a direction opposite to that of rotational speed. The tangential blade speed is $250 \mathrm{~m} / \mathrm{s}$. Evaluate (i) The change in total enthalpy of air between the inlet and outlet of the rotor (ii) The power in kW if the mass flow rate is $10 \mathrm{~kg} / \mathrm{s}$ (iii) The change in total temperature across the rotor.(4c, 8, June/July18)

- Axial flow turbine ie $U_{1}=U_{2}=U$
- Air enters in an axial flow turbine tangential component of the absolute velocity $600 \mathrm{~m} / \mathrm{s}$ in the direction of rotation
$\overrightarrow{V_{u 1}}=600 \mathrm{~m} / \mathrm{s}$ in the direction to that of rotational speed
At the rotor exit, the tangential component of the absolute velocity is $100 \mathrm{~m} / \mathrm{s}$ in a direction opposite to that of rotational speed.
$\overleftarrow{V_{u 2}}=100 \mathrm{~m} / \mathrm{s}$ opposite to the direction to that of rotational speed ie. Direction of $u$ and $\mathrm{V}_{\mathrm{u} 2}$ are opposite to each other ie $\mathrm{V}_{\mathrm{u} 2}$ direction is negative $\mathrm{V}_{\mathrm{u} 2}$
- Tangential blade speed $U=250 \mathrm{~m} / \mathrm{s}$


## To determine

$$
\text { i) } \Delta h_{o}=\text { ? ii) } P=\text { ? if } m=10 \mathrm{~kg} / \mathrm{s} \mathrm{iii)} \Delta \mathrm{~T}_{\mathrm{o}}=\text { ? }
$$

$$
\frac{E}{\dot{m}}=\frac{1}{g_{c}}\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right) ; \quad \frac{E}{\dot{m}}=\frac{1}{g_{c}}\left(\overrightarrow{V_{u 1}}+\overleftrightarrow{V_{u 2}}\right) U \text { as } U_{1}=U_{2}=U
$$

$$
\frac{E}{\dot{m}}=(600+100) 250=175000 \mathrm{~J} / \mathrm{kg} \quad(175 \mathrm{~kJ} / \mathrm{kg})
$$

i) $\Delta h_{0}=\frac{E}{\dot{m}}=175 \mathrm{~kJ} / \mathrm{kg}$
ii) $\quad E=\dot{m} \frac{E}{\dot{m}}=10 \times 175=1750 \mathrm{~kW}\left(\mathrm{~kW}\right.$ since $\frac{E}{\dot{m}}$ is in $\left.\mathrm{kJ} / \mathrm{kg}\right)$
iii) $\Delta h_{0}=C_{p}\left(\Delta T_{0}\right)$

$$
175=1.005 \Delta T_{0} \quad \text { as } C_{p} \text { for air is } 1.005 \mathrm{~kJ} / \mathrm{kg}
$$

$$
\Delta T_{0}=174.13^{\circ} \mathrm{C}
$$

2. Air enters in an axial flow turbine with a tangential component of the absolute velocity $600 \mathrm{~m} / \mathrm{s}$ in the direction of rotation. At the rotor exit, the tangential component of the absolute velocity is $100 \mathrm{~m} / \mathrm{s}$ in a direction same to that of rotational speed. The tangential blade speed is $250 \mathrm{~m} / \mathrm{s}$. Evaluate (i) The change in total enthalpy of air between the inlet and outlet of the rotor (ii) The power in kW if the mass flow rate is $10 \mathrm{~kg} / \mathrm{s}$ (iii) The change in total temperature across the rotor
3. In a certain turbo machine the fluid enters the rotor with the absolute velocity having an axial component of $10 \mathrm{~m} / \mathrm{s}$ and a tangential component, in the direction of
the rotors motion is $16 \mathrm{~m} / \mathrm{s}$. The tangential speed of the rotor at inlet is $33 \mathrm{~m} / \mathrm{s}$. At the outlet of the rotor, the tangential speed of the rotor is $8 \mathrm{~m} / \mathrm{s}$ and absolute velocity of the fluid is $16 \mathrm{~m} / \mathrm{s}$ in axial direction. Evaluate the energy transfer between the fluid and rotor. Is this turbo machine power absorbing and power generating? What is the change in total pressure if the process is loss free and fluid is water Also calculate the blade angles

## Given Data

Axial component of absolute of velocity at inlet $V_{m 1}=10 \mathrm{~m} / \mathrm{s}$,
Tangential component at inlet, $\overrightarrow{V_{u 1}}=16 \mathrm{~m} / \mathrm{s}$,
Tangential speed of the rotor at inlet, $U_{1}=33 \mathrm{~m} / \mathrm{s}$
Tangential speed of the rotor at outlet $=U_{1}=8 \mathrm{~m} / \mathrm{s}$,
Absolute velocity of the fluid is $16 \mathrm{~m} / \mathrm{s}$ in axial direction ie $V_{2}=16 \mathrm{~m} / \mathrm{s}$ and $\alpha_{2}=90^{\circ}$ To determine
$\frac{E}{\dot{m}}=$ ?, Is the turbomachine is power absorbing or power generating? $\Delta \mathrm{p}=$ ? if fluid is water

Solution:
Note that $U_{1}=33 \mathrm{~m} / \mathrm{s}>\overrightarrow{V_{u 1}}=16 \mathrm{~m} / \mathrm{s}$
Hence

$\alpha_{2}=90^{\circ}$


$$
\overrightarrow{V_{u 2}}=0
$$

$\frac{E}{\dot{m}}=\frac{1}{g_{c}}\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right) ; \quad \frac{E}{\dot{m}}=(16 * 33-0) ; \quad \frac{E}{\dot{m}}=528 \mathrm{~J} / \mathrm{kg}$
Since $\frac{E}{\dot{m}}=$ is + ve This machine is power developing machine
ii) For compressible fluid, $\Delta h_{0}=\frac{\Delta P_{0}}{\rho}$
$528=\frac{\Delta P_{0}}{1000} ; \quad \Delta P_{0}=528000 \mathrm{~N} / \mathrm{m}^{2}\left(\Delta P_{0}\right.$ is $\mathrm{N} / \mathrm{m}^{2}$ since $\Delta h_{0}$ is in $\left.\mathrm{J} / \mathrm{kg}\right) ;$
$\Delta P_{0}=528 k P a$
iii) Blade angles

## Inlet blade angle

From Inlet velocity triangle, $\tan \beta_{1}=\frac{V_{m 1}}{U_{1}-\overline{V_{u 1}}} ; \quad \tan \beta_{1}=\frac{10}{33-16} ; \quad \beta_{1}=30.465^{\circ}$

## Outlet blade angle

From outlet velocity triangle, $\quad \tan \beta_{2}=\frac{V_{m 2}}{U_{2}} ; \tan \beta_{2}=\frac{16}{8} ; \quad \beta_{2}=63.43^{\circ}$
Inlet velocity of the fluid
$V_{1}=\sqrt{V_{u 1}^{2}+V_{m 1}^{2}} ; \quad V_{1}=\sqrt{16^{2}+10^{2}} ; \quad V_{1}=18.867 \mathrm{~m} / \mathrm{s}$

## Outlet guide blade angle $\boldsymbol{\alpha}_{1}$

$\tan _{1}=\frac{V_{m 1}}{V_{u 1}} ; \tan \alpha_{1}=\frac{10}{16} ; \alpha_{1}=32^{\circ}$

## Axial thrust

$F_{a}=\frac{\dot{m}}{g_{c}}\left(V_{m 1}-V_{m 2}\right) \quad$ Newton; $F_{a}=1(10-16) ; \quad F_{a}=-6 \mathrm{~N}$
Tangential Thrust
$F_{u}=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right)$ Newton $; F_{u}=1(16-0) N ; \quad F_{u}=16 N$
4. The following data refers to a turbo-machine. Inlet velocity of whirl $=16 \mathrm{~m} / \mathrm{s}$, velocity of flow $=10 \mathrm{~m} / \mathrm{s}$, blade speed $=33 \mathrm{~m} / \mathrm{s}$, outlet blade speed $=8 \mathrm{~m} / \mathrm{s}$ Discharge is radial with an absolute velocity of $16 \mathrm{~m} / \mathrm{s}$. If water is the working fluid flowing at the rate of $1 \mathrm{~m}^{3} / \mathrm{s}$. Calculate the following i) Power in kW ii) Change in total pressure in $\mathrm{kN} / \mathrm{m}^{2}$ iii) Degree of reaction iv) Utilization factor (3b, 08, June/July18 15 scheme)

Inlet velocity of whirl $=16 \mathrm{~m} / \mathrm{s}$, ie $\overrightarrow{V_{u 1}}=16 \mathrm{~m} / \mathrm{s}$,
velocity of flow $=10 \mathrm{~m} / \mathrm{s}, V_{m 1}=10 \mathrm{~m} / \mathrm{s}$,
blade speed $=33 \mathrm{~m} / \mathrm{s}$ at inlet, $U_{1}=33 \mathrm{~m} / \mathrm{s}$
outlet blade speed $=8 \mathrm{~m} / \mathrm{s}=U_{2}=8 \mathrm{~m} / \mathrm{s}$,
Discharge is radial with an absolute velocity of $16 \mathrm{~m} / \mathrm{s}$ ie $V_{2}=\frac{16 \mathrm{~m}}{\mathrm{~s}}$ and $\alpha_{2}=90^{\circ}$
If water is the working fluid flowing at the rate of $1 \mathrm{~m}^{3} / \mathrm{s} . Q=1 \mathrm{~m}^{3} / \mathrm{s}$
To determine
i)Power in kW ie $\mathrm{E}=$ ? li)Change in total pressure in $\mathrm{kN} / \mathrm{m}^{2} \Delta P_{0}=$ ? iii$) \mathrm{R}=$ ? Iv) $\varepsilon=$ ?

Solution:
Note that $U_{1}=33 \mathrm{~m} / \mathrm{s}>\overrightarrow{V_{u 1}}=16 \mathrm{~m} / \mathrm{s}$
Hence

$\alpha_{2}=90^{\circ}$

$\mathrm{V}_{\mathrm{u} 2}=0$

## i) Power in kW

$\frac{E}{\dot{m}}=\frac{1}{g_{c}}\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right)$;
$\frac{E}{\dot{m}}=(16 * 33-0) ; \quad \frac{E}{\dot{m}}=528 \mathrm{~J} / \mathrm{kg}$
Since $\frac{E}{\dot{m}}=$ is + ve This machine is power developing machine

$$
\dot{m}=\rho Q ; \dot{m}=1000 * 1 ; \dot{m}=1000 \mathrm{~kg} / \mathrm{s}
$$

$E=\dot{m} \frac{E}{\dot{m}^{\prime}} ; E=1000 * 528 \mathrm{~J} / \mathrm{s} ; \quad E=\frac{528000 \mathrm{~J}}{s}=528 \mathrm{~kW}$
ii) Change in total pressure in $\mathbf{k N} / \mathbf{m}^{\mathbf{2}}$

For compressible fluid, $\Delta h_{0}=\frac{\Delta P_{0}}{\rho} ; 528=\frac{\Delta P_{0}}{1000} ; \Delta P_{0}=528000 \mathrm{~N} / \mathrm{m}^{2}$;
$\left(\Delta P_{0}\right.$ is $\mathrm{N} / \mathrm{m}^{2}$ since $\Delta h_{0}$ is in $\left.\mathrm{J} / \mathrm{kg}\right) ; \Delta P_{0}=528 \mathrm{kPa}$
iii) Degree of reaction

$$
\begin{aligned}
& R=\frac{\frac{E}{\dot{m}}-\left(\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}\right)}{\frac{E}{\dot{m}}} ; \quad R=1-\frac{\left(V_{1}^{2}-V_{2}^{2}\right)}{2 g_{c} \frac{E}{\dot{m}}} \\
& V_{1}^{2}=V_{u 1}^{2}+V_{m 1}^{2} ; \quad V_{1}^{2}=16^{2}+10^{2} ; \quad V_{1}^{2}=356 ; \quad V_{2}^{2}=16^{2} ; V_{2}^{2}=256 \\
& R=1-\frac{(356-256)}{2 * 528} ; R=0.91
\end{aligned}
$$

## iV) Utilization factor

$\varepsilon=\frac{\frac{E}{\dot{m}}}{\frac{E}{\dot{m}}+\left(\frac{V_{2}^{2}}{2 g_{c}}\right)} ; \quad \quad \varepsilon=\frac{528}{528+\left(\frac{256}{2}\right)} ; \quad \varepsilon=0.804$

Determine blade angles, Axial and tangential thrust in the above problem

## v) Blade angles

## Inlet blade angle

From Inlet velocity triangle, $\tan \beta_{1}=\frac{V_{m 1}}{U_{1}-\overline{V_{u 1}}} ; \quad \tan \beta_{1}=\frac{10}{33-16} ; \quad \beta_{1}=30.465^{\circ}$

## Outlet blade angle

From outlet velocity triangle, $\quad \tan \beta_{2}=\frac{V_{m 2}}{U_{2}} ; \quad \tan \beta_{2}=\frac{16}{8} ; \quad \beta_{2}=63.43^{\circ}$

## Outlet guide blade angle $\alpha_{1}$

$$
\tan \alpha_{1}=\frac{V_{m 1}}{\overline{V_{u 1}}} ; \tan \alpha_{1}=\frac{10}{16} ; \alpha_{1}=32^{\circ}
$$

## vi)Axial thrust

$$
\begin{aligned}
& F_{a}=\frac{\dot{m}}{g_{c}}\left(V_{m 1}-V_{m 2}\right) \quad \text { Newton } \\
& F_{a}=1(10-16) ; F_{a}=-6 \mathrm{~N}
\end{aligned}
$$

## Tangential Thrust

$$
F_{U}=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) \text { Newton; } F_{U}=1(16-0) \mathrm{N} ; \quad F_{U}=16 \mathrm{~N}
$$

5. Water approaches the impeller of a mixed flow pump with an absolute velocity having tangential and axial components each of $17 \mathrm{~m} / \mathrm{s}$. At the rotor exit the radial and tangential components of the absolute velocity are $13 \mathrm{~m} / \mathrm{s}$ and $25 \mathrm{~m} / \mathrm{s}$ respectively. The tangential blade speed at inlet and exit are $12 \mathrm{~m} / \mathrm{s}$ and $47 \mathrm{~m} / \mathrm{s}$ Find
i) Change in enthalpy across the rotor
ii) Total change in pressure across the rotor
iii) Change in static pressure
iv) Degree of reaction (2b. $10 \mathrm{Dec} / \mathrm{Jan} 17)^{*}$

Water approaches the impeller of a mixed flow pump absolute velocity having tangential and axial components each of $17 \mathrm{~m} / \mathrm{s}$. ie $\overrightarrow{V_{u 1}}=17 \mathrm{~m} / \mathrm{s} ; V_{m 1}=17 \mathrm{~m} / \mathrm{s}$;
At the rotor exit the radial and tangential components of the absolute velocity are
$13 \mathrm{~m} / \mathrm{s}$ and $25 \mathrm{~m} / \mathrm{s} \overrightarrow{V_{u 2}}=25 \mathrm{~m} / \mathrm{s} ; V_{m 2}=13 \mathrm{~m} / \mathrm{s}$
The tangential blade speed at inlet and exit are $12 \mathrm{~m} / \mathrm{s}$ and $47 \mathrm{~m} / \mathrm{s}$
$U_{1}=12 \mathrm{~m} / \mathrm{s} ; U_{2}=47 \mathrm{~m} / \mathrm{s}$
i) Change in enthalpy across the rotor

$$
\frac{E}{\dot{m}}=\frac{1}{g_{c}}\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right) ; \frac{E}{\dot{m}}=(17 * 12)-(25 * 47) ; \frac{E}{\dot{m}}=-971 \mathrm{~J} / \mathrm{kg}
$$

ii) Total change in pressure across the rotor

$$
\Delta h_{0}=\frac{\Delta P_{0}}{\rho} ; 971=\frac{\Delta P_{0}}{1000^{\prime}} ; \quad \Delta P_{0}=971000 \mathrm{~N} / \mathrm{m}^{2}
$$

## iii) Change in static enthalpy

$\Delta h_{0}=h_{02}-h_{01} ; \Delta h_{0}=\left(h_{2}+\frac{V_{2}^{2}}{2 g_{c}}\right)-\left(h_{1}+\frac{V_{1}^{2}}{2 g_{c}}\right) ; \Delta h_{0}=\left(h_{2}-h_{1}\right)+\left(\frac{V_{2}^{2}-V_{1}^{2}}{2 g_{c}}\right)$
$V_{1}^{2}=V_{u 1}^{2}+V_{m 1}^{2} ; V_{1}^{2}=17^{2}+17^{2} ; V_{1}^{2}=578 ; \quad V_{2}^{2}=V_{u 2}^{2}+V_{m 2}^{2} ;$
$V_{2}^{2}=25^{2}+13^{2} ;$
$V_{2}^{2}=794$
$971=\left(h_{2}-h_{1}\right)+\left(\frac{794-578}{2}\right) ;$

$$
\left(h_{2}-h_{1}\right)=863 \mathrm{~J} / \mathrm{kg}
$$

iv) Change in static pressure
$p_{o}=p+\frac{\rho V^{2}}{2 g_{c}} ; \Delta p_{o}=p_{o 2}-p_{o 1} ; \Delta p_{o}=\left(p_{2}+\frac{\rho V_{2}^{2}}{2 g_{c}}\right)-\left(p_{1}+\frac{\rho V_{1}^{2}}{2 g_{c}}\right)$
$\Delta p_{o}=\left(p_{2}-p_{1}\right)+\frac{\rho\left(V_{2}^{2}-V_{1}^{2}\right)}{2 g_{c}} ; 971000=\left(p_{2}-p_{1}\right)+\frac{1000(794-578)}{2} ;$
Change in static pressure $\left(p_{2}-p_{1}\right)=863000 \mathrm{~N} / \mathrm{m}^{2}$

## Degree of reaction

$R=\frac{\frac{E}{\dot{m}}-\left(\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}\right)}{\frac{E}{\dot{m}}} ; \quad R=1-\frac{\left(V_{1}^{2}-V_{2}^{2}\right)}{2 g_{c} \frac{E}{\dot{m}}} ; R=1-\frac{(578-794)}{2 *(-971)} ; R=0.796$
6. In an inward flow radial hydraulic turbine for maximum utilisation factor show that , $\alpha_{1}=\cot ^{-1} \sqrt{\frac{1-R}{1-\varepsilon} \varepsilon}$ where $\alpha_{1}=$ nozzle angle, $\mathrm{R}=$ Degree of reaction, $\varepsilon$ is the utilization factor Assuming the radial velocity component is constant through out and there is no tangential component absolute velocity component at outlet (3a,10 , Dec12) (4b, 8, June/July18)

Given Data :

- Radial turbine ie $U_{1} \neq U_{1}$
- Assuming the radial velocity component is constant through out
$V_{m 1}=V_{m 2}=V_{m}$
there is no tangential component absolute velocity component at outlet

$$
\overrightarrow{V_{u 2}}=0
$$

outlet velocity triangle


## Inlet velocity triangle

$$
\begin{aligned}
& \epsilon=\frac{V_{1}^{2}-V_{2}^{2}}{V_{1}^{2}-R V_{2}^{2}} ; \\
& \sin \alpha_{1}=\frac{V_{m}}{V_{1}} ; \quad V_{1}=V_{m} \operatorname{cosec} \alpha_{1} \\
& \epsilon=\frac{V_{m}^{2} \operatorname{cosec}^{2} \alpha_{1}-V_{m}^{2}}{V_{m}^{2} \operatorname{cosec}^{2} \alpha_{1}-R V_{m}^{2}} ; \quad \epsilon=\frac{\operatorname{cosec}^{2} \alpha_{1}-1}{\operatorname{cosec}^{2} \alpha_{1}-R} \\
& \operatorname{cosec} V_{1}^{2} \alpha_{1}^{2}=1+{V_{m}^{2}}_{2}^{2} \\
& \epsilon=\frac{1+\cot ^{2} \alpha_{1}-1}{1+\cot ^{2} \alpha_{1}-R} ; \quad \epsilon=\frac{\cot ^{2} \alpha_{1}}{1-R+\cot ^{2} \alpha_{1}} \\
& \epsilon(1-R)+\epsilon \cot ^{2} \alpha_{1}=\cot ^{2} \alpha_{1} ; \epsilon(1-R)=\cot ^{2} \alpha_{1}(1-\epsilon) \\
& \epsilon(1-R) \\
& (1-\epsilon)
\end{aligned} \cot ^{2} \alpha_{1} ; \quad \alpha_{1}=\cot ^{-1} \sqrt{\frac{(1-R) \epsilon}{(1-\epsilon)}}
$$

7. In an slow speed inward flow radial hydraulic turbine, degree of reaction is $R$ and utlilization factor is $\varepsilon$. Assuming the radial velocity component is constant through out and there is no tangential component absolute velocity component at outlet, show that the inlet nozzle angle is given by $\alpha_{1}=\cot ^{-1} \sqrt{\frac{(1-R) \epsilon}{(1-\epsilon)}}$
8. Show that for an axial flow turbine under maximum utilization factor condition, the speed ratio is $\emptyset$ is given by $\frac{U}{V_{1}}=\frac{2}{3} \cos \alpha_{1}$ where $U$ is the tangential speed of the rotor and $\mathrm{V}_{1}$ is the tangential jet velocity of the fluid. Assume flow velocity is to remain constant and $\alpha_{1}$ is the Take degree of reaction $=1 / 4$, ( $\left.3 \mathrm{~b} .10 \mathrm{Dec} / \mathrm{Jan} 2016\right)^{*}$

Axial flow turbine ---- $U_{1}=U_{2}=U$

Utillization factor is maximum ie $\alpha_{2}=90^{\circ}$

## Outlet velocity triangle



Degree of reaction $=1 / 4$
Assume flow velocity is constant from inlet to outlet

$$
\text { ie } V_{m 1}=V_{m 2}
$$

Prove $\frac{U}{V_{1}}=\frac{2}{3} \cos \alpha_{1}$
Inlet Velocity triangle


Substituting 2 and 3 in 1
$R=1-\frac{V_{1}^{2}-V_{m 1}^{2}}{2 g_{c} \frac{\overrightarrow{V_{u 1}} U}{g_{c}}}$
From inlet velocity triangle $\quad V_{u 1}^{2}=V_{1}^{2}-V_{m 1}^{2}$
Hence, $R=1-\frac{V_{u 1}^{2}}{2 V_{u 1} U} ; \quad R=1-\frac{\overrightarrow{V_{u 1}}}{2 U} ; R=1-\frac{V_{1} \cos \alpha_{1}}{2 U} \quad$ as $\overrightarrow{V_{u 1}}=V_{1} \cos \alpha_{1}$
$\frac{1}{4}=1-\frac{\mathrm{V}_{1} \cos \alpha_{1}}{2 U} \quad ; \quad \frac{3}{4}=\frac{\mathrm{V}_{1} \cos \alpha_{1}}{2 U} ; \quad \frac{U}{V_{1}}=\frac{2}{3} \cos \alpha_{1}$
9. A radial outward flow turbomachine has no inlet whirl. The blade speed at the exit is twice at inlet. Radial velocity is constant throughout. Taking the inlet blade angle as $45^{\circ}$, show that the degree of reaction, $R=\frac{2+\cot \beta_{2}}{4}$ Where $\beta_{2}$ is the blade speed at exit wrt tangential direction (3a,10June/July 16, ) (4b,10June/July 17 ) (4b,10June/July 13 ) (4a. 10, Dec12)

## Given Data:

A radial outward flow turbomachine has no inlet whirl ie $\overrightarrow{V_{u 1}}=0$
Hence Inlet velocity triangle


The blade speed at the exit is twice at inlet.
$U_{2}=2 U_{1} ;$
the inlet blade angle as $45^{\circ}, \quad$ ie $\quad \beta_{1}=45^{\circ}$
The radial component of absolute velocity remains constant throughout ie $V_{m 1}=$ $V_{m 2}=V_{m}$
$R=1-\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c} \frac{E}{\dot{m}}}-\cdots-\cdots---A$
$V_{1}=V_{m 1}=V_{m} \quad---------1$
f
rom Inlet velocity triangle asType equation here. $\alpha_{1}=90^{\circ}$ )
Substituting 1,in A $R=1-\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c} \frac{E}{\ddot{m}}} ; \quad R=1-\frac{V_{m}^{2}-V_{2}^{2}}{2 g_{c} \frac{E}{\ddot{m}}}$
Outlet velocity triangle


From outlet velocity triangle $V_{2}^{2}=V_{u 2}^{2}+V_{m}^{2}$;

$$
V_{m}^{2}-V_{2}^{2}=V_{u 2}^{2}
$$

And $\frac{E}{\dot{m}}=\frac{1}{g_{c}}\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) U ; \quad \frac{E}{\dot{m}}=-\frac{1}{g_{c}} \overrightarrow{V_{u 2}} U_{2} \quad$ as as $\overrightarrow{V_{u 1}}=0$
Hence, $\quad R=1-\frac{-V_{u 2}^{2}}{2\left(-U_{2} \overrightarrow{V_{u 2}}\right)^{2}} ; \quad R=1+\frac{-\overrightarrow{V_{u 2}}}{2\left(u_{2}\right)} \cdots-\cdots-\cdots-\cdots-\cdots-\cdots-\cdots-\cdots$
From Inlet velocity triangle
$\tan \beta_{1}=\frac{V_{m 1}}{U_{1}} ; \quad \tan 45=\frac{V_{m 1}}{U_{1}} ; \quad 1=\frac{V_{m}}{U_{1}} ; \quad U_{1}=V_{m}$
$U_{2}=2 U_{1} ; \quad U_{2}=2 V_{m}---------3$
From outlet velocity triangle
$\tan \beta_{2}=\frac{V_{m 2}}{U_{2}-\overline{V_{u 2}}} ;$

$$
U_{2}-\overrightarrow{V_{u 2}}=V_{m 2} \operatorname{Cot} \beta_{2}
$$

$\overrightarrow{V_{u 2}}=U_{2}-V_{m 2} \operatorname{Cot} \beta_{2} ; \quad \overrightarrow{V_{u 2}}=2 V_{m}-V_{m} \operatorname{Cot} \beta_{2}$
Substituting 3 and 4 in 2
$R=1+\frac{-\left(2 V_{m}-V_{m} \cot \beta_{2}\right)}{2\left(2 V_{m}\right)} ; \quad R=1+\frac{-\left(2-\cot \beta_{2}\right)}{2(2)}$
$R=1+\frac{-2+\cot \beta_{2}}{4} ; \quad R=\frac{4-2+\cot \beta_{2}}{4} \quad R=\frac{2+\cot \beta_{2}}{4}$
10. An Inward radial flow reaction turbine has radial discharge at outlet The outer blade angle is $45^{\circ}$. The radial component of absolute velocity remains constant. Assuming the the tangential speed of the rotor at inlet to be twice the tangential speed of rotor at exit., determine the energy transfer per unit flow depending on mass and degree of reaction. Assume $V_{m}=\sqrt{2 g_{c}}$ if the values of degree of reaction respectively are 0 and 1 , what are the corresponding values of energy transfer per unit mass of the fluid (4b,10 Dec15/Jan16)

## Data Given

Radial flow turbine $U_{1} \neq U_{2}$, radial discharge at outlet ie $\alpha_{2}=90^{\circ}$
Outlet velocity Triangle

outlet blade angle of $45^{\circ}$.ie $\beta_{2}=45^{\circ}$
The radial component of absolute velocity remains constant throughout ie $V_{m 1}=V_{m 2}=V_{m}$
$V_{m 1}=V_{m 2}=V_{m}=\sqrt{2 g_{c}} ;$
The blade speed at inlet is twice that at outlet $\mathrm{U}_{1}=2 \mathrm{U}_{2}$
To Express $\frac{E}{m}=f(\alpha 1) \quad \mathrm{R}=f(\alpha 1)$
$\alpha_{1}=$ ? When $\mathrm{R}=0, \frac{E}{m}=$ ? for that $\alpha_{1}$
$\alpha_{1}=$ ? When $\mathrm{R}=1, \frac{E}{m}=$ ? for that $\alpha_{1}$
Inlet Velocity Triangle

$\frac{E}{\dot{m}}=\frac{\overrightarrow{V_{u 1}} U_{1}}{g_{c}}$
as $\overrightarrow{V_{u 2}}=0$ $\qquad$

Note that here $\mathrm{g}_{\mathrm{c}}$ is included in above equation since $V_{m 1}=V_{m 2}=V_{m}=\sqrt{2 g_{c}}$

## From Outlet velocity triangle

$\tan \beta_{2}=\frac{V_{m 2}}{U_{2}} ; \quad \tan 45=\frac{V_{m 2}}{U_{2}} ; \quad 1=\frac{V_{m}}{U_{2}} ; \quad U_{2}=V_{m}$
$U_{1}=2 U_{2} ; \quad U_{1}=2 V_{m}----e q n 1$
$\tan \alpha_{1}=\frac{V_{m}}{\overrightarrow{V_{u 1}}} ; \quad \overrightarrow{V_{u 1}}=V_{m} \cot \alpha_{1}-=======$ eqn 2
Substituting 1 and 2 in $A$
$\frac{E}{\dot{m}}=\frac{V_{m} \cot \alpha_{1}\left(2 V_{m}\right)}{g_{c}} \quad ; \quad \frac{E}{\dot{m}}=\frac{2 V_{m}^{2} \cot \alpha_{1}}{g_{c}} \quad ; \quad \frac{E}{\dot{m}}=\frac{2 * 2 \mathrm{~g}_{\mathrm{c}} \cot \alpha_{1}}{g_{c}} ;$
$\frac{E}{\dot{m}}=4 \cot \alpha_{1}$
$R=1-\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c} \frac{E}{\dot{m}}}$ $\qquad$

From outlet velocity triangle, $\mathrm{V}_{2}=\mathrm{V}_{\mathrm{m} 2}=\mathrm{V}_{\mathrm{m} 1}$
$R=1-\frac{V_{1}^{2}-V_{m 1}^{2}}{2 g_{c} \frac{E}{\dot{m}}} ; \quad R=1-\frac{V_{u 1}^{2}}{2 g_{c} \frac{E}{\dot{m}}} \quad ; \quad R=1-\frac{V_{u 1}^{2}}{2 U_{1} V_{u 1}} ; \quad R=1-\frac{V_{u 1}}{2 U_{1}} ;$
$R=1-\frac{V_{m} \cot \alpha 1}{2 V_{m}} ; \quad R=1-\frac{\cot \alpha_{1}}{4} ; \quad R=\frac{\mathbf{4}-\cot \alpha_{1}}{4}$
At what value of $\alpha_{1}$, will the degree of reaction be zero
$0=\frac{4-\cot \alpha_{1}}{4} ; \quad \cot \alpha_{1}=4 ;$
$\alpha_{1}=$
the corresponding values of energy transfer per unit mass

$$
\frac{E}{\dot{m}}=4 \cot \alpha_{1} ; \quad \frac{E}{\dot{m}}=4 * 4 ; \quad \frac{E}{\dot{m}}=16 \mathrm{~J} / \mathrm{kg}
$$

At what value of $\alpha_{1}$, will the degree of reaction be 1
$1=\frac{4-\cot \alpha_{1}}{4} ;$
$\tan \alpha_{1}=\frac{1}{0} \quad \tan \alpha_{1}=\infty ;$

$$
\cot \alpha_{1}=0 ;
$$

$$
\alpha_{1}=90^{\circ}
$$

the corresponding values of energy transfer per unit mass
$\frac{E}{\dot{m}}=4 \cot \alpha_{1} ; \quad \frac{E}{\dot{m}}=4 * 0 ; \quad \frac{E}{\dot{m}}=0 \mathrm{~J} / \mathrm{kg}$
11. An Inward radial flow reaction turbine has radial discharge at outlet with outlet blade angle of $45^{\circ}$. The radial component of absolute velocity remains constant throughout and equal to $\sqrt{2 g H}$ where g is the acceleration due to gravity and H is the constant head. The blade speed at inlet is twice that at outlet. Express the energy transfer per unit mass and the degree of reaction in terms of $\alpha_{1}$, where $\alpha_{1}$ is the direction of the absolute velocity at inlet with respect to the blade velocity at inlet. At what value $\alpha_{1}$ will be the degree of reaction zero and unity? What are the corresponding values of energy transfer per unit mass

Radial flow turbine $U_{1} \neq U_{2}$, radial discharge at outlet ie $\alpha_{2}=90^{\circ}$
Outlet velocityy triangle

outlet blade angle of $45^{\circ}$.ie $\beta_{2}=45^{\circ}$
The radial component of absolute velocity remains constant throughout and equal to $\sqrt{2 g H}$ ie $V_{m 1}=V_{m 2}=V_{m}=\sqrt{2 g H}$

The blade speed at inlet is twice that at outlet $\mathrm{U}_{1}=2 \mathrm{U}_{2}$

To Express $\frac{E}{m}=f\left(\alpha_{1}\right) \quad \mathrm{R}=f(\alpha 1)$
$\alpha_{1}=$ ? When $R=0, \frac{E}{m}=$ ? for that $\alpha_{1}$
$\alpha_{1}=$ ? When $R=1, \frac{E}{m}=$ ? for that $\alpha_{1}$
Inlet Velocity Triangle

$\frac{E}{\dot{m}}=\frac{1}{g_{c}} \overrightarrow{V_{u 1}} U_{1}$ as as $\overrightarrow{V_{u 2}}=0$
From Outlet velocity triangle
$\tan \beta_{2}=\frac{V_{m 2}}{U_{2}} ; \quad \tan 45=\frac{V_{m 2}}{U_{2}} ; 1=\frac{V_{m}}{U_{2}} ; \quad U_{2}=V_{m}$
$U_{1}=2 U_{2} ; \quad U_{1}=2 V_{m}------------1$
$\tan \alpha_{1}=\frac{V_{m}}{\overline{V_{u 1}}} \quad$ ie $\overrightarrow{V_{u 1}}=V_{m} \cot \alpha_{1}--------------2$
Substituting 1 and 2 in A

$$
\begin{aligned}
& \frac{E}{\dot{m}}=\frac{1}{g_{c}} V_{m} \cot \alpha_{1} * V_{m} \quad ; \quad \frac{E}{\dot{m}}=\frac{1}{g_{c}} V_{m}^{2} \cot \alpha_{1} \quad ; \frac{E}{\dot{m}}=\frac{1}{g_{c}} 2 g H \cot \alpha_{1} ; \\
& \frac{E}{\dot{m}}=\frac{1}{g_{c}} 2 g H \cot \alpha_{1} \\
& \mathrm{R}=1-\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c} \frac{E}{\dot{m}}}
\end{aligned}
$$

From outlet velocity triangle, $V_{2}=V_{m 2} ; \quad V_{2}=V_{m 1}$ as $V_{m 2}=V_{m 1}$

$$
R=1-\frac{V_{1}^{2}-V_{m 1}^{2}}{2 g_{c} \frac{E}{\dot{m}}} ; \quad R=1-\frac{V_{u 1}^{2}}{2 g_{c} \frac{E}{\dot{m}}} ; \quad R=1-\frac{V_{u 1}^{2}}{2 g_{c} \frac{1}{g_{c}} \overline{u_{u 1} U_{1}}} ; \quad R=1-\frac{\overrightarrow{V_{u 1}}}{2 U_{1}}
$$

$R=1-\frac{V_{m} \cot \alpha_{1}}{2 V_{m}} ; \quad \quad R=1-\frac{\cot \alpha_{1}}{4} ; \quad \boldsymbol{R}=\frac{4-\cot \alpha_{1}}{4}$
$\boldsymbol{\alpha}_{\mathbf{1}}=$ ? $\quad$ When $R=0 ; \quad \frac{E}{m}=$ ? for that $\alpha_{1}$
$0=\frac{4-\cot \alpha_{1}}{4} ; \quad \cot \alpha_{1}=4 ; \quad \alpha_{1}=$
the corresponding values of energy transfer per unit mass
$\frac{E}{\dot{m}}=\frac{1}{g_{c}} 2 g H \cot \alpha_{1} ; \quad \frac{E}{\dot{m}}=\frac{1}{1} 2 g H * 4 ; \quad \frac{E}{\dot{m}}=8 g H$
At what value of $\alpha_{1}$, will the degree of reaction be 1
$1=\frac{4-\cot \alpha_{1}}{4} ;$

$$
\cot \alpha_{1}=0 ;
$$

$\tan \alpha_{1}=\frac{1}{0} \quad \tan \alpha_{1}=\infty ; \quad \alpha_{1}=90^{\circ}$
the corresponding values of energy transfer per unit mass
$\frac{E}{\dot{m}}=\frac{1}{g_{c}} 2 g H \cot \alpha_{1} ; \quad \frac{E}{\dot{m}}=4 g H * 0 ; \quad \frac{E}{\dot{m}}=0 \mathrm{~J} / \mathrm{kg}$
12. An inward flow radial turbine has nozzle angle $\alpha$ and rotor blades are radial entry. The radial velocity is constant and there is no whirl velocity at discharge. Show that the utilization factor is equal to $\varepsilon=\frac{2 \cos ^{2} \alpha_{1}}{1+\cos ^{2} \alpha_{1}}$
13. An inward flow radial turbine has nozzle angle $\alpha$ and rotor blades are radial entry. The radial velocity is constant and there is no whirl velocity at discharge. Show that the utilization factor is equal to $\varepsilon=\frac{2 \cos ^{2} \alpha_{1}}{1+\cos ^{2} \alpha_{1}}$
14. In an axial flow turbine, for maximum utilization factor, prove that speed ratio is given by $\emptyset=\frac{\cos \alpha_{1}}{2(1-R)}$
15. The velocity of steam in a Delaval turbine is $1200 \mathrm{~m} / \mathrm{s}$. The nozzle angle being $22^{\circ}$. and rotor blades are equiangular. Assuming the relative velocity of fluid at inlet and exit to be equal and the tangential speed is $400 \mathrm{~m} / \mathrm{s}$. Determine (i) the blade angles at inlet and exit (ii) the tangential force on the blade ring and (iii) power developed in kW , if mass flow rate is $1 \mathrm{~kg} / \mathrm{s}$, iv) . the utilization factor (3a. $10 \mathrm{Dec} / \mathrm{Jan} \mathrm{2016)*}$ Assume $V_{r 1}=V_{r 2}$ (3b. 10 Dec17/Jan 2018)
Delaval turbine is Impulse turbine
le $R=0 \quad$ and $U_{1}=U_{2}=U$

- Velocity of steam from nozzle $=V_{1}=1200 \mathrm{~m} / \mathrm{s}$, nozzle angle , $\alpha_{1}=22^{\circ}$
- the rotor blades are equiangular ie $\beta_{1}=\beta_{2}$
- Tangential speed $U=400 \mathrm{~m} / \mathrm{s}$,
- $V_{r 1}$ equals to $V_{r 2}$ ie $V_{r 1}=V_{r 2}$


## To determine

i) Rotor blade angle $\beta_{1}=$ ?, $\beta_{2}=$ ?., ii) tangential force $F_{u}=$ ? iii) $P=$ ?
iv) Utilization factor $=\varepsilon=$ ?

Inlet Velocity Triangle


Outlet velocity triangle

## From inlet velocity triangle

| $\overrightarrow{V_{u 1}}=V_{1} \cos \alpha_{11} ;$ | $\overrightarrow{V_{u 1}}=1200 \operatorname{Cos} 22 ;$ | $\overrightarrow{V_{u 1}}=1112.62 \mathrm{~m} / \mathrm{s} ;$ |
| :--- | :--- | ---: |
| $V_{m 1}=V_{1} \sin \alpha_{1} ;$ | $V_{m 1}=1200 \sin 22 ;$ | $V_{m 1}=449.527 \mathrm{~m} / \mathrm{s}$ |
| $\tan \beta_{1}=\frac{V_{m 1}}{\overrightarrow{V_{u 1}-U_{1}} ;}$ | $\tan \beta_{1}=\frac{449.527}{111.2 .62-400} ;$ | $\beta_{1}=32.24^{\circ}$ |

$\operatorname{Sin} \beta_{1}=\frac{V_{m 1}}{V_{r 1}} ;$
$\operatorname{Sin} 32.24=\frac{449.527}{V_{r 1}}$;
$V_{r 1}=842.65 \mathrm{~m} / \mathrm{s}$
$\beta_{1}=\beta_{2}$ (blades are equiangular); $\beta_{1}=\mathbf{3 2 . 2 4}{ }^{\circ} ; V_{r 1}$ equals to $V_{r 2}$ ie $V_{r 1}=V_{r 2}$
Hence $V_{r 2}=842.65 \mathrm{~m} / \mathrm{s}$
From outlet velocity triangle
$\overleftarrow{V_{u 2}}=V_{r 2} \cos \beta_{2}-U ; \quad \overleftarrow{V_{u 2}}=842.65 \cos 32.24-400 ; \quad \overleftarrow{V_{u 2}}=312.732 \mathrm{~m} / \mathrm{s}$

## ii) Tangential force

Tangential force $=F_{u}=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}\right)$
Note that + sign since direction of $\mathrm{Vu2}$ is opposite to the direction of $\mathrm{V}_{\mathrm{u} 1}$
$F_{u}=\frac{1}{1}(1112.62+312.732) \quad$ assuming $m=1 \mathrm{~kg} / \mathrm{s}$

$$
F_{u}=1425.35 \mathrm{~N} / \mathrm{kg} / \mathrm{s}
$$

## Power:

$$
\begin{array}{lll}
\frac{E}{\dot{m}}=\frac{\dot{1}}{g_{c}}\left(\overrightarrow{V_{u 1}}+\overleftrightarrow{V_{u 2}}\right) U ; & \frac{E}{\dot{m}}=\frac{\dot{1}}{1}(1112.62+312.732) 400 ; ~ & E \\
E=\dot{m} & =570140.8 \mathrm{~J} / \mathrm{kg} \\
E & E & E=1 \times 570140.8 ;
\end{array}
$$

## Utilization factor

$\epsilon=\frac{\boldsymbol{V}_{\mathbf{1}}^{2}-\boldsymbol{V}_{2}^{2}}{\boldsymbol{V}_{\mathbf{1}}^{2}-\boldsymbol{R} \boldsymbol{V}_{\mathbf{2}}^{2}} ; \epsilon=\frac{\boldsymbol{V}_{\mathbf{1}}^{\mathbf{2}}-\boldsymbol{V}_{\mathbf{2}}^{2}}{\boldsymbol{V}_{\mathbf{1}}^{2}}$ as $R=0$
$\sin \beta_{2}=\frac{V_{m 2}}{V_{r 2}} ; \quad \sin 32.24=\frac{V_{m 2}}{842.65} ; \quad V_{m 2}=449.526 \mathrm{~m} / \mathrm{s}$
$V_{2}=\sqrt{V_{u 2}^{2}+V_{m 2}^{2}} ; \quad V_{2}=\sqrt{312.732^{2}+449.526^{2}} ; \quad V_{2}=369.06 \mathrm{~m} / \mathrm{s}$
$\epsilon=\frac{1200^{2}-369.06^{2}}{1200^{2}} ; \quad \epsilon=0.905$
16. At a nozzle exit of a steam turbine, the absolute steam velocity is $300 \mathrm{~m} / \mathrm{s}$. The rotor speed is $150 \mathrm{~m} / \mathrm{s}$ at a point where the nozzle angle is $18^{\circ}$. If the outlet rotor blade angle is $3.5^{\circ}$ less than the inlet blade angle, find the power output from the stage, for a steam flow rate of $8.5 \mathrm{~kg} / \mathrm{s}$. Assuming $\mathrm{V}_{\mathrm{r} 1}=\mathrm{V}_{\mathrm{r} 2}$ find utilization factor. Specify how you would alter the blade design so that utilization may become maximum under the given circumstances
17. In a delaval steam turbine nozzle angle at inlet is $18^{\circ}$. The relative velocity is reduced to the exit at $6 \%$ when steam flows over the moving blades. The output of the turbine is $120 \mathrm{~kJ} / \mathrm{kg}$ of steam. If the blades are equiangular, find i) speed ratio ii) velocity of steam from nozzle iii) blade speed for maximum utlization
18. At a stage of an impulse turbine the mean blade dia is 0.75 m , is rotational speed being 3500 rpm . The absolute velocity of fluid discharging form a nozzle inclined at $20^{\circ}$ to the plane of the wheel is $275 \mathrm{~m} / \mathrm{s}$. If the utilization factor is 0.9 and the relative velocity at rotor exit is 0.9 times that at the inlet, find the inlet and exit rotor angle.Also find the power output from stage for mass flow rate of $2 \mathrm{~kg} / \mathrm{s}$ and axial thrust on the shaft
19. At a stage of an impulse turbine, the mean blade dia is 80 cm , its rpm 3000 rpm . The absolute velocity of fluid discharging form a nozzle inclined at $20^{\circ}$ to the plane of the wheel is $300 \mathrm{~m} / \mathrm{s}$. If the utilization factor is 0.85 and the relative velocity at rotor exit is equals at inlet, find the inlet and exit rotor angle. Also find the power output from stage for mass flow rate of $1 \mathrm{~kg} / \mathrm{s}$ (4b,10, Dec 18/Jan19)
20. An impulse turbine the mean blade dia is 0.75 m , with a speed of 2800 rpm . The absolute velocity of jet leaving a nozzle inclined at $18^{\circ}$ to the plane of the wheel is $280 \mathrm{~m} / \mathrm{s}$. If the utilization factor is 0.88 and the relative velocity at rotor exit at inlet remains same, Determine i) the inlet and outlet blade angles ii) work done iii) power output for a mass flow rate of $10 \mathrm{~kg} / \mathrm{s}$ (3b. 10, June/July18)
21. The following data refer to an axial flow impulse steam turbine: Steam flow rate $=20 \mathrm{~kg} / \mathrm{s}$, blade speed ratio $=0.5$, blade velocity coefficient $\mathrm{V}_{\mathrm{r} 1} / \mathrm{V}_{\mathrm{r} 2}=0.9$, the nozzle angle at the rotor inlet $=30^{\circ}$ such as to make the whirl velocity at inlet is positive, rotor speed $=4000 \mathrm{rpm}$, mean diameter of the rotor $=60 \mathrm{~cm}$. Find the rotor blade angles if the rotor blades are equiangular. Find also the power output, axial thrust and the utilization factor. Sketch the velocity triangles
22. In an axial flow turbine, the discharge blade angle are $20^{\circ}$ each, for both the stator and the rotor. The steam speed at the exit of the fixed blade is $140 \mathrm{~m} / \mathrm{s}$. The ratio of $\frac{v_{a}}{u}=0.7$ at the entry and 0.76 at the exit of the rotor blade. Find i) the inlet rotor blade angle, ii) the power developed by the blade ring for mass flow rate of $2.6 \mathrm{~kg} / \mathrm{s}$ iii) Degree of reaction (3b. 10 June/July 16) (3b. 10 June/July 13)
axial flow turbine $U_{1}=U_{2}=U$
the discharge blade angle are $20^{\circ}$ each, for both the stator and the rotor.
ie $\alpha_{1}=20^{\circ} ; \beta_{2}=20^{\circ}$;
The steam speed at the exit of the fixed blade is $140 \mathrm{~m} / \mathrm{s}$ ie $V_{1}=140 \mathrm{~m} / \mathrm{s}$
The ratio of $\frac{V_{a}}{u}=0.7$ at the entry and 0.76 at the exit of the rotor blade.
le $\frac{V_{a 1}}{U}=0.7$ and $\frac{V_{a 2}}{U}=0.76$

$$
\begin{array}{lll}
\overrightarrow{V_{u 1}}=V_{1} \cos \alpha_{1} ; & \overrightarrow{V_{u 1}}=140 \cos 20 ; & \overrightarrow{V_{u 1}}=131.56 \mathrm{~m} / \mathrm{s} \\
V_{a 1}=V_{1} \sin \alpha_{1} ; & V_{a 1}=140 \sin 20 ; & V_{a 1}=47.88 \mathrm{~m} / \mathrm{s}
\end{array}
$$

$\begin{array}{lll}\frac{V_{a 1}}{U}=0.7 ; & \frac{47.88}{U}=0.7 ; & U=68.40 \mathrm{~m} / \mathrm{s} \\ \frac{V_{a 2}}{U}=0.76 ; & \frac{V_{a 2}}{68.40}=0.76 ; & V_{a 2}=51.98 \mathrm{~m} / \mathrm{s}\end{array}$
$\overrightarrow{V_{u 1}}>U$, Hence Inlet velocity triangle is as follows

$\tan \beta_{1}=\frac{V_{a 1}}{\overline{V_{u 1}}-\mathrm{U}} ; \quad \quad \tan \beta_{1}=\frac{47.88}{131.56-68.40} ;$
$\beta_{1}=37.16^{\circ}$
$\frac{V_{a 2}}{X}=\tan \beta_{2} ; \quad \frac{51.98}{X}=\tan 20 ; \quad X=142.81 ;$
$V_{r 2} \cos \beta_{2}=142.81$
$V_{r 2} \cos \beta_{2}>U$


$$
\begin{array}{llr}
\overleftarrow{V_{u 2}}=V_{r 2} \cos \beta_{2}-U ; & \overleftarrow{V_{u 2}}=74.40 \mathrm{~m} / \mathrm{s} \\
\frac{E}{\dot{m}}=\frac{\left(\overline{V_{u 1}}+\widetilde{V_{u 2}}\right) U}{g_{c}} ; & \frac{E}{\dot{m}}=\frac{(131.56+74.40) 68.40}{1} ; & \frac{E}{\dot{m}}=14.08 * 10^{3} \mathrm{~J} / \mathrm{kg} ; \\
E=\dot{m} \frac{E}{\dot{m}} ; & E=2.6 * 14.08 * 10^{3} & E=36.62 * 10^{3} \mathrm{~W} \\
R=1-\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}} ; & V_{1}^{2}=140^{2} ; & \\
V_{2}^{2}=V_{u 2}^{2}+V_{a 2}^{2} ; & V_{2}^{2}=74.40^{2}+51.98^{2} ; & V_{2}^{2}=8237.28 \\
R=1-\frac{140^{2}-8237.28}{2 * 14.08 * 10^{3}} ; & R=0.5964 &
\end{array}
$$

23. Air flows axially through a axial flow turbine at a mean radius of 0.2 m . If the tangential component of absolute velocity reduced by $20 \mathrm{~m} / \mathrm{s}$ during passage through the rotor, find the power developed by the turbine for a flow rate $100 \mathrm{~m}^{3} / \mathrm{s}$ at a point, where the pressure and temperature are 1 bar and $27^{\circ} \mathrm{C}$. The rotational speed of the rotor is 3000 rpm
24. Liquid water lows at a rate of $31.5 \mathrm{~kg} / \mathrm{s}$ through a rotor of an axial flow turbine, where inlet and outlet mean diameters are 18.5 cm and 20 cm respectively. The other data are: speed $=6000 \mathrm{rpm}, \mathrm{V}_{1}=35 \mathrm{~m} / \mathrm{s}$ and is directed axially. $\mathrm{V}_{2}=160 \mathrm{~m} / \mathrm{s}$ such that $\alpha_{2}=30^{\circ}$. Using mean inlet and outlet diameter find i) Torque exerted ii) $V_{r 1}$ and $V_{r 2}(3 \mathrm{c}, 06$, Dec18/Jan19,10scheme)
$\dot{m}=\frac{31.5 \mathrm{~kg}}{\mathrm{~s}}$; axial $D_{1}=18.5 \mathrm{~cm}=0.185 \mathrm{~m} ; D_{2}=20 \mathrm{~cm}=0.2 \mathrm{~m} ; N=6000 \mathrm{rpm}$;
$\mathrm{V}_{1}=35 \mathrm{~m} / \mathrm{s}$ and is directed axially $\mathrm{V}_{1}=35 \mathrm{~m} / \mathrm{s} ; \alpha_{1}=90^{\circ} ; \mathrm{V}_{2}=160 \mathrm{~m} / \mathrm{s} ; \alpha_{2}=30^{\circ}$


$$
\begin{array}{llc}
U_{1}=\frac{\pi D_{1} N}{60} ; & U_{1}=\frac{\pi x 0.185 \times 6000}{60} ; & U_{1}=58.12 \mathrm{~m} / \mathrm{s} \\
U_{2}=\frac{\pi D_{2} N}{60} ; & U_{2}=\frac{\pi \times 0.2 x 6000}{60} ; & U_{2}=62.83 \mathrm{~m} / \mathrm{s} \\
\overrightarrow{V_{u 1}}=V_{1} \cos \alpha_{1} ; & \overrightarrow{V_{u 1}}=35 \cos 90 & \overrightarrow{V_{u 1}}=0 \\
V_{m 1}=V_{1} \sin \alpha_{1} ; & V_{m 1}=35 \sin 90 & \overrightarrow{V_{m 1}}=35 \mathrm{~m} / \mathrm{s} \\
\overrightarrow{V_{u 2}}=V_{2} \cos \alpha_{2} ; & \overrightarrow{V_{u 2}}=160 \cos 30 & \overrightarrow{V_{u 2}}=138.56 \mathrm{~m} / \mathrm{s} \\
V_{m 2}=V_{2} \sin \alpha_{2}=160 \sin 30=80 \mathrm{~m} / \mathrm{s} & \\
U_{2}<\overrightarrow{V_{u 2}}, \text { Hence outlet velocity triangle as given below } &
\end{array}
$$



Torque exerted $=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}} R_{1}-\overrightarrow{V_{u 2}} R_{2}\right)$;
$T=\frac{31.5}{1}\left(0-138.56 * \frac{0.2}{2}\right) ; \quad T=-13.856 \mathrm{Nm}$
From Inlet velocity triangle ; $V_{r 1}=U_{1} ; V_{r 1}=62.83 \mathrm{~m} / \mathrm{s}$;
From outlet velocity triangle : $\tan \beta_{2}=\frac{V_{m 2}}{\overline{V_{u 2}}-U_{2}}$
Assuming flow velocity is constant $V_{m 2}=V_{m 1} ; V_{m 2}=35 \mathrm{~m} / \mathrm{s}$
$\tan \beta_{2}=\frac{V_{m 2}}{\overline{V_{u 2}}-U_{2}} ;$
$\tan \beta_{2}=\frac{35}{138.56-62.83} ;$
$\beta_{2}=24.8^{0}$
$\sin \beta_{2}=\frac{V_{m 2}}{V_{r 2}} ;$

$$
\sin 24.8=\frac{35}{V_{r 2}}
$$

$$
V_{r 2}=83.42 \mathrm{~m} / \mathrm{s}
$$

25. An inward radial flow hydraulic turbine water enters with an absolute velocity of $15 \mathrm{~m} / \mathrm{s}$ with a nozzle angle of $15^{\circ}$. The speed of the rotor is 400 rpm . Diameter of the rotor at inlet and outlet are 75 cm and 50 cm respectively. The fluid leaves the rotor radially with an absolute velocity of $5 \mathrm{~m} / \mathrm{s}$. Determine i) The blade angles ii) workdone iii) utilization factor ( $3 \mathrm{~b}, 08$, Dec18/Jan19,15 scheme)
$V_{1}=15 \mathrm{~m} / \mathrm{s} ; \alpha_{1}=15^{0} ; N=400 \mathrm{rpm} ; D_{1}=0.75 \mathrm{~m} ; D_{2}=0.5 \mathrm{~m}$
The fluid leaves the rotor radially with an absolute velocity of $5 \mathrm{~m} / \mathrm{s} . \alpha_{2}=90^{\circ} ; V_{2}=5 \mathrm{~m} /$ $s ;$
$\beta_{1}=? ; \beta_{2}=? \frac{E}{\dot{m}}=? ; \epsilon=$ ?
$U_{1}=\frac{\pi D_{1} N}{60} ;$
$U_{1}=\frac{\pi * 0.75 * 400}{60} ;$

$$
U_{2}=\frac{\pi D_{2} N}{60}
$$

$$
U_{2}=\frac{\pi * 0.5 * 400}{60}
$$

$$
\overrightarrow{V_{u 1}}=V_{1} \cos \alpha_{1}
$$

$$
\overrightarrow{V_{u 1}}=15 \cos 15 ;
$$

$$
\begin{aligned}
U_{1} & =15.70 \mathrm{~m} / \mathrm{s} \\
U_{2} & =10.47 \mathrm{~m} / \mathrm{s} \\
\overrightarrow{V_{u 1}} & =14.49 \mathrm{~m} / \mathrm{s} \\
V_{m 1} & =3.88 \mathrm{~m} / \mathrm{s}
\end{aligned}
$$

$V_{m 1}=V_{1} \sin \alpha_{1} ;$
$V_{m 1}=15 \sin 15 ;$

$$
\overrightarrow{V_{u 1}}<U_{1}
$$


$\tan \beta_{1}=\frac{V_{m 1}}{U_{1}-\overline{V_{u 1}}} ; \quad \quad \tan \beta_{1}=\frac{3.88}{15.70-14.49} ; \quad \beta_{1}=72.67^{\circ}$


U2

\[

\]

Utilization factor

$$
\epsilon=\frac{\frac{E}{\dot{m}}}{\frac{E}{\dot{m}}+\frac{V_{2}^{2}}{2 g_{c}}} ; \quad \in=\frac{227.49}{227.49+\frac{5^{2}}{2 * 1}} ;
$$

$$
\epsilon=0.9479
$$

26. An inward flow reaction turbine has outer and inner diameter of the wheel as 1 m and 0.5 m respectively.. The vanes are radial at inlet, and discharge is radial at outlet and water enters the blade at an angle of $10^{\circ}$. Assume the velocity of flow is constant and equal to $3 \mathrm{~m} / \mathrm{s}$. Find i) Speed of the wheel ii) outlet blade angle iii) Degree of reaction (2c. 10 June/July 17) )(4b,10,June/July14)*

Inward flow turbine; Inner Diameter=1m ie $D_{1}=1 \mathrm{~m}$; Outer Diameter $D_{2}=$ $0.5 \mathrm{~m} \alpha_{1}=10^{0}$. Assume the velocity of flow is constant and equal to $3 \mathrm{~m} / \mathrm{s} . V_{f 1}=$ $V_{f 2}=3 \mathrm{~m} / \mathrm{s} ; N=? ; R=$ ?


From inlet velocity triangle $\tan \alpha_{1}=\frac{V_{m 1}}{U_{1}} ; \quad \tan 10=\frac{3}{U_{1}} ; \quad U_{1}=17.01 \mathrm{~m} / \mathrm{s}$;
$U_{1}=\frac{\pi D_{1} N}{60} ;$
$17.01=\frac{\pi * 1 * N}{60} ;$
$U_{2}=\frac{\pi D_{2} N}{60}$;
$U_{2}=\frac{\pi * 0.5 * 324.94}{60} ;$
$N=324.94 \mathrm{rpm}$;
$\tan \beta_{2}=\frac{V_{m 2}}{U_{2}} ;$
$\tan \beta_{2}=\frac{3}{8.5} ;$ $U_{2}=8.5 \mathrm{~m} / \mathrm{s} ;$
$R=1-\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c} \frac{E}{\dot{m}}} ;$
$\frac{E}{\dot{m}}=\frac{\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right)}{g_{c}}$;
From Inlet and outlet triangles
$\overrightarrow{V_{u 1}}=U_{1} ; \overrightarrow{V_{u 2}}=0$
$\frac{E}{\dot{m}}=\frac{\left(U_{1} U_{1}+0\right)}{g_{c}} ; \quad \quad \frac{E}{\dot{m}}=\frac{17.01 * 17.01+0}{1} ; \quad \quad \frac{E}{\dot{m}}=289.34 \mathrm{~J} / \mathrm{kg}$;
$V_{1}^{2}=V_{u 1}^{2}+V_{m 1}^{2} ; \quad V_{1}^{2}=17.01^{2}+3^{2} ; \quad V_{1}^{2}=298.34 ; \quad V_{2}^{2}=3^{2}$
$R=1-\frac{298.34-9}{2 * 289.34} ; \quad R=0.5$
27. The mean diameter of axial flow steam turbine is 50 cm . The maximum utilisation factor is 0.9 and degree of reaction is 0.5 . The mass flow rate of steam is $10 \mathrm{~kg} / \mathrm{s}$. The
speed of the blade is 2000rpm . Calculate i) Inlet and exit absolute velocities ii) Power developed (3c. 08, Dec12)
Axial : $D=D_{1}=D_{2}=50 \mathrm{~cm}=0.5 \mathrm{~m} ; \quad \epsilon_{\max }=0.9 ; R=0.5 ; \dot{m}=10 \mathrm{~kg} / \mathrm{s} ; N=$ 2000rpm
$U=\frac{\pi D N}{60} ;$
$U=\frac{\pi \times 0.5 \times 2000}{60}$
$U=52.36 \mathrm{~m} / \mathrm{s}$
$\epsilon=\frac{V_{1}^{2}-V_{2}^{2}}{V_{1}^{2}-R V_{2}^{2}} ;$
$0.9=\frac{V_{1}^{2}-V_{2}^{2}}{V_{1}^{2}-0.5 V_{2}^{2}}$
$0.9 V_{1}^{2}-\left(0.9 * 0.5 V_{2}^{2}\right)=V_{1}^{2}-V_{2}^{2} ;$
$R=50 \%$, ie $V_{r 1}=V_{2}, V_{r 2}=V_{1}, \alpha_{1}=\beta_{2}, \alpha_{2}=\beta_{1}$
$\alpha_{2}=90^{\circ}$ since turbine is for maximum utilization
$\alpha_{2}=\beta_{1}$ for $50 \% \mathrm{R}$ Hence $\beta_{1}=90^{\circ}$


U

## Power Developed

$E=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U$
From inlet velocity triangle $\overrightarrow{V_{u 1}}=\mathrm{U}=52.36$; From outlet velocity triangle $\overrightarrow{V_{u 2}}=0$
Hence $E=\frac{\dot{2}}{1}(52.36+0) 52.36$;

$$
E=5.483 * 10^{3} \mathrm{Watts}
$$

## Exit absolute velocity

$\frac{E}{\dot{m}}=\frac{5.483 * 10^{3}}{2}$;
$\frac{E}{\dot{m}}=2741.5 \mathrm{~J} / \mathrm{kg}$
$\in=\frac{\frac{E}{\dot{m}}}{\frac{E}{\dot{m}}+\frac{V_{2}^{2}}{2 g_{c}}} ; \quad 0.9=\frac{2741.5}{2741.5+\frac{V_{2}^{2}}{2 * 1} ;} \quad 27415+\frac{V_{2}^{2}}{2 * 1}=3046.11 ;$
$V_{2}^{2}=609.22 ; \quad V_{2}=24.68 m / s$

## Inlet absolute velocity

From outlet velocity triangle
$V_{r 2}^{2}=V_{2}^{2}+U^{2} ; \quad V_{r 2}^{2}=609.22+52.36^{2} ; V_{r 2}^{2}=3350.67 V_{r 2}=57.88 \mathrm{~m} / \mathrm{s}$
$V_{1}=V_{r 2}$ since $50 \% \mathrm{R} \quad V_{1}=57.88 \mathrm{~m} / \mathrm{s}$
28. At a $50 \%$ reaction stage axial flow turbine, the mean blase diameter is 0.6 mtr . The maximum utilization factor is 0.85 and steam flow rate is $12 \mathrm{~kg} / \mathrm{s}$. Calculate the inlet and outlet absolute velocities and power developed if the speed is 2500rpm (3b. 10, June/July14)

Axial : $D=D_{1}=D_{2}=60 \mathrm{~cm}=0.6 \mathrm{~m} ; \in_{\max }=0.85 ; R=0.5 ; \dot{m}=10 \mathrm{~kg} / \mathrm{s} ; N=$ 2000rpm
$U=\frac{\pi D N}{60} ; U=\frac{\pi x 0.6 \times 2000}{60}=62.83 \mathrm{~m} / \mathrm{s}$
$\epsilon=\frac{V_{1}^{2}-V_{2}^{2}}{V_{1}^{2}-R V_{2}^{2}} ; \quad 0.9=\frac{V_{1}^{2}-V_{2}^{2}}{V_{1}^{2}-0.5 V_{2}^{2}}$
$0.9 V_{1}^{2}-0.9 \times 0.5 V_{2}^{2}=V_{1}^{2}-V_{2}^{2} ; \quad V_{1}^{2}=5.5 V_{2}^{2}-\cdots-\cdots-\cdots----1$
$R=50 \%$, ie $V_{r 1}=V_{2}, V_{r 2}=V_{1}, \alpha_{1}=\beta_{2}, \alpha_{2}=\beta_{1}$
$\alpha_{2}=90^{\circ}$ since turbine is for maximum utilization
$\alpha_{2}=\beta_{1}$ for $50 \%$ R Hence $\beta_{1}=90^{\circ}$


U

## Power Developed

$E=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U$
From inlet velocity triangle $\overrightarrow{V_{u 1}}=U=62.83$; From outlet velocity triangle $\mathrm{V}_{\mathrm{u} 1}=0$
Hence $E=\frac{2}{1}(62.83+0) 62.83 ; \quad E=7.895 * 10^{3}$ Watts

## Exit absolute velocity

$\frac{E}{\dot{m}}=\frac{7.895 * 10^{3}}{2} ;$
$\frac{E}{\dot{m}}=3947.5 \mathrm{~J} / \mathrm{kg}$
$\in=\frac{\frac{E}{\dot{m}}}{\frac{E}{\dot{m}}+\frac{V_{2}^{2}}{2 g_{c}}} ;$
$0.9=\frac{3947.5}{3947.5+\frac{V_{2}^{2}}{2 * 1}} ;$
$3947.5+\frac{V_{2}^{2}}{2 * 1}=4386.11 ;$
$V_{2}^{2}=877.22 ; \quad V_{2}=\mathbf{2 9 . 6 1 m} / \boldsymbol{s}$

## Inlet absolute velocity

From outlet velocity triangle
$V_{r 2}^{2}=V_{2}^{2}+U^{2} ; \quad V_{r 2}^{2}=877.22+62.83^{2} ; V_{r 2}^{2}=4824.83 \quad V_{r 2}=69.46 \mathrm{~m} / \mathrm{s}$
$V_{1}=V_{r 2}$ since $50 \% \mathrm{R} \quad V_{1}=69.46 \mathrm{~m} / \mathrm{s}$
29. At a $50 \%$ reaction stage axial flow turbine, the mean blade diameter is 60 cm . The maximum utilization factor is 0.9 . Steam flow rate is $10 \mathrm{~kg} / \mathrm{s}$. Calculate the inlet and outlet absolute velocities and power developed if the speed is 2000rpm
30. The mean rotor blade speed of an axial speed of an axial flow turbine stage with a degree of reaction of $50 \%$ is $210 \mathrm{~m} / \mathrm{s}$. The steam emerges from nozzle inclined at $28^{\circ}$ to the wheel plane with an axial velocity component which is equal to blade speed. Assuming symmetric inlet and outlet velocity triangles. Find the rotor blade angles and utilization factor. Find also the degree of reaction to make the utilization maximum, if the axial velocity and the blade speed as well as the nozzle remain the same above(3b. 10, Dec14/Jan 15)*

The mean rotor blade speed of axial flow turbine stage with $50 \%$ reaction is $210 \mathrm{~m} / \mathrm{s}$ ie $\mathrm{U}=210 \mathrm{~m} / \mathrm{s}, \mathrm{R}=0.5$ ie $\alpha_{1}=\beta_{2}, \alpha_{2}=\beta_{1}$

Steam emerges from the nozzle inclined at $28^{\circ}$ to the plane of the wheel with axial component equal to the blade speed ie $\alpha_{1}=28^{\circ}, \mathrm{V}_{\mathrm{m} 1}=\mathrm{U}=210$

## To determine

$$
\varepsilon=? ; \quad \beta_{1}=? \quad \beta_{2}=?
$$

$\mathbf{R}=$ ? for maximum utilization if the axial velocity, blade speed and nozzle angle remain the same.


## Rotor Blade angles

$\tan \alpha_{1}=\frac{V_{m 1}}{\overrightarrow{V_{u 1}}} ;$
$\tan 28=\frac{210}{\overrightarrow{V_{u 1}}}$

$$
\overrightarrow{V_{u 1}}=395 \mathrm{~m} / \mathrm{s}
$$

$X=\overrightarrow{V_{u 1}}-U$

$$
X=395-210 ;
$$

$$
X=185 \mathrm{~m} / \mathrm{s}
$$

$$
\tan \beta_{1}=\frac{V_{m 1}}{X}
$$

$$
\tan \beta_{1}=\frac{210}{195}
$$

$$
\beta_{1}=48.62^{\circ}
$$

$\alpha_{2}=\beta_{1} ;$

$$
\alpha_{1}=48.62^{\circ}
$$

$\beta_{2}=\alpha_{1} ;$

$$
\beta_{2}=28^{\circ}
$$

## Utilisation factor

$\operatorname{Sin} \beta_{1}=\frac{V_{m 1}}{V_{r 1}} ;$
$\operatorname{Sin} 48.62=\frac{210}{V_{r 1}} ;$
$V_{r 1}=279.87 \mathrm{~m} / \mathrm{s}$
$V_{2}=V_{r 1}(50 \% \mathrm{R})$ ie $V_{2}=279.87 \mathrm{~m} / \mathrm{s}$
$\operatorname{Sin} \alpha_{1}=\frac{V_{m 1}}{V_{1}} ;$
$\operatorname{Sin} 28=\frac{210}{V_{1}}$
$V_{1}=447.9 \mathrm{~m} / \mathrm{s}$
$\epsilon=\frac{V_{1}^{2}-V_{2}^{2}}{V_{1}^{2}-R V_{2}^{2}} ;$
$\epsilon=\frac{447.9^{2}-279.87^{2}}{447.9^{2}-0.5 \times 279.87^{2}} ;$
$\epsilon=0.757$

Find also the degree of reaction to make the utilization ma maximum, if the axial velocity and the blade speed as well as the nozzle remain the same above

For maximum utilization outlet velocity triangle


$$
\begin{aligned}
& V_{m 1}=U=210 \mathrm{~m} / \mathrm{s} ; V_{m 2}=210 \mathrm{~m} / \mathrm{s} \\
& V_{\mathrm{m} 2}=\mathrm{V}_{2} \text { as } \alpha_{2}=90^{\circ} \\
& R=1-\frac{V_{1}^{2}-V_{2}^{2}}{2 \frac{E}{\dot{m}}} ; \\
& \frac{E}{\dot{m}}=\frac{\overrightarrow{V_{u 1} U}}{g_{c}} \quad \text { as } \quad \overrightarrow{V_{u 2}}=0 \\
& \frac{E}{\dot{m}}=\frac{395 * 210}{1} ; \quad \frac{E}{\dot{m}}=82950 \mathrm{~J} / \mathrm{kg} \\
& R=1-\frac{447.9^{2}-210^{2}}{2 \times 82950} ; \\
& R=0.0565 \\
& \epsilon=\frac{V_{1}^{2}-V_{2}^{2}}{V_{1}^{2}-R V_{2}^{2}} ; \quad \quad \epsilon=\frac{447.9^{2}-210^{2}}{447.9^{2}-0.0565 \times 210^{2}} \\
& \epsilon=0.79
\end{aligned}
$$

31. The following data refer to a $50 \%$ degree of reaction axial flow turbomachine. Inlet fluid velocity $=230 \mathrm{~m} / \mathrm{s}$, inlet rotor angle $=60^{\circ}$, Inlet guide angle $=30^{\circ}$, outlet rotor angle $25^{\circ}$, Find utilization factor , axial thrust and power output per unit mass flow. (3b,10,Dec13/Jan14) $R=0.5 ; \quad$ axial flow turbomachine $U_{1}=U_{2}=U$ Inlet fluid velocity $=230 \mathrm{~m} / \mathrm{s}, \quad V_{1}=230 \mathrm{~m} / \mathrm{s}$;
inlet rotor angle $=60^{\circ}, \beta_{1}=60^{\circ}$;
Inlet guide angle $=30^{\circ}$ please note that this is exit guide blade angle Hence this is not $\alpha_{1}$ outlet rotor angle $25^{\circ}$ ie $\beta_{2}=25^{\circ}$ $\epsilon=? ; \quad F_{a}=$ ? ; $E=$ ? if $\dot{m}=1 \mathrm{~kg} / \mathrm{s}$


## utilization factor

Since $50 \% \mathrm{R} \quad \alpha_{1}=\beta_{2} \dot{ } \quad \alpha_{1}=25^{\circ} ; \quad \alpha_{2}=\beta_{1} ; \quad \alpha_{2}=60^{\circ}$
$\overrightarrow{V_{u 1}}=V_{1} \cos \alpha_{1} ;$
$\overrightarrow{V_{u 1}}=230 \cos 25$

$$
\begin{aligned}
& \overrightarrow{V_{u 1}}=208.45 \mathrm{~m} / \mathrm{s} \\
& V_{m 1}=97.2 \mathrm{~m} / \mathrm{s}
\end{aligned}
$$

$V_{m 1}=V_{1} \operatorname{Sin} \alpha_{1} ;$
$V_{m 1}=230 \sin 25$
$\operatorname{Sin} \beta_{1}=\frac{V_{m 1}}{V_{r 1}} ; \quad \operatorname{Sin} 60=\frac{97.2}{V_{r 1}} ; \quad V_{r 1}=112.24 \mathrm{~m} / \mathrm{s}$
$V_{2}=V_{r 1} ; \quad V_{2}=112.24 \mathrm{~m} / \mathrm{s} ; \quad \alpha_{2}=\beta_{1} ; \alpha_{2}=60^{\circ}$ for $50 \% \mathrm{R}$
$\overleftarrow{V_{u 2}}=V_{2} \cos \alpha_{2} ; \quad \overleftarrow{V_{u 2}}=112.24 \cos 60 \quad \overleftarrow{V_{u 2}}=56.11 \mathrm{~m} / \mathrm{s}$
$V_{m 2}=V_{2} \operatorname{Sin} \alpha_{2} ; \quad V_{m 2}=112.24 \sin 60 \quad V_{m 2}=97.2 \mathrm{~m} / \mathrm{s}$
$U=\overrightarrow{V_{u 1}}-\mathrm{X} ; \quad U=\overrightarrow{V_{u 1}}-V_{r 1} \cos \beta_{1} ; \quad U=208.45-112.24 \cos 60 ; U=152.33 \mathrm{~m} / \mathrm{s}$
$\frac{E}{\dot{m}}=\frac{1}{g_{c}}\left(\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U ; \quad \quad \frac{E}{\dot{m}}=\frac{1}{1}(208.45+56.11) 152.33 ; \quad \frac{E}{\dot{m}}=40300.42 \mathrm{~J} / \mathrm{kg}$
$\epsilon=\frac{\frac{E}{\dot{\dot{n}}}}{\frac{E}{\dot{\dot{m}}+\frac{V_{2}^{2}}{2 g_{c}}} ;} \quad \in=\frac{40300.42}{40300.42+\frac{12.24^{2}}{2 * 1}} ;$

## axial thrust

$F_{a}=\frac{\dot{m}}{g_{c}}\left(V_{m 1}-V_{m 2}\right) ; \quad F_{a}=0$ since $V_{m 1}=V_{m 2}$

## Power:

$E=\dot{m} \frac{E}{\dot{m}^{\prime}}$
$E=1 * 40300.42$
$E=40300.42 W$
32. A mixed flow turbine handling water operates under a static head of 65 m . In steady flow the static pressure at the rotor inlet is is 3.5 atm (guage). The absolute at the rotor inlet is directed at an angle of $25^{\circ}$ to the tangent so that whirl velocity is positive. The absolute velocity at the exit is purely axial. If the degree of reaction for the machine is 0.47 and the utilisation factor is 0.896 . Compute the tangential blade speed as well as the inlet blade angle. Find the work output per unit mass flow of water. (4b. 10, Dec12)
$p_{o}=0 ; V_{o}=0 ; Z_{o}=65 \mathrm{~m} ; p_{o}=3.5 \mathrm{~atm}=3.5 * 1.03 \mathrm{bar} ; Z_{1}=0$
$\alpha_{1}=25^{\circ}$; The absolute velocity at the exit is purely axial ie $\alpha_{1}=90^{\circ} ; R=0.47 ;$
$\varepsilon=0.896$
$U_{1}=? ; \beta_{1}=? ; \frac{E}{\dot{m}}=$ ?

## Tangential speed of rotor

Applying burnollis equation
$\frac{p_{o}}{\omega}+\frac{V_{o}^{2}}{2 g}+Z_{o}=\frac{p_{1}}{\omega}+\frac{V_{1}^{2}}{2 g}+Z_{1} ; \quad 0+0+65=\frac{3.5 * 1.03 * 10^{5}}{9810}+\frac{V_{1}^{2}}{2 * 9.81}+0 ;$
$V_{1}^{2}=575.52 ;$

$$
\begin{array}{lll}
\varepsilon=\frac{V_{1}^{2}-V_{2}^{2}}{V_{1}^{2}-R V_{2}^{2}} ; & 0.896=\frac{575.52-V_{2}^{2}}{575.52-0.47 * V_{2}^{2}} ; & V_{2}^{2}=102.01 \\
R=1-\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c} \frac{E}{\dot{m}}} ; & 0.47=1-\frac{575.52-102.01}{2 * 21.74 * U_{1}} ; & U_{1}=20.30 \mathrm{~m} / \mathrm{s}
\end{array}
$$

## Inlet Blade angle

$$
\begin{array}{lll}
\frac{E}{\dot{m}}=\frac{\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right)}{g_{c}} ; & \overrightarrow{V_{u 2}}=0 \text { as } \alpha_{2}=0 & \text { hence } \frac{E}{\dot{m}}=\frac{V_{u 1} U_{1}}{g_{c}} \\
V_{u 1}=V_{1} \cos \alpha_{1} ; & V_{u 1}=23.99 \cos 25 ; & V_{u 1}=21.74 \mathrm{~m} / \mathrm{s} \\
\frac{E}{\dot{m}}=\frac{V_{u 1} U_{1}}{g_{c}} ; & \frac{E}{\dot{m}}=\frac{21.74 * 20.30}{1} ; & \frac{E}{\dot{m}}=437.62 \mathrm{~J} / \mathrm{kg} \\
\tan \beta_{1}=\frac{V_{m 1}}{\overrightarrow{V_{u 1}}-\mathrm{U}} ; V_{m 1}=V_{1} \sin \alpha_{1} ; V_{m 1}=23.99 \sin 25 ; V_{m 1}=10.14 \mathrm{~m} / \mathrm{s} \\
\tan \beta_{1}=\frac{10.14}{21.74-20.30} ; & \beta_{1}=82.90^{0} &
\end{array}
$$

33. A hydraulic reaction turbine of the radial inward flow type works under a head of 160 m of water. At the point of fluid entry, the rotor blade angle is $119^{\circ}$ and diameter of the runner is 3.65 m . At the exit , the runner diameter is 2.45 m . If the absolute velocity of the wheel outlet is radially directed with a magnitude of $15.5 \mathrm{~m} / \mathrm{s}$ and the radial component of velocity at the inlet is $10.3 \mathrm{~m} / \mathrm{s}$. Find the power developed by the machine, assuming that the $88 \%$ of the available head of the machine is converted into work and the flow rate is $110 \mathrm{~m}^{3} / \mathrm{s}$. Find also the degree of reaction and utilization factor (4b,08, June/July 18,15 scheme)
$H=160 m ; \beta_{1}=119^{\circ} ; D_{1}=3.65 m D_{2}=2.45 m ;$
the absolute velocity of the wheel outlet is radially directed with a magnitude of $15.5 \mathrm{~m} / \mathrm{s}$ $\alpha_{2}=90^{\circ} ; V_{2}=15.5 \mathrm{~m} / \mathrm{s}$;
The radial component of velocity at the inlet is $10.3 \mathrm{~m} / \mathrm{s} . V_{m 2}=10.3 \mathrm{~m} / \mathrm{s}$ $E=$ ? ; the $88 \%$ of the available head of the machine is converted into work $\eta_{h}=88 \%$ flow rate is $110 \mathrm{~m}^{3} / \mathrm{s} \quad Q=110 \mathrm{~m}^{3} / \mathrm{s} ; R=$ ? $\in=$ ?



U2

$$
\begin{aligned}
& \eta_{h}=\frac{\frac{E}{\dot{m}}}{g H} ; \quad \frac{E}{\dot{m}}=\frac{\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right)}{g_{c}} ; \quad V_{u 2}=0 \text { as } \alpha_{2}=90^{\circ} ; \quad \frac{E}{\dot{m}}=\frac{V_{u 1} U_{1}}{g_{c}} \\
& \overrightarrow{V_{u 1}}=U_{1}-X ; \quad \frac{V_{m 1}}{X}=\tan \beta_{1} ; \frac{10.3}{X}=\tan (180-119) ; X=5.709 \mathrm{~m} / \mathrm{s} \\
& \overrightarrow{V_{u 1}}=U_{1}-5.709 \\
& \frac{E}{\dot{m}}=\frac{V_{u 1} U_{1}}{g_{c}} ; \frac{E}{\dot{m}}=\frac{\left(U_{1}-5.709\right) U_{1}}{1} \\
& \eta_{h}=\frac{\frac{E}{\dot{m}}}{g H} ; \quad 0.88=\frac{\left(U_{1}-5.709\right) U_{1}}{9.81 * 160} ; \\
& 1381.248=U_{1}^{2}-5.709 U_{1} ; \\
& U_{1}^{2}-5.709 U_{1}-1381.248=0 ; U_{1}=40.13 \mathrm{~m} / \mathrm{s} ; \\
& \overrightarrow{V_{u 1}}=U_{1}-5.709 ; \quad \overrightarrow{V_{u 1}}=40.13-5.709 ; \quad \overrightarrow{V_{u 1}}=34.4 \mathrm{~m} / \mathrm{s} \\
& \frac{E}{\dot{m}}=\frac{34.4 * 40.13}{1} ; \quad \quad \frac{E}{\dot{m}}=1380.47 \mathrm{~J} / \mathrm{kg} \\
& V_{1}^{2}=V_{u 1}^{2}+V_{m 1}^{2} ; \quad V_{1}^{2}=V_{u 1}^{2}+V_{m 1}^{2} ; V_{1}^{2}=34.4^{2}+10.3^{2} ; V_{1}^{2}=; V_{2}^{2}=15.5^{2} \\
& R=1-\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c} \frac{E}{\dot{m}}} ; \\
& R=1-\frac{34.4^{2}+10.3^{2}-15.5^{2}}{2 * 1380.47} ; \\
& R=0.62 \\
& \in=\frac{\frac{E}{\dot{m}}}{\frac{E}{\dot{m}}+\frac{V_{2}^{2}}{2 g_{c}}} ; \\
& \epsilon=\frac{1380.47}{1380.47+\frac{15.5^{2}}{2 * 1}} ; \\
& \epsilon=0.92
\end{aligned}
$$

## Power Absorbing machine

According to the direction fluid flow power absorbing turbo machine can be classified into axial and radial flow power absorbing turbo machine

All are centrifugal turbo machines are radial flow power absorbing turbo machines
In axial flow power absorbing turbo machine $U_{1}=U_{2}=U$

In radial flow power absorbing turbo machine $U_{1} \neq U_{2}$

In power absorbing turbo machine
$\frac{E}{\dot{m}}=\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right) \quad$ is negative $\quad$ ie $\overrightarrow{V_{u 2}} U_{2}>\overrightarrow{V_{u 1}} U_{1}$
Turning angle of fluid from inlet to outlet is small

## Axial flow Compressor

General Inlet velocity triangle


General outlet velocity triangle


In axial flow power absorbing turbomachine, since $U_{1}=U_{2}$ outlet and inlet velocity triangles can be drawn with common base

$\gamma$ are called air angles
$\gamma 0$ is called air angle at inlet, $\gamma_{1}$ is called as air angle at outlet
output per unit mass $\frac{E}{\dot{m}}=\left(V_{u 1} U_{1}-V_{u 2} U_{2}\right) \quad$ This expression will have negative value in power absorbing machine
therefore, generally In power absorbing we express Input/per unit mass
Input/per unit mass ie $-\frac{E}{\dot{m}}=\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right)$

## le negative of output =Input

1. Define degree of reaction for an axial flow machine. Prove that degree of reaction for an axial flow device (assuming constant velocity of flow ) is given by
$R=\frac{V_{f}}{2 U}\left(\frac{\tan \beta_{1}+\tan \beta_{2}}{\tan \beta_{1} * \tan \beta_{2}}\right)$ where $\beta_{1}$ and $\beta_{2}$ are the angles made with tangent to the blades (4a. 10, Dec13/Jan 14)( 4a. 10, Dec18/Jan 19) (4a. 10 Dec17/Jan 2018)

$R=\frac{\frac{U_{1}^{2}-U_{2}^{2}}{2}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2}}{\frac{V_{1}^{2}-V_{2}^{2}}{2}+\frac{U_{1}^{2}-U_{2}^{2}}{2}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2}}=\frac{\frac{U_{1}^{2}-U_{2}^{2}}{2}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2}}{\frac{E}{\dot{m}}}$
$U_{1}=U_{1}=U ; \frac{E}{\dot{m}}=\left(V_{u 1}-V_{u 2}\right) \mathrm{U}$
Hence, $\quad R=\frac{-\left(\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2}\right)}{\left(\overline{V_{u 1}}-\overrightarrow{v_{u 2}}\right) \mathrm{U}} ; \quad R=\frac{-\left(V_{r 1}^{2}-V_{r 2}^{2}\right)}{2\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) \mathrm{U}}$
$V_{r 1}^{2}=V_{a}^{2}+X^{2} ; \quad V_{r 1}^{2}=V_{a}^{2}+\left(V_{a} \tan \gamma_{1}\right)^{2}$
$V_{r 2}^{2}=V_{a}^{2}+Y^{2} ; \quad V_{r 2}^{2}=V_{a}^{2}+\left(V_{a} \tan \gamma_{2}\right)^{2}$
$R=\frac{-\left(\left(V_{a}^{2}+\left(V_{a} \tan \gamma_{1}\right)^{2}\right)-\left(V_{a}^{2}+\left(V_{a} \tan \gamma_{2}\right)^{2}\right)\right)}{2\left(V_{a} \tan \gamma_{0}-V_{a} \tan \gamma_{3}\right) \mathrm{U}} ; \quad \mathrm{R}=\frac{V_{a}^{2}\left(\tan ^{2} \gamma_{2}-\tan ^{2} \gamma_{1}\right)}{2 \mathrm{~V}_{\mathrm{a}}\left(\tan \gamma_{0}-\tan \gamma_{3}\right) U}$
$\mathrm{R}=\frac{V_{a}\left(\tan ^{2} \gamma_{2}-\tan ^{2} \gamma_{1}\right)}{2\left(\tan \gamma_{2}-\tan \gamma_{1}\right) U} \quad$ since, $\tan \gamma_{1}-\tan \gamma_{2}=\tan \gamma_{3}-\tan \gamma_{0}$
$\mathrm{R}=\frac{V_{a}\left(\tan \gamma_{1}+\tan \gamma_{2}\right)}{2 \mathrm{U}}$
$\gamma_{1}=180-\beta_{1} ; \tan _{1}=\tan \left(180-\beta_{1}\right) ; \tan \gamma_{1}=\cot \beta_{1}$
$\gamma_{2}=180-\beta_{1} ; \tan \gamma_{2}=\tan \left(180-\beta_{2}\right) ; \tan \gamma_{2}=\cot \beta_{2}$
Hence , $R=\frac{V_{a}\left(\cot \beta_{1}+\cot \beta_{2}\right)}{2 \mathrm{U}}$;
$R=\frac{V_{a}\left(\frac{1}{\tan \beta_{1}}+\frac{1}{\tan \beta_{2}}\right)}{2 \mathrm{U}} ; ; R=\frac{V_{a}\left(\tan \beta_{2}+\tan \beta_{1}\right)}{2 \mathrm{U}\left(\tan \beta_{1} * \tan \beta_{2}\right)}$
2. Draw the velocity triangles for axial flow compressor. From the triangles show that degree of reaction for axial flow compressor is given by $R=\frac{V_{a}}{2 U}\left(\cot \beta_{1}+\cot \beta_{2}\right)$ refer previous problem
3. With the help of inlet and outlet velocity diagrams, show that the degree of reaction for an axial flow compressor is given by $R=\frac{V_{a x}}{2 U}\left(\tan \gamma_{1}+\tan \gamma_{2}\right)$ Assume axial velocity to remain constant. $\gamma_{1}$ and $\gamma_{2}$ are angles made by relative velocities with the axial direction (4a,10, June/July13) refer solution 38
4. Draw velocity triangles for the following types of vanes of centrifugal pumps and compressors i) Backward curved vane ii) Radial vane iii) Forward curved vane (3b. 06, Dec12)
5. The total power input at a stage in an axial -flow compressor with symmetric inlet and outlet velocity triangles $(R=0.5)$ is $27.85 \mathrm{~kJ} / \mathrm{kg}$ of air flow. If the blade speed is $180 \mathrm{~m} / \mathrm{s}$ throughout the rotor, draw the velocity triangles and compute the inlet and outlet rotor blade angles Do you recommend the use of such compressors? Comment on the results you have obtained. Assume axial velocity component to be $120 \mathrm{~m} / \mathrm{s}(4 \mathrm{a}, 10$, Dec15/Jan16)
$R=0.5 ; \frac{E}{\dot{m}}=27.85 \mathrm{~kJ} / \mathrm{kg} ; \frac{E}{\dot{m}}=27850 \mathrm{~J} / \mathrm{kg} ; U=180 \mathrm{~m} / \mathrm{s} ; \beta_{1}=? ; \beta_{2}=?$;
$V_{m 1}=V_{m 2}=120 \mathrm{~m} / \mathrm{s}$


$$
\begin{aligned}
& \Delta V_{u}=\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right) \\
& -\frac{E}{\dot{m}}=\frac{\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right) \mathrm{U}}{g_{c}} ; 27850=\frac{\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right) 180}{1} ;\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right)=154.72 \mathrm{~m} / \mathrm{s} \\
& \left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right)+\mathrm{X}+\mathrm{X}=\mathrm{U} ; \quad 154.72+2 \mathrm{X}=180 ; \mathrm{X}=12.64 \mathrm{~m} / \mathrm{s} \\
& \tan \alpha_{1}=\frac{V_{m 1}}{X} ; \quad \tan \alpha_{1}=\frac{120}{12.64} ; \alpha_{1}=83.98^{\circ} \\
& \tan \beta_{1}=\frac{V_{m 1}}{U-X} ; \quad \tan \beta_{1}=\frac{120}{180-12.64} ; \beta_{1}=35.64^{\circ} \\
& \beta_{2}=\alpha_{1}=83.98^{o}
\end{aligned}
$$

6. Draw the velocity triangles at inlet and outlet of an axial flow compressor form the following data. Degree of reaction 0.5 ., inlet blade angle $45^{\circ}$, axial velocity of flow which is constant throughout $120 \mathrm{~m} / \mathrm{s}$, speed of rotation 6500 rpm , radius of rotation 20 cm , blade speed at inlet is equal to blade speed at outlet. Calculate angles at inlet and outlet. Also calculate power needed to handle $1.5 \mathrm{~kg} / \mathrm{s}$ (4b. 10, Dec14/Jan 15)
$R=0.5 ; \beta_{1}=45^{0} ; V_{m 1}=V_{m 2}=120 \mathrm{~m} / \mathrm{s} ; N=6500 \mathrm{rpm} ; R=\frac{D}{2}=0.2 \mathrm{~m} ;$
$U_{1}=U_{2} ; \beta_{2}=? \alpha_{1}=? \alpha_{2}=? E=? ; \dot{m}=1.5 \mathrm{~kg} / \mathrm{s}$


$$
\begin{aligned}
& U=\frac{\pi D N}{60} ; U=\frac{\pi x 0.4 \times 6500}{60}=136.13 \mathrm{~m} / \mathrm{s} ; \\
& \tan \beta_{1}=\frac{V_{m 1}}{U-X} ; \tan 45=\frac{120}{136.13-X} ; \quad X=16.13 \mathrm{~m} / \mathrm{s} \\
& \tan \alpha_{1}=\frac{V_{m 1}}{X} ; \tan \alpha_{1}=\frac{120}{16.13} ; \alpha_{1}=82.34^{o} \\
& \beta_{2}=\alpha_{1}=82.34^{o} \\
& -\frac{E}{\dot{m}}=\frac{\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right) \mathrm{U}}{g_{c}} \\
& \left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right)=\mathrm{U}-2 \mathrm{X} ;\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right)=136.13-(2 * 16.13) ; \\
& \left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right)=103.87 \mathrm{~m} / \mathrm{s} \\
& \frac{E}{1.5}=\frac{(103.87) 136.13}{1} ; E=21.20 * 10^{3} \mathrm{~W}
\end{aligned}
$$

7. An axial flow compressor of $50 \%$ reaction design has blades with inlet and outlet angles of $44^{\circ}$ and $13^{\circ}$ respectively. The compressor is to produce a pressure ratio 5:1 with an overall isentropic efficiency of $87 \%$ when the inlet temperature is 290 K . The mean blade speed and axial velocity are constant throughout the compressor.

Assume that blade velocity is $180 \mathrm{~m} / \mathrm{s}$ and work input factor is 0.85 , Find the number of stages required and the change of entropy (4b. 10 Dec17/Jan 2018)
$R=50 \% ; \beta_{2}=44^{\circ} ; \beta_{1}=13^{\circ} ;$
The compressor is to produce a pressure ratio of 6:1 ie $\frac{p_{k+1}}{p_{1}}=5 ; \eta_{0}=0.87 ; T_{01}=290 \mathrm{~K}$ The blade speed and axial velocity are constant throughout the compressor.
ie $U_{1}=U_{2}=U$ and $V_{a 1}=V_{a 2}=V_{a 2}$
$U=180 \mathrm{~m} / \mathrm{s} ; k=$ ? when $\Omega=0.85$


## the number of stages for work done factor is unity

$R=\frac{V_{a}\left(\tan \beta_{2}+\tan \beta_{1}\right)}{2 \mathrm{U}\left(\tan \beta_{1} * \tan \beta_{2}\right)} ;$

$$
0.5=\frac{V_{a}(\tan 44+\tan 13)}{2 * 180 *(\tan 44 * \tan 13)} ; \quad V_{a}=33.54 \mathrm{~m} / \mathrm{s}
$$

$\tan \beta_{2}=\frac{V_{a}}{Y} ; \quad Y=\overrightarrow{V_{u 1}} ;$ $\tan \beta_{2}=\frac{V_{a}}{\overline{V_{u 1}}} ;$
$\tan 44=\frac{33.54}{\overrightarrow{V_{u 1}}} ;$
$\overrightarrow{V_{u 1}}=34.73 \mathrm{~m} / \mathrm{s}$
$\overrightarrow{V_{u 2}}=U-Y$;
$\overrightarrow{V_{u 2}}=180-34.73$
$\overrightarrow{V_{u 2}}=145.26 \mathrm{~m} / \mathrm{s}$
$-\frac{E}{\dot{m}}=\frac{\Omega\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right) U}{g_{c}} ; \quad \quad$ Increase in entalphy $\Delta h_{o} /$ stage $=\frac{0.85(145.26-34.73) 180}{1}$,
$\Delta h_{o} /$ stage $=16911.09 \mathrm{~J} / \mathrm{kg}$
$\eta_{0}=\frac{\Delta h_{0 s}}{\Delta h_{0}} ; \quad \quad \eta_{0}=\frac{C_{p}\left(T_{o s k+1}-T_{01}\right)}{\Delta h_{0}} ; \quad \eta_{0}=\frac{C_{p} T_{01}\left(\frac{T_{o s k+1}}{T_{01}}-1\right)}{\Delta h_{0}}$
$\eta_{0}=\frac{C_{p} T_{01}\left(\left(\frac{p_{k+1}}{p_{1}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\Delta h_{0}} ; \quad \Delta h_{0}=\frac{C_{p} T_{01}\left(\left(\frac{p_{k+1}}{p_{1}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\eta_{0}} ;$
$\Delta h_{0}=\frac{C_{p} T_{01}\left(\left(\frac{p_{k+1}}{p_{1}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\eta_{0}} ; \quad\left(\Delta h_{0}\right)_{\text {total }}=\frac{1005 * 290\left[(5)^{0.286}-1\right]}{0.85} ; \quad\left(\Delta h_{0}\right)_{\text {total }}=200431.22 \mathrm{~J} / \mathrm{kg}$
Number of stages, $k,=\frac{\left(\Delta h_{0}\right)_{\text {total }}}{\Delta h_{o} / \text { stage }} ; \quad k=\frac{200431.22}{16911.09} ; \quad k=11.85 \quad$ say 12 stages
8. A single stage axial blower with no inlet guide vanes is running at 3600 rpm . The mean diameter of the rotor is 16 cm and the mass flow rate of air through the blower is $0.45 \mathrm{~kg} / \mathrm{s}$. In the rotor the air is turned such that the absolute velocity of air at exit makes angle of $20^{\circ}$ with respect to the axis. Assuming that the axial component of fluid remains constant, determine power input and degree of reaction. Assume that the density of air is constant at $1.185 \mathrm{~kg} / \mathrm{m}^{3}$ and area of flow is $0.02 \mathrm{~m}^{2}$ ( $4 \mathrm{~b}, 10$ Dec 13/Jan14)
axial blower ie $U_{1}=U_{2}=U$; no inlet guide vanes $\alpha_{1}=90^{\circ}$
$N=3600 \mathrm{rpm}$; The mean diameter of the rotor is $16 \mathrm{~cm}, D_{1}=D_{2}=D=0.16 \mathrm{~m}$ $\dot{m}=0.45 \mathrm{~kg} / \mathrm{s}$;
In the rotor the air is turned such that the absolute velocity of air at exit makes angle of $20^{\circ}$ with respect to the axis $\gamma_{3}=20^{\circ}$;
Assuming that the axial component of fluid remains constant $V_{f 1}=V_{f 2}=V_{f}$
$E=$ ?; $\quad R=$ ?
$\rho=1.185 \mathrm{~kg} / \mathrm{m}^{3}$; area of flow is $0.02 \mathrm{~m}^{2}$ ie $A_{f}=0.02 \mathrm{~m}^{2}$

$$
\begin{array}{lll}
U=\frac{\pi D N}{60} ; & U=\frac{\pi * 0.16 * 3600}{60} & U=30.15 \mathrm{~m} / \mathrm{s} \\
\dot{m}=\rho A_{f} V_{f} ; & 0.45=1.185 * 0.02 * V_{f} ; & V_{f}=18.98 \mathrm{~m} / \mathrm{s}
\end{array}
$$



## Power Input

$\tan \gamma_{3}=\frac{\overrightarrow{v_{u 2}}}{V_{f}} ;$
$\tan 20=\frac{\overrightarrow{V_{u 2}}}{18.98} ;$
$\overrightarrow{V_{u 2}}=6.91 \mathrm{~m} / \mathrm{s}$
$-\frac{E}{\dot{m}}=\frac{\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right) \mathrm{U}}{g_{c}} ;$
$-\frac{E}{\dot{m}}=\frac{(6.91-0) 30.15}{1} \quad-\frac{E}{\dot{m}}=208.28 \mathrm{~J} / \mathrm{kg}$
$-E=\dot{m} *\left(-\frac{E}{\dot{m}}\right) ;$

$$
-E=0.45 * 208.28 \quad-E=93.72 W
$$

Power Input= 93.72W

Degree of reaction
$\cos \gamma_{3}=\frac{V_{f}}{V_{2}} ;$
$V_{1}=V_{f} ;$
$-\frac{E}{\dot{m}}=208.28 \mathrm{~J} / \mathrm{kg}$;
$\frac{E}{\dot{m}}=-208.28 \mathrm{~J} / \mathrm{kg}$
$R=1-\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c} \frac{E}{\dot{m}}} ; \quad R=1-\frac{18.98^{2}-20.19^{2}}{2 * 1 *(-208.28)} ; \quad R=0.886$

## Radial flow Power absorbing machine

## Types of vanes in centrifugal pump:

Backward curved vane: $\boldsymbol{\beta}_{\mathbf{2}}<\mathbf{9 0}^{\boldsymbol{o}}$


Outlet velocity triangle


Inlet velocity triangle


U1

As $\beta_{2}<90^{0} \cot \beta_{2}$ is positive. Therefore as flow rate Q increases head $H_{e}$ decreases. Most preferable design

## Forward curved vane: $\boldsymbol{\beta}_{\mathbf{2}}>\mathbf{9 0}^{\circ}$



Outlet velocity triangle


Inlet velocity triangle


U1

If $\beta_{2}>90^{\circ} K_{2}$ becomes negative as $\cot \beta_{2}$ is negative. Therefore as Q increases $H_{e}$ increases This design is unstable since head goes on increases as head increases

## Radial vanes: $\boldsymbol{\beta}_{\mathbf{2}}=\mathbf{9 0}^{\boldsymbol{o}}$



Outlet velocity triangle


Inlet velocity triangle


U1
9. Draw the velocity diagram for a power absorbing radial flow turbo machine and show that

$$
R=\frac{1}{2}\left(1+\frac{V_{m 2} \cot \beta_{2}}{U_{2}}\right)(4 \mathrm{a} .10, \text { Dec } 14 / \mathrm{Jan} 15)
$$

## Radial flow compressors

Generally $\overrightarrow{V_{u 1}}=0$ (whirl velocity (tangential component) at inlet is zero) Hence Inlet velocity triangle


U1

Outlet velocity triangle


Input/per unit mass $\left(-\frac{E}{\dot{m}}\right)=\left(\overrightarrow{V_{u 2}} U_{2}-\overrightarrow{V_{u 1}} U_{1}\right)$
Input/per unit mass $\left(-\frac{E}{\dot{m}}\right)=\overrightarrow{V_{u 2}} U_{2} \quad$ as $V_{u 1}=0$
$\mathrm{U}_{2}=\overrightarrow{V_{u 2}}+Y$
$\tan \beta_{2}=\frac{V_{m 2}}{Y} ; \quad Y=V_{m 2} \cot \beta_{2} ; \quad U_{2}=\overrightarrow{V_{u 2}}+V_{a} \cot \beta_{2}$
$\overrightarrow{V_{u 2}}=U_{2}-V_{m 2} \cot \beta_{2}$
Input, $\left(-\frac{E}{\dot{m}}\right)=\left(\mathrm{U}_{2}-V_{m 2} \cot \beta_{2}\right) U_{2}$

## Degree of Reaction

$R=1-\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c} \frac{E}{\dot{m}}} \cdots \cdots-\cdots-\cdots$
$V_{1}^{2}=V_{m 1}^{2}=V_{m 2}^{2} ; \quad V_{1}^{2}-V_{2}^{2}=V_{m 2}^{2}-V_{2}^{2} ; \quad V_{2}^{2}=V_{u 2}^{2}+V_{m 2}^{2} ; \quad V_{m 2}^{2}-V_{2}^{2}=-V_{u 2}^{2}$
$V_{1}^{2}-V_{2}^{2}=-V_{u 2}^{2}-----------1$
$\frac{E}{\dot{m}}=-U_{2} \overrightarrow{V_{u 2}}$ $\qquad$
$\frac{E}{\dot{m}}=-\mathrm{U}_{2}\left(\mathrm{U}_{2}-V_{m 2} \cot \beta_{2}\right)$
Substituting 1 and 2 in A
$R=1-\frac{-V_{u 2}^{2}}{2\left(-\mathrm{U}_{2} V_{u 2}\right)} ; \quad R=1-\frac{\overrightarrow{V_{u 2}}}{2\left(\mathrm{U}_{2}\right)} ; \quad R=1-\frac{\mathrm{U}_{2}-V_{m 2} \cot \beta_{2}}{2\left(\mathrm{U}_{2}\right)} ;$
$R=1-\frac{1}{2}+\frac{V_{m 2} \cot \beta_{2}}{2\left(\mathrm{U}_{2}\right)} ; \quad \mathrm{R}=\frac{1}{2}\left(1+\frac{V_{m 2} \cot \beta_{2}}{\mathrm{U}_{2}}\right)$
10. Derive an expression for degree of reaction for radial outward flow machine and explain briefly the effect of $\beta_{2}$, balde angle at exit with repect to tangential direction ( $4 \mathrm{a}, 10$ ,june/July 17)

## Solution same as Problem number 9

11. Derive theoretical head capacity relation in case of radial flow pump (Centrifugal )
$H=U_{2}^{2}-\frac{U_{2}^{2} Q \cot \beta_{2}}{A_{2}} \beta_{2}=$ Discharge blade angle with respect to tangential direction.
Explain the effect of discharge angle on it ( $4 \mathrm{~b} .08, \frac{\text { Dec18 }}{\mathrm{Jan} 19}, 15$ scheme)

$$
H=\frac{U_{2}^{2}}{g_{c}}-\frac{U_{2}^{2} Q \cot \beta_{2}}{A_{2} g_{c}}(4 a .08, \text { June/July18, } 15 \text { scheme })
$$



Inlet velocity triangle
$\mathrm{V}_{\mathrm{u} 1}=0 ; \mathrm{V}_{\mathrm{m} 1}=\mathrm{V}_{1} ; \quad \tan \beta_{1}=\frac{V_{1}}{U_{1}}$


Outlet velocity triangle
$\overrightarrow{V_{u 2}}=U_{2}-X ; \quad \tan \beta_{2}=\frac{V_{m 2}}{X} ; \quad X=V_{m 2} \cot \beta_{2} ; \quad \overrightarrow{V_{u 2}}=U_{2}-V_{m 2} \cot \beta_{2}$
$\frac{E}{\dot{m}}=\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right)$
$\frac{E}{\dot{m}}=-\overrightarrow{V_{u 2}} U_{2}$ as $\overrightarrow{V_{u 1}}=0$
Output $=-\overrightarrow{V_{u 2}} U_{2} ; \quad-$ Output $=\overrightarrow{V_{u 2}} U_{2} ; \quad$ Input $=\overrightarrow{V_{u 2}} U_{2} ;$
$\mathrm{g} H_{e}=\mathrm{V}_{\mathrm{u} 2} \mathrm{U}_{2} ; \quad H_{e}=\frac{V_{u 2} U_{2}}{g}$
Substituting $\overrightarrow{V_{u 2}}=U_{2}-V_{m 2} \cot \beta_{2}$ in above equation
$H_{e}=\frac{\left(U_{2}-V_{m 2} \cot \beta_{2}\right) \mathrm{U}_{2}}{g} ; H_{e}=\frac{U_{2}^{2}}{g}-\frac{V_{m 2} \mathrm{U}_{2} \cot \beta_{2}}{g}--e q n 1$
$Q=A_{f} V_{f} ; \quad Q=\pi D_{2} B_{2} V_{m 2} ; \quad V_{m 2}=\frac{Q}{\pi D_{2} B_{2}}-e q n 2$
Substituting 2 in 1
$H_{e}=\frac{U_{2}^{2}}{g}-\left(\frac{Q}{\pi D_{2} B_{2}} * \frac{\mathrm{U}_{2} \cot \beta_{2}}{g}\right)$
$H_{e}=K_{1}-K_{2} Q$ where $K_{1}=\frac{U_{2}^{2}}{g}$ and $K_{2}=\frac{\mathrm{U}_{2} \cot \beta_{2}}{\pi D_{2} B_{2} g}$
Above equation is called as $\mathrm{H}-\mathrm{Q}$ characteristic equation
If $\beta_{2}<90^{\circ} K_{2}$ becomes positive as $\cot \beta_{2}$ is positive. Therefore as Q increases $H_{e}$ decreases
If $\beta_{2}>90^{\circ} K_{2}$ becomes negative as $\cot \beta_{2}$ is negative. Therefore as Q increases $H_{e}$ increases If $\beta_{2}=90^{\circ} K_{2}$ becomes zero as $\cot \beta_{2}$ is zero. Therefore as Q increases $H_{e}$ remains constant Above characteristics can be plotted as shown in fig

12. Derive head - capacity relationship for centrifugal pumps and explain the effect of discharge angle on it (4b,10, Dec16/Jan17)(4a,10,June/July14)

## Solution is same as above question 11

13. The internal and external diameters of the impeller of a centrifugal pump are 20 cm and 40 cm respectively. The pump is running at 1200 rpm . The vane angle of impeller at inlet is $20^{\circ}$. The water enters the impeller radially and velocity of flow is constant. Calculate work done by the impeller / kg of water for the following two cases
i) When vane angle at outlet is $90^{\circ}$
ii) When vane angle at outlet is $100^{\circ}(4 \mathrm{~b}, 10 \mathrm{Dec} 16 / \mathrm{Jan} 17)$
$D_{1}=0.2 \mathrm{~m} ; D_{2}=0.4 \mathrm{~m} ; N=1200 \mathrm{rpm} ; \beta_{1}=20^{\circ} ; \beta_{2}=90^{\circ} ; V_{f 1}=V_{f 2} ; \frac{E}{m}=$ ?
i) When $\beta_{2}=90^{\circ}$ ii) when $\beta_{2}=100^{\circ}$

When $\beta_{2}=90^{\circ}$
$U_{1}=\frac{\pi D_{1} N}{60} ; U_{1}=\frac{\pi * 0.2 * 1200}{60}=12.56 \mathrm{~m} / \mathrm{s} ; U_{2}=\frac{\pi D_{2} N}{60} ; U_{1}=\frac{\pi * 0.4 * 1200}{60}=25.13 \mathrm{~m} / \mathrm{s} ;$


$\frac{E}{m}=\frac{\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right)}{g_{c}} ; \overrightarrow{V_{u 1}}=0 ; \overrightarrow{V_{u 2}}=U_{2} ; \frac{E}{m}=\frac{-U_{2} U_{2}}{g_{c}} ; \frac{E}{m}=\frac{-25.13 * 25.13}{1}$
$\frac{E}{m}=-631.51 \mathrm{~J} / \mathrm{kg} ;-$ sign indicates the input to the pump
ii) When $\beta_{2}=110^{\circ}$


U1

$\tan \beta_{1}=\frac{V_{m 1}}{U_{1}} ; \tan 20=\frac{V_{m 1}}{12.56} ; V_{m 1}=4.57 \mathrm{~m} / \mathrm{s} ; V_{m 2}=V_{m 1}=4.57 \mathrm{~m} / \mathrm{s} ;$
$\overrightarrow{V_{u 1}}=0 ; \quad \overrightarrow{V_{u 2}}=U_{2}-X ; X=V_{m 2} \cot (180-100) ; X=4.57 * \cot 80 ; X=0.805 m$
$\overrightarrow{V_{u 2}}=25.13-0.805 ; \overrightarrow{V_{u 2}}=24.325 \mathrm{~m} / \mathrm{s}$;
$\frac{E}{m}=\frac{\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right)}{g_{c}} ; \overrightarrow{V_{u 1}}=0 ; ; \frac{E}{m}=\frac{-\overrightarrow{V_{u 2}} U_{2}}{g_{c}} ; \frac{E}{m}=\frac{-24.325 * 25.13}{1} ; \frac{E}{m}=-611.28 \mathrm{~J} / \mathrm{kg}$
-sign indicates the input to the pump
14. A centrifugal pump delivers water against a head of 25 m . The radial velocity of flow is $3.5 \mathrm{~m} / \mathrm{s}$ and is constant ., the flow rate of water is $0.05 \mathrm{~m}^{3} / \mathrm{s}$. The blades are radial at tip and pump runs at 1500 rpm . Determine i) Diameter at tip ii) width of blade at tip iii) inlet diffuser angle at impeller exit (4b,10, June/July16)
$H=25 \mathrm{~m} ; V_{m 2}=V_{m 1}=3.5 \mathrm{~m} / \mathrm{s} ; Q=0.05 \mathrm{~m}^{3} / \mathrm{s} ; \beta_{2}=90^{\circ} ; N=1500 \mathrm{rpm} ;$
Assuming Hydrulaic efficiency is $100 \%$

$$
-\frac{E}{\dot{m}}=g H ; \frac{E}{\dot{m}}=-9.81 * 25 ; \frac{E}{\dot{m}}=-245.25 \mathrm{~J} / \mathrm{kg}
$$



U1


$$
\frac{E}{m}=\frac{\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right)}{g_{c}} ; \quad \overrightarrow{V_{u 1}}=0 ; \quad \overrightarrow{V_{u 2}}=U_{2} ; \quad \frac{E}{m}=\frac{-U_{2} U_{2}}{g_{c}} ;
$$

$$
-245.25=-\frac{\mathrm{U}_{2}^{2}}{1} ; \quad U_{2}=15.66 \mathrm{~m} / \mathrm{s}
$$

$$
15.66=\frac{\pi D_{2} * 1500}{60} ; \quad D_{2}=0.199 \mathrm{~m}
$$

$$
Q=\pi D_{2} B_{2} V_{m 2} ; 0.05=\pi * 0.199 * B_{2} * 3.5 ; B_{2}=0.022 m
$$

## UNIT 3

## STEAM TURBINE

1. Define steam turbine. List the differences between Impulse and reaction steam turbines (5a. 08, Dec15/Jan16)(5a, 06, June/July18)
2. Briefly explain velocity compounding (5b. 08, Dec15/Jan16)
3. Derive the condition for maximum utilisation factor for impulse turbine (5a,10, June/July17)
4. Draw the inlet and exit velocity triangles for a single stage steam turbine. Further prove that maximum blade efficiency is given by

$$
\eta_{\max }=\cos ^{2} \alpha_{1}
$$

Assume $V_{r 1}=V_{r 2}$ and $\beta_{1}=\beta_{2}$ (7a. 10, June/July13) (5a. 08, June/July18,15CBCS)
5. Write a note on compounding of steam turbines and explain any two types of compounding with neat sketches (5b. 10, Dec16/Jan17) Show the velocity and pressure variations across the turbine (5a,10, Dec13/Jan14)
6. Define compounding .List different types of compounding. Explain any one method of compounding with neat sketch showing variations of pressure and velocity of steam (5a, 8,June/July18 15CBCS)
7. What is necessity of compounding of steam turbines and Discuss two types of compounding with neat sketches (5a. 10, Dec17/Jan18)what is compounding 5a. 08, Dec18/Jan19)
8. What is compounding or staging? Name the different compounding methods (5a, 04, June/July14)
9. With neat sketch, explain the pressure - velocity compounding of steam turbine (5a,08, June/July16)( 5b, 06, June/July18)
10. Show that the maximum blade efficiency $\eta_{\text {blade } \max }=\frac{2 \cos ^{2} \alpha_{1}}{1+\cos ^{2} \alpha_{1}}$ for a $50 \%$ reaction Parsons turbine (4a,10,Dec18/19) (6a,08,CBCS 15,Dec18/19)
11. For a $50 \%$ reaction turbine show that $\alpha_{1}=\beta_{2}$ and $\alpha_{2}=\beta_{1}$, where $\alpha_{1}$ and $\beta_{1}$ are the inlet angles of fixed and moving blades, $\alpha_{2}$ and $\beta_{2}$ are the outlet angles of fixed and moving blades (5a, 08 , Dec 12)

## Definition of Steam turbine(*)

Steam Turbine is is a power generating machine in which pressure energy of the steam is converted into mechanical energy due to dynamic action

Classification of steam turbine:

1. Based on working principle : a. Impulse Turbine b. Reaction turbine
2. Based on staging :a. Single stage b. Multi stage

Working Principle of Impulse turbine : The high pressure and high temperature steam generated in the steam generator is expanded in a steam nozzle or fixed blade passages and expanded steam with high velocity made to pass through the moving blades which is mounted on the shaft. In moving blades decrease in velocity and pressure of steam takes place which results in force impart on the moving blades. The resulting force rotates the rotor.

Steam turbine generally axial flow turbine $U_{1}=U_{2}=U$
Differences between Impulse and Reaction turbines(***)

| SI no | Impulse | Reaction |
| :--- | :--- | :--- |
| 1. | High Pressure and High temperature <br> steam is expanded in set of nozzle <br> and pressure energy is completely <br> converted into kinetic energy and <br> steam with high velocity directed to <br> set of moving blades where kinetic <br> energy absorbed in blades and <br> converted into impulse This impulse <br> set the blade into motion | High pressure stem is directly passed into the <br> blades and pressure of the steam continuously <br> drops and velocity increases. The steam leaving <br> the blades will exert reactive force in the <br> backward direction of flow and reactive force set <br> the blade in motion |
| 2. | Blades are symmetrical in shape | Blades are aerofoil in shape |
| 3. | The pressure of steam remains <br> constant when it flows through the <br> moving blades | The pressure of steam continuously drops when it <br> flows through the moving blades |
| 4. | Impulsive force is converted into work | Reactive force is converted into work |
| 5. | Low efficiency | Relatively high efficiency |
| 6 | High speed | Relatively low speed |
| 7. | Compact | Bulky |
| 8. | Less stages required | More stages required for the same power <br> generation |
| 9. | Used for small power generation | Used for medium and large power generation |



## Single Stage Impulse Turbine : De Laval Turbine

Working Principle: In a single stage impulse turbine high pressure steam enters set of nozzle (part of stator or casing) and expands completely in nozzle which results in conversion of pressure energy to kinetic energy. The steam with Kinetic energy made to flow through moving blades mounted on the rotor wherein change in velocity takes place which results in change in momentum takes place. This results in the rotation of rotor. There is no pressure drop as the stem flow through the passages of moving blades. Hence the relative velocity between steam and moving blades remains constant over the blades. Hence the degree of reaction is zero


Analysis on single stage Impulse turbine: (***)


Forces on the blade:

## Tangential force: (***)

$F_{t}=\frac{m\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right)}{g_{c}}$
or

$$
F_{t}=\frac{m\left(\overrightarrow{v_{u 1}}+\overleftarrow{V_{u 2}}\right)}{g_{c}}
$$

## Axial thrust:

$F_{a}=\frac{m\left(V_{f_{1}}-V_{f 2}\right)}{g_{c}}$ Newton

## Energy Per unit mass

$\frac{E}{m}=\frac{m\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) U}{g_{c}}$
J/kg Or

$$
\frac{E}{m}=\frac{m\left(\overline{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U}{g_{c}}
$$

Power
$E=\frac{m\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) U}{g_{c}} \quad$ Watts
Blade efficiency ( ${ }^{* * *}$ ): It is defined as the ratio of workdone per kg of steam by the rotor to the energy available at the inlet per kg of steam
$\eta_{b}=\frac{\text { workdone per } \mathrm{kg} \text { of steam by the rotor }}{\text { Energy available at the inlet per } \mathrm{kg} \text { of stam }}$
$\eta_{b}=\frac{\frac{E}{m}}{\frac{V_{1}^{2}}{2 g_{c}}} ; \quad \eta_{b}=\frac{\frac{m\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) U}{g_{c}}}{\frac{V_{1}^{2}}{2 g_{c}}} ; \quad \quad \eta_{b}=\frac{2\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) U}{V_{1}^{2}} \quad$ Also $\eta_{b}=\frac{2\left(\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U}{V_{1}^{2}}$

## Stage Efficiency:(***)

It is the ratio of work done per kg of steam by the rotor to the isentropic enthalpy change per kg of steam in the nozzle
$\eta_{\text {stage }}=\frac{\frac{E}{m}}{\Delta h_{0 s}}=\frac{\left(\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U}{\Delta h_{0 s}}=\frac{\left(\overrightarrow{V_{u 1}}+\overleftarrow{v_{u 2}}\right) U}{\frac{V_{1}^{2}}{2}} * \frac{\frac{V_{1}^{2}}{2}}{\Delta h_{0 s}}=\eta_{\mathrm{b}} * \eta_{\text {nozzle }}$

## Condition for maximum Efficiency (******)


$\frac{E}{m}=\left(\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U ; \quad \frac{E}{m}=U \Delta V_{u} ;$
From velocity triangle, $\Delta V_{u}=V_{\mathrm{r}_{1}} \cos \beta_{1}+V_{\mathrm{r} 2} \cos \beta_{2}$
Hence, $\frac{E}{m}=\frac{U\left(V_{r 1} \operatorname{Cos} \beta_{1}+V_{r 2} \operatorname{Cos} \beta_{2}\right)}{g_{c}} ; \quad \frac{E}{m}=\frac{U V_{r 1} \operatorname{Cos} \beta_{1}\left(1+\frac{V_{r 2} \operatorname{Cos} \beta_{2}}{V_{r_{1}} \operatorname{Cos} \beta_{1}}\right)}{g_{c}}$
$\frac{\mathrm{V}_{\mathrm{r} 2}}{V_{r_{1}}}=C_{b}$ (blade friction coefficient); $\frac{\operatorname{Cos} \beta_{2}}{\operatorname{Cos} \beta_{1}}=K$, constant
$\frac{E}{m}=\frac{U V_{r 1} \operatorname{Cos} \beta_{1}\left(1+\mathrm{C}_{\mathrm{b}} K\right)}{g_{c}} ; \quad$ But from Inlet velocity triangle, $V_{r 1} \operatorname{Cos} \beta_{1}=V_{1} \operatorname{Cos} \alpha_{1}-U$
$\frac{E}{m}=\frac{U\left(V_{1} \operatorname{Cos} \alpha_{1}-U\right)\left(1+\mathrm{C}_{\mathrm{b}} K\right)}{g_{c}}$
$\eta_{b}=\frac{\frac{E}{m}}{\frac{V_{1}^{2}}{2 g_{c}}} ; \quad \eta_{b}=\frac{\frac{U\left(V_{1} \operatorname{Cos} \alpha_{1}-U\right)\left(1+\mathrm{C}_{\mathrm{b}} K\right)}{g_{c}}}{\frac{V_{1}^{2}}{2 g_{c}}} ; \quad \eta_{\mathrm{b}}=\frac{2 U\left(V_{1} \operatorname{Cos} \alpha_{1}-U\right)\left(1+\mathrm{C}_{\mathrm{b}} K\right)}{V_{1}^{2}}$
$\eta_{b}=2 \frac{\mathrm{U}}{V_{1}} x \frac{\left(V_{1} \cos \alpha_{1}-U\right)}{V_{1}} x\left(1+\mathrm{C}_{\mathrm{b}} K\right) ; \quad \quad \eta_{\mathrm{b}}=2 \phi\left(\cos \alpha_{1}-\emptyset\right)\left(1+\mathrm{C}_{\mathrm{b}} K\right)$ where $\phi=\frac{\mathrm{U}}{V_{1}}$
For max efficiency
$\frac{\partial \eta}{\partial \phi}=0 ; \quad \frac{\partial}{\partial \phi}\left(2 \emptyset\left(\cos \alpha_{1}-\emptyset\right)\left(1+\mathrm{C}_{\mathrm{b}} K\right)\right)=0 ; \quad \frac{\partial}{\partial \phi}\left(2 \emptyset\left(\cos \alpha_{1}-\emptyset\right)\right)=0$
$\frac{\partial}{\partial \emptyset}\left(\varnothing \cos \alpha_{1}-\Phi^{2}\right)=0 ; \quad \cos \alpha_{1}-2 \emptyset=0 ; \quad \emptyset=\frac{\cos \alpha_{1}}{2}$
Substituting $\emptyset=\frac{\cos \alpha_{1}}{2}$ in $\eta_{b}=2 \phi\left(\cos \alpha_{1}-\emptyset\right)\left(1+\mathrm{C}_{\mathrm{b}} K\right)$ will give max efficiency
$\eta_{b}=2 \frac{\cos \alpha_{1}}{2}\left(\cos \alpha_{1}-\frac{\cos \alpha_{1}}{2}\right)\left(1+\mathrm{C}_{\mathrm{b}} K\right)$
$\eta_{b}=\frac{\cos ^{2} \alpha_{1}}{2}\left(1+\mathrm{C}_{\mathrm{b}} K\right)$
If rotor blade angles are equiangular
If $V_{r 1}=V_{r 2} ; \beta_{1}=\beta_{2}$
$\eta_{\text {bmax }}=\frac{\cos ^{2} \alpha_{1}}{2} * 2 ; \quad \quad \eta_{b \max }=\cos ^{2} \alpha_{1}$

## Necessity of compounding:(*****)

Single stage impulse turbine operates at very high speed.
High speeds are undesirable for the following reasons

- High speed causes high blade tip stresses due to centrifugal forces acting at the tip of blade
- Large losses due to disc friction
- Low efficiencies due to large exit steam velocity in the turbine
- Gear trains with large efficiencies and high speed ratios must be used to match between the turbine speed and the driven component speed since most driven machines run at speeds around a few thousand RPM at most

Reasonable blade tip speeds are obtained in impulse turbines by the compounding stage.

## Definition of Compounding(******)

Compounding is the method of reducing blade speed for a given overall pressure drop. Multiple rotors are mounted on common shaft in series and velocity is obsorbed in stages as it flows over the blades

## Types of Compounding(*******)

1. Velocity compounded turbine
2. Pressure compounded turbine
3. Velocity and pressure compounded turbine

Velocity compounded turbine: compounding involves in which the whole pressure drop occurs in one set of stationary blades or nozzles where as all the kinetic energy is absorbed in usually two, three or even four rows of moving blades with a row of stationary blades between every pair of them. The total energy of the stream can be absorbed by all the rows in succession until the kinetic energy at the end of last row becomes negligible.


When the steam flows through the nozzle steam expands nearly to atmospheric pressure and velocity increases.

While steam flows through moving blades velocity decreases while steam pressure remains constant While steam flows through the stationary (fixed) blades both pressure and velocity remains constant Both stationary blades and moving blades are symmetrical

The first row of the moving blades absorbs most of jet energy while latter absorbs comparatively less

## Advantages:

1. Maximum possible pressure energy is converted into kinetic energy in nozzles of first stage and there is no pressure drop in stages and hence the stress in the turbine is less
2. Fewer stages are sufficient due large kinetic energy drop compared to pressure compounding
3. Compact compared to pressure compounding

## Disadvantage:

1. The friction losses are more due to high velocity of steam

## Pressure Compounding



It is equivalent to a number of simple impulse stages put together. It is the type of compounding in which pressure drop occur in each stator row. Between the two moving blade rows there is a row of nozzles are often referred to as diaphragms.

In the row of nozzle pressure decreases and velocity increases. In rows of moving blade velocity decreases while pressure remains constant.

Advantages: High efficiency because very high velocities are avoided.
Disadvantages: Leakage loss is higher compared to velocity compounding

## Velocity and pressure compounded steam turbine




In this method high rotor speeds are reduced without sacrificing the efficiency or the output. Pressure drop from boiler pressure to the condenser pressure occurs in two stages

First and second stage taken separately are identical to a velocity compounding consists of set of nozzle and rows of moving blade fixed to the shaft and rows of fixed blades to casing in which pressure decreases and velocity increases in the nozzle. While moving through the moving blades velocity decreases while pressure remains constant where as while the steam flows through the fixed blade pressure and velocity remains constant

$\left(\frac{E}{m}\right)_{I}=\frac{U\left(\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}\right)}{g_{c}}=\frac{U *\left(\Delta V_{u}\right)_{I}}{g_{c}}$ $\qquad$
From velocity triangle for I stage, $\left(\Delta V_{u}\right)_{I}=\left(V_{r 1} \operatorname{Cos} \beta_{1}+V_{r 2} \operatorname{Cos} \beta_{2}\right)$
Hence $\left(\frac{E}{m}\right)_{I}=\frac{U\left(V_{r 1} \operatorname{Cos} \beta_{1}+V_{r 2} \operatorname{Cos} \beta_{2}\right)}{g_{c}}$
If $V_{r 1}=V_{r 2}$ and $\beta_{1}=\beta_{2}, \quad\left(\frac{E}{m}\right)_{I}=\frac{U * 2 V_{r 1} \operatorname{Cos} \beta_{1}}{g_{c}}$
But from Inlet velocity triangle of Ist stage, $V_{r 1} \operatorname{Cos} \beta_{1}=V_{1} \operatorname{Cos} \alpha_{1}-U$
$\left(\frac{E}{m}\right)_{I}=\frac{U * 2\left(V_{1} \operatorname{Cos} \alpha_{1}-U\right)}{g_{c}}$ $-1$
$\left(\frac{E}{m}\right)_{I I}=\frac{U\left(\overline{V_{u 3}}+\overline{V_{u 4}}\right)}{g_{c}}=\frac{U *\left(\Delta V_{u}\right)_{I I}}{g_{c}}$
From triangle for II stage, $\left(\Delta V_{u}\right)_{I i}=\left(V_{r 3} \operatorname{Cos} \beta_{3}+V_{r 4} \operatorname{Cos} \beta_{4}\right)$

If $V_{r 3}=V_{r 4}$ and $\beta_{3}=\beta_{4}, \quad\left(\frac{E}{m}\right)_{I}=\frac{U * 2 V_{r 3} \cos \beta_{3}}{g_{c}}$
But from Inlet velocity triangle of II stage, $V_{r 3} \operatorname{Cos} \beta_{3}=V_{3} \operatorname{Cos} \alpha_{3}-U$
$\left(\frac{E}{m}\right)_{I I}=\frac{2 U\left(V_{3} \operatorname{Cos} \alpha_{3}-U\right)}{g_{c}}$
If $V_{3}=V_{2}$ and $\alpha_{3}=\alpha_{2}, \quad\left(\frac{E}{m}\right)_{I I}=\frac{2 U\left(V_{2} \operatorname{Cos} \alpha_{2}-U\right)}{g_{c}}$
But from outlet velocity triangle of Ist stage, $V_{2} \operatorname{Cos} \alpha_{2}=V_{r 2} \operatorname{Cos} \beta_{2}-U$
$V_{r 2}=V_{r 2}$ and $\beta_{2}=\beta_{1} ;$ Hence, $V_{2} \operatorname{Cos} \alpha_{2}=V_{r 1} \operatorname{Cos} \beta_{1}-U$
Substituting above relation in $\left(\frac{E}{m}\right)_{I I}$
$\left(\frac{E}{m}\right)_{I I}=\frac{2 U\left(V_{r 1} \operatorname{Cos} \beta_{1}-U-U\right)}{g_{c}} ;$

$$
\left(\frac{E}{m}\right)_{I I}=\frac{2 U\left(V_{r 1} \operatorname{Cos} \beta_{1}-2 U\right)}{g_{c}}
$$

But from Inlet velocity triangle of Ist stage, $V_{r 1} \operatorname{Cos} \beta_{1}=V_{1} \operatorname{Cos} \alpha_{1}-U$
$\left(\frac{E}{m}\right)_{I I}=\frac{2 U\left(V_{1} \operatorname{Cos} \alpha_{1}-U-2 U\right)}{g_{c}} ;$
$\left(\frac{E}{m}\right)_{I I}=\frac{2 U\left(V_{1} \operatorname{Cos} \alpha_{1}-3 U\right)}{g_{c}}$
$\left(\frac{E}{m}\right)_{T}=\left(\frac{E}{m}\right)_{I}+\left(\frac{E}{m}\right)_{I I} ;$
$\left(\frac{E}{m}\right)_{T}=\frac{2 U\left(V_{1} \operatorname{Cos} \alpha_{1}-U\right)}{g_{c}}+\frac{2 U\left(V_{1} \operatorname{Cos} \alpha_{1}-3 U\right)}{g_{c}} ;$
$\left(\frac{E}{m}\right)_{T}=\frac{2 U\left(V_{1} \operatorname{Cos} \alpha_{1}-U+V_{1} \operatorname{Cos} \alpha_{1}-3 U\right)}{g_{c}}$
$\left(\frac{E}{m}\right)_{T}=\frac{2 U\left(2 V_{1} \operatorname{Cos} \alpha_{1}-4 U\right)}{g_{c}} ;$
$\left(\frac{E}{m}\right)_{T}=\frac{4 U\left(V_{1} \operatorname{Cos} \alpha_{1}-2 U\right)}{g_{c}}$ for 2 stages

In general form
$\left(\frac{E}{m}\right)_{T}=\frac{2 n U\left(V_{1} \operatorname{Cos} \alpha_{1}-n U\right)}{g_{c}}$ for $n$ stages
Blade efficiency
$\eta_{b}=\frac{\left(\frac{E}{m}\right)_{T}}{\frac{V_{1}^{2}}{2 g_{c}}} ;$
$\eta_{b}=\frac{\frac{4 U\left(V_{1} \operatorname{Cos} \alpha_{1}-2 U\right)}{g_{c}}}{\frac{V_{1}^{2}}{2 g_{c}}} ;$
$\eta_{b}=\frac{8 \mathrm{U}\left(\mathrm{V}_{1} \cos \alpha_{1}-2 \mathrm{U}\right)}{V_{1}^{2}}$
$\eta_{b}=\frac{8 U}{V_{1}} x \frac{\left(\mathrm{~V}_{1} \cos \alpha_{1}-2 \mathrm{U}\right)}{V_{1}} ;$
$\eta_{b}=8 \Phi x\left(\cos \alpha_{1}-2 \Phi\right)$

For max efficiency
$\frac{\partial \eta}{\partial \emptyset}=0 ; \quad \frac{\partial}{\partial \emptyset}\left(8 \Phi x\left(\cos \alpha_{1}-2 \Phi\right)\right)=0 ; \quad \frac{\partial}{\partial \emptyset}\left(\Phi \cos \alpha_{1}-2 \Phi^{2}\right)=0$
$\cos \alpha_{1}-4 \Phi=0 ; \quad \Phi=\frac{\cos \alpha_{1}}{4}$ condition for max efficiency for 2 stages
Substituting $\Phi=\frac{\cos \alpha_{1}}{4}$ in $\eta_{\mathrm{b}}=8 \Phi x\left(\cos \alpha_{1}-2 \Phi\right)$ will give max efficiency
$\eta_{\text {bmax }}=8 \frac{\cos \alpha_{1}}{4}\left(\cos \alpha_{1}-2 \frac{\cos \alpha_{1}}{4}\right) ; \quad \quad \eta_{\text {bmax }}=\cos ^{2} \alpha_{1}$

## Reaction Turbine

In the case of reaction turbine, the moving blades of a turbine are shaped in such a way that the steam expands and drops in pressure as it passes through them. As a result of pressure decrease in the moving blade, a reaction force will be produced. This force will make the

blades to rotate.

## Impulse Reaction turbine

In the impulse reaction turbine, power is generated by the combination of impulse action (Impulse force) and reaction (Reactive force) by expanding the steam in both fixed blades and moving blades. In fixed blades as velocity increases as steam expands where as in moving blades both pressure and velocity decreases. In other words in Impulse reaction turbine both pressure energy is converted into work

## Degree of Reaction

Degree of reaction defined as ratio of_static enthalpy drop to stagnation enthalpy drop in the stage
$R=\frac{\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}}{\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}} ; \quad \quad \frac{E}{m}=\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}$

For Axial flow turbine $\mathrm{U}_{1}=\mathrm{U}_{2}$
$R=\frac{-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}}{\frac{E}{m}} ; \quad \quad R=\frac{V_{r 2}^{2}-V_{r 1}^{2}}{2 \frac{E}{m}}$
Also
$R=\frac{\left(\Delta h_{0}\right)_{\text {moving blade }}}{\left(\Delta h_{0}\right)_{\text {fixed blade }}+\left(\Delta h_{0}\right)_{\text {moving blade }}}$
$\left(\Delta h_{0}\right)_{\text {fixed blade }}=\frac{V_{1}^{2}-\varphi V_{2}^{2}}{2 \eta_{n}} ;\left(\Delta h_{0}\right)_{\text {moving blade }}=\frac{V_{r 2}^{2}-\varphi V_{r 1}^{2}}{2 \eta_{n}}$
$\varphi=$ carry over factor ; $\eta_{n}=$ nozzle efficiency
Derive an expression for Degree of Reaction for axial reaction turbine(***)
$R=\frac{\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}}{\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}} ; \quad \frac{E}{m}=\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}$
For Axial flow turbine $\mathrm{U}_{1}=\mathrm{U}_{2}$
$\mathrm{R}=\frac{-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}}{\frac{E}{m}}$
$\mathrm{R}=\frac{V_{r 2}^{2}-V_{r 1}^{2}}{2 g_{c} \frac{E}{m}}-\cdots-\cdots-\cdots$
$\left(\frac{E}{m}\right)=U\left(\Delta V_{u}\right)$

$\Delta V_{u}=X+Y$
$\frac{V_{f}}{X}=\tan \beta_{1} \quad ; \frac{V_{f}}{Y}=\tan \beta_{2}$
$X=V_{f} \cot \beta_{1} ; Y=V_{f} \cot \beta_{2}$
$\Delta V_{u}=V_{f} \cot \beta_{1}+V_{f} \cot \beta_{2}$
$\left(\frac{E}{m}\right)=\frac{U\left(V_{f} \cot \beta_{1}+V_{f} \cot \beta_{2}\right)}{g_{c}} ;$
$\left(\frac{E}{m}\right)=\frac{U\left(\cot \beta_{1}+\cot \beta_{2}\right) V_{f}}{g_{c}} \ldots-\cdots-\cdots-\cdots$
$\frac{V_{f}}{V_{r 1}}=\sin \beta_{1} ; \quad V_{r 1}=V_{f} \operatorname{cosec} \beta_{1} \quad \frac{V_{f}}{V_{r 2}}=\sin \beta_{2} \quad V_{r 2}=V_{f} \operatorname{cosec} \beta_{2}$
Substituting 1 and 2 in equation $A$
$R=\frac{\left(V_{f} \operatorname{cosec} \beta_{2}\right)^{2}-\left(V_{f} \operatorname{cosec} \beta_{1}\right)^{2}}{2 \mathrm{U}\left(\cot \beta_{1}+\cot \beta_{2}\right) V_{f}} ;$
$R=\frac{\mathrm{V}_{\mathrm{f}}^{2}\left(\operatorname{cosec}^{2} \beta_{2}-\operatorname{cosec}^{2} \beta_{1}\right)}{2 \mathrm{U}\left(\cot \beta_{1}+\cot \beta_{2}\right) \mathrm{V}_{\mathrm{f}}} ; \quad R=\frac{V_{f}\left(1+\cot ^{2} \beta_{2}-\left(1+\cot ^{2} \beta_{1}\right)\right)}{2 \mathrm{U}\left(\cot \beta_{1}+\cot \beta_{2}\right)} ; \quad R=\frac{V_{f}\left(\cot ^{2} \beta_{2}-\cot ^{2} \beta_{2}\right)}{2 \mathrm{U}\left(\cot \beta_{1}+\cot \beta_{2}\right)}$
$R=\frac{V_{f}\left(\cot \beta_{1}+\cot \beta_{2}\right)\left(\cot \beta_{2}-\cot \beta_{1}\right)}{2 U\left(\cot \beta_{1}+\cot \beta_{2}\right)} ; \quad R=\frac{V_{f}\left(\cot \beta_{2}-\cot \beta_{1}\right)}{2 \mathrm{U}} ; \quad R=\frac{V_{f}}{2 \mathrm{U}}\left(\cot \beta_{2}-\cot \beta_{1}\right)$
$R=\frac{V_{f}}{2 \mathrm{U}}\left(\frac{1}{\tan \beta_{2}}-\frac{1}{\tan \beta_{1}}\right) ; \quad R=\frac{V_{f}}{2 \mathrm{U}}\left(\frac{\tan \beta_{1}-\tan \beta_{2}}{\tan \beta_{1} \cdot \tan \beta_{2}}\right)$

## Condition for $50 \%$ reaction turbine $\left({ }^{* * * * * *)}\right.$

$R=\frac{V_{f}}{2 \mathrm{U}}\left(\cot \beta_{2}-\cot \beta_{1}\right)$
For $50 \%$ reaction $R=\frac{1}{2}$
$\frac{1}{2}=\frac{V_{f}}{2 \mathrm{U}}\left(\cot \beta_{2}-\cot \beta_{1}\right) ; \quad U=V_{f}\left(\cot \beta_{2}-\cot \beta_{1}\right)------------1$
From Inlet velocity triangle
$R=\mathrm{V}_{\mathrm{u} 1}-\mathrm{X}$
But $\quad \tan \beta_{1}=\frac{V_{f}}{X} ; \quad X=V_{f} \cot \beta_{1}$
$\tan \alpha_{1}=\frac{V_{f}}{V_{u 1}} ; \quad V_{u 1}=V_{f} \cot \alpha_{1}$
Hence, $\mathrm{U}=V_{f} \cot \alpha_{1}-V_{f} \cot \beta_{1}$
$U=V_{f}\left(\cot \alpha_{1}-\cot \beta_{1}\right)----------2$
1=2; $\quad V_{f}\left(\cot \beta_{2}-\cot \beta_{1}\right)=V_{f}\left(\cot \alpha_{1}-\cot \beta_{1}\right) ; \quad \cot \beta_{2}=\cot \alpha_{1} ; \quad \boldsymbol{\beta}_{2}=\boldsymbol{\alpha}_{1}$
From outlet velocity triangle
$U=Y-\overrightarrow{V_{u 1}}$
But $\quad \tan \beta_{2}=\frac{V_{f}}{Y} ; \quad Y=V_{f} \cot \beta_{2} ; \quad \tan \alpha_{2}=\frac{V_{f}}{V_{u 2}} ; \overleftarrow{V_{u 2}}=V_{f} \cot \alpha_{2}$
Hence, $U=V_{f} \cot \beta_{2}-V_{f} \cot \alpha_{2} ; \quad U=V_{f}\left(\cot \beta_{2}-\cot \alpha_{2}\right)-----------3$
$1=3 ; \quad V_{f}\left(\cot \beta_{2}-\cot \beta_{1}\right)=V_{f}\left(\cot \beta_{2}-\cot \alpha_{2}\right) ; \quad \cot \beta_{1}=\cot \alpha_{2} ; \quad \boldsymbol{\beta}_{1}=\boldsymbol{\alpha}_{\mathbf{2}}$
Hence in $50 \%$ reaction turbine
$\beta_{2}=\alpha_{1} ; \quad \beta_{1}=\alpha_{2}$
Hence both Inlet and Outlet triangle in 50\% Reaction turbine are symmetrical
Hence $\mathbf{V}_{\mathrm{r} 1}=\mathrm{V}_{2} ; \mathrm{V}_{\mathrm{r} 2}=\mathrm{V}_{1}$

## Efficiency of 50\% reaction turbine(***)

$\eta=\frac{\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}}{\frac{V_{1}^{2}}{2 g_{c}}+\frac{U_{1}^{2}-U_{2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}}=\frac{\frac{E}{m}}{\frac{V_{1}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}}$
$\eta=\frac{\frac{E}{m}}{\frac{V_{1}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}}}--$ eqn A as $U_{1}=U_{2}=U$ for axial flow turbine
$\frac{E}{m}=\frac{U\left(\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}\right)}{g_{c}}$

$\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}=V_{1} \cos \alpha_{1}+V_{2} \cos \alpha_{2}$
$\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}=V_{1} \cos \alpha_{1}+V_{r 1} \cos \beta_{1}$
But $V_{r 1} \cos \beta_{1}=V_{1} \cos \alpha_{1}-U$
$\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}=V_{1} \cos \alpha_{1}+\mathrm{V}_{1} \cos \alpha_{1}-\mathrm{U}$
$\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}=2 V_{1} \cos \alpha_{1}-U$
$\frac{E}{m}=\frac{\mathrm{U}\left(2 V_{1} \cos \alpha_{1}-\mathrm{U}\right)}{g_{c}}$
$\frac{E}{m}=\frac{2 V_{1} U \cos \alpha_{1}-U^{2}}{g_{c}}$
$\frac{E}{m}=\frac{V_{1}^{2}\left(\frac{2 U \cos \alpha_{1}}{V_{1}}-\frac{U^{2}}{V_{1}^{2}}\right)}{g_{c}}$
But $\frac{U}{V_{1}}$ speed ratio $\Phi$
$\frac{E}{m}=\frac{V_{1}^{2}\left(2 \Phi \cos \alpha_{1}-\Phi^{2}\right)}{g_{c}}$ $\qquad$
$\frac{V_{1}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 g_{c}} ; \quad \frac{V_{1}^{2}}{2 g_{c}}+\frac{V_{r 2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}}{2 g_{c}}$
$V_{r 2}=V_{1}(50 \% \mathrm{R})$
$\frac{V_{1}^{2}}{2 g_{c}}+\frac{V_{1}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}}{2 g_{c}} ;$

$$
\frac{V_{1}^{2}}{g_{c}}-\frac{V_{r_{1}^{2}}^{2}}{2 g_{c}}--1
$$

From outlet velocity triangle and applying cosine rule $V_{r 1}^{2}=V_{1}^{2}+U^{2}-2 V_{1} U \cos \alpha_{1}$

Hence, eqn 1 becomes

$$
\frac{V_{1}^{2}}{g_{c}}-\frac{V_{1}^{2}+U^{2}-2 V_{1} U \cos \alpha_{1}}{2 g_{c}} ;
$$

$\frac{V_{1}^{2}}{2 g_{c}}+\frac{V_{r 2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}}{2 g_{c}}=\frac{V_{1}^{2}}{g_{c}}-\frac{V_{1}^{2}+U^{2}-2 V_{1} U \cos \alpha_{1}}{2 g_{c}} ; \quad \frac{V_{1}^{2}}{2 g_{c}}+\frac{V_{r 2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}}{2 g_{c}}=\frac{V_{1}^{2}}{g_{c}}-\frac{V_{1}^{2}}{2 g_{c}}-\frac{U^{2}}{2 g_{c}}+\frac{2 V_{1} U \cos \alpha_{1}}{2 g_{c}}$
$\frac{V_{1}^{2}}{2 g_{c}}+\frac{V_{r 2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}}{2 g_{c}}=\frac{V_{1}^{2}}{2}-\frac{U^{2}}{2}+\frac{2 V_{1} U \cos \alpha_{1}}{2}$
$\frac{V_{1}^{2}}{2 g_{c}}+\frac{V_{r 2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}}{2}=\frac{V_{1}^{2}}{2 g_{c}}\left(1-\frac{U^{2}}{V_{1}^{2}}+\frac{2 V_{1} U \cos \alpha_{1}}{V_{1}^{2}}\right)$
$\frac{V_{1}^{2}}{2 g_{c}}+\frac{V_{r 2}^{2}}{2 g_{c}}-\frac{V_{r 1}^{2}}{2 g_{c}}=\frac{V_{1}^{2}}{2 g_{c}}\left(1-\Phi^{2}+2 \Phi \cos \alpha_{1}\right)$
$\eta_{b}=\frac{\frac{V_{1}^{2}\left(2 \Phi \cos \alpha_{1}-\Phi^{2}\right)}{g_{c}}}{\frac{V_{1}^{2}}{2 g_{c}}\left(1-\Phi^{2}+2 \Phi \cos \alpha_{1}\right)} ; \quad \eta_{b}=\frac{2\left(2 \Phi \cos \alpha_{1}-\Phi^{2}\right)}{\left(1-\Phi^{2}+2 \Phi \cos \alpha_{1}\right)}$
$\eta_{b}=\frac{2\left(2 \Phi \cos \alpha_{1}-\Phi^{2}+1-1\right)}{\left(1-\Phi^{2}+2 \Phi \cos \alpha_{1}\right)} ; \quad \eta_{b}=\frac{2\left(2 \Phi \cos \alpha_{1}-\Phi^{2}+1\right)-2}{\left(1-\Phi^{2}+2 \Phi \cos \alpha_{1}\right)} ; \quad \eta_{b}=2-\frac{2}{\left(1-\Phi^{2}+2 \Phi \cos \alpha_{1}\right)}$
for max efficiency
$\frac{\partial \eta_{b}}{\partial \varnothing}=0$
$\frac{\partial}{\partial \phi}\left(2-\frac{2}{\left(1-\Phi^{2}+2 \Phi \cos \alpha_{1}\right)}\right)=0 ;$
$\frac{\partial}{\partial \emptyset}\left(\frac{2}{\left(1-\Phi^{2}+2 \Phi \cos \alpha_{1}\right)}\right)=0$
$\frac{\partial}{\partial \emptyset}\left(1-\Phi^{2}+2 \Phi \cos \alpha_{1}\right)=0 ; \quad 0-2 \Phi+2 \cos \alpha_{1}=0 ; \quad 2 \Phi=2 \cos \alpha_{1} ; \quad \Phi=\cos \alpha_{1}$
$\Phi=\cos \alpha_{1}$ condition for max efficiency for 2 stages

## Substituting

$\Phi=\cos \alpha_{1}$ in $\eta_{b}=2-\frac{2}{\left(1-\Phi^{2}+2 \Phi \cos \alpha_{1}\right)}$
will give max efficiency
$\eta_{b \max }=2-\frac{2}{\left(1-\cos ^{2} \alpha_{1}+2 \cos \alpha_{1} \cos \alpha_{1}\right)}$
$\eta_{\text {bmax }}=2-\frac{2}{\left(1+\cos ^{2} \alpha_{1}\right)}$
$\eta_{b \max }=\frac{2\left(1+\cos ^{2} \alpha_{1}\right)-2}{\left(1+\cos ^{2} \alpha_{1}\right)}$
$\eta_{b \max }=\frac{2 \cos ^{2} \alpha_{1}}{\left(1+\cos ^{2} \alpha_{1}\right)}$

## Numerical Problems

1. The following data refers to Delaval turbine. Velocity of steam at exit of the nozzle is $1000 \mathrm{~m} / \mathrm{s}$ with a nozzle angle $20^{\circ}$. The blade velocity is $400 \mathrm{~m} / \mathrm{s}$ and blades are equiangular. Assume a mass flow rate of $1000 \mathrm{~kg} / \mathrm{hr}$, friction coefficient 0.8 , nozzle efficiency is 0.95 , calculate i) blade angles ii) Work done /per of steam iii) Power developed iv) Blade efficiency v) Stage efficiency (5b. 10, June/July17) (5b. 10, Dec14/Jan15)

## Given Data:

Delaval turbine is Impulse turbine
le $R=0 \quad$ and $U_{1}=U_{2}=U$

- Velocity of steam from nozzle $=V_{1}=1000 \mathrm{~m} / \mathrm{s}$, nozzle angle $=\alpha_{1}=20^{\circ}$
- the rotor blades are equiangular ie $\beta_{1}=\beta_{2}$
- Tangential speed $=U=400 \mathrm{~m} / \mathrm{s}$,
- $\dot{m}=1000 \mathrm{~kg} / \mathrm{hr} ; \dot{m}=0.28 \mathrm{~kg} / \mathrm{s}$
- friction coefficient 0.8 ie $\frac{V_{r 2}}{V_{r 1}}=0.8$
- $\quad \eta_{\text {nozzle }}=0.95$
- To determine
i) Rotor blade angle $\beta_{1}=$ ?, $\beta_{2}=$ ?., ii) $E=$ ?iii) $\eta_{\text {blade }}=$ ? iv) $\eta_{\text {stage }}$ ?

Inlet Velocity Triangle


## Blade angles

## From inlet velocity triangle

$\overrightarrow{V_{u 1}}=V_{1} \cos \alpha_{1} ; \quad \overrightarrow{V_{u 1}}=1000 \cos 20 ; \quad \quad \overrightarrow{V_{u 1}}=939.69 \mathrm{~m} / \mathrm{s}$
$V_{m 1}=V_{1} \operatorname{Sin} \alpha_{1} \quad V_{m 1}=1000 \sin 20 ; \quad V_{m 1}=342.02 \mathrm{~m} / \mathrm{s}$
$\tan \beta_{1}=\frac{V_{m 1}}{V_{u 1}-U} ; \quad \tan \beta_{1}=\frac{342.02}{939.69-400} ; \beta_{1}=32.36^{\circ}$
$\beta_{1}=\beta_{2}$ (blades are equiangular); $\beta_{2}=32.36^{\circ}$

## Work done /per of steam

$\sin \beta_{1}=\frac{V_{m 1}}{V_{r 1}} ; \sin 32.36=\frac{342.02}{V_{r 1}} ; V_{r 1}=639 \mathrm{~m} / \mathrm{s}$
$\frac{V_{r 2}}{V_{r 1}}=0.8 ; \quad V_{r 2}=0.8 ; \quad V_{r 2}=511.2 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}=511.2 \cos 32.36 ; V_{r 2} \cos \beta_{2}=431.81 ; \quad U=400 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}>U$, Hence, Outlet velocity triangle as given below


From outlet velocity triangle
$\overleftarrow{V_{u 2}}=V_{r 2} \cos \beta_{2}-U ; \quad \overleftarrow{V_{u 2}}=431.81-400 ; \quad \overleftarrow{V_{u 2}}=31.81 \mathrm{~m} / \mathrm{s}$

## Power:

$\frac{E}{\dot{m}}=\frac{\left(\overline{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U}{g_{c}} ; \quad \frac{E}{\dot{m}}=\frac{(939.69+31.81) 400}{1} ; \quad \frac{E}{\dot{m}}=388600 \mathrm{~J} / \mathrm{kg}$

$$
E=\dot{m} \frac{E}{\dot{m}} ; \quad E=0.28 * 388600 ; \quad E=108808 \mathrm{~W} ; E=108.808 \mathrm{~kW}
$$

## Blade efficiency

$\eta_{b}=\frac{\frac{E}{\dot{m}}}{\frac{V_{1}^{2}}{2 g_{c}}} ; \quad \eta_{b}=\frac{388600}{\frac{1000^{2}}{2}} ; \quad \eta_{b}=0.772$

## Stage Efficiency:

$\eta_{\text {stage }}=\eta_{b} \eta_{\text {nozzle }} ; \quad \eta_{\text {stage }}=0.7772 * 0.95 \quad \eta_{\text {stage }}=0.7383$
ii) Tangential force

Tangential force,$F_{u}=\dot{m}\left(\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}\right) ; \quad F_{u}=0.28(939.69+31.81) ; \quad F_{u}=272.02 \mathrm{~N}$
Axial thrust : $F_{a}=\dot{m}\left(V_{m 1}-V_{m 2}\right)$
$\operatorname{Sin} \beta_{2}=\frac{V_{m 2}}{V_{r 2}} ; \quad \operatorname{Sin} 32.36=\frac{V_{m 2}}{511.2} ; \quad V_{m 2}=273.61 \mathrm{~m} / \mathrm{s}$
$F_{a}=\dot{m}\left(V_{m 1}-V_{m 2}\right) ; \quad F_{a}=0.28(342.02-273.61) F_{a}=19.15 N$

## Graphical solution



Scale $1 \mathrm{~cm}=100 \mathrm{~m} / \mathrm{s}$

1. $U=400 \mathrm{~m} / \mathrm{s} ; U=4 \mathrm{~cm} ; 2 . \quad V_{1}=1000 \mathrm{~m} / \mathrm{s} ; \quad V_{1}=10 \mathrm{~cm} \alpha_{1}=20^{0}$
2. Complete triangle (right side) 4. Measure $V_{r 1}$ and $\beta_{1}$ ie $V_{r 1}=63.89 \mathrm{~mm} \beta_{1}=32^{0}$
3. $V_{r 2}=0.8 V_{r 1} V_{r 2}=0.8 * 63.89=51.11 \mathrm{~mm} ; \quad \beta_{2}=\beta_{1}$ (blades are equianglular) $\beta_{2}=32^{0}$
4. Draw $V_{r 2}=51.11 \mathrm{~mm}$ at an angle $\beta_{2}=32^{0}$ measuring from right and complete right triangle
5. Measure $\Delta V_{u}$ ie $\Delta V_{u}=9.731 \mathrm{~cm}$ ie $\Delta V_{u}=973.1 \mathrm{~m} / \mathrm{s} ; V_{m 1}=3.42 \mathrm{~cm}$ ie $V_{m 1}=\frac{342 \mathrm{~m}}{\mathrm{~s}}$
$V_{m 2}=2.708 \mathrm{~cm}=270.8 \mathrm{~m} / \mathrm{s}$

## Calculation

## Power

$$
\begin{aligned}
& \frac{E}{\dot{m}}=\frac{\left(\overrightarrow{V_{u 1}}+\widehat{V_{u 2}}\right) U}{g_{c}} ; \quad \frac{E}{\dot{m}}=\frac{\Delta V_{u} U}{g_{c}} \frac{E}{\dot{m}}=\frac{973.1 * 400}{1} ; \quad \frac{E}{\dot{m}}=389240 \mathrm{~J} / \mathrm{kg} \\
& E=\dot{m} \frac{E}{\dot{m}} ; \quad E=0.28 * 389240 ; E=108987 \mathrm{~W} ; E=108.987 \mathrm{~kW}
\end{aligned}
$$

## Blade efficiency

$\eta_{b}=\frac{\frac{E}{\dot{m}}}{\frac{V_{1}^{2}}{2 g_{c}}} \quad \quad \eta_{b}=\frac{389240}{\frac{1000^{2}}{2}} ; \quad \eta_{b}=0.778$

## Stage Efficiency:

$\eta_{\text {stage }}=\eta_{b} \eta_{\text {nozzle }} ; \quad \eta_{\text {stage }}=0.778 * 0.95 \quad \eta_{\text {stage }}=0.739$
10\% Difference between theoretical and graphical solution is permitted
2. Steam issues from a nozzle of a Delaval turbine with a of $1200 \mathrm{~m} / \mathrm{s}$. The nozzle angle is $20^{\circ}$. The blade speedy is $400 \mathrm{~m} / \mathrm{s}$. The inlet and outlet blades are equal. Assume a mass flow rate of $1000 \mathrm{~kg} / \mathrm{hr}$, calculate i) blade angles ii) relative velocities of blade entering ii) Axial thrust iii) Power developed iv) Blade efficiency Assume K=0.8 (5b. 10, Dec18/Jan19)
3. Steam issues from a nozzle of a Delaval turbine with a of $1000 \mathrm{~m} / \mathrm{s}$. The nozzle angle is $20^{\circ}$. The blade speedy is $400 \mathrm{~m} / \mathrm{s}$. The inlet and outlet blades are equal. Assume a mass flow rate of $900 \mathrm{~kg} / \mathrm{hr}$, calculate i) blade angles ii) relative velocities if blade velocity coefficient is 0.8 ii) Tangential force on the blades iii) Power developed iv) Blade efficiency (5b. 10, Dec17/Jan18)
4. The data pertaining to an impulse turbine is as follows: Steam velocity $=500 \mathrm{~m} / \mathrm{s}$, blade speed $=200 \mathrm{~m} / \mathrm{s}$, exit angle at moving blade $=25^{\circ}$ measured from tangential direction, nozzle angle $=20^{\circ}$. Neglecting the effect of friction when passing through blade passages, calculate : i) Inlet angle of moving blade ii) Exit velocity and direction iii) Work done per kg of steam iv) Power developed v) Diagram efficiency (5b,16, June/July14)
$V_{1}=500 \mathrm{~m} / \mathrm{s} ; U=200 \mathrm{~m} / \mathrm{s} ; \beta_{2}=25^{\circ}$; Nozzle angle $=20^{\circ}$ ie $\alpha_{1}=20^{\circ}$
Neglecting the effect of friction when passing through blade passages, $V_{r 1}=V_{r 2}$
Inlet blade angle $\beta_{1}$

$$
\overrightarrow{V_{u 1}}=V_{1} \cos \alpha_{1} ; \quad \overrightarrow{V_{u 1}}=500 \cos 20 ; \quad \overrightarrow{V_{u 1}}=469.85 \mathrm{~m} / \mathrm{s}
$$


$V_{m 1}=V_{1} \operatorname{Sin} \alpha_{1} \quad V_{m 1}=500 \sin 20 ; \quad V_{m 1}=171.01 \mathrm{~m} / \mathrm{s}$
$\tan \beta_{1}=\frac{V_{m 1}}{V_{u 1}-U} ; \quad \tan \beta_{1}=\frac{171.01}{469.85-200} ; \beta_{1}=32.36^{\circ}$

## Exit velocity and direction

$\beta_{2}=25^{\circ}$ (given)
$\sin \beta_{1}=\frac{V_{m 1}}{V_{r 1}} \quad ; \quad \sin 32.36=\frac{171.01}{V_{r 1}} ; V_{r 1}=319.50 \mathrm{~m} / \mathrm{s}$
$V_{r 2}=V_{r 1} ; \quad ; \quad V_{r 2}=319.50 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}=319.50 \cos 25 ; V_{r 2} \cos \beta_{2}=289.56 ; \quad U=200 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}>U$, Hence, Outlet velocity triangle as given below


## From outlet velocity triangle

$\overleftarrow{V_{u 2}}=V_{r 2} \cos \beta_{2}-U ; \quad \overleftarrow{V_{u 2}}=289.56-200 ; \quad \overleftarrow{V_{u 2}}=89.56 \mathrm{~m} / \mathrm{s}$
$\operatorname{Sin} \beta_{2}=\frac{V_{m 2}}{V_{r 2}} ; \quad \operatorname{Sin} 25=\frac{V_{m 2}}{319.50} ; \quad V_{m 2}=135.02 \mathrm{~m} / \mathrm{s}$
$V_{2}^{2}=V_{u 2}^{2}+V_{m 2}^{2} ; \quad V_{2}=\sqrt{V_{u 2}^{2}+V_{m 2}^{2}} ; \quad V_{2}=\sqrt{89.56^{2}+135.02^{2}} ; \quad V_{2}=162.02 \mathrm{~m} / \mathrm{s}$
$\tan \alpha_{2}=\frac{V_{m 2}}{V_{u 2}} ; \quad \quad \tan \alpha_{2}=\frac{135.02}{89.56} ; \quad \alpha_{2}=56.44^{\circ}$

## Work done /kg of steam

$\frac{E}{\dot{m}}=\frac{\left(\overline{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U}{g_{c}} ; \quad \frac{E}{\dot{m}}=\frac{(469.85+89.56) 200}{1} ; \quad \frac{E}{\dot{m}}=111882 \mathrm{~J} / \mathrm{kg}$

## Power

Assume_ $\dot{m}=1 \mathrm{~kg} / \mathrm{s}$

$$
E=\dot{m} \frac{E}{\dot{m}} ; \quad E=1 * 111882 ; \quad E=111882 W ; E=111.882 k W
$$

## Diagram efficiency

$\eta_{b}=\frac{\frac{E}{\dot{m}}}{\frac{V_{1}^{2}}{2 g_{c}}} ; \quad \eta_{b}=\frac{111882}{\frac{500^{2}}{2}} ; \quad \eta_{b}=0.895$

## Tangential force

Tangential force , $F_{u}=\dot{m}\left(\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}\right) ; F_{u}=1(469.85+89.56) ; \quad F_{u}=559.41 \mathrm{~N}$
Axial thrust : $F_{a}=\dot{m}\left(V_{m 1}-V_{m 2}\right)$
$F_{a}=\dot{m}\left(V_{m 1}-V_{m 2}\right) ; \quad F_{a}=1(171.01-135.02) \quad F_{a}=35.99 \mathrm{~N}$
5. The following particulars refer to a single impulse turbine. Mean diameter of blade ring $=2.5 \mathrm{~m}$, speed $=3000 \mathrm{rpm}$. Nozzle angle $20^{\circ}$, ratio of blade velocity to steam $=0.4$, blade friction factor $=0.8$, blade angle at exit is $3^{\circ}$ less than that at inlet. Steam flow rate $36000 \mathrm{~kg} / \mathrm{hr}$. Draw the velocity diagram and calculate i) power developed ii) blade efficiency ( 5b. 08, Dec18/Jan19 CBCS)
Mean diameter of blade ring $=2.5 \mathrm{~m} D_{1}=D_{1}=D=2.5 \mathrm{~m} ; ~ N=3000 \mathrm{rpm} ; \alpha_{1}=20^{0}$ ratio of blade velocity to steam $=0.4$ ie $\frac{U}{V_{1}}=0.4$; blade friction factor $=0.8$ ie $\frac{V_{r 2}}{V_{r 1}}=0.8$
blade angle at exit is $3^{\circ}$ less than that at inlet ie $\beta_{2}=\beta_{1}-3 ; \quad \dot{m}=36000 \mathrm{~kg} / \mathrm{hr}, \dot{m}=10 \mathrm{~kg} / \mathrm{s}$
$E=? ; \quad \eta_{b}=$ ?

## Power

$U=\frac{\pi D N}{60} ; \quad U=\frac{\pi * 2.5 * 3000}{60} ; \quad U=392.7 \mathrm{~m} / \mathrm{s}$
$\frac{U}{V_{1}}=0.4 ; \quad \frac{392.69}{V_{1}}=0.4 ; \quad V_{1}=981.75 \mathrm{~m} / \mathrm{s}$
$\overline{V_{u 1}}=V_{1} \cos \alpha_{1} ; \quad \overline{V_{u 1}}=981.75 \cos 20 ; \quad \quad \overline{V_{u 1}}=922.54 \mathrm{~m} / \mathrm{s}$

$V_{m 1}=V_{1} \operatorname{Sin} \alpha_{1} \quad V_{m 1}=981.75 \sin 20 ; \quad V_{m 1}=335.78 \mathrm{~m} / \mathrm{s}$
$\tan \beta_{1}=\frac{V_{m 1}}{\overline{V_{u 1}}-U} ; \quad \tan \beta_{1}=\frac{335.78}{922.54-392.7} \quad ; \quad \beta_{1}=32.36^{\circ}$
$\beta_{2}=\beta_{1}-3 ; \quad \beta_{2}=32.36-3 ; \quad \beta_{2}=29.36$
$\sin \beta_{1}=\frac{V_{m 1}}{V_{r 1}} \quad ; \sin 32.36=\frac{335.78}{V_{r 1}} ; V_{r 1}=627.34 \mathrm{~m} / \mathrm{s}$
$\frac{V_{r 2}}{V_{r 1}}=0.8 ; \quad \frac{V_{r 2}}{627.35}=0.8 ; \quad V_{r 2}=501.88 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}=501.88 \cos 29.36 ; V_{r 2} \cos \beta_{2}=437.42 ; U=392.7 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}>U$, Hence, Outlet velocity triangle as given below

$\overleftarrow{V_{u 2}}=V_{r 2} \cos \beta_{2}-U ; \overleftarrow{V_{u 2}}=437.42-392.7 ; \quad \overleftarrow{V_{u 2}}=44.71 \mathrm{~m} / \mathrm{s}$
$\frac{E}{\dot{m}}=\frac{\left(\overline{V_{u 1}}+\overline{V_{u 2}}\right) U}{g_{c}} ; \quad \frac{E}{\dot{m}}=\frac{(922.54+44.71) 392.7}{1} ; \quad \frac{E}{\dot{m}}=379841.15 \mathrm{~J} / \mathrm{kg}$
$\dot{m}=10 \mathrm{~kg} / \mathrm{s} ; \quad E=\dot{m} \frac{E}{\dot{m}} ; \quad E=10 * 379841.15 ; \quad E=3798411.5 \mathrm{~W} ; E=3798.41 \mathrm{~kW}$

## Blade Efficiency

$\eta_{b}=\frac{\frac{E}{\dot{m}}}{\frac{V_{1}^{2}}{2 g_{c}}} ; \quad \eta_{b}=\frac{379841.15}{\frac{981.75^{2}}{2}} ; \quad \eta_{b}=0.788$
6. In a single stage impulse turbine the mean diameter of blades is 1 m . It runs at 3000 rpm . The steam is supplied from a nozzle at a velocity of $350 \mathrm{~m} / \mathrm{s}$ and the nozzle angle is $20^{\circ}$. The rotor blades are equianglular. The blade friction factor is 0.86 . Draw the velocity diagram and calculate the power developed if the axial thrust is 117.72 Newtons ( $5 b, 10$, Dec13/Jan14) (5c,08, June/July18)
7. In a single stage impulse turbine the mean diameter of blades is 80 cm . It runs at 3000 rpm . The steam issues from a nozzle with a velocity of $300 \mathrm{~m} / \mathrm{s}$ and the nozzle angle $20^{\circ}$. The rotor blades are equiangular. The blade velocity coefficient is 0.85 . what is the power developed when the axial thrust is 140 Newtons (6b,08, June/July,15,18CBCS)

Mean diameter of blades $=80 \mathrm{~cm} \quad D_{1}=D_{1}=D=0.8 \mathrm{~m} ; N=3000 \mathrm{rpm} ; V_{1}=300 \mathrm{~m} / \mathrm{s} ; \alpha_{1}=$ $20^{0}$

The rotor blades are equiangular. $\beta_{2}=\beta_{1}$; blade friction factor $=0.85$ ie $\frac{V_{r 2}}{V_{r 1}}=0.85$ $E=?$; The axial thrust is 140 Newtons ie $F_{a}=140 \mathrm{~N}$

## Inlet blade angle $\beta_{1}$

$\overrightarrow{V_{u 1}}=V_{1} \cos \alpha_{1} ; \quad \quad \overrightarrow{V_{u 1}}=300 \cos 20 ; \quad \quad \overrightarrow{V_{u 1}}=281.91 \mathrm{~m} / \mathrm{s}$
$U=\frac{\pi D N}{60} ; \quad U=\frac{\pi * 0.8 * 3000}{60} ; \quad U=125.66 \mathrm{~m} / \mathrm{s}$

$V_{m 1}=V_{1} \operatorname{Sin} \alpha_{1} \quad V_{m 1}=300 \sin 20 ; \quad V_{m 1}=102.61 \mathrm{~m} / \mathrm{s}$
$\tan \beta_{1}=\frac{V_{m 1}}{V_{u 1}-U} ; \quad \tan \beta_{1}=\frac{102.61}{281.91-125.66} ; \beta_{1}=33.29^{\circ}$
$\beta_{2}=\beta_{1} ; \quad \beta_{2}=33.29^{\circ}$
$\sin \beta_{1}=\frac{V_{m 1}}{V_{r 1}} ; \quad \sin 33.29=\frac{102.61}{V_{r 1}} ; \quad V_{r 1}=186.95 \mathrm{~m} / \mathrm{s}$
$\frac{V_{r 2}}{V_{r 1}}=0.85 ; \quad \frac{V_{r 2}}{186.95}=0.85 ; \quad V_{r 2}=158.9 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}=158.9 \cos 33.29 ; V_{r 2} \cos \beta_{2}=132.83 \mathrm{~m} / \mathrm{s} ; \quad U=125.66 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}>U$, Hence, Outlet velocity triangle as given below


## From outlet velocity triangle

$\overleftarrow{V_{u 2}}=V_{r 2} \cos \beta_{2}-U ; \quad \overleftarrow{V_{u 2}}=132.82-125.66 ; \quad \overleftarrow{V_{u 2}}=7.17 \mathrm{~m} / \mathrm{s}$
$\frac{E}{\dot{m}}=\frac{\left(\overline{V_{u 1}}+\overline{V_{u 2}}\right) U}{g_{c}} ; \quad \frac{E}{\dot{m}}=\frac{(281.91+7.17) 125.66}{1} ; \quad \frac{E}{\dot{m}}=36325.54 \mathrm{~J} / \mathrm{kg}$
$\operatorname{Sin} \beta_{2}=\frac{V_{m 2}}{V_{r 2}} ; \quad \operatorname{Sin} 33.29=\frac{V_{m 2}}{158.9} ; \quad V_{m 2}=87.22 \mathrm{~m} / \mathrm{s}$
$F_{a}=\dot{m}\left(V_{m 1}-V_{m 2}\right) ; 140=\dot{m}(102.61-87.22) ; \quad \dot{m}=9.09 \mathrm{~kg} / \mathrm{s}$
$E=\dot{m} \frac{E}{\dot{m}} ; \quad E=9.09 * 36325.54 ; \quad E=330372.6 \mathrm{~W} ; E=330.37 \mathrm{~kW}$
8. The simple impulse turbine has a mean blade speed of $200 \mathrm{~m} / \mathrm{s}$. The nozzles are inclined at $20^{\circ}$ to the planes of rotation of the blades. The steam velocity from nozzles is $600 \mathrm{~m} / \mathrm{s}$. The turbine uses $3500 \mathrm{~kg} / \mathrm{hr}$ of steam. The absolute velocity at exit is along the axis of turbine Determine i) Inlet and exit angles of blades ii) Power output of turbine iii) Diagram efficiency (5a. 10, Dec16/Jan17)

## Inlet and exit angles of blades

$U=200 \mathrm{~m} / \mathrm{s} ; \alpha_{1}=20^{\circ} ; \quad V_{1}=600 \mathrm{~m} / \mathrm{s} ; \dot{m}=3500 \mathrm{~kg} / \mathrm{hr} ; \dot{m}=0.972 \mathrm{~kg} / \mathrm{s}$
The absolute velocity at exit is along the axis of turbine ie $V_{2}$ is axial $\alpha_{2}=90^{\circ}$
$\overrightarrow{V_{u 1}}=V_{1} \cos \alpha_{1} ; \quad \overrightarrow{V_{u 1}}=600 \cos 20 ; \quad \overrightarrow{V_{u 1}}=563.82 \mathrm{~m} / \mathrm{s}$
$V_{m 1}=V_{1} \operatorname{Sin} \alpha_{1} ; \quad V_{m 1}=600 \sin 20 ; \quad V_{m 1}=205.21 \mathrm{~m} / \mathrm{s}$

$\tan \beta_{1}=\frac{V_{m 1}}{V_{u 1}-U} ; \quad \tan \beta_{1}=\frac{205.21}{563.82-200} \quad ; \quad \beta_{1}=29.42^{\circ}$
$\sin \beta_{1}=\frac{V_{m 1}}{V_{r 1}} ; \quad \sin 29.42=\frac{205.21}{V_{r 1}} ; \quad V_{r 1}=418.17 \mathrm{~m} / \mathrm{s}$
, Hence outlet velocity triangle is as given below


$$
\begin{array}{lc}
\text { Assume } V_{r 2}=V_{r 1} ; & V_{r 2}=418.17 \mathrm{~m} / \mathrm{s} \\
\cos \beta_{2}=\frac{U}{V_{r 2}} ; & \cos \beta_{2}=\frac{200}{418.17^{2}} ; \quad \beta_{2}=61.42^{\circ}
\end{array}
$$

## Power output of turbine

$\frac{E}{\dot{m}}=\frac{\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) U}{g_{c}} ; \overrightarrow{V_{u 2}}=0$ as $\alpha_{2}=90^{\circ} ; \quad \frac{E}{\dot{m}}=\frac{(563.82-0) 200}{1} ; \quad \frac{E}{\dot{m}}=112764 \mathrm{~J} / \mathrm{kg}$
$E=\dot{m} \frac{E}{\dot{m}} ; \quad E=0.972 * 112764 ; E=109606.6 \mathrm{~W} ; E=109.606 \mathrm{~kW}$

## Diagram efficiency

$\eta_{b}=\frac{\frac{E}{\dot{m}}}{\frac{V_{1}^{2}}{2 g_{c}}} ; \quad \eta_{b}=\frac{109606.6}{\frac{600^{2}}{2}} ; \quad \eta_{b}=0.608$
9. One stage of an impulse turbine consists of a nozzle and one ring of moving blades. The nozzle is inclined a $22^{\circ}$ to the tangential speed of blades and the blade tip angles are equiangular and equal to $35^{\circ}$ (a) Find the blade speed, diagram efficiency by neglecting losses, if the velocity of steam at the exit of the nozzle is $660 \mathrm{~m} / \mathrm{s}$ (b) If the relative velocity of steam is reduced by $15 \%$ in passing through the blade ring. Find the blade speed, diagram efficiency and end thrust on the shaft when the blade ring develops 1745 kW
10. Steam flows through the nozzle with a velocity of $450 \mathrm{~m} / \mathrm{s}$ at a direction which is inclined at an angle of $16^{\circ}$ to the wheel tangent. Steam comes out of the moving blades with a velocity of $100 \mathrm{~m} / \mathrm{s}$ in the direction of $110^{\circ}$ with the direction of blade motion. The blades are equiangular and the steam flow rate is $10 \mathrm{~kg} / \mathrm{s}$. Find (i) Power developed (ii) the power loss due to friction (iii) Axial thrust (iv) blade efficiency and (v) blade coefficient
11. Dry saturated steam at 10atmospheric pressure is supplied to single rotor impulse wheel, the condenser pressure being 0.5 atmosphere with the nozzle efficiency of 0.94 and the nozzle angle at the rotor inlet is $18^{\circ}$ to the wheel plane. The rotor blades which move with the speed of $450 \mathrm{~m} / \mathrm{s}$ are equiangular. If the coefficient velocity for the rotor blades is 0.92 . find (i) the specific power output (ii) the rotor efficiency (iii) the stage efficiency (iv) axial thrust (v) Velocity and the direction of exit steam (5b,12, Dec 12)

- Dry saturated steam at 10 atmospheric pressure is supplied to single rotor impulse wheel the steam enters nozzle at 10 atmospheric pressure and dry
- the nozzle efficiency of $0.94 ; \eta_{n}=0.94$
- nozzle angle at the rotor inlet is $18^{\circ}$ to the wheel plane $\alpha_{1}=18^{\circ}$
- The rotor blades which move with the speed of $450 \mathrm{~m} / \mathrm{s}$ are equiangular ie $\mathrm{U}=450 \mathrm{~m} / \mathrm{s}$ and $\beta_{1}=\beta_{2}$
- If the coefficient velocity for the rotor blades is 0.92 ie $\frac{V_{r 2}}{V_{r 1}}=0.92$
find (i) the specific power output ie $E=$ ? (ii) the rotor efficiency $\eta_{b}=$ ? (iii) the stage efficiency $\eta_{s}$ =? (iv) axial thrust $\mathrm{F}_{\mathrm{a}}=$ ? ( v ) the direction of exit steam $\alpha_{2}=$ ?
$h_{1}=h_{g}$ at $10 \mathrm{bar}=2780 \mathrm{~kJ} / \mathrm{kg}$
$h_{2}=2270 \mathrm{~kJ} / \mathrm{kg}$ from mollier diagram


$V_{1}=\sqrt{2\left(h_{1}-h_{2}\right) 10^{3} \eta_{n}} ; \quad V_{1}=\sqrt{2(2780-2270) 10^{3} x 0.94} ; \quad V_{1}=979.2 \mathrm{~m} / \mathrm{s}$
Take scale $1 \mathrm{~cm}=100 \mathrm{~m} / \mathrm{s}$


Measure $\Delta V_{u}=9.237 \mathrm{~cm} ; \Delta V_{u}=9.237 * 100=92.37 \mathrm{~m} / \mathrm{s}$
$\frac{E}{m}=\frac{\Delta V_{u} U}{g_{c}} ; \quad \frac{E}{m}=\frac{(923.7) \times 450}{1} ; \quad \frac{E}{m}=415665 \mathrm{~J} / \mathrm{kg}$

## ii) Rotor efficiency

Blade $\eta=\frac{\frac{E}{m}}{\frac{V}{\frac{V_{1}^{2}}{2}}} ; \quad \eta=\frac{415665}{\frac{979.2^{2}}{2}} ; \quad \eta=0.867$

## iii) stage efficiency $\eta_{s}=\eta_{n} \eta_{b}$

$\eta_{s}=0.867 x 0.94 \quad \eta_{s}=0.814$
iv) Axial thrust
$V_{m 1}=3.025 \mathrm{~cm}$;
$V_{m 1}=3.025 * 100 \mathrm{~m} / \mathrm{s} ; \quad V_{m 1}=302.5 \mathrm{~m} / \mathrm{s}$
$V_{m 2}=2.784 \mathrm{~cm} ; \quad V_{m 2}=2.784 * 100 \mathrm{~m} / \mathrm{s} ; \quad V_{m 2}=278.4 \mathrm{~m} / \mathrm{s}$ Assume $\dot{m}=1 \mathrm{~kg} / \mathrm{s}$
$F_{a}=\dot{m}\left(V_{m 1}-V_{m 2}\right) ; \quad F_{a}=1(302.5-278.4) \quad F_{a}=24.1 \mathrm{~N}$

## Analytical method

$$
\begin{array}{lll}
\overrightarrow{V_{u 1}}=V_{1} \cos \alpha_{1} ; & \overrightarrow{V_{u 1}}=979.2 \cos 18 ; & \overrightarrow{V_{u 1}}=931.27 \mathrm{~m} / \mathrm{s} \\
V_{m 1}=V_{1} \operatorname{Sin} \alpha_{1} ; & V_{m 1}=979.2 \sin 18 ; & V_{m 1}=302.58 \mathrm{~m} / \mathrm{s}
\end{array}
$$


$\tan \beta_{1}=\frac{V_{m 1}}{V_{u 1}-U} ; \quad \tan \beta_{1}=\frac{302.58}{931.27-450} ; \beta_{1}=32.15^{\circ}$
$\beta_{2}=\beta_{1} ; \quad \beta_{2}=32.15^{\circ}$
$\sin \beta_{1}=\frac{V_{m 1}}{V_{r 1}} ; \quad \sin 32.15=\frac{302.58}{V_{r 1}} ; \quad V_{r 1}=568.61 \mathrm{~m} / \mathrm{s}$
$\frac{V_{r 2}}{V_{r 1}}=0.92 ; \quad \frac{V_{r 2}}{568.61}=0.92 ; \quad V_{r 2}=523.12 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}=523.12 \cos 32.15 ; V_{r 2} \cos \beta_{2}=442.92 \mathrm{~m} / \mathrm{s} ; \quad U=450 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}<U$, Hence, Outlet velocity triangle as given below

$\overrightarrow{V_{u 2}}=U-V_{r 2} \cos \beta_{2} ; \quad \overrightarrow{V_{u 2}}=450-442.92 ; \quad \overrightarrow{V_{u 2}}=7.08 \mathrm{~m} / \mathrm{s}$
$\frac{E}{\dot{m}}=\frac{\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) U}{g_{c}} ; \quad \frac{E}{\dot{m}}=\frac{(931.27-7.08) 450}{1} ; \quad \frac{E}{\dot{m}}=415885.5 \mathrm{~J} / \mathrm{kg}$

## ii) Rotor efficiency

Blade $\eta=\frac{\frac{E}{m}}{\frac{V_{1}^{2}}{2}} ; \quad \eta=\frac{415885.5}{\frac{979.2^{2}}{2}} ; \quad \eta=0.867$

## iii) stage efficiency $\eta_{s}=\eta_{n} \eta_{b}$

$\eta_{s}=0.867 x 0.94 \quad \eta_{s}=0.814$
iv) Axial thrust
$\operatorname{Sin} \beta_{2}=\frac{V_{m 2}}{V_{r 2}} ; \quad \operatorname{Sin} 32.15=\frac{V_{m 2}}{523.12} ; \quad V_{m 2}=278.37 \mathrm{~m} / \mathrm{s} ;$ Assume $\dot{m}=1 \mathrm{~kg} / \mathrm{s}$
$F_{a}=\dot{m}\left(V_{m 1}-V_{m 2}\right) ; F_{a}=1(302.5-278.37) ; \quad F_{a}=24.12 N$

## (v) Velocity and the direction of exit steam

$V_{2}^{2}=V_{u 2}^{2}+V_{m 2}^{2} ; \quad V_{2}=\sqrt{V_{u 2}^{2}+V_{m 2}^{2}} ; \quad V_{2}=\sqrt{7.08^{2}+278.37^{2}} ; \quad V_{2}=278.46 \mathrm{~m} / \mathrm{s}$
$\tan \alpha_{2}=\frac{V_{m 2}}{V_{u 2}} ; \quad \quad \tan \alpha_{2}=\frac{278.37}{7.08} ; \quad \alpha_{2}=88.54^{\circ}$
12. In a two row velocity compounded impulse steam turbine, the steam from the nozzle issues at a velocity of $600 \mathrm{~m} / \mathrm{s}$. The nozzle angle is $20^{\circ}$ to the plane of rotation of the wheel. The mean diameter of rotor is 1 m and the speed is 3000 rpm . Both rows of moving blades have equiangular blades. The intermediate row of fixed guide blades makes the steam flow again at $20^{\circ}$ to the second moving blade ring. The frictional losses in each row are $3 \%$. Find i) The inlet and outlet angles of moving blades of each row ii) The inlet blade angle of the guide blade iii) The power output of first and second moving blade rings for unit mass flow rate iv) the blade efficiency v) the stage efficiency (assume nozzle efficiency $=0.95$ ) the steam from the nozzle issues at a velocity of $600 \mathrm{~m} / \mathrm{s}$ ie $V_{1}=600 \mathrm{~m} / \mathrm{s}$ $\alpha_{1}=20^{\circ}$; The mean diameter of rotor is 1 m ie $D_{1}=1 \mathrm{~m} ; N=3000 \mathrm{rpm}$ Both rows of moving blades have equiangular blades. Ie $\beta_{1}=\beta_{2}$ and $\beta_{3}=\beta_{4}$ The intermediate row of fixed guide blades makes the steam flow again at $20^{\circ}$ to the second moving blade ring . ie $\alpha_{3}=20^{\circ}$
The frictional losses in each row are $3 \%$. le $\frac{V_{r 2}}{V_{r 1}}=\frac{V_{3}}{V_{2}}=\frac{V_{r 4}}{V_{r 3}}=1-0.03$;

$$
\frac{V_{r 2}}{V_{r 1}}=\frac{V_{3}}{V_{2}}=\frac{V_{r 4}}{V_{r 3}}=0.97
$$

i) $\beta_{1}=\beta_{2}=? ; \quad \beta_{3}=\beta_{4}=$ ? ii) $\left(\frac{E}{\dot{m}}\right)_{I}=$ ? and $\left(\frac{E}{\dot{m}}\right)_{I I}=?$ iii) $\eta_{b}=$ ? iv) $\eta_{s}=$ ? if $\eta_{n}=0.95$

$$
U=\frac{\pi D N}{60}
$$

$U=\frac{\pi * 1 * 3000}{60}$
$U=157.07 \mathrm{~m} / \mathrm{s}$


1. Draw $U=3,14 \mathrm{~cm}$ ie $\frac{157.07}{50}$
2. Draw line $V_{1}=600 \mathrm{~m} / \mathrm{s}$ ie 12 cm at an angle $\alpha_{1}=20^{\circ}$
3. Join end of $U$ and $V_{1}$ ie
4. In a Curtis stage with two rows of moving blades the rotor are equiangular. The first rotor has angle of $29^{\circ}$ each while second rotor has angle of $32^{\circ}$ each. The velocity of steam at the exit of nozzle is $530 \mathrm{~m} / \mathrm{s}$ and the blade coefficients are 0.9 in the first, 0.95 in the stator and in the second rotor. If the absolute velocity at the stage exit should be axial, find i) Mean blade speed ii) The rotor efficiency iii) The power output for a flow rate of $32 \mathrm{~kg} / \mathrm{s}(5 \mathrm{~b}, 12$, June/July16)

Two rows of moving blades the rotor are equiangular ie $\beta_{1}=\beta_{2} ; \quad \beta_{3}=\beta_{4}$
The first rotor has angle of $29^{\circ}$ each $\beta_{1}=\beta_{2}=29^{\circ} ; \beta_{3}=\beta_{4}=32^{0}$
The velocity of steam at the exit of nozzle is $530 \mathrm{~m} / \mathrm{s} V_{1}=530 \mathrm{~m} / \mathrm{s}$
Blade coefficients are 0.9 in the first ie $\frac{V_{r 2}}{V_{r 1}}=0.9$;
Blade coefficients 0.95 in the stator ie $\frac{V_{3}}{V_{2}}=0.95$;
Blade coefficients 0.95 in the second rotor ie $\frac{V_{r 4}}{V_{r 3}}=0.95$
If the absolute velocity at the stage exit should be axial ie $\alpha_{4}=90^{\circ}$
Assume $U=3 \mathrm{~cm}$
Start from last triangle (4)

1. Draw $U=30 \mathrm{~mm}$ for 2 stage
2. Draw $V_{4}$ line vertical since $\alpha_{4}=90^{\circ}$
3. Draw $V_{r 4}$ line at an angle $32^{0}, V_{4}$ Line and $V_{r 4}$ line intersect each other, measure $V_{r 4}=35.38 \mathrm{~mm} ; \frac{V_{r 4}}{V_{r 3}}=0.95 ; \frac{35.38}{V_{r 3}}=0.95 ; V_{r 3}=37.24 \mathrm{~mm}$;
4. Draw $V_{r 3}$ line equal to 37.24 mm
5. Draw $V_{3}$ line joining right end of $U$ and end of $V_{r 3}$ line measure $V_{3}$ ie 37.24 mm
6. Draw $U=30 \mathrm{~mm}$ for first stage,
7. Draw $V_{r 2}$ line from right end of $U$ of first stage at an angle $\beta_{2}=29^{0}$
8. Left end of the $U$ of first stage velocity triangle as centre draw an arc of radius $V_{3}=37.24 \mathrm{~mm}$ to cut $V_{r 2}$ line
9. Join left end of $U$ of First stage velocity triangle to intersection point of arc and $V_{r 2}$ line ie $V_{2}$ line, Measure $V_{r 2}$ ie 92.74 mm
$\frac{V_{r 2}}{V_{r 1}}=0.9 ; \frac{92.74}{V_{r 1}}=0.9 ; V_{r 1}=103.04 \mathrm{~mm}$
10. Draw $V_{r 1}$ line from right end of $U$ of the first stage velocity triangle measuring 103.04 mm at an angle $\beta_{1}=29^{\circ}$
11. Join end of $V_{r 1}$ line with left end of $U$ of first stage velocity triangle ie $V_{1}$ line
12. Measure $V_{1}$ ie 130.09 mm at $\alpha_{1}=23^{0}$

$V_{1}=130.09 \mathrm{~mm}$ on the drawing
Actual $V_{1}=530 \mathrm{~m} / \mathrm{s}$
Hence $13.009 \mathrm{~cm}=530 \mathrm{~m} / \mathrm{s}$ ie $1 \mathrm{~cm}=\frac{530}{13.009} \mathrm{~m} / \mathrm{s} ; 1 \mathrm{~cm}=40.74 \mathrm{~m} / \mathrm{s}$

## Mean Blade speed

Mean blade speed $U=(3 \mathrm{~cm} * 40.74) \mathrm{m} / \mathrm{s} ; \quad U=122.22 \mathrm{~m} / \mathrm{s}$

## Rotor Efficiency

$\left(\Delta V_{u}\right)_{I}=17.123 * 40.74 \mathrm{~m} / \mathrm{s} ;\left(\Delta V_{u}\right)_{I}=697.59 \mathrm{~m} / \mathrm{s}$
$\left(\Delta V_{u}\right)_{I I}=6.158 * 40.74 \mathrm{~m} / \mathrm{s} ;\left(\Delta V_{u}\right)_{I I}=250.87 \mathrm{~m} / \mathrm{s}$
$\Delta V_{u}=\left(\Delta V_{u}\right)_{I}+\left(\Delta V_{u}\right)_{I I} ; \Delta V_{u}=697.59+250.87 ; \Delta V_{u}=948.47 \mathrm{~m} / \mathrm{s}$
$\frac{E}{m}=\frac{\Delta V_{u} U}{g_{c}} ; \quad \frac{E}{m}=\frac{948.47 * 122.22}{1} ; \quad \frac{E}{m}=115920.91 \mathrm{~J} / \mathrm{kg}$
$\eta_{b}=\frac{\frac{E}{m}}{\frac{V_{1}^{2}}{2 g_{c}}} ; \quad \eta_{b}=\frac{115920.91}{\frac{50^{2}}{2 * 1}} ; \quad \eta_{b}=0.825$

## The power output for a flow rate of $32 \mathrm{~kg} / \mathrm{s}$

$$
E=\dot{m} \frac{E}{\dot{m}} ; \quad E=32 * 115920.91 ; E=3709469.12 \mathrm{~W} ; E=3.709 \mathrm{MW}
$$

14. In a curtis stage turbine steam enters the first row of moving blades at $700 \mathrm{~m} / \mathrm{s}$. The outlet angles of the first rotor blade, the stator blade and the last rotor blade are respectively, $23^{\circ}$, $19^{\circ}$ and $37^{\circ}$. If the mean bade speed is $160 \mathrm{~m} / \mathrm{s}$ and the blade coefficient is 0.93 for all blades and steam flow rate is $162 \mathrm{~kg} / \mathrm{min}$, Discharge is axial. estimate: i) Power developed in the stage ii) rotor efficiency iii) axial thrust and iv) tangential force on the blades
15. In a curtis stage turbine steam enters the first row of moving blades at $700 \mathrm{~m} / \mathrm{s}$. The outlet angles of the firstrotor blade, the stator blade and the last rotor bade are respectively, $23^{\circ}$, $19^{\circ}$ and $37^{\circ}$.and the blade coefficient is 0.93 for all blades and steam flow rate is $162 \mathrm{~kg} / \mathrm{min}$, Discharge is axial. estimate: i) Power developed in the stage ii) rotor efficiency iii) axial thrust and iv) tangential force on the blades
16. A curtis impulse stage has two rotors moving with an average tangential speed of $250 \mathrm{~m} / \mathrm{s}$. The fluid relative velocity is reduced $10 \%$ in its passage over every blade, whether fixed or moving. The nozzle is inclined at an angle of $17^{\circ}$ to the wheel tangent, has an efficiency of 0.92 . The inlet angle of the first rotor blade is $22^{\circ}$. The intermediate stator inlet and exit angles are respectively $31.5^{\circ}$ and $\mathbf{2 0 ^ { \circ }}$. Assuming that the second rotor is of equiangular. Find: i) the absolute velocity $\mathrm{V}_{1}$ and the speed ratio ii) the ratio of work output from the second rotor to that of the first rotor iii) stage efficiency and iv) the power output and axial thrust for a flow of $5 \mathrm{~kg} / \mathrm{s}$ of steam over the blade
17. The mean rotor blade speed of an axial flow turbine stage with $50 \%$ reaction is $200 \mathrm{~m} / \mathrm{s}$. The steam emerges from the nozzle at $28^{\circ}$ to the wheel plane with axial velocity component equal to the blade speed. Assuming symmetric inlet and outlet velocity triangles, find the rotor blade angles and utilization factor
18. A Parsons turbine is running at 1200 rpm . The mean rotor diameter is 1 m . Blade outlet angle is $23^{\circ}$, speed ratio is 0.75 , stage efficiency is 0.8 . Find the isentropic enthalpy drop in this stage ( $6 \mathrm{~b}, 08$ Deec18/Jan19, 15 CBCS)

Parson turbine ie $50 \%$ Reaction turbine; $N=1200 \mathrm{rpm} ; D=1 \mathrm{~m} ; \beta_{2}=23^{\circ}$;
Speed ratio $=0.75$ ie $\frac{U}{V_{1}}=0.75 ; \eta_{s}=0.8$
For $50 \% R$ turbine $\alpha_{1}=\beta_{2} ; \alpha_{1}=23^{\circ}$
$U=\frac{\pi D N}{60}$;
$U=\frac{\pi * 1 * 1200}{60}$;
$U=62.83 \mathrm{~m} / \mathrm{s}$
$\frac{U}{V_{1}}=0.75 ;$
$\frac{62.83}{V_{1}}=0.75 ;$
$V_{1}=83.78 \mathrm{~m} / \mathrm{s}$

$\begin{array}{lll}\overrightarrow{V_{u 1}}=V_{1} \cos \alpha_{1} ; & \overrightarrow{V_{u 1}}=83.78 \cos 23 ; & \overrightarrow{V_{u 1}}=77.12 \mathrm{~m} / \mathrm{s} \\ V_{m 1}=V_{1} \sin \alpha_{1} ; & V_{m 1}=83.78 \sin 23 & V_{m 1}=32.73 \mathrm{~m} / \mathrm{s}\end{array}$
For $50 \% R$ turbine,$\quad V_{r 2}=V_{1} ; \quad V_{r 2}=83.78 \mathrm{~m} / \mathrm{s}$
$\overleftarrow{V_{u 2}}=V_{r 2} \cos \beta_{2}-U ; \quad \overleftarrow{V_{u 2}}=83.78 \cos 23-62.83 ; \quad \overleftarrow{V_{u 2}}=14.28 \mathrm{~m} / \mathrm{s}$
$\frac{E}{\dot{m}}=\frac{\left(\overline{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U}{g_{c}} ; \quad \frac{E}{\dot{m}}=\frac{(77.12+14.29) 62.83}{1} ; \quad \frac{E}{\dot{m}}=5743.29 \mathrm{~J} / \mathrm{kg} ;$

$$
\Delta h_{0}=\frac{E}{\dot{m}^{\prime}} \quad \Delta h_{0}=5743.29 \mathrm{~J} / \mathrm{kg}
$$

$\eta_{s}=\frac{\Delta h_{0}}{\Delta h_{0 S}} ; \quad 0.8=\frac{5743.29}{\Delta h_{0 s}} ; \quad \Delta h_{0 s}=7179.11 \mathrm{~J} / \mathrm{kg}$

## Graphical Solution

Parson turbine ie $50 \%$ Reaction turbine; $N=1200 \mathrm{rpm} ; D=1 \mathrm{~m} ; \beta_{2}=23^{\circ}$;
Speed ratio $=0.75$ ie $\frac{U}{V_{1}}=0.75 ; \eta_{s}=0.8$
For $50 \% R$ turbine $\alpha_{1}=\beta_{2} ; \alpha_{1}=23^{\circ}$
$U=\frac{\pi D N}{60}$;
$U=\frac{\pi * 1 * 1200}{60}$;
$U=62.83 \mathrm{~m} / \mathrm{s}$
$\frac{U}{V_{1}}=0.75 ;$
$\frac{62.83}{V_{1}}=0.75 ;$
$V_{1}=83.78 \mathrm{~m} / \mathrm{s}$

Scale $1 \mathrm{~cm}=20 \mathrm{~m} / \mathrm{s} ; \quad U=\frac{62.83}{20} \mathrm{~cm} ; U=3.142 \mathrm{~cm} ; \quad V_{1}=\frac{83.78}{20} \mathrm{~cm} ; V_{1}=4.189 \mathrm{~cm}$


$$
\begin{gathered}
\Delta V_{u}=4.57 \mathrm{~cm} ; \quad \Delta V_{u}=4.57 * 20 ; \quad \Delta V_{u}=91.4 \mathrm{~m} / \mathrm{s} \\
\frac{E}{\dot{m}}=\frac{\left(\overline{V_{u 1}}+\overleftarrow{V_{u 2}}\right) \mathrm{U}}{g_{c}} ; \quad \frac{E}{\dot{m}}=\frac{\left(\Delta V_{u}\right) U}{g_{c}} \quad \frac{E}{\dot{m}}=\frac{91.4 * 62.83}{1} ; \quad \frac{E}{\dot{m}}=5742.62 \mathrm{~J} / \mathrm{kg} ; \\
\Delta h_{0}=\frac{E}{\dot{m}^{;}} \quad \Delta h_{0}=5742.62 \mathrm{~J} / \mathrm{kg} \\
\eta_{s}=\frac{\Delta h_{0}}{\Delta h_{0 s}} ; \quad 0.8=\frac{5742.62}{\Delta h_{0 s}} ; \quad \Delta h_{0 s}=7178.33 \mathrm{~J} / \mathrm{kg}
\end{gathered}
$$

19. The following particulars refer to a stage of a parsons steam turbine. Mean diameter of blade ring $=70 \mathrm{~cm}$, steam velocity at inlet of moving blades $=160 \mathrm{~m} / \mathrm{s}$, outlet blade angles of moving blades $\beta_{2}=20^{\circ}$, steam flow through the blades $=7 \mathrm{~kg} / \mathrm{s}$ and speed 1500 rpm ,$\eta=0.8$. Draw the velocity diagram and find the following: i) Blade inlet angle ii) Power developed in the stage iii) Available isentropic enthalpy drop (5b, 08,June/July1815CBCS)

Parson Turbine- $50 \% ; D=70 \mathrm{~cm} D=0.7 \mathrm{~m}$;
steam velocity at inlet of moving blades $=160 \mathrm{~m} / \mathrm{s}, \quad V_{1}=160 \mathrm{~m} / \mathrm{s}$;
outlet blade angles of moving blades $\beta_{2}=20^{\circ}$,
steam flow through the blades $=7 \mathrm{~kg} / \mathrm{s} \quad \dot{m}=7 \mathrm{~kg} / \mathrm{s} ; \quad N=1500 \mathrm{rpm} ; \quad \eta=0.8$
i) Blade inlet angle $\beta_{1}=$ ?
ii) Power developed in the stage $E=$ ?
iii) Available isentropic enthalpy drop $\Delta h_{o s}=$ ?

$$
U=\frac{\pi D N}{60} ; \quad U=\frac{\pi * 0.7 * 1500}{60} ; \quad U=54.98 \mathrm{~m} / \mathrm{s}
$$

For $50 \% R$ turbine $\alpha_{1}=\beta_{2} ; \quad \alpha_{1}=20^{\circ}$


$\overline{V_{u 1}}=V_{1} \cos \alpha_{1} ; \quad \quad \overline{V_{u 1}}=160 \cos 20 ; \quad \overline{V_{u 1}}=150.35 \mathrm{~m} / \mathrm{s}$
$V_{m 1}=V_{1} \operatorname{Sin} \alpha_{1} ; \quad V_{m 1}=160 \operatorname{Sin} 20 \quad V_{m 1}=54.72 \mathrm{~m} / \mathrm{s}$
For $50 \% R$ turbine, $\quad V_{r 2}=V_{1} ; \quad V_{r 2}=160 \mathrm{~m} / \mathrm{s}$
$\overleftarrow{V_{u 2}}=V_{r 2} \cos \beta_{2}-U ; \quad \overleftarrow{V_{u 2}}=160 \cos 20-54.98 ; \quad \overleftarrow{V_{u 2}}=95.37 \mathrm{~m} / \mathrm{s}$
$\frac{E}{\dot{m}}=\frac{\left(\overline{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U}{g_{c}} ; \quad \frac{E}{\dot{m}}=\frac{(150.35+95.37) 54.98}{1} ; \quad \frac{E}{\dot{m}}=13509.68 \mathrm{~J} / \mathrm{kg} ;$

$$
\Delta h_{0}=\frac{E}{\dot{m}^{j}} \quad \Delta h_{0}=13509.68 \mathrm{~J} / \mathrm{kg}
$$

$\eta_{s}=\frac{\Delta h_{0}}{\Delta h_{0 s}} ; \quad 0.8=\frac{13509.68}{\Delta h_{0 s}} ; \quad \Delta h_{0 s}=16887.10 \mathrm{~J} / \mathrm{kg}$

## Graphical Solution

Parson Turbine-50\%; $D=70 \mathrm{~cm} D=0.7 \mathrm{~m}$;
steam velocity at inlet of moving blades $=160 \mathrm{~m} / \mathrm{s}, \quad V_{1}=160 \mathrm{~m} / \mathrm{s}$;
outlet blade angles of moving blades $\beta_{2}=20^{\circ}$,
steam flow through the blades $=7 \mathrm{~kg} / \mathrm{s} \quad \dot{m}=7 \mathrm{~kg} / \mathrm{s} ; \quad N=1500 \mathrm{rpm} ; \quad \eta=0.8$
i) Blade inlet angle $\beta_{1}=$ ?
ii) Power developed in the stage $E=$ ?
iii) Available isentropic enthalpy drop $\Delta h_{o s}=$ ?

$$
U=\frac{\pi D N}{60} ; \quad U=\frac{\pi * 0.7 * 1500}{60} ; \quad U=54.98 \mathrm{~m} / \mathrm{s}
$$

For $50 \% R$ turbine $\alpha_{1}=\beta_{2} ; \quad \alpha_{1}=20^{\circ}$
Scale : $1 \mathrm{~cm}=10 \mathrm{~m} / \mathrm{s} ; \quad U=\frac{54.98}{10} \mathrm{~cm} ; U=5.498 \mathrm{~cm} ; V_{1}=\frac{160}{20} \mathrm{~cm} ; V_{1}=16 \mathrm{~cm}$


$$
\Delta V_{u}=24.57 \mathrm{~cm} ; \quad \Delta V_{u}=24.57 * 10 ; \quad \Delta V_{u}=245.7 \mathrm{~m} / \mathrm{s}
$$

$\frac{E}{\dot{m}}=\frac{\left(\overline{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U}{g_{c}} ; \quad \frac{E}{\dot{m}}=\frac{\left(\Delta V_{u}\right) U}{g_{c}} \quad \frac{E}{\dot{m}}=\frac{245.72 * 54.98}{1} ; \quad \frac{E}{\dot{m}}=13509.68 \mathrm{~J} / \mathrm{kg} ;$

$$
\Delta h_{0}=\frac{E}{\dot{m}^{;}} \quad \Delta h_{0}=13509.68 \mathrm{~J} / \mathrm{kg}
$$

$$
\eta_{s}=\frac{\Delta h_{0}}{\Delta h_{0 s}} ; \quad 0.8=\frac{13509.68}{\Delta h_{0 s}} ; \quad \Delta h_{0 s}=16887.11 \mathrm{~J} / \mathrm{kg}
$$

20. The following data refer to a $50 \%$ reaction turbine $\mathrm{D}=1.5 \mathrm{~m} \rho=\frac{U}{V_{1}}=0.72 ; \beta_{2}=20^{\circ}$,
$N=3000 \mathrm{rpm}$ find $i$ ) blade efficiency ii) Determine percentage increase in the blade efficiency and rotor speed if the rotor is designed to run at its best theoretical speed, the exit angle $\alpha_{1}$ is $20^{\circ}$. Blade efficiency for the best speed is given by $\frac{2 \cos ^{2} \alpha_{1}}{1+\cos ^{2} \alpha_{1}}(7 \mathrm{~b}, 10$, June/July 13)
$50 \%$ Reaction turbine; $; D=1.5 \mathrm{~m} ; \quad \rho=\frac{U}{V_{1}}=0.72 ; \quad \beta_{2}=20^{\circ} ; \mathrm{N}=3000 \mathrm{rpm}$;
$\eta_{b}=$ ? ii) Determine percentage increase in the blade efficiency and rotor speed if the rotor is designed to run at its best theoretical speed, the exit angle $\alpha_{1}$ is $20^{\circ}$. Blade efficiency for the best speed is given by $\frac{2 \cos ^{2} \alpha_{1}}{1+\cos ^{2} \alpha_{1}}$
For $50 \% R$ turbine $\alpha_{1}=\beta_{2} ; \quad \alpha_{1}=20^{\circ}$

$$
U=\frac{\pi D N}{60} ; \quad U=\frac{\pi * 1.5 * 3000}{60} ; \quad U=235.61 \mathrm{~m} / \mathrm{s}
$$


$\frac{U}{V_{1}}=0.72 ;$

$$
\frac{235.62}{V_{1}}=0.72 ;
$$

$$
V_{1}=327.25 \mathrm{~m} / \mathrm{s}
$$

$\overrightarrow{V_{u 1}}=V_{1} \cos \alpha_{1} ; \quad \overrightarrow{V_{u 1}}=327.25 \cos 20 ; \quad \overrightarrow{V_{u 1}}=307.51 \mathrm{~m} / \mathrm{s}$
$V_{m 1}=V_{1} \operatorname{Sin} \alpha_{1} ; \quad V_{m 1}=327.25 \operatorname{Sin} 20 \quad V_{m 1}=119.27 \mathrm{~m} / \mathrm{s}$
For $50 \% R$ turbine, $\quad V_{r 2}=V_{1} ; \quad V_{r 2}=327.25 \mathrm{~m} / \mathrm{s}$
$\overleftarrow{V_{u 2}}=V_{r 2} \cos \beta_{2}-U ; \quad \overleftarrow{V_{u 2}}=327.25 \cos 20-235.61 ; \quad \overleftarrow{V_{u 2}}=71.90 \mathrm{~m} / \mathrm{s}$
$\frac{E}{\dot{m}}=\frac{\left(\overrightarrow{V_{u 1}}+\overrightarrow{V_{u 2}}\right) U}{g_{c}} ; \quad \frac{E}{\dot{m}}=\frac{(307.51+71.90) 235.61}{1} ; \quad \frac{E}{\dot{m}}=89393.82 \mathrm{~J} / \mathrm{kg} ;$

$$
\begin{aligned}
& V_{m 2}=V_{m 1} ; \quad V_{m 2}=119.27 \mathrm{~m} / \mathrm{s} ; \quad V_{2}^{2}=V_{u 2}^{2}+V_{m 2}^{2} \\
& V_{2}^{2}=71.90^{2}+119.27^{2} ; \quad V_{2}^{2}=19394.94 \\
& \eta_{b}=\frac{\frac{E}{\dot{m}}}{\frac{E}{\dot{m}}+\frac{V_{2}^{2}}{2 g_{c}}} ; \quad \eta_{b}=\frac{89393.82}{89393.82+\frac{19394.94}{2 * 1} ; \quad \eta_{b}=0.902}
\end{aligned}
$$

For best theoretical speed $\eta_{b 1}=\frac{2 \cos ^{2} \alpha_{1}}{1+\cos ^{2} \alpha_{1}}$
$\eta_{b 1}=\frac{2 \cos ^{2} 20}{1+\cos ^{2} 20} ; \quad \eta_{b 1}=0.937$
Percentage increase in efficiency $\frac{\eta_{b 1}-\eta_{b}}{\eta_{b}} * 100$
$\frac{93.7-90.2}{90.2} \times 100 ; \quad 3.88 \%$
optimum speed ratio for maximum efficiency $\emptyset=\cos \alpha_{1}$
$\frac{U}{V_{1}}=\cos \alpha_{1} ; \frac{U}{V_{1}}=\cos 20 ; \quad \frac{U}{V_{1}}=0.94 ; \frac{U}{327.25}=0.94 ; \quad U=307.51 \mathrm{~m} / \mathrm{s}$
$U=\frac{\pi D N}{60} ;$
$307.51=\frac{\pi * 1.5 * N}{60} ; \quad N=3915.33 \mathrm{rpm}$
21. In a reaction turbine, the inlet and outlet blade angles are $50^{\circ}$ and $20^{\circ}$ respectively. Steam enters at $18^{\circ}$ to the plane wheel and leaves at $40^{\circ}$. The rotor speed is $260 \mathrm{~m} / \mathrm{s}$. Calculate the speed ratio , specific work and degree of reaction (5c. 08, Dec15/Jan16) Reaction turbine
the inlet and outlet blade angles are $50^{\circ}$ and $20^{\circ}$ respectively ie $\beta_{1}=50^{\circ}$; $\beta_{2}=20^{\circ}$
Steam enters at $18^{\circ}$ to the plane wheel and leaves at $40^{\circ}$ ie $\alpha_{1}=18^{0} ; \alpha_{2}=40^{0}$
The rotor speed is $260 \mathrm{~m} / \mathrm{s}$ ie $U=260 \mathrm{~m} / \mathrm{s}$
Scale $1 \mathrm{~cm}=50 \mathrm{~m} / \mathrm{s}$


Draw line U
2. Draw $V_{1}$ line at an angle at $\alpha_{1}=18^{0}$
3. Draw $V_{r 1}$ line at an angle $\beta_{1}=50^{0} ; V_{1}$ line and $V_{r 1}$ line intersect each other ie end of $V_{1}$ and $V_{r 1}$
4. Draw $V_{r 2}$ line at an angle $\beta_{1}=20^{0}$
5. Draw $V_{2}$ line at an angle at $\alpha_{1}=40^{\circ} ; V_{r 2}$ line and $V_{2}$ line intersect each other ie is the end of $V_{2}$ and $V_{r 2}$

## Speed ratio

Measure $V_{1}$ ie 7.517 cm ie $V_{1}=7.517 * 50 V_{1}=375.85 \mathrm{~m} / \mathrm{s}$
Speed ratio $=\frac{U}{V_{1}}$ ie Speed ratio $=\frac{260}{375.85}$ Speed ratio $=0.69$

## Specific work output

Measure $\Delta V_{u}=11.133 \mathrm{~cm} ; \quad \Delta V_{u}=11.133 * 50 \quad \Delta V_{u}=555.65 \mathrm{~m} / \mathrm{s}$
$\frac{E}{\dot{m}}=\frac{\Delta V_{u} U}{g_{c}} ; \quad \frac{E}{\dot{m}}=\frac{555.65 * 260}{1} ; \quad \frac{E}{\dot{m}}=\frac{144729 \mathrm{~J}}{\mathrm{~kg}}$

## Degree of Reaction

Measure $V_{2}$ ie 5.2 cm cm ie $V_{1}=5.2 * 50 \quad V_{1}=260 \mathrm{~m} / \mathrm{s}$

$$
R=\frac{\frac{E}{m}-\frac{\left(V_{1}^{2}-V_{2}^{2}\right)}{2 g_{c}} ;}{\frac{E}{m}} ; \quad R=1-\frac{\left(V_{1}^{2}-V_{2}^{2}\right)}{\frac{E}{m} 2 g_{c}} ; \quad R=1-\frac{375.85^{2}-260^{2}}{144729 * 2 * 1} \quad R=0.254
$$

22. At a stage in reaction turbine the mean blade ring diameter is 1 m and the turbine runs at a speed of $50 \mathrm{rev} / \mathrm{s}$. The blades are designed for $50 \%$ reaction with exit angles $60^{\circ}$ and inlet angles $40^{\circ}$ with respect to the axial direction. The turbine is supplied with steam at the rate of $60000 \mathrm{~kg} / \mathrm{hr}$ and the stage efficiency is $85 \%$. Determine a) the power output of the stage, (b) the ideal specific enthalpy drop in the stage in $\mathrm{kJ} / \mathrm{kg}$ and c ) the percentage increase in relative velocity
23. One stage of an impulse turbine consists of a nozzle and one ring of moving blades. The nozzle is inclined a $22^{\circ}$ to the tangential speed of blades and the blade tip angles are equiangular and equal to $35^{\circ}$ (a) Find the blade speed, diagram efficiency by neglecting losses, if the velocity of steam at the exit of the nozzle is $660 \mathrm{~m} / \mathrm{s}$ (b) If the relative velocity of steam is reduced by $15 \%$ in passing through the blade ring. Find the blade speed, diagram efficiency and end thrust on the shaft when the blade ring develops 1745 kW
24. A $50 \%$ reaction steam turbine, running at 7445 rpm develops 5 MW and has a steam mass flow rate of $6.5 \mathrm{~kg} / \mathrm{kWhr}$. At a particular stage in the expansion the absolute pressure is 85 kPa at a steam dryness fraction of 0.94 . If the exit angle of the blade is $70^{\circ}$ measured from the axial flow direction, and the outlet relative velocity of the steam is 1.3 times the mean blade speed, find the blade height if the ratio of rotor hub diameter to blade height is 14
25. In a reaction turbine, the blade tips are inclined at $35^{\circ}$ and $20^{\circ}$ in the direction of rotor. The stator blades are the same shape as the moving blades, but reversed in direction. At a certain place in the turbine, the drum is 1 m diameter and the blades are 10 cm high. At this place, the steam has pressure of 1.75 bar and dryness is 0.935 . If the speed of the turbine is 250 rpm and the steam passes through the blades without shock find the mass of steam flow and power developed in the ring of moving blades
26. Consider a 2 stage velocity compounded axial flow impulse steam turbine. The absolute velocity of steam entering the first row of moving blades $=450 \mathrm{~m} / \mathrm{s}$. The steam leaves the last row of moving blades axially. The blade angles at inlet and outlet of both the rotors are the same and equal to $30^{\circ}$. Sketch the velocity triangle at inlet and outlet of each stage separately. Find the blade speed
27. The velocity of steam at the exit of a nozzle is $440 \mathrm{~m} / \mathrm{s}$ which is compounded in an impulse turbine by passing successively through moving, fixed, and finally through a second ring of moving blades, The tip angles of moving blades through out the turbine are $30^{\circ}$.Assume loss of $10 \%$ in velocity due to friction when the steam passes over a blade ring. Find the velocity of moving blades in order to have a final discharge of steam as axial. Also determine the diagram efficiency
28. Given data for a two-wheel velocity compounded Curtis steam turbine stage are as follows: mean rotor speed $=450 \mathrm{~m} / \mathrm{s}$. Rotor exit angles are $22^{\circ}$ and $33^{\circ}$ respectively for the 2 rotors, stator blade exit angle $=20^{\circ}$. Blade velocity coefficient for each blade (stator and rotors) $=$ 0.95 . Assume axial discharge (assume rotors are to be equiangular). Draw velocity triangles to a scale. Find nozzle angle at inlet and the rotor efficiency
29. The following details refers to a Curtis turbine: i) both rotors are equiangular (ii) rotor blade angles are $29^{\circ}$ in first rotor and $32^{\circ}$ in second rotor (iii) absolute velocity of steam entering the first row of blades is $530 \mathrm{~m} / \mathrm{s}$ iv) blade coefficients are 0.9 in first rotor, 0.91 in stator and 0.93 in second rotor v) the absolute velocity is axial from the second rotor. Find graphically or otherwise a) mean blade speed b) power output for a flow rate of $3.2 \mathrm{~kg} / \mathrm{s}$

## HYDRAULIC TURBINES

1. Classify Hydraulic turbines with example (6a, 05, Dec13/Jan14)
2. With mathematical expression, define the following i) Hydraulic efficiency ii) Mechanical efficiency iii) overall efficiency iv) Volumetric efficiency ( $8 a, 08 D e c 18 /$ Jan19,15 scheme) $(6 a, 08$, Dec12)
3. Obtain an expression for the workdone per second by water on the runner a pelton wheel and hydraulic efficiency (6a, 10,June/July14)
4. Show that for maximum efficiency of pelton wheel the bucket velocity is equal to half of the jet velocity $U=\frac{V_{1}}{2}(7 a, 08 D e c 18 / J a n 19,15$ scheme $)(7 a, 08$, June / July18,15 scheme)
5. Show that for a Pelton turbine the maximum hydraulic efficiency is given by $\eta_{\max }=\frac{1+C_{b} \cos \beta_{2}}{2}$ where $C_{b}$ is the blade velocity coefficient and $\beta_{2}$ is the blade discharge angle (6a, 08, June/July 16) (6a, 08, Dec15/Jan 16) Draw the inlet and exit velocity triangles for a pelton wheel turbine (5a, 10, Dec13/Jan 14) (6b, 08,Dec17/Jan18)
6. Derive an expression for maximum hydraulic efficiency of a Pelton wheel in terms of runner tip angle and bucket velocity coefficient (6a, 10,June/July18)
7. Draw an neat sketch of a Francis turbine and draw velocity triangles at inlet and outlet (6c, 05, Dec13/Jan14)
8. Define the draft tubes with neat sketch. Explain different type of draft tubes (6a, 05,June/July 17) (6b, 05,June/July 17)
9. Explain the function of draft tubes and mention its types ( $6 b, 04$, June/July 16 ) (6b, 04, Dec15/Jan 16) (6a, 05,Dec17/Jan18)
10. Write short note on draft tubes in a reaction hydraulic turbine (6a, 04,Dec14/Jan15)
11. Show that pressure at the exit of the reaction turbine with draft tube is less than atmospheric pressure (8a,08,June/July18, 15 scheme)
12. With a meat sketch, explain the working of Kaplan turbine, Mention the functions of draft tube (6a, 10, Dec16/Jan17)
13. Draw the cross sectional view of a Kaplan turbine and explains its working. Also sketch the velocity triangles at inlet and outlet (6a, 10, Dec18/Jan19)
14. Define mechanical efficiency and overall efficiency of turbines

Hydraulic turbine is a turbomachine which converts Hydraulic energy into mechanical energy by dynamic action of water flowing from a high level. Hydrualic energy is in the fom of potential and kinetic

## Classifiacation

1. Based on the type of hydraulic enrgy at the inlet of turbine:
i) Impulse turbine in which inlet energy is in kinetic form ex: Pelton wheel, Turgo wheel
ii) Reaction turbine in which inlet energy is in the form of kinetic and pressure Ex : Francis , Propeller, Kaplan, tubular Bulb
2. Based on the direction of flow of water through the runner
i) Tangential flow in which water flows in a direction to path of the rotation example: Pelton wheel
ii) Radial flow -a) radial inward b) radial outward In radial inward water flows along radius of runner from outer diameter to inner diameter ex Francis
In radial outward flow turbine water flows from inner diameter to outer diameter ex: Forneyron
iii) Axial flow: water flows parallel to the axis of the turbine Ex Kaplan turbine
iv) Mixed flow : water enters radially at outer periphery and leaves axially example : modern Francis turbine
3. Based on the pressure head under which turbine work
i) High Head Impulse turbine example: Pelton wheel
ii) Medium Head reaction turbine Ex : Frnacis
iii) Low Head reaction turbine Ex: Kaplan , Propeller
4. Based on the specific speed of the turbine
i) Low specific speed, Impulse turbine Ex Pelton wheel
ii) Medium specific reaction turbine Ex Francis turbine
iii) High specific speed reaction turbine Ex Kaplan and propeller turbine

## Efficiencies in Hydraulic turbine

1. Hydraulic Efficiency is defined as the ratio of Power developed by the runner to water power available at the inlet of turbine
$\eta_{h}=\frac{P_{R}}{P_{w}} ;$
$\eta_{h}=\frac{E}{\omega Q H}$ where $E$ is calculated from Eulers turbine equation and Q is the discharge in $m^{3} / \mathrm{s}, \mathrm{H}$ is the net pressure head available at the inlet of turbine
In Pelton wheel at the inlet of turbine water power is in the form of Kinetic energy Hence, $\eta_{h}=\frac{E}{\frac{1}{2} \dot{m} V_{1}^{2}}$ where $\dot{m}$ is the mass flow rate of water flowing through the runner $V_{1}$ is the velocity of water enters the turbine
2. Mechanical Efficiency: is the ratio of Power developed at the shaft of turbine to the power developed at the runner
$\eta_{\text {mech }}=\frac{P_{s}}{P_{R}} ; \quad \eta_{\text {mech }}=\frac{P_{s}}{E}$
3. Overall efficiency : is the ratio of power developed at the shaft to the water power available at the inlet of turbine
$\eta_{0}=\frac{P_{s}}{P_{w}} ; \quad \eta_{0}=\frac{P_{R}}{P_{w}} * \frac{P_{s}}{P_{R}} ; \quad \eta_{0}=\eta_{h} * \eta_{\text {mech }}$
4. Volumetric Efficiency: is the ratio of actual volume of water used in the energy transfer to the volume of water supplied to the turbine
$\eta_{V}=\frac{Q_{a}}{Q_{t h}}$
If the volumetric efficiency is given in the problem, then actual hydraulic efficiency is

$$
\eta_{h a}=\eta_{h} * \eta_{V}
$$

## Pressure Heads:

Gross Head, $H_{g}$ : Pressure head of water available at the Dam
Friction Head $_{f}$ : Pressure head of water lost due to friction in the penstock which supplies the water from Dam to turbine

Net Head $H$ : Pressure Head available at the inlet of turbine $H=H_{g}-H_{f}$

## Pelton wheel

The water from the reservoir at higher position flows down through penstocks end of which is fitted with nozzle. In a nozzle potential energy is converted into kinetic energy. The high velocity from the exit of nozzle strikes the buckets fitted at the periphery of the rotor at centre. Water while passing through the buckets there is change in velocity and direction which results in change in momentum. The tangential force induced due to change in tangential component of fluid in buckets sets the rotor in rotary motion. Thus kinetic energy of fluid converted into work.


The tangential force =mass flow rate $*$ change in velocity of fluid in tangential direction
$F_{u}=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) ; \quad F_{u}=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}}+\overleftrightarrow{V_{u 2}}\right)$

Torque $\quad T=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}\right) * R ; \quad T=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}} R+\overleftarrow{V_{u 2}} R\right)$
Power: $E=\frac{\dot{m}}{g_{c}}\left(\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U$
Axial thrust: $F_{a}=\frac{\dot{m}}{g_{c}}\left(V_{f 1}-V_{f 2}\right) N$
Important design parameters for Pelton wheel
$>$ Jet velocity emerging from nozzle $V_{1}=C_{V} \sqrt{2 g H}$; where $C_{V}$ is coefficient of velocity ie 0.96 to $0.98, H$ is the net head available ie $H_{g}-H_{f}$, where $H_{g}$ is the gross head available at the Dam, $H_{f}$ is the friction loss in penstocks
$>$ Speed ratio $\phi=\frac{U}{\sqrt{2 g H}}$ ie 0.43 to 0.46
$>$ Jet ratio $m: \frac{D}{d}$ where $D$ is the runner diameter, $d$ is the jet diameter ie 14 to 16
> No of Buckets $Z=\frac{m}{2}$ ie $Z=\frac{D}{2 d}$

## Hydraulic Efficiency ( Theoritical)

Blade efficiency or Diagram efficiency or Utilization factor is given by is difined as the ratio of power developed by the runner to the water power available in the turbine
$\eta_{b}=\frac{\text { Power developed by the runner }}{\text { water power }}$
$\eta_{b}=\frac{m \Delta V_{u} U}{\omega Q H} ; \quad \eta_{b}=\frac{\rho Q \Delta V_{u} U}{\rho g Q H}$

$$
\eta_{b}=\frac{\Delta V_{u} U}{g H}
$$

Water power $=\omega$ QH where $\omega$ is specific weight of the fluid (Since here fluid is water $\omega$ is $9810 \mathrm{~N} / \mathrm{m} 3, \mathrm{Q}$ is the rate of flow of water in $\mathrm{m}^{3} / \mathrm{s}$ and H is the net head available at the inlet of turbine

Above equation is holds good for all the hydraulic turbine
For Impulse turbine (Pelton wheel) water power also equal to $m \frac{V_{1}^{2}}{2}$
$\eta_{b}=\frac{m\left(\left(\overrightarrow{V_{u 1}}+\overrightarrow{V_{u 2}}\right)\right) U}{\frac{m V_{1}^{2}}{2}} / \eta_{b}=\frac{m\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) U}{\frac{m V_{1}^{2}}{2}} ;$

$$
\eta_{b}=\frac{2 \Delta V_{u} U}{V_{1}^{2}}
$$

Above equation is holds good only for impulse turbine
II) Volumetric Efficiency: It is the ratio of quantity of water actually striking the runner to the quantity of water supplied to the runner
$\eta_{v}=\frac{Q_{a}}{Q_{t h}}=\frac{Q-\Delta Q}{Q} \quad$ where $\Delta Q$ is the amount of water that slips directly to the tail race without striking or it is known as leakage or loss

Actual Hydraulic efficiency is the product of theoretical hydraulic efficiency and Volumetric efficiency
$\eta_{h}=\eta_{b} \eta_{v}$
iii) Mechanical Efficiency: is the ratio of shaft power output by the turbine to the power developed by the runner
$\eta_{m}=\frac{\text { Shaft Power out put }}{\text { Power developed by the runnerwater power }}$
$\boldsymbol{\eta}_{\boldsymbol{m}}=\frac{\boldsymbol{P}_{\boldsymbol{s}}}{\rho \boldsymbol{Q} \Delta \boldsymbol{V}_{\boldsymbol{u}} \boldsymbol{U}}$
iv) Overall efficiency: is defined as ratio of shaft output power by the turbine to the water power available at inlet of the turbine
$\eta_{o}=\frac{\text { Shaft Power out put }}{\text { water power }} ;$

$$
\eta_{o}=\frac{P_{s}}{\omega Q H}
$$

$\eta_{o}=\eta_{\text {hact }} * \eta_{m}$

$$
\eta_{o}=\eta_{\text {htheortical }} x \eta_{v} x \eta_{m}
$$

Generator Efficiency: is the ratio of Generator output to Power at the shaft
$\eta_{o}=\frac{P_{g}}{P_{s}}$
It converts large portion of velocity energy rejected from the runner into useful pressure energy

Work done by the Pelton wheel

$\frac{E}{\dot{m}}=\frac{1}{g_{c}}\left(\overrightarrow{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U ;$
$\overrightarrow{V_{u 1}}=V_{1} ; \quad V_{r 1}=V_{1}-U ; \quad$ Blade friction coefficient $K=\frac{V_{r 2}}{V_{r 1}}$
$V_{r 2}=K V_{r 1} ; \quad V_{r 2}=K\left(V_{1}-U\right)$
From outlet velocity triangle; $\overleftarrow{V_{u 2}}=V_{r 2} \cos \beta_{2}-U ; \overleftarrow{V_{u 2}}=K\left(V_{1}-U\right) \cos \beta_{2}-U$
$\dot{m}=\rho Q ;$
$\frac{E}{\dot{m}}=\frac{1}{g_{c}}\left(V_{1}+\left(K\left(V_{1}-U\right) \cos \beta_{2}-U\right)\right) U$
$\frac{E}{\dot{m}}=\frac{1}{g_{c}}\left[V_{1}-U+K\left(V_{1}-U\right) \cos \beta_{2}\right] U ;$
$\frac{E}{\dot{m}}=\frac{1}{g_{c}}\left(V_{1}-U\right)\left(1+K \cos \beta_{2}\right) U$
$\frac{E}{\rho Q}=\frac{1}{g_{c}}\left(V_{1}-U\right)\left(1+K \cos \beta_{2}\right) U ; \quad E=\frac{1}{g_{c}}\left(V_{1}-U\right)\left(1+K \cos \beta_{2}\right) U$

## Blade efficiency/Hydraulic efficiency

$\eta_{b}=\frac{\frac{E}{\dot{\dot{n}}}}{\frac{V_{1}^{2}}{2 g_{c}}} ;$
$\eta_{b}=\frac{\frac{1}{g_{c}}\left(V_{1}-U\right)\left(1+K \cos \beta_{2}\right) U}{\frac{V_{1}^{2}}{2 g_{c}}} ;$
$\eta_{b}=\frac{\left(V_{1}-U\right)\left(1+K \cos \beta_{2}\right) U}{\frac{V_{1}^{2}}{2}} ;$
$\eta_{b}=\frac{2\left(V_{1}-U\right)}{V_{1}} * \frac{U}{V_{1}} *\left(1+K \cos \beta_{2}\right)$

Speed ratio $\Phi=\frac{U}{V_{1}}$
$\eta_{b}=2(1-\Phi) \Phi\left(1+K \cos \beta_{2}\right)$
For Maximum efficiency
$\frac{d \eta_{b}}{d \Phi}=0 ;$
$\frac{d\left(2(1-\Phi) \Phi\left(1+K \cos \beta_{2}\right)\right)}{d \Phi}=0 ;$
$2\left(1+K \cos \beta_{2}\right) \frac{d((1-\Phi) \Phi)}{d \Phi}=0$
$\frac{d(1-\Phi) \Phi}{d \Phi}=0 ;$
$\frac{d\left(\Phi-\Phi^{2}\right)}{d \Phi}=0 ; \quad 1-2 \Phi=0 ;$
$\Phi=\frac{1}{2} ;$
$\frac{U}{V_{1}}=\frac{1}{2} ;$
$U=\frac{V_{1}}{2}$

Hence blade speed $=50 \%$ of jet velocity for maximum efficiency
Max Efficiency $\eta_{b \max }=2\left(1-\frac{1}{2}\right) \frac{1}{2}\left(1+K \cos \beta_{2}\right) ; \quad \eta_{b \max }=2 * \frac{1}{2} * \frac{1}{2}\left(1+K \cos \beta_{2}\right)$
$\eta_{b \max }=\frac{\left(1+K \cos \beta_{2}\right)}{2}$

Main Components of Francis Turbine


The major components of Francis turbine are

## 1. Spiral Casing

Spiral casing is the inlet medium of water to the turbine. The water flowing from the reservoir or dam is made to pass through this pipe with high pressure.

To maintain the same pressure the diameter of the casing is gradually reduced, so as to maintain the pressure uniform, thus uniform momentum or velocity striking the runner blades.

## 2. Stay Vanes

Stay vanes and guide vanes guides the water to the runner blades. Stay vanes remain stationary at their position and reduces the swirling of water due to radial flow, as it enters the runner blades. Thus making turbine more efficient.

## 3. Guide Vanes

Guide vanes change their angle as per the requirement to control the angle of striking of water to turbine blades to increase the efficiency. They also regulate the flow rate of water into the runner blades thus controlling the power output of a turbine according to the load on the turbine.

## 4. Runner Blades

The performance and efficiency of the turbine is dependent on the design of the runner blades. In a Francis turbine, runner blades are divided into 2 parts. The lower half is made in the shape of small bucket so that it uses the impulse action of water to rotate the turbine.

The upper part of the blades use the reaction force of water flowing through it. These two forces together makes the runner to rotate.

## 5. Draft Tube

The pressure at the exit of the runner of Reaction Turbine is generally less than atmospheric pressure. The water at exit cannot be directly discharged to the tail race. A tube or pipe of gradually increasing area is used for discharging water from the exit of turbine to the tail race.

This tube of increasing area is called Draft Tube. One end of the tube is connected to the outlet of runner while the other end is sub-merged below the level of water in the tail-race.

## Working Principle

Francis Turbines are generally installed with their axis vertical. Water with high head (pressure) enters the turbine through the spiral casing surrounding the guide vanes. The water looses a part of its pressure in the volute (spiral casing) to maintain its speed. Then water passes through guide vanes where it is directed to strike the blades on the runner at optimum angles. As the water flows through the runner its pressure and angular momentum reduces. This reduction imparts reaction on the runner and power is transferred to the turbine shaft.

If the turbine is operating at the design conditions the water leaves the runner in axial direction. Water exits the turbine through the draft tube, which acts as a diffuser and reduces the exit velocity of the flow to recover maximum energy from the flowing water

In Francis turbine the pressure and velocity of the fluid decreases as it flows through the moving blades. Hence it converts both the kinetic energy and pressure energy is converted into work

The water coming out of runner blades would lack both the kinetic energy and pressure energy, so we use the draft tube to recover the pressure as it advances towards tail race, but still we cannot recover the pressure to that extent that we can stop air to enter into the runner housing thus causing cavitation.

Velocity triangle


## Applications of Francis Turbine

 electricity.- Mixed flow turbine is also used in irrigation water pumping sets to pump water from ground for irrigation.
- It is efficient over a wide range of water head and flow rate.
- It is most efficient hydro-turbine we have till date.


## Analysis of Francis Turbine:

$\frac{E}{\boldsymbol{m}}=\overrightarrow{V_{u 1}} U_{1} \quad$ as $\overrightarrow{V_{u 2}}=\mathbf{0}$ where $m=\rho \mathrm{Q}$
$\mathrm{Q}=\left(1-\%\right.$ of Blockage) $\boldsymbol{\pi} \mathrm{D}_{1} \mathrm{~B}_{1} \mathrm{~V}_{\mathrm{f} 1}=(1-\%$ of Blockage $) \boldsymbol{\pi} \mathrm{D}_{2} \mathrm{~B}_{2} \mathrm{~V}_{\mathrm{f} 2}$

## Inlet Velocity Triangle

If $V_{u 1}>U_{1}$


If $\mathrm{U}_{1}>\mathrm{V}_{\mathrm{u} 1}$


U1

Outlet Velocity Triangle


U2
$V_{u 2}=0$

Hydraulic Efficiency:

Blade efficiency or Diagram efficiency or Utilization factor is given by is difined as the ratio of power developed by the runner to the water power available in the turbine
$\eta_{b}=\frac{\text { Power developed by the runner }}{\text { water power }}$
$\eta_{h(t h)}=\frac{\dot{m}\left(\overrightarrow{V_{u 1} U_{1}}-\overrightarrow{V_{u 2}} U_{2}\right)}{\omega Q H} ; \eta_{h(t h)}=\frac{\rho Q\left(\overrightarrow{V_{u 1}} U_{1}\right)}{\rho g Q H} \quad \overrightarrow{V_{u 2}}=0 ; \dot{m}=\rho Q ; \omega=\rho g$
$\boldsymbol{\eta}_{\boldsymbol{h}(\boldsymbol{t h})}=\frac{\overrightarrow{V_{u 1}} U_{1}}{\boldsymbol{g} \boldsymbol{H}}$
II) Volumetric Efficiency: It is the ratio of quantity of water actually striking the runner to the quantity of water supplied to the runner
$\eta_{v}=\frac{Q_{a}}{Q_{t h}}=\frac{Q-\Delta Q}{Q} \quad$ where $\Delta Q$ is the amount of water that slips directly to the tail race without striking or it is known as leakage or loss

Actual Hydraulic efficiency is the product of theoretical hydraulic efficiency and Volumetric efficiency
$\eta_{h}=\eta_{b} \eta_{v}$
iii) Mechanical Efficiency: is the ratio of shaft power output by the turbine to the power developed by the runner
$\eta_{m}=\frac{\text { Shaft Power out put }}{\text { Power developed by the runnerwater power }}$
$\boldsymbol{\eta}_{\boldsymbol{m}}=\frac{\boldsymbol{P}_{\boldsymbol{s}}}{\boldsymbol{\rho Q \Delta V _ { u }} \boldsymbol{U}}$
iv) Overall efficiency: is defined as ratio of shaft output power by the turbine to the water power available at inlet of the turbine
$\eta_{o}=\frac{\text { Shaft Power out put }}{\text { water power }} ;$

$$
\eta_{o}=\frac{P_{s}}{\omega Q H}
$$

$\eta_{o}=\eta_{\text {hact }} * \eta_{m} \quad \eta_{o}=\eta_{\text {htheortical }} x \eta_{v} x \eta_{m}$
Generator Efficiency : is the ratio of Generator output to Power at the shaft
$\eta_{o}=\frac{P_{g}}{P_{s}}$
Working Proportions of Frnancis turbine
Speed ratio: $\phi=\frac{U_{1}}{\sqrt{2 g H}}$
Flow ratio $\psi=\frac{V_{f 1}}{\sqrt{2 g H}}$
Area of flow=(1-Blockage fraction) $\boldsymbol{\pi} \mathrm{D}_{1} \mathrm{~B}_{1}$
Generally Radial flow velocity is constant $\mathrm{V}_{\mathrm{f} 1}=\mathrm{V}_{\mathrm{f} 2}$ and $\mathrm{V}_{\mathrm{r} 2}$ is greater than $\mathrm{V}_{\mathrm{r} 1}$
Overall efficiency and Mechanical efficiency is same as Pelton wheel

## Important points

$\mathrm{U}_{1} \neq \mathrm{U}_{2}\left(\mathrm{U}_{1}\right.$ is not equal to $\mathrm{U}_{2}$ ie $\mathrm{U}_{1}=\pi D_{1} N / 60$ and $\mathrm{U}_{2}=\pi D_{2} N / 60$
$\alpha_{2}$ is $90^{\circ}$ and $\mathrm{V}_{\mathrm{u} 2}=0$
Area of flow=(1-Blockage fraction) $\boldsymbol{\pi} \mathrm{D}_{1} \mathbf{B}_{1}$

## Kaplan Turbine

## Schematic Diagram of Kaplan Turbine and working principle:

Scroll casing: The water from the penstock enters the scroll casing. The main function of spiral casing is to provide an uniform distribution of water around the runner and hence to provide constant flow velocity

Guide vanes: Water from the Scroll casing into guide vanes. Main function is i) to regulate the quantity of water entering the runner and ii) to direct the water on to the runner

Runner: This houses the moving vanes or runner blades usually 4 to 6 . From the guide vane directed to the moving vanes. As the water flows through the moving vanes both pressure
and velocity decreases. Here both pressure energy and kinetic energy converted into power which is is responsible for the rotation of the shaft.

Draft Tube: The water from the runner flows to the tail race through the draft tube. The shape of draft tube is in diverging in nature.

The main function of draft tube is i) It permits a negative or suction head established at the runner exit

It converts large portion of velocity energy rejected from the runner into useful pressure energy


## Working Principle

Velocity triangle


The water from the pen-stock enters into the scroll casing. The water moves into the scroll casing and the guide vanes directs the water from the casing to the blades of the runner. The vanes are adjustable and can adjust itself according to the requirement of flow rate. As the water moves over the blades it starts rotating due to reaction force of the water. The blades in the Kaplan turbine is also adjustable. From the runner blades, the water enters into the draft tube where its pressure energy and kinetic energy decreases. Actually here the K.E. is gets converted into pressure energy results in increased pressure of the water. Finally the water discharged to the trail race. The rotation of the turbine is used to rotate the shaft of generator for electricity production and for some other mechanical work.

## Advantages

- It can work more efficiently at low water head and high flow rates as compared with other types of turbines.
- It is smaller in size.
- It is easy to construct and space requirement is less.
- The Efficiency of Kaplan turbine is very high as compares with other hydraulic turbine.


## Disadvantages

Cavitation is the major problem in this turbine. Use of draft tube and proper material generally stainless steel for the runner blades may reduce the cavitation problem to a greater extent.

## Application

This turbine is used in power generation (mostly electricity) where water is available at low head and at higher flow rates.

This is the all about Kaplan Turbine. If you find anything missing or incorrect than lets us notify through your valuable comments. And if this article has enhanced some knowledge in you than don't forget to like and share it on Facebook, Google+, Twitter and on other social medial networks.

It is an axial flow reaction turbine Here $U_{1}=U_{2}=U$
U is based on Outer rim Diameter ie $\mathrm{D}_{\mathrm{o}} \mathrm{U}=\pi D_{o} N / 60$
$\mathrm{Q}=\frac{\pi\left(D_{o}^{2}-D_{h}^{2}\right)}{4} \mathrm{~V}_{\mathrm{f} 1}$
Speed ratio: $\phi=\frac{U_{1}}{\sqrt{2 g H}}$
Flow ratio $\psi=\frac{V_{f 1}}{\sqrt{2 g H}}$
$V_{f 1}=V_{f 2}$

Draft tubes

In power turbines like reaction turbines, Kaplan turbines, or Francis turbines, a diffuser tube is installed at the exit of the turbine, known as draft tube. ${ }^{\text {[1] }}$

This draft tube at the end of the turbine increases the pressure of the exiting fluid at the expense of its velocity. This means that the turbine can reduce pressure to a higher extent without fear of back flow from the tail race.

By placing a draft tube (also called a diffuser tube or pipe) at the exit of the turbine, the turbine pressure head is increased by decreasing the exit velocity, and both the overall efficiency and the output of the turbine can be improved. The draft tube works by converting some of the kinetic energy at the exit of the turbine runner into the useful pressure energy

## Types of Draft tubes



1. Conical diffuser or straight divergent tube-This type of draft tube consists of a conical diffuser with half angle generally less than equal to $10^{\circ}$ to prevent flow separation. It is usually employed for low specific speed, vertical shaft francis turbine. Efficiency of this type of draft tube is $90 \%$
2. Simple elbow type draft Tube-It consists of an extended elbow type tube. Generally, used when turbine has to be placed close to the tail-race. It helps to cut down the cost of excavation and the exit diameter should be as large as possible to recover kinetic energy at the outlet of runner. Efficiency of this kind of draft tube is less almost 60\%
3. Elbow with varying cross section-It is similar to the Bent Draft tube except the bent part is of varying cross section with rectangular outlet.the horizontal portion of draft tube is generally inclined upwards to prevent entry of air from the exit end

## Draft tube analysis

## WATER FRDM TURBINE



$$
\frac{p_{2}}{\omega}+\frac{V_{2}^{2}}{2 g}+Z_{2}=\frac{p_{3}}{\omega}+\frac{V_{3}^{2}}{2 g}+Z_{3}+\text { hydraulic losses in Draft tube } h_{L}
$$

Draft tube efficiency $\eta_{\mathrm{d}=} \frac{\text { Actual regain of pressure Head }}{\text { Velocity head at entrance to draft tube }}$
$\eta_{\mathrm{d}=} \frac{\frac{V_{3-}^{2}-V_{2}^{2}}{2 g}-h_{L}}{\frac{V_{2}^{2}}{2 g}}$

## Important Note:

If Draft tube is fitted at the exit of Francis and Kaplan turbine
Then theoretical Efficiency is
$\boldsymbol{\eta}_{\boldsymbol{h ( \text { theoritical } )}}=\frac{H-\frac{V_{3}^{2}}{2 g}}{H}$

## Numerical Problems:

## Pelton wheel

1. A pelton wheel turbine is required to develop 10 MW of power when working under a head of 200 m . The runner is having a speed of 650 rpm . Assuming overall efficiency of $88 \%$.
Determine i) quantity of water required ii) Diameter of the wheel. Take $\mathrm{C}_{\mathrm{v}}=0.98$ and value of $\phi=0.48$
2. A pelton wheel produces 15500 kW under a head of 350 m at 500 rpm . If overall efficiency of the wheel is $84 \%$ Find: i) Required number of jets and diameter of each jet ii) number of buckets iii) Tangential force exerted
3. In a power station single jet Pelton wheel produces 23110 kW under a head of 1770 m while running at 750 rpm . Estimate i) jet diameter ii) Mean diameter of the runner iii) Number of buckets Assume $C_{v}=0.97 ; \phi=0.46 ; \eta_{t}=0.85$ (6b, 06,June/July18) $\left.P_{S}=23110 \mathrm{~kW} ; H=1770 \mathrm{~m} ; N=750 \mathrm{rpm} ; \mathrm{i}\right) d=$ ? ii) $D=$ ? iii) $n=$ ?
i) Diameter of jet

Overall efficiency is not given Hence Assume overall efficiency $=88 \%$
$\eta_{o}=\frac{P_{S}}{\omega Q_{T} H} ; \quad 0.85=\frac{23110 * 10^{3}}{9810 * Q_{T} * 1770} ; \quad Q_{T}=1.566 \mathrm{~m}^{3} / \mathrm{s}$
$V_{1}=C_{v} \sqrt{2 g H} ;$
$V_{1}=0.97 \sqrt{2 * 9.81 * 1770}$
$V_{1}=180.76 \mathrm{~m} / \mathrm{s}$
$Q_{T}=n \frac{\pi d^{2}}{4} V_{1} ;$
$1.566=1 * \frac{\pi d^{2}}{4} * 180.76 ;$
$d=0.105 m$

## ii) Mean diameter of runner

Assume $\phi=0.46$
$\phi=\frac{U}{\sqrt{2 g H}} ;$
$0.46=\frac{U}{\sqrt{2 * 9.81 * 1770}}$
$U=85.72 \mathrm{~m} / \mathrm{s}$
$U=\frac{\pi D N}{60} ;$
$85.72=\frac{\pi * D * 750}{60}$
$D=2.18 m$
iii) Number of buckets
$Z=\frac{m}{2}+15 ;$
$Z=\frac{m}{2}+15 ;$
$Z=\frac{D}{2 d}+15 ;$
$Z=\frac{2.18}{2 * 0.105}+15 ;$
$Z=25.38 ;$
$Z=26$
4. In a power station single jet Pelton wheel produces 23110 kW under a head of 1770 m while running at 750 rpm . Estimate i) jet diameter ii) Mean diameter of the runner iii) Number of buckets Assume the necessary data suitably. (6b, 06,Dec14/Jan15)
$P_{S}=23110 \mathrm{~kW}$; $H=1770 \mathrm{~m} ; N=750 \mathrm{rpm}$; i) $d=$ ? ii) $D=$ ? iii) $n=$ ? iv)Diameter of jet=? Overall efficiency is not given Hence Assume overall efficiency $=88 \%$
$\eta_{o}=\frac{P_{S}}{\omega Q_{T} H} ;$

$$
0.88=\frac{23110 * 10^{3}}{9810 * Q_{T} * 1770} ; \quad Q_{T}=1.512 \mathrm{~m}^{3} / \mathrm{s}
$$

Assume $\mathrm{C}_{\mathrm{v}}=1$ as it has not been given in the data
$V_{1}=C_{v} \sqrt{2 g H} ;$
$V_{1}=\sqrt{2 * 9.81 * 1770}$
$V_{1}=186.35 \mathrm{~m} / \mathrm{s}$
$Q_{T}=n \frac{\pi d^{2}}{4} V_{1} ;$
$1.512=1 * \frac{\pi d^{2}}{4} * 186.35 ;$
$d=0.1016 m$

## iv) Mean diameter of runner

Assume $\phi=0.46$
$\phi=\frac{U}{\sqrt{2 g H}} ;$
$0.46=\frac{U}{\sqrt{2 * 9.81 * 1770}}$
$U=85.72 \mathrm{~m} / \mathrm{s}$
$U=\frac{\pi D N}{60} ;$
$85.72=\frac{\pi * D * 750}{60}$
$D=2.18 m$
v) Number of buckets
$Z=\frac{m}{2}+15 ;$
$Z=\frac{m}{2}+15 ;$
$Z=\frac{D}{2 d}+15 ;$
$Z=\frac{2.18}{2 * 0.1016}+15 ;$
$Z=25.72 ;$
$Z=26$
5. A pelton wheel is required to develop 12000 kW with a head of 400 m . The wheel speed is 720 rpm . Assuming $\phi=0.45, \mathrm{C}_{\mathrm{V}}=0.98, \eta_{\mathrm{o}}=86 \%$ and approximate jet ratio $=8$, Design the machine and specify a) bucket circle diameter b) number of buckets and 3) Number of jet
6. A pelton wheel produces 15500 kW under a head of 350 m at 500 rpm . IF the overall efficiency of the wheel is $84 \%$. Find i) Required number of jets and diameter of each jet ii) Number of buckets iii) Tangential force exerted Assume : jet ratio $=9.5 ; Q=160^{\circ} ; \phi=$ 0.46 (6b,10, Dec18/Jan19)
$\left.P_{s}=15500 \mathrm{~kW} ; H=350 \mathrm{~m} ; \quad N=500 \mathrm{rpm} ; \eta_{o}=0.84 ; i\right) n=? ; d=$ ? ii) $Z=$ ? iii) $F_{t}=$ ?
jet ratio $m=9.5$ ie $\frac{D}{d}=9.5 ; Q=160^{\circ}$ ie The angle of deflection of the jet is $160^{\circ}$;
$\phi=0.46$
i) Required number of jets and diameter of each jet
$\beta_{2}=180-$ Defelction angle; $\beta_{2}=180-160 \quad \beta_{2}=20^{0}$
Assume $C_{v}=1$
$V_{1}=C_{v} \sqrt{2 g H} ; \quad V_{1}=1 \sqrt{2 * 9.81 * 350} \quad V_{1}=82.86 \mathrm{~m} / \mathrm{s}$
$\phi=\frac{U}{\sqrt{2 g H}} ;$
$0.46=\frac{U}{\sqrt{2 * 9.81 * 350}}$
$U=38.12 \mathrm{~m} / \mathrm{s}$
$U=\frac{\pi D N}{60} ;$
$38.12=\frac{\pi * D * 500}{60}$ $D=1.46 m$

Dia meter of jet
$\frac{D}{d}=9.5 ;$
$\frac{1.46}{d}=9.5 ;$
$d=0.154 m$
Dia meter of jet $d=0.154 m$
$\eta_{o}=\frac{P_{S}}{\omega Q_{T} H} ;$

$$
0.85=\frac{15500 * 10^{3}}{9810 * Q_{T} * 350}
$$

$Q_{T}=5.311 \mathrm{~m}^{3} / \mathrm{s}$
$Q_{T}=n * \frac{\pi d^{2}}{4} * V_{1} ;$
$5.31=n * \frac{\pi 0.154^{2}}{4} * 82.86$
$n=3.44$ jets
$n=4$ jets
Number of jets $n=4$
ii) Number of bucket
$Z=\frac{m}{2}+15 ;$
$Z=\frac{9.5}{2}+15 ;$
$Z=19.75 ; \quad Z=20$
iii) Tangential force exerted

$$
\overrightarrow{V_{u 1}}=V_{1}
$$

$$
\overrightarrow{V_{u 1}}=82.86 \mathrm{~m} / \mathrm{s}
$$

$V_{r 1}=V_{1}-U ;$
$V_{r 1}=82.86-38.12$
$V_{r 1}=44.74 \mathrm{~m} / \mathrm{s}$
Since blade coefficient K is not given consider it is 1 ie $V_{r 2}=V_{r 1} ; \quad V_{r 2}=44.74 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}=44.74 \cos 20 ;$
$V_{r 2} \cos \beta_{2}=42.04 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}>U ;$


$$
\begin{array}{lll}
\overleftarrow{V_{u 2}}=V_{r 2} \cos \beta_{2}-U ; & \overleftarrow{V_{u 2}}=42.04-38.12 ; & \overleftarrow{V_{u 2}}=3.92 \mathrm{~m} / \mathrm{s} \\
\dot{m}=\rho Q_{T} ; & \dot{m}=1000 * 5.31 & 5311 \mathrm{~kg} / \mathrm{m}^{3} \\
F_{t}=\dot{m}\left(\overline{V_{u 1}}+\overleftarrow{V_{u 2}}\right) ; & F_{t}=5311(82.86+3.92) & F_{t}=460.889 * 10^{3} \mathrm{~N}
\end{array}
$$

7. Two jet strike at buckets of a Pelton wheel , which is having shaft power as 14715 kW . The diameter of each jet is given as 150 mm . If the net head on the turbine is 500 m , find the overall efficiency, take $C_{v}=1.0$ and speed ratio $=0.46$. If the blade angle at outlet is $15^{0}$ and reduction in relative velocity over the bucket is $5 \%$, find the hydraulic efficiency (6b, 10,Dec 13/14)
$n=2 ; \quad P_{s}=14715 \mathrm{~kW} ; \quad d=150 \mathrm{~mm} ; d=0.15 \mathrm{~m} ; \quad H=500 \mathrm{~m} ; \quad \eta_{o}=? \quad C_{v}=1.0$
speed ratio $=0.46$ ie $\phi=0.46 ; \quad \beta_{2}=15^{0}$;
reduction in relative velocity over the bucket is $5 \%$ ie $K=1-0.05$ ie $\frac{V_{r 2}}{V_{r 1}}=0.95 ; \eta_{h}=$ ?
i) overall efficiency
$V_{1}=C_{v} \sqrt{2 g H} ; \quad V_{1}=1 \sqrt{2 * 9.81 * 500} \quad V_{1}=99.04 \mathrm{~m} / \mathrm{s}$
$Q_{T}=n \frac{\pi d^{2}}{4} V_{1}$
$Q_{T}=2 * \frac{\pi * 0.15^{2}}{4} * 99.04 ;$
$Q_{T}=3.5 \mathrm{~m}^{3} / \mathrm{s}$
$\eta_{o}=\frac{P_{S}}{\omega Q_{T} H} ;$
$\eta_{o}=\frac{14715 * 10^{3}}{9810 * 3.5 * 500}$
$\eta_{o}=0.8256$
ii) Hydraulic Efficiency
$\phi=\frac{U}{\sqrt{2 g H}} ;$
$0.46=\frac{U}{\sqrt{2 * 9.81 * 500}}$
$U=45.56 \mathrm{~m} / \mathrm{s}$
$\overrightarrow{V_{u 1}}=V_{1} ; \quad \overrightarrow{V_{u 1}}=99.04 \mathrm{~m} / \mathrm{s}$
$V_{r 1}=V_{1}-U ;$
$V_{r 1}=99.04-45.56$
$V_{r 1}=53.48 \mathrm{~m} / \mathrm{s}$
$\frac{V_{r 2}}{V_{r 1}}=0.95$;
$\frac{V_{r 2}}{53.48}=0.95$
$V_{r 2}=50.81 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}=50.81 \cos 15 ;$
$V_{r 2} \cos \beta_{2}=49.07 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}>U ;$

$\overleftarrow{V_{u 2}}=V_{r 2} \cos \beta_{2}-U ; \quad \overleftarrow{V_{u 2}}=49.07-45.56 ; \quad \overleftarrow{V_{u 2}}=3.51 \mathrm{~m} / \mathrm{s}$
$\eta_{b}=\frac{\left(\overline{V_{u 1}}+\overline{V_{u 2}}\right) U}{\frac{1}{2} V_{1}^{2}} ; \quad \eta_{b}=\frac{(99.04+3.51) 45.56}{\frac{1}{2} * 99.04^{2}} \quad \eta_{b}=0.9526$
8. A three jet Pelton wheel is required to generate 10000 kW under a head of 400 m . The blade angle at outlet is $15^{\circ}$ and reduction in relative velocity over the buckets is $5 \%$. If overall efficiency is $80 \%, C_{v}=0.98$ and speed ratio $=0.46$ Find i) Diameter of jet ii) Total flow in $\mathrm{m}^{3} / \mathrm{s}$ iii) Force exerted by a jet on the buckets
9. The penstock supplies water from a reservoir to the Pelton wheel with a gross head of 500 m . One third is lost in friction in the penstock. The rate of flow of water through the nozzle fitted at the end of penstock is $2 \mathrm{~m}^{3} / \mathrm{s}$. The angle of deflection of the jet is $165^{\circ}$. Determine the power given by the water to the runner and also hydraulic efficiency of the Pelton wheel. Take speed ratio 0.45 and $C_{v}=1.0$ (6b, 10, Dec16/Jan17) gross head of 500 m . le $H_{g}=500 \mathrm{~m}$;
One third is lost in friction in the penstock ie $H_{f}=\frac{1}{3} H_{g}$ ie $H_{f}=\frac{1}{3} * 500 ; H_{f}=166.66 \mathrm{~m}$
$Q=2 \mathrm{~m}^{3} / \mathrm{s} ; \quad$ The angle of deflection of the jet is $165^{\circ} ;$
speed ratio 0.45 ie $\phi=0.45 ; \quad$ and $C_{v}=1.0$

## Power given by the water to the runner

Net Head available ie $H=H_{g}-H_{f} ; \quad H=500-166.67 \quad H=333.33 \mathrm{~m}$
$\beta_{2}=180-$ Defelction angle; $\beta_{2}=180-165 \quad \beta_{2}=15^{0}$
$V_{1}=C_{v} \sqrt{2 g H} ;$
$V_{1}=1 \sqrt{2 * 9.81 * 333.33}$
$V_{1}=80.87 \mathrm{~m} / \mathrm{s}$
$\phi=\frac{U}{\sqrt{2 g H}} ;$
$0.45=\frac{U}{\sqrt{2 * 9.81 * 333.33}}$
$U=36.39 \mathrm{~m} / \mathrm{s}$
$\overrightarrow{V_{u 1}}=V_{1}$;
$\overrightarrow{V_{u 1}}=80.87 \mathrm{~m} / \mathrm{s}$
$V_{r 1}=V_{1}-U$;
$V_{r 1}=80.87-36.39$
$V_{r 1}=44.48 \mathrm{~m} / \mathrm{s}$

Since blade coefficient K is not given consider it is 1 ie $V_{r 2}=V_{r 1} ; \quad V_{r 2}=44.48 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}=44.48 \cos 15 ; \quad V_{r 2} \cos \beta_{2}=42.96 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}>U ;$

$\overleftarrow{V_{u 2}}=V_{r 2} \cos \beta_{2}-U ;$

$$
\overleftarrow{V_{u 2}}=42.96-36.39
$$

$$
\overline{V_{u 2}}=6.57 \mathrm{~m} / \mathrm{s}
$$

$\frac{E}{\dot{m}}=\frac{\left(\overline{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U}{g_{c}} ;$

$$
E=\frac{\dot{m}\left(\overline{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U}{g_{c}}
$$

$$
E=\frac{\rho Q_{T}\left(\overline{V_{u 1}}+\overleftarrow{V_{u 2}}\right) U}{g_{c}}
$$

$E=\frac{1000 * 2 *(80.87+6.57) * 36.39}{1} ;$
$E=6.363 * 10^{6} W$
$E=\frac{1000 * 2 *(80.87+6.57) 36.39}{1} ;$

$$
\eta_{b}=\frac{\left(\overrightarrow{V_{u 1}}+\overleftrightarrow{V_{u 2}}\right) U}{\frac{1}{2} V_{1}^{2}} ; \quad \eta_{b}=\frac{(80.87+6.57) 36.39}{\frac{1}{2} * 80.87^{2}} \quad \eta_{b}=0.973
$$

10. A double jet pelton wheel develops 1200 MHP with an overall efficiency of $82 \%$ and head is 60 m . The speed ratio $=12$ and nozzle coefficient $=0.97$. Find the diameter of jet, wheel diameter, and wheel speed in rpm
11. A double over hung pelton wheel unit is to produce 30000 kW at the generator under an effective head of 300 m at base of the nozzle. Find the size of the jet , mean diameter of the runner, speed and specific speed of each pelton turbine. Assume generator efficiency $=93 \%$, Pelton wheel efficiency $=85 \%$, speed ratio $=0.46$, jet velocity coefficient $=0.97$, and jet ratio 12 (6b, 8,June/July18 15 scheme)

Double over hung wheel
$P_{g}=30000 \mathrm{~kW} ; H=300 \mathrm{~m} ; d=? ; D=? ; N=? N_{s}=? \eta_{g}=93 \% ; \eta_{0}=85 \% ; \phi=0.46 ;$
$C_{v}=0.97 ; m=\frac{D}{d}=12$
i) Size of jet

$$
\eta_{g}=\frac{P_{s}}{P_{g}} ; \quad 0.93=\frac{P_{s}}{30000} ; \quad P_{s}=27900 k W
$$

Since there are two pelton wheel connected
Power at the shaft of each Pelton wheel $=\frac{27900}{2} \quad P_{s-e a c h}=13950 \mathrm{~kW}$
$\eta_{o}=\frac{P_{S-e a c h}}{\omega Q_{T} H} ;$
$0.85=\frac{13950 * 10^{3}}{9810 * Q_{T-e a c h} * 300}$
$Q_{T-e a c h}=5.58 \mathrm{~m}^{3} / \mathrm{s}$
$V_{1}=C_{v} \sqrt{2 g H} ;$
$V_{1}=0.97 \sqrt{2 * 9.81 * 300}$
$V_{1}=74.42 \mathrm{~m} / \mathrm{s}$
$Q_{T-\text { each }}=n \frac{\pi d^{2}}{4} V_{1}$
$5.58=1 * \frac{\pi * d^{2}}{4} * 74.42 ;$

$$
d=0.309 m
$$

ii) Mean Diameter
$\phi=\frac{U}{\sqrt{2 g H}} ;$
$0.46=\frac{U}{\sqrt{2 * 9.81 * 300}}$
$U=35.29 \mathrm{~m} / \mathrm{s}$
$m=\frac{D}{d}=12 ;$
$\frac{D}{0.309}=12$
$D=3.708 m$
$U=\frac{\pi D N}{60} ;$
$35.29=\frac{\pi * 3.708 * N}{60}$

$$
N=181.76 \mathrm{rpm}
$$

iii) Specific speed
$N_{S}=\frac{N \sqrt{P}}{H^{5 / 4}}$;

$$
N_{s}=\frac{181.76 \sqrt{13950}}{300^{5 / 4}}
$$

$$
N_{s}=17.19
$$

12. A pelton wheel is designed to develop 12000 kW of power at an overall efficiency of $86 \%$.

The speed is 0.46 times the jet velocity. Assuming a nozzle coefficient of 0.975 and an approximate jet ratio of 10 , calculate the wheel diameter, number of jets diameter of each jet and number of buckets
13. In a power station . a pelton wheel produces 15000 kW under a head of 350 m while running at 500 rpm . Assume a turbine efficiency of 0.84 , coefficient of velocity for nozzle as 0.98 , speed ratio 0.46 and bucket velocity coefficient 0.86 , Calculate i) number of jet ii) Diameter of each jet iii) Tangential force on the buckets if the bucket deflect the jet through $165^{\circ}$ (7b, 8,Dec18/Jan19, 15 scheme)
$P_{s}=15000 \mathrm{~kW} ; H=350 \mathrm{~m} ; N=500 \mathrm{rpm} ; \eta_{0}=0.84 ; C_{v}=0.98 ; \phi=0.46 ; K=0.86 ;$
i) $n=$ ? ii) $d=$ ? $i \overline{i i}$ ) $F_{t}=$ ? bucket deflect the jet through $165^{\circ}$ ie $\beta_{2}=180-165 ; \beta_{2}=15^{\circ}$
i) number of jet
$\eta_{o}=\frac{P_{S}}{\omega Q_{T} H} ;$
$0.84=\frac{15000 * 10^{3}}{9810 * Q_{T} * 350}$
$Q_{T}=5.20 \mathrm{~m}^{3} / \mathrm{s}$
$V_{1}=C_{v} \sqrt{2 g H} ;$

$$
V_{1}=0.98 \sqrt{2 * 9.81 * 350}
$$

$$
V_{1}=81.21 \mathrm{~m} / \mathrm{s}
$$

$\phi=\frac{U}{\sqrt{2 g H}} ;$
$0.46=\frac{U}{\sqrt{2 * 9.81 * 350}}$
$U=38.12 \mathrm{~m} / \mathrm{s}$
$U=\frac{\pi D N}{60} ;$
$38.12=\frac{\pi * D * 500}{60}$
$D=1.46 m$

Assuming jet ratio 12 (not given)
$m=\frac{D}{d}=12 ;$

$$
\frac{1.46}{d}=12
$$

$$
d=0.1213 m
$$

$Q_{T}=n \frac{\pi d^{2}}{4} V_{1}$
$5.20=n * \frac{\pi * 0.1213^{2}}{4} * 81.21 ;$
$n=5.54$ say 6
Diameter of each jet ie $d=0.1213 m$
iii) Tangential force on the buckets if the bucket deflect the jet through $165^{0}$
$\overrightarrow{V_{u 1}}=V_{1} ;$

$$
\overrightarrow{V_{u 1}}=81.21 \mathrm{~m} / \mathrm{s}
$$

$V_{r 1}=V_{1}-U ;$
$V_{r 1}=81.21-38.12$
$V_{r 1}=43.09 \mathrm{~m} / \mathrm{s}$
$K=0.86 ;$
$\frac{V_{r 2}}{V_{r 1}}=0.86$
$\frac{V_{r 2}}{43.09}=0.86$
$V_{r 2}=37.06 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}=37.06 \cos 15 ;$
$V_{r 2} \cos \beta_{2}=35.79 \mathrm{~m} / \mathrm{s}$
$V_{r 2} \cos \beta_{2}<U ;$


$$
\begin{array}{lll}
\overrightarrow{V_{u 2}}=U-V_{r 2} \cos \beta_{2} ; & \overrightarrow{V_{u 2}}=38.12-35.79 ; & \overrightarrow{V_{u 2}}=2.33 \mathrm{~m} / \mathrm{s} \\
\dot{m}=\rho Q_{T} ; & \dot{m}=1000 * 5.20 & \dot{m}=5200 \mathrm{~kg} / \mathrm{m}^{3} \\
F_{t}=\dot{m}\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) ; & F_{t}=5200(81.21-2.33) & F_{t}=410.176 * 10^{3} \mathrm{~N}
\end{array}
$$

14. A double jet Pelton wheel is supplied with water through a pipeline 1600 m long from reservoir in which the level of the water is 350 m above that of the Pelton wheel. The turbine runs at 500 rpm and develops an output of 6800 kW . If the pipe losses are $10 \%$ of the gross head and friction coefficient $\mathrm{f}=0.005$. Determine i) the diameter of the pipe ii) The cross section of each jet iii) Mean diameter of the bucket circle. Assume that $\mathrm{C}_{\mathrm{j}}$ of jet is equal to 0.98 , bucket speed is equal to 0.45 times the jet velocity and turbine efficiency is 0.86
15. The supply to a single jet Pelton wheel is from a reservoir 310 m above the nozzle center through a pipe 67.5 cm diameter, 5.6 km long. The friction coefficient for pipe is 0.008 . The jet has a diameter of 9 cm and its velocity coefficient 0.97 , The blade speed ratio is 0.47 and the buckets deflect the water through $170^{\circ}$. The relative velocity is of water is reduced by $15 \%$ in passing over the buckets. Determine the hydraulic and overall efficiency of system if mechanical efficiency is $88 \%$
16. A pelton wheel turbine has 2 wheels and 2 jets ( one jet for one wheel ) producing 42.5 MW per wheel under a head of 730 m . Estimate the speed of the wheel if runner diameter is 4 m . Draw the inlet and outlet velocity triangles and calculate the hydraulic efficiency. If the volumetric efficiency is $98 \%$, find the discharge through the nozzle and jet diameter. Take $\mathrm{C}_{\mathrm{V}}=0.98 ; \frac{U}{V_{1}}=0.47 ; \beta_{2}=15^{\circ}$
17. A Francis turbine works under a head of 260 m and develops 16.2 MW at a speed of $600 \mathrm{r} / \mathrm{min}$. The volume flow rate through the machine is $7 \mathrm{~m}^{3} / \mathrm{s}$. If outside wheel diameter is 1.5 m and axial wheel width at inlet is 135 mm , find overall efficiency , hydraulic efficiency, and inlet angles of guide blades and rotor angles. Assume a volumetric efficiency of 0.98 and
velocity at draft tube exit to be $17.7 \mathrm{~m} / \mathrm{s}$. The whirl velocity component at the wheel exit is zero
18. The internal and external diameters of an inward flow reaction turbine are 1.2 m and 0.6 m respectively. The head on the turbine is 22 m and velocity of flow through the runner is constant and is equal to $2.5 \mathrm{~m} / \mathrm{s}$. The guide blade angle is $10^{\circ}$ and runner vanes are radial at inlet. If the discharge at outlet is radial. Find i) speed of turbine ii) Vane angle at outlet iii) Hydraulic efficiency iv) Draw velocity triangles (5b,10, June/July2013)
$D_{1}=1.2 m ; \quad D_{2}=0.6 m ; H=22 m ; V_{f 1}=V_{f 2}=2.5 \mathrm{~m} / \mathrm{s}$; The guide blade angle is $10^{\circ}$ ie $\alpha_{1}=10^{\circ}$
runner vanes are radial at inlet ie $\beta_{1}=90^{\circ}$ If the discharge at outlet is radial $\alpha_{2}=90^{\circ}$;i) $N=$ ? ;
ii) $\beta_{2}=$ ? iii) $\eta_{h}=$ ?

## Speed of the turbine


$\mathrm{V}_{\mathrm{m}} 1=\mathrm{V} \Gamma 1$
$\beta 1=90^{\circ}$
U1
$\tan \alpha_{1}=\frac{V_{f 1}}{V_{u_{1}}} ;$
$\tan 10=\frac{2.5}{\overline{V_{u 1}}} ;$
$\overrightarrow{V_{u 1}}=14.18 \mathrm{~m} / \mathrm{s} ;$
From Inlet velocity triangle $U_{1}=\overrightarrow{V_{u 1}} ; \quad U_{1}=14.18 \mathrm{~m} / \mathrm{s}$
$U_{1}=\frac{\pi D_{1} N}{60} ;$
$14.18=\frac{\pi * 1.2 * N}{60}$
$N=225.65 \mathrm{rpm}$

## $\underline{\text { Vane angle at outlet }}$

$\mathrm{V} 2=\mathrm{Vm} 2$


U2

$$
U_{2}=\frac{\pi D_{2} N}{60} ; \quad U_{2}=\frac{\pi * 0.6 * 225.65}{60} \quad U_{2}=7.09 \mathrm{~m} / \mathrm{s}
$$

From outlet velocity traingle $\tan \beta_{2}=\frac{V_{f 2}}{U_{2}} ; \quad \tan \beta_{2}=\frac{2.5}{7.09} ; \quad \beta_{2}=19.42^{\circ}$

## Hydraulic efficiency

$\eta_{h}=\frac{\overrightarrow{V_{11}} U_{1}}{g H} ;$

$$
\eta_{h}=\frac{14.18 * 14.18}{9.81 * 22}
$$

$$
\eta_{h}=0.9317
$$

19. The following data is given for a Francis turbine: net head $=70 \mathrm{~m}$, speed=600rpm, shaft power $=367.5 \mathrm{~kW}$, Overall efficiency $=85 \%$, Hydraulic efficiency $=95 \%$, flow ratio $=0.25$, width ratio $=0.1$, outer to inner diameter ratio $=2.0$, the thickness of vanes occupies $10 \%$ of the circumferential area of the runner, Velocity of flow is constant at inlet and outlet, and discharge is radial at outlet. Determine 1) Guide blade angle ii) Runner vane angles at inlet and outlet and iii) Diameter of runner at inlet and outlet and iv) Width of the wheel at inlet ( $6 \mathrm{c}, 10$,Dec12)
$H=70 \mathrm{~m} ; ~ N=600 \mathrm{rpm} ; \quad P_{s}=367.5 \mathrm{~kW} ; \quad \eta_{0}=85 \% ; \eta_{h}=95 \%$,
flow ratio $=0.25$ ie $\varphi=\frac{V_{f 1}}{\sqrt{2 g H}}=0.25 ; \quad$ breadth ratio $=0.1$ ie $\frac{B_{1}}{D_{1}}=0.1$
outer diameter of runner $=2$ times inner diameter of runner, ie $D_{1}=2 D_{2}$
velocity of flow is constant at inlet and outlet ie $V_{f 1}=V_{f 2}$
the thickness of vanes occupies $10 \%$ of the circumferential area of the runner $C=1-0.1=0.9$
discharge is radial at outlet $\alpha_{2}=90^{\circ}$;i) $\alpha_{1}=$ ?
ii) Runner vane angles at inlet and outlet ie $\beta_{1}=$ ?; $\beta_{2}=$ ?
iii) $D_{1}=$ ? ; $D_{2}=$ ?

Width of the wheel at inlet ie $B_{1}=$ ?

## Diameter of runner at inlet and outlet

$\varphi=\frac{V_{f 1}}{\sqrt{2 g H}}=0.25$;
$V_{f 1}=0.25 \sqrt{2 \times 9.81 \times 70}$
$V_{f 1}=9.26 \mathrm{~m} / \mathrm{s}$
$\eta_{0}=\frac{P_{S}}{\omega Q H} ;$
$0.85=\frac{367.5 * 10^{3}}{9810 * Q * 70}$
$Q=0.63 \mathrm{~m}^{3} / \mathrm{s}$
$Q=C \pi D_{1} B_{1} V_{f 1} ;$
$0.63=0.9 \pi D_{1} * 0.12 D_{1} * 9.26$
$D_{1}=0.448 \mathrm{~m}$

Diameter at inlet $D_{1}=0.448 \mathrm{~m}$
$D_{1}=2 D_{2} ; \quad 0.448=2 D_{2} ; \quad D_{2}=0.224 m \quad$ Diameter at outlet $=0.224 \mathrm{~m}$
Diameter at outlet $D_{2}=0.2225 \mathrm{~m}$

## Guide blade angle

$U_{1}=\frac{\pi D_{1} N}{60}$;

$$
U_{1}=\frac{\pi \times 0.448 \times 600}{60}
$$

$$
U_{1}=14.07 \mathrm{~m} / \mathrm{s}
$$

$$
\begin{array}{lrl}
\eta_{h}=\frac{\overrightarrow{V_{u 1}} U_{1}}{g H} ; & 0.95 & =\frac{\overrightarrow{V_{u 1}} \times 14.07}{9.81 \times 70} \\
\tan \alpha_{1}=\frac{V_{f 1}}{\overrightarrow{V_{u 1}}} ; & \tan \alpha_{1} & =\frac{9.26}{46.36} ;
\end{array}
$$

Guide blade angle=11.29 ${ }^{\circ}$
Runner vane angles at inlet and outlet ie $\beta_{1}=$ ?; $\beta_{2}=$ ?
$U_{1}<\overrightarrow{V_{u 1}}$

$\tan \beta_{1}=\frac{V_{f 1}}{V_{u 1}-U_{1}} ; \quad \quad \tan \beta_{1}=\frac{9.26}{46.36-14.07} \quad \beta_{1}=16^{\circ}$
Runner blade angle at inlet=18.14 ${ }^{\circ}$


$$
\begin{array}{ll}
U_{2}=\frac{\pi D_{2} \mathrm{~N}}{60} ; & U_{2}=\frac{\pi x 0.224 \times 600}{60} ; \\
V_{f 2}=V_{f 1} ; & V_{f 2}=9.26 \mathrm{~m} / \mathrm{s}
\end{array}
$$

From outlet velocity triangle
$\tan \beta_{2}=\frac{V_{f 2}}{U_{2}} ;$
$\tan \beta_{2}=\frac{9.26}{7.037}$
$\beta_{2}=52.76^{\circ}$

Runner blade angle at outlet $=52.76^{\circ}$

## Width of the wheel at inlet

20. The following data is given for a Francis turbine: net head $=70 \mathrm{~m}$, speed=600rpm, shaft power $=368 \mathrm{~kW}, \eta_{\mathrm{o}}=86 \%, \eta_{H}=95 \%$, flow ratio $=0.25$, breadth to diameter ratio $=0.12$, outer diameter of runner $=2$ times inner diameter of runner, velocity of flow is constant at inlet
and outlet, the thickness of vanes occupies $10 \%$ of the circumferential area of the runner and discharge is radial at outlet. Determine 1) Guide blade angle ii) Runner vane angles at inlet and outlet and iii) Diameter of runner at inlet and outlet and iv) Width of the wheel at inlet
$H=70 \mathrm{~m}$; $N=600 \mathrm{rpm}$; shaft power=368kW ie $P_{s}=368 \mathrm{~kW} ; \eta_{o}=86 \%, \quad \eta_{H}=95 \%$,
flow ratio $=0.25$ ie $\varphi=\frac{V_{f 1}}{\sqrt{2 g H}}=0.25 ; \quad$ breadth ratio $=0.12$ ie $\frac{B_{1}}{D_{1}}=0.12$
outer diameter of runner $=2$ times inner diameter of runner, ie $D_{1}=2 D_{2}$
velocity of flow is constant at inlet and outlet ie $\mathrm{V}_{\mathrm{f} 1}=\mathrm{V}_{\mathrm{f} 2}$
the thickness of vanes occupies $10 \%$ of the circumferential area of the runner $\mathrm{C}=1-0.1=0.9$
discharge is radial at outlet $\alpha_{2}=90^{\circ}$
$\alpha_{1}=$ ?;
Runner vane angles at inlet and outlet ie $\beta_{1}=$ ?; $\beta_{2}=$ ?
Width of the wheel at inlet ie $B_{1}=$ ?


Flow ratio $=\frac{V_{f 1}}{\sqrt{2 g H}}=0.25 ; \quad V_{f 1}=0.25 \sqrt{2 x 9.81 \times 70}=9.26 \mathrm{~m} / \mathrm{s}$
$\eta_{0}=86 \%$,

$$
\eta_{\mathrm{o}}=\frac{P}{\omega Q H} ;
$$

$$
0.86=\frac{368 \times 10^{3}}{9810 \times Q \times 70}
$$

$Q=0.623 \mathrm{~m}^{3} / \mathrm{s} ;$

$$
Q=C \pi D_{1} B_{1} V_{f 1}
$$

$$
0.623=0.9 \mathrm{x} \pi x D_{1} x 0.12 D_{1} \times 9.26
$$

Diameter at inlet $\mathrm{D}_{1}=0.445 \mathrm{~m}$
$\mathrm{D}_{1}=2 \mathrm{D}_{2} ;$
$0.445=2 \mathrm{D}_{2}$;
$U_{1}=\frac{\pi x 0.445 \times 600}{60}$
$\eta_{h}=\frac{V_{u 1} U_{1}}{g H} ;$
$0.86=\frac{\overrightarrow{V_{u 1}} \times 13.98}{9.81 \times 70} ;$
$\tan \alpha_{1}=\frac{V_{f}}{V_{u 1}}$
$\tan \alpha_{1}=\frac{9.26}{42.24}$ ie $\alpha_{1}=12.36^{\circ}$
Guide blade angle $=12.36^{\circ}$

$$
\tan \beta_{1}=\frac{V_{f 1}}{V_{u 1}-U_{1}} ; \quad \quad \tan \beta_{1}=\frac{9.26}{42.24-13.98} ; \quad \beta_{1}=18.14^{\circ}
$$

## $\underline{\text { Runner blade angle at inlet }=18.14^{\circ}}$

$\frac{U_{1}}{U_{2}}=\frac{\frac{\pi D_{1} N}{60}}{\frac{\pi D_{2} N}{60}} ;$
$\frac{U_{1}}{U_{2}}=\frac{D_{1}}{D_{2}} ;$
$\frac{13.98}{U_{2}}=\frac{2}{1} ;$

$$
U_{2}=6.99 \mathrm{~m} / \mathrm{s}
$$

$\tan \beta_{2}=\frac{V_{f 2}}{U_{2}} ;$
$\tan \beta_{2}=\frac{9.26}{6.99} ;$

$$
\beta_{2}=52.95^{0}
$$

Runner blade angle at outlet $=52.95^{\circ}$
Width of the blade at inlet $=0.12 \mathrm{D}_{1}=0.12 \times 0.445=0.534 \mathrm{~m}$
21. The following data is given for a Francis turbine: net head $=70 \mathrm{~m}$, speed $=600 \mathrm{rpm}$, shaft power $=368 \mathrm{~kW}, \eta_{\mathrm{O}}=86 \%, \eta_{H}=95 \%$, flow ratio $=0.25$, breadth to diameter ratio $=0.12$, outer diameter of runner $=2$ times inner diameter of runner, velocity of flow is constant at inlet and outlet, the thickness of vanes occupies $10 \%$ of the circumferential area of the runner and discharge is radial at outlet. Determine 1) Guide blade angle ii) Runner vane angles at inlet and outlet and iii) Diameter of runner at inlet and outlet and iv) Width of the wheel at inlet
22. In a Francis turbine, the discharge is radial, the blade speed at inlet is $25 \mathrm{~m} / \mathrm{s}$. At the inlet tangential component of velocity is $18 \mathrm{~m} / \mathrm{s}$. The radial velocity of flow is constant and equal to $2.5 \mathrm{~m} / \mathrm{s}$. Water flows at the rate of $0.8 \mathrm{~m}^{3} / \mathrm{s}$. The utilization factor is 0.82 , Find i) Eulers head ii) Power developed iii) Inlet blade angle iv) Degree of reaction. Draw the velocity triangles (6c,08, June/July16)
the discharge is radial ie $\alpha_{2}=90^{\circ}$; , the blade speed at inlet is $25 \mathrm{~m} / \mathrm{s} U_{1}=25 \mathrm{~m} / \mathrm{s}$
At the inlet tangential component of velocity is $18 \mathrm{~m} / \mathrm{s} . \overrightarrow{V_{u 1}}=18 \mathrm{~m} / \mathrm{s}$
The radial velocity of flow is constant and equal to $2.5 \mathrm{~m} / \mathrm{s} . V_{f 2}=V_{f 1}=2.5 \mathrm{~m} / \mathrm{s}$
Water flows at the rate of $0.8 \mathrm{~m}^{3} / \mathrm{s} Q=0.8 \mathrm{~m}^{3} / \mathrm{s}$
The utilization factor is $0.82, \varepsilon=0.82$
i) Eulers head $=? \quad \frac{\overrightarrow{V_{11}} U_{1}}{g}=$ ? ii) $E=$ ? $\quad$ iii) $\beta_{1}=$ ? iv) $R=$ ?
i) Eulers head
$H_{e}=\frac{\overrightarrow{V_{u 1}} U_{1}}{g} ; \quad H_{e}=\frac{18 * 25}{9.81} ; \quad H_{e}=45.87 m$
ii) Power developed
$\frac{E}{m}=\frac{\overrightarrow{V_{u 1}} U_{1}}{g_{c}} ; \quad E=m \frac{\overrightarrow{V_{1}} U_{1}}{g_{c}} ; \quad E=\rho Q \frac{\overrightarrow{V_{u 1}} U_{1}}{g_{c}} ; \quad E=1000 * 0.8 \frac{18 * 25}{1} \quad E=360000 \mathrm{~W}$
iii) Inlet blade angle

$$
U_{1}>\overrightarrow{V_{u 1}}
$$



$$
\tan \beta_{1}=\frac{V_{f 1}}{U_{1}-\overline{V_{u 1}}} ; \quad \quad \tan \beta_{1}=\frac{2.5}{25-18} \quad \beta_{1}=19.65^{\circ}
$$

iv) Degree of reaction
$R=\frac{\frac{E}{m}}{\frac{E}{m}+\frac{V_{2}^{2}}{2 g_{c}}} ; \quad \frac{E}{m}=\frac{\overrightarrow{V_{u 1}} U_{1}}{g_{c}} \quad \frac{E}{m}=\frac{18 * 25}{1} \quad \frac{E}{m}=450 \mathrm{~J} / \mathrm{kg} ; \quad V_{2}=V_{f 2}=2.5 \mathrm{~m} / \mathrm{s}$
$R=\frac{450}{450+\frac{2.5^{2}}{2 * 1}} \quad ; \quad R=0.993$
15. An inward flow reaction turbine with radial discharge having overall efficiency $80 \%$ when power developed is 147 kW .The head is 8 m . The peripheral velocity of the fluid is $0.96 \sqrt{2 g H}$. The flow velocity of the fluid is $0.36 \sqrt{2 g H}$. The speed of the rotor is 1500 rpm and hydraulic losses is $22 \%$ of available energy. Determine the following : i) Inlet guide vane and blade angles ii) Diameter of the rotor iii) width of the rotor ( $6 \mathrm{c}, 08$, Dec15/Jan 16)
$\eta_{0}=80 \% ; P_{s}=147 \mathrm{~kW} H=8 \mathrm{~m} ;$
The peripheral velocity of the fluid is $0.96 \sqrt{2 g H}$ ie $U_{1}=0.96 \sqrt{2 g H}$;
The flow velocity of the fluid is $0.36 \sqrt{2 g H}$ ie $V_{f 1}=0.36 \sqrt{2 g H} ; \quad N=1500 \mathrm{rpm}$
Hydrulic losses 22\% available energy $H_{\text {losses }}=0.22 \mathrm{H}$
$\eta_{h}=\frac{H-H_{\text {losses }}}{H} ;$

$$
\begin{array}{ll}
\eta_{h}=\frac{H-0.22 H}{H} ; & \eta_{h}=0.78 \\
& \alpha_{1}=? ; \beta_{1}=? ; \beta_{2}=?
\end{array}
$$

i) Inlet guide vane and blade angles
ii) Diameter of the rotor $D_{2}=$ ?
iii) width of the rotor $B_{1}=$ ?;

Inlet guide vane and blade angles
$U_{1}=0.96 \sqrt{2 g H} ; \quad U_{1}=0.96 \sqrt{2 * 9.81 * 8} \quad U_{1}=12.03 \mathrm{~m} / \mathrm{s}$
$V_{f 1}=0.36 \sqrt{2 g H} ;$
$V_{f 1}=0.36 \sqrt{2 * 9.81 * 8}$
$V_{f 1}=4.51 \mathrm{~m} / \mathrm{s}$
$\eta_{h}=\frac{\overrightarrow{V_{u 1}} U_{1}}{g H} ;$
$0.78=\frac{\overrightarrow{V_{u 1}} * 12.03}{9.81 * 8}$
$\overrightarrow{V_{u 1}}=5.09 \mathrm{~m} / \mathrm{s}$
$U_{1}>\overrightarrow{V_{u 1}}$ Hence, Inlet triangle as given below

$\tan \alpha_{1}=\frac{V_{f 1}}{\overrightarrow{V_{u 1}} ;}$

$$
\begin{gathered}
\tan \alpha_{1}=\frac{4.51}{5.09} \\
\tan \beta_{1}=\frac{4.51}{12.03-5.09}
\end{gathered}
$$

$$
\alpha_{1}=41.54^{\circ}
$$

$\tan \beta_{1}=\frac{V_{f 1}}{U_{1}-\overrightarrow{V_{u 1}}} ;$

$$
\beta_{1}=33.02^{\circ}
$$

## Diameter of the rotor

$$
U_{1}=\frac{\pi D_{1} N}{60} ;
$$

$$
12.03=\frac{\pi x D_{1} \times 1500}{60}
$$

$$
D_{1}=0.1531 m
$$

## width of the rotor

$\eta_{0}=\frac{P_{S}}{\omega Q H} ;$
$0.8=\frac{147 * 10^{3}}{9810 * Q * 8}$
$Q=2.34 m^{3} / s$
$Q=C \pi D_{1} B_{1} V_{f 1} \quad$ Take $\mathrm{C}=1$ since blockage is not given
$2.34=1 * \pi * 0.1531 * B_{1} * 4.51 ; \quad B_{1}=1.07 m$
23. An Inward flow reaction turbine works under a head of 110 m . The inlet and outlet diameters of the runner are 1.5 m and 1.0 m respectively. The width of the runner is constant throughout as 150 mm . The blade angle at outlet is $15^{\circ}$. The hydraulic efficiency is 0.9 . Calculate i) The speed of the turbine ii) The blade angles iii) The power developed when the discharge velocity is $6 \mathrm{~m} / \mathrm{s}(6 \mathrm{c}, 10, \mathrm{Dec} 14 / \mathrm{Jan} 15)$
$H=110 m ; D_{1}=1.5 \mathrm{~m} ; D_{2}=1.0 \mathrm{~m} ; \quad B_{1}=B_{2}=150 \mathrm{~mm} B_{1}=B_{2}=0.15 \mathrm{~m} ; \beta_{2}=15^{\circ}$
$\eta_{h}=0.9$; i) $N=? \quad$ ii) $\quad \beta_{1}=? \quad \beta_{2}=?$ iii) $E=? \quad V_{2}=6 \mathrm{~m} / \mathrm{s}$

## i) The speed of the turbine

$$
V_{f 2}=V_{2}=6 \mathrm{~m} / \mathrm{s} ; \quad V_{f 2}=6 \mathrm{~m} / \mathrm{s}
$$


$\tan \beta_{2}=\frac{V_{f 2}}{U_{2}} ;$
$\tan 15=\frac{6}{U_{2}} ;$
$U_{2}=22.39 \mathrm{~m} / \mathrm{s}$
$U_{2}=\frac{\pi D_{2} N}{60}$
$22.39=\frac{\pi * 1.0 * N}{60}$;
$N=427.62 r p m$
$U_{1}=\frac{\pi D_{1} N}{60} ;$
$U_{1}=\frac{\pi x 1,5 \times 427.62}{60}$
$U_{1}=33.59 \mathrm{~m} / \mathrm{s}$
$\eta_{h}=\frac{\overrightarrow{V_{11}} U_{1}}{g H}$;
$0.9=\frac{\overrightarrow{V_{u 1}} * 33.59}{9.81 * 110}$
$\overrightarrow{V_{u 1}}=28.91 \mathrm{~m} / \mathrm{s}$
$U_{1}>\overrightarrow{V_{u 1}}$ Hence, Inlet triangle as given below


Assuming $V_{f 1}=V_{f 2}=6 \mathrm{~m} / \mathrm{s}$
$\tan \beta_{1}=\frac{V_{f 1}}{U_{1}-\overline{u_{11}}} ;$
$\tan \beta_{1}=\frac{6}{33.59-28.91}$
$\beta_{1}=52.04^{\circ}$
$\tan \alpha_{1}=\frac{V_{f 1}}{\overline{V_{u 1}}} ;$
$\tan \alpha_{1}=\frac{6}{28.91} ;$
$\alpha_{1}=11.72^{\circ}$
The power developed
$Q=C \pi D_{1} B_{1} V_{f 1} \quad$ Take $\mathrm{C}=1$ since blockage is not given
$Q=1 * \pi * 1.5 * 0.15 * 6 ; \quad Q=4.24 m^{3} / \mathrm{s}$
$\frac{E}{m}=\frac{\overrightarrow{V_{u 1}} U_{1}}{g_{c}} ;$
$E=m \frac{\overline{\overrightarrow{V_{1}} U_{1}}}{g_{c}} ;$
$E=\rho Q \frac{\overrightarrow{\bar{u}_{11}} U_{1}}{g_{c}}$
$E=1000 * 4.24 * \frac{28.91 * 33.59}{1} ; \quad E=4.11 * 10^{6} \mathrm{~W}$
24. Design an inward flow Francis turbine whose power output is 330 kW under a head of 70 m running at $750 \mathrm{rpm} ., \eta_{h}=94 \%, \eta_{0}=85 \%$. The flow ratio at inlet is 0.15 , the breadth ratio is 0.1 . The outer diameter of the runner is twice the inner diameter of runner. The thickness of the vanes occupy $6 \%$ the circumferential area of the runner. Flow velocity is constant and discharge is radial at outlet
25. Two inwards flow reaction turbine have the same runner diameter of 0.6 m and the same hydraulic efficiency. They work under the same head and have the same velocity of flow of $6 \mathrm{~m} / \mathrm{s}$. One runner $A$ revolves at 520 rpm and has an inlet vane angle of $65^{\circ}$. If the other runner $B$ has an inlet vane angle of $110^{\circ}$, at what speed should it run?. Assume for both the turbine, the discharge is radial at outlet
26. A Francis turbine works a head of 180 m while running at 750 rpm . The outer and inner diameter of the runner is 1.4 m and 0.85 m . The water enters the runner with a velocity of $30 \mathrm{~m} / \mathrm{s}$. The outlet angle of the guide blade is $10^{\circ}$. Estimate the runner blade angles at inlet and outlet if the discharge is radial and velocity of flow is constant through the runner. Also, calculate the hydraulic efficiency
27. A medium Francis turbine has diameter 75 cm and width 10 cm . Water leaves the guide vanes at a velocity of $16 \mathrm{~m} / \mathrm{s}$ inclined at $25^{\circ}$ with the runner periphery. The net head is 20 m . The overall and hydraulic efficiencies are $80 \%$ and $90 \%$ respectively. Assuming that $8 \%$ of the flow area is lost due to the runner vanes thickness, calculate the runner vane angle at inlet and outlet, Power output by the runner,speed and specific speed of machine and mechanical efficiency
28. A Francis turbine required to develop a power of 330 kW under a head of 30 m while running at 350 rpm , if $\eta_{0}=85 \%, \eta_{\mathrm{h}}=88 \%, \varphi=0.75, \psi=0.25$ and diameter ratio of outer to inner diameter $=2$, calculate the stator and rotor angles and the dimensions of the runner.
29. A Francis turbine has to be designed to give an output of 500MHP under a head of 80 m . The rotational speed is 700 rpm . Determine the main dimensions of the runner and the guide vane and runner blade angles assuming the following data: Hydraulic losses 10\%; flow ratio $=0.15$; ratio of inner to outer diameters $=0.5$; ratio of width to diameter at inlet $=0.1$; overall efficiency=82\%; Area blocked by thickness of runner vane=15\%
30. A Francis turbine is working under a head of 100 m and the discharge $5 \mathrm{~m}^{3} / \mathrm{s}$. The velocity of flow is assumed constant through the runner is $16 \mathrm{~m} / \mathrm{s}$. The runner blade angle at inlet is $90^{\circ}$. The width of the blades at inlet is 0.15 times at the inlet diameter, the outer diameter is 0.6 times the inlet diameter. Find the hydraulic efficiency when the wheel is rotating at 500 rpm and discharge is axial. Assume that $10 \%$ of the flow area is blocked by the thickness of the blades
31. Francis turbine has a cylindrical draft tube 2.5 m in diameter. The velocity of water at inlet to the draft tube is $5 \mathrm{~m} / \mathrm{s}$. Calculate the percentage gain in power output if the outlet diameter is changed to 3.5 m . The draft tube efficiency is $75 \%$. Assume the available head at inlet is 5 m

## KAPLAN TURBINE

32. A Kaplan turbine develops 10 MW under an effective head of 8 m . The overall efficiency is 0.86 , the speed ratio is 2.0 and the flow ratio is 0.6 . The hub diameter is 0.35 times the outside diameter of the wheel. Find the diameter and speed of the turbine $(6 \mathrm{c}$, 08,Dec17/Jan18)
$P_{s}=10 \mathrm{MW}=10000 \mathrm{~kW} ; \quad H=8 ; \eta_{0}=0.86 ;$ speed ratio $\phi=2.0 ;$ Flow ratio $\varphi=0.6$ The hub diameter is 0.35 times the outside diameter of the wheel ie $D_{h}=0.35 D_{o} ; D_{o}=? N=$ ?

$$
\text { speed ratio } \phi=2.0 ; \quad \frac{U}{\sqrt{2 g H}}=2.0 ; \quad \frac{U}{\sqrt{2 * 9.81 * 8}}=2.0 \quad ; \quad U=25.05 \mathrm{~m} / \mathrm{s}
$$

$\frac{V_{f 1}}{\sqrt{2 g H}}=0.6 ;$

$$
\frac{V_{f 1}}{\sqrt{2 * 9.81 * 8}}=0.6 ;
$$

$$
V_{f 1}=12.52 \mathrm{~m} / \mathrm{s}
$$

Diameter of the turbine
$\eta_{0}=\frac{P_{S}}{\omega Q H} ; \quad 0.86=\frac{10 * 10^{6}}{9810 * Q * 8} \quad Q=148.16 \mathrm{~m}^{3} / \mathrm{s}$
$D_{h}=0.35 D_{o}$;

$$
D_{h}=0.35 D_{0}
$$

$Q=\frac{\pi\left(D_{0}^{2}-D_{h}^{2}\right)}{4} * V_{f 1} ; \quad 148.16=\frac{\pi\left(D_{0}^{2}-0.35^{2} D_{0}^{2}\right)}{4} * 12.52 ; \quad 148.16=\frac{\pi D_{0}^{2}\left(1-0.35^{2}\right)}{4} *$
12.52
$D_{0}^{2}=17.17 m^{2} ; \quad D_{o}=4.14 m$

## Speed of the turbine

$U=\frac{\pi D_{0} N}{60} ;$

$$
25.05=\frac{\pi * 4.14 * N}{60}
$$

$$
N=115.56 \mathrm{rpm}
$$

33. A Kaplan turbine produces 30000 kW under a head of 9.6 m , while running at 65.2 rpm . The discharge through the turbine is $350 \mathrm{~m}^{3} / \mathrm{s}$. The diameter of the runner is 7.4 m . The hub diameter is 0.432 times the tip diameter. Calculate i) Turbine efficiency ii) Specific speed of the turbine iii) Speed ratio (based on tip diameter) iv) Flow ratio (8b,08,June/July18,15 scheme)
$P_{s}=30000 \mathrm{~kW} ; ~ ; H=9.6 \mathrm{~m} ; N=80 \mathrm{rpm} \quad Q=350 \mathrm{~m}^{3} / \mathrm{s} ; D_{o}=7.4 \mathrm{~m} ; D_{h}=0.432 D_{o}$
i) $\eta_{0}=$ ? $\left.i i\right) N_{s}=$ ?; iii) $\phi=$ ?

## i) Turbine efficiency

$\eta_{o}=\frac{P_{S}}{\omega Q H} ;$

$$
\frac{30000 * 10^{3}}{9810 * 350 * 9.6}
$$

$$
\eta_{o}=0.91
$$

## Specific speed of the turbine

$N_{S}=\frac{N \sqrt{P_{S}}}{H^{5 / 4}} ;$

$$
N_{S}=\frac{80 \sqrt{30000}}{9.6^{5 / 4}}
$$

$$
N_{s}=820
$$

Speed ratio (based on tip diameter)
$U=\frac{\pi D_{o} N}{60} ;$

$$
U=\frac{\pi * 7.4 * 80}{60}
$$

$$
U=31 \mathrm{~m} / \mathrm{s}
$$

$\emptyset=\frac{U}{\sqrt{2 g H}} ; \quad \emptyset=\frac{31}{\sqrt{2 * 9.81 * 9.6}} \quad \emptyset=2.25$
Flow ratio
$D_{h}=0.432 D_{o} ;$

$$
D_{h}=0.432 * 7.4
$$

$$
D_{h}=3.2 \mathrm{~m} / \mathrm{s}
$$

$Q=\frac{\pi\left(D_{0}^{2}-D_{h}^{2}\right)}{4} V_{f} ;$

$$
350=\frac{\pi\left(7.4^{2}-3.2^{2}\right)}{4} V_{f}
$$

$$
V_{f}=10 \mathrm{~m} / \mathrm{s}
$$

$$
\varphi=\frac{V_{f}}{\sqrt{2 g H}} ;
$$

$$
\varphi=\frac{10}{\sqrt{2 * 9.81 * 9.6}}
$$

$$
\varphi=0.73
$$

34. A Kaplan turbine has an outer dia of 8 m and inner diameter 3 m and develops 30000 kW at 80 rpm under a head of 12 m . The discharge through the runner is $300 \mathrm{~m}^{3} / \mathrm{s}$. If the hydraulic efficiency is $95 \%$, determine i) Inlet and outlet blade angels ii) Mechanical efficiency iii) Overall efficiency (6b,10, June/July14)
$D_{o}=8 \mathrm{~m} ; D_{h}=3 \mathrm{~m} ; P_{s}=30000 \mathrm{~kW} ; N=80 \mathrm{rpm} ; H=12 \mathrm{~m} ; ~ Q=300 \mathrm{~m}^{3} / \mathrm{s} ; \eta_{h}=0.95$ i) $\beta_{1}=$ ?; $\beta_{2}=$ ? ii) $\eta_{\text {mech }}=$ ?; iii) $\eta_{0}=$ ?

## Inlet and outlet blade angels

$U=\frac{\pi D_{o} N}{60}$;
$U=\frac{\pi * 8 * 80}{60}$
$U=33.51 \mathrm{~m} / \mathrm{s}$
$U_{1}=U_{2}=U$
$\eta_{h}=\frac{\overrightarrow{V_{u 1}} U}{g H}$;
$0.95=\frac{\overrightarrow{V_{u 1}} \times 33.51}{9.81 \times 12}$
$\overrightarrow{V_{u 1}}=3.337 \mathrm{~m} / \mathrm{s}$
$U_{1}>\overrightarrow{V_{u 1}}$ Hence, Inlet triangle as given below

$Q=\frac{\pi\left(D_{0}^{2}-D_{h}^{2}\right)}{4} V_{f} ;$

$$
300=\frac{\pi\left(8^{2}-3^{2}\right)}{4} V_{f}
$$

$$
V_{f}=6.94 \mathrm{~m} / \mathrm{s}
$$

$\tan \beta_{1}=\frac{V_{f}}{U-\overline{V_{u 1}}} ;$
$\tan \beta_{1}=\frac{6.94}{33.51-3.337}$
$\beta_{1}=12.96^{\circ}$
$\tan \alpha_{1}=\frac{V_{f}}{\overrightarrow{V_{u 1}}} ;$
$\tan \alpha_{1}=\frac{6.94}{3.337} ;$
$\alpha_{1}=64.32^{\circ}$

$\tan \beta_{2}=\frac{V_{f}}{U} ;$
$\tan \beta_{2}=\frac{6.94}{33.51}$

$$
\beta_{2}=11.7^{\circ}
$$

Overall efficiency

$$
\eta_{o}=\frac{P_{S}}{\omega Q H} ;
$$

$$
\eta_{o}=\frac{30000 * 10^{3}}{9810 * 300 * 12}
$$

$$
\eta_{o}=0.849
$$

$\eta_{o}=\eta_{h} \eta_{\text {mech }}$
$0.849=0.95 * \eta_{\text {mech }}$

$$
\eta_{\text {mech }}=0.8936
$$

35. A Kaplan turbine generates 45 MW under a head of 22 m . The overall efficiency is $90 \%$ and ratio of outlet to hub diameters is 2.85 . Calculate the speed, specific speed and diameters of the runner. Assume $\phi=2.2 ; \psi=0.8$
36. A Kaplan turbine develops 9000 kW under a head of 10 m . Overall efficiency of the turbine is $85 \%$. The speed ratio based on outer diameter is 2.2 and flow ratio is 0.66 . Diameter of the boss is 0.4 times the outer diameter of the runner. Determine the diameter of the runner, boss diameter and specific speed of the runner
37. A Kaplan turbine develops 2 MW at a head of 30 m . The flow and speed ratio are 0.5 and 2.0 m respectively. The hub diameter is 0.3 times the outer diameter of the runner. Calculate the runner diameter and speed of the turbine when the overall efficiency is $85 \%$
38. A Kaplan turbine working under a head of 15 m develops 7350 kW . The outer diameter of the runner is 4 m and hub diameter $=2 \mathrm{~m}$. The guide blade angle at the extreme edge of the runner is $30^{\circ}$. The hydraulic and the overall efficiency of the turbine are $90 \%$ and $85 \%$ respectively. If the velocity of whirl is zero at outlet determine i) runner vane angle at inlet and outlet at the extreme edge of the runner ii) speed of the turbine
39. A Kaplan turbine working under a head of 20 m develops 11772 kW of shaft power. The outer diameter of runner is 3.5 m and hub diameter is 1.75 m . The guide blade angle at the extreme edge of the runner is $35^{\circ}$. The hydraulic and overall efficiencies of the turbines are $88 \%$ and $84 \%$ respectively. If the velocity of whirl is zero at outlet, determine i) Runner vane angle at the inlet and outlet at the extreme edge of the runner ii) speed of the turbine( $8 \mathrm{~b}, 08, \mathrm{Dec} 18$ )
$H=20 \mathrm{~m} ; \quad P_{S}=11772 \mathrm{~kW} ; D_{o}=3.5 \mathrm{~m} ; \quad D_{h}=1.75 \mathrm{~m} ; \eta_{h}=0.88 ; \eta_{0}=0.84 ;$
The guide blade angle at the extreme edge of the runner is $35^{\circ} \alpha_{1}=35^{\circ}$;
If the velocity of whirl is zero at outlet ie $\overrightarrow{V_{u 2}}=0 ;$ i) $\beta_{1}=$ ? $\quad \beta_{2}=$ ? ii) $N=$ ?
$\eta_{0}=\frac{P_{S}}{\omega Q H} ;$
$0.84=\frac{11772 * 10^{3}}{9810 * Q * 20}$
$Q=71.42 \mathrm{~m}^{3} / \mathrm{s}$
$Q=\frac{\pi\left(D_{0}^{2}-D_{h}^{2}\right)}{4} * V_{f 1} ;$
$71.42=\frac{\pi\left(3.5^{2}-1.75^{2}\right)}{4} * V_{f 1}$
$V_{f 1}=9.89 \mathrm{~m} / \mathrm{s}$

$$
\begin{array}{lll}
\tan \alpha_{1}=\frac{V_{f 1}}{\overrightarrow{V_{u 1}} ;} & \tan 35=\frac{9.89}{\overrightarrow{V_{u 1}} ;} & \overrightarrow{V_{u 1}}=14.12 \mathrm{~m} / \mathrm{s} \\
\eta_{h}=\frac{\overrightarrow{V_{u 1}} U}{g H} ; & 0.88=\frac{14.12 * U}{9.81 * 20} ; & U=12.23 \mathrm{~m} / \mathrm{s}
\end{array}
$$

$\overrightarrow{V_{u 1}}>U$, hence velocity triangle as given below

$\tan \beta_{1}=\frac{V_{f}}{\overline{V_{u 1}-U}} ;$
$\tan \beta_{1}=\frac{9.89}{14.12-12.23}$
$\beta_{1}=79.16^{\circ}$


U2
$U_{2}=U_{1}=U ; \quad V_{f 2}=V_{f 1}=V_{f}$
$\tan \beta_{2}=\frac{V_{f}}{U} ; \quad \quad \tan \beta_{2}=\frac{9.89}{12.23} ; \quad \boldsymbol{\beta}_{2}=38.96^{\circ}$

## speed of the turbine

$U=\frac{\pi D_{0} N}{60} ;$
$12.23=\frac{\pi * 1.75 * N}{60} ;$
$N=133.47 r p m$
40. A Kaplan turbine produces 10 MW at head of 25 m . The runner and hub diameters are 3 m and 1.2 m respectively. The inlet and outlet are right angled triangles. Calculate the speed, and outlet angles of the guide and runner blades if the hydraulic and overall efficiencies are 96 and 85 percent respectively.
41. Determine the efficiency of a Kaplan turbine developing 2940kW under a head of 5 m . It is provided with a draft tube with its inlet diameter 3 m set at 1.6 m above the tailrace level. A vacuum pressure gauge is connected to draft tube inlet indicates a reading of 5 m of water. Assume that draft tube efficiency is 78\%
42. A Kaplan turbine model built to a reduced scale of $1: 10$ develops 25 MHP when run at 400 rpm under the head of 6 m . If its overall efficiency is $85 \%$. What flow rate should be supplied to the model? If the prototype machine works under a head of 40 m , compute the
speed, power output and discharge of the machine. Assume same overall efficiency for the model and prototype
29 A propeller turbine has outer diameter of 4.5 m and inner diameter 2 m . It develops $20,605 \mathrm{~kW}$ under a head of 20 m at 137 rpm , the hydraulic efficiency is 0.94 , overall efficiency is 0.88 Find i) the Runner blade angles ii) Discharge through the runner ( $6 \mathrm{c}, 10$,June/July 17)
$D_{o}=4.5 m ; \quad D_{h}=2 m ; P_{s}=20605 \mathrm{~kW} ; \quad H=20 \mathrm{~m} ; \quad N=137 \mathrm{rpm} ; \quad \eta_{h}=0.94 ; \quad \eta_{o}=0.88$
i) $\beta_{1}=$ ? $\quad \beta_{2}=$ ? ii) $Q=$ ?
ii) Discharge through the runner
$\eta_{0}=\frac{P_{S}}{\omega Q H} ;$
$0.88=\frac{20605 * 10^{3}}{9810 * Q * 20}$
$Q=119.34 \mathrm{~m}^{3} / \mathrm{s}$

## i) the Runner blade angles

$U=\frac{\pi D_{0} N}{60} ;$

$$
U=\frac{\pi * 4.5 * 137}{60}
$$

$$
U=32.28 \mathrm{~m} / \mathrm{s}
$$

$\eta_{h}=\frac{\overrightarrow{V_{u 1}} U}{g H}$;
$0.94=\frac{\overrightarrow{V_{u 1}} * 32.28}{9.81 * 20} ;$

$$
\overrightarrow{V_{u 1}}=5.71 \mathrm{~m} / \mathrm{s}
$$

$U_{1}>\overrightarrow{V_{u 1}}$ Hence, Inlet triangle as given below


$$
\begin{array}{lcc}
Q=\frac{\pi\left(D_{0}^{2}-D_{h}^{2}\right)}{4} V_{f} ; & 119.34=\frac{\pi\left(4.5^{2}-2^{2}\right)}{4} V_{f} & V_{f}=9.35 \mathrm{~m} / \mathrm{s} \\
\tan \beta_{1}=\frac{V_{f}}{U-\overline{V_{u 1}}} ; & \tan \beta_{1}=\frac{9.35}{32.28-5.71} & \beta_{1}=19.38^{\circ} \\
\tan \alpha_{1}=\frac{V_{f}}{\overline{V_{u 1}}} ; & \tan \alpha_{1}=\frac{9.35}{5.71} ; & \alpha_{1}=58.58^{\circ}
\end{array}
$$



$$
\begin{aligned}
& U_{2}=U_{1}=U ; \quad V_{f 2}=V_{f 1}=V_{f} \\
& \tan \beta_{2}=\frac{V_{f}}{U} ;
\end{aligned} \quad \tan \beta_{2}=\frac{9.35}{32.28^{\prime}} \quad \boldsymbol{\beta}_{2}=16.15^{\circ}
$$

MODULE 5
Centrifugal Pumps

1. Define a Centrifugal pump. With usual notations, derive theortical head -capacity relationship for a centrifugal pump (7a,8,Dec15/Jan16)
2. Define the following with respect to centrifugal pumps: i) Manometric head ii) Manometric efficiency iii) Overall efficiency (7b, 6,Dec16/Jan 17)
3. What is priming ? How priming will be done in centrifugal pumps ? (7b, 04, Dec12)
4. Explain the following with reference to centrifugal pump ; i) Manometric efficiency with expression ii) Cavitation in pumps iii) Need for priming iv) Pumps in series ( $6 \mathrm{a}, 10$,June July 13)(7a, 10,June/July 18)
5. Define the following :i) Suction head ii) Delivery Head iii) Manometric Head iv) Net positive suction head (9a, 8, Dec18/Jan19,15 scheme)
6. With reference to the centrifugal pump explain what do you mean by i) Net positive section Head (NPSH) (7a, 6,Dec13/Jan 14)
7. Explain the phenomenon of cavitation in centrifugal pump (7b, 4,June/July16) (7c, 4,Dec13/Jan 14)
8. What is Cavitation? What are the causes for cavitation? Explain the steps to be taken to avoid cavitiation (7a, 6, Dec18/19)
9. What is Cavitation? What are its effects (7b,4,Dec15/Jan16)
10. Explain the following, with reference to the centrifugal pump: i) Slip and it effects ii) Cavitaiton, its effect and remedies to it iii) Difference between manometric head and NPSH (7a, 10,Dec17/Jan18)
11. What are the applications of multi-stage centrifugal pump? With a sketch, explain centrifugal pumps in series and parallel (7a, 8,June/July16)(7a,08,Dec12)
12. Explain with a neat sketch, multistage centrifugal compressor (7a, 5June July 17)
13. Explain with neat sketch , different casings of pump and label the parts (7b, 5June July 17) (7b, 6, Dec18/19)
14. What is minimum starting speed of a centrifugal pump? Derive an expression for minimum starting speed of a centrifugal pump (7a, 6,Dec16/Jan 17) (7a,6,Dec14/Jan15) (7a,12,June/July14)
15. Show that the pressure rise in the impeller of a centrifugal pump when the frictional and other losses in the impeller are neglected is given
$\frac{1}{2 g}\left(V_{f 1}^{2}+U_{2}^{2}-V_{f 2}^{2} \operatorname{cosec}^{2} \beta_{2}\right)$
Where $\mathrm{V}_{\mathrm{f} 1}$ and $\mathrm{V}_{\mathrm{f} 2}$ are the flow velocities at inlet and outlet of the impeller, $U_{2}=$ Tangential speed of the impeller at the exit, $\beta_{2}=$ Exit blade angle (7c,8,Dec15/Jan16) (9a, 8,June/July18 15 sheme)

Centrifugal pump is defined as a power absorbing machine in which the dynamic pressure generated by the forced vertex motion of the blades lifts the water from a low level to high level at the expense of mechanical energy. In other words it is defined as a turbomachine in which mechanical energy is converted into pressure energy. It is radial inward power absorbing machine

## Classification of centrifugal pump

1. According to shape of impeller and casing
a) Volute or spiral casing type b) Vortex (whirlpool) casing c) Diffuser type
2. According to type of impeller
a) Closed or shrouded impeller b) Semi- open impeller c) open impeller
3. According to working head
a) Low head centrifugal pump b) Medium head centrifugal pump iii) High Head centrifugal pump

## Definitions with respect to centrifugal pump

1. Suction Head $\left(h_{s}\right)$ : It is the vertical distance between the centre line of the pump and the water surface in the sump
2. Delivery Head $\left(h_{d}\right)$ : It is the vertical distance between the centre line of the pump and the water surface at the delivery tank
3. Static Head ( h ) : It is the vertical distance between the liquid level in the sump and the delivery tank ie $h=h_{s}+h_{d}$
4. Total Head: The net work done by the pump on the water should be enough to overcome the static head and also total loss in the system due to friction, turbulence, foot valves and bends, while providing the kinetic energy of water at the delivery $\operatorname{tank} \frac{v_{d}^{2}}{2 g}$
Thus $h_{e}=h+h_{f}+\frac{v_{d}^{2}}{2 g}$

$$
\begin{aligned}
& h_{f}=h_{f s}+h_{f d} \\
& h_{f s}=\frac{4 f L_{s} V_{s}^{2}}{2 g d_{s}} ; \quad Q=\frac{\pi d_{s}^{2}}{4} * V_{s} ; \quad V_{s}^{2}=\frac{16 Q}{\left(\pi d_{s}^{2}\right)^{2}} ; h_{f s}=\frac{4 f L_{s}}{2 g d_{s}} x \frac{16 Q^{2}}{\pi^{2} d_{s}^{4}} ; \quad h_{f s}=\frac{64 f L_{s} Q^{2}}{2 g \pi^{2} d_{s}^{5}} \\
& h_{f d}=\frac{4 f L_{d} V_{d}^{2}}{2 g d_{d}} ; \quad Q=\frac{\pi d_{d}^{2}}{4} * V_{d} ; \quad V_{d}^{2}=\frac{16 Q}{\left(\pi d_{d}^{2}\right)^{2}} \quad h_{f d}=\frac{4 f L_{d}}{2 g d_{d}} x \frac{16 Q^{2}}{\pi^{2} d_{d}^{4}} ; \quad h_{f d}=\frac{64 f L_{d} Q^{2}}{2 g \pi^{2} d_{d}^{5}} \\
& \frac{V_{d}^{2}}{2 g}=\frac{16 Q^{2}}{\pi^{2} d_{d}^{4}} \times \frac{1}{2 g}
\end{aligned}
$$

5. Manometric Head: It is pressure head against which pump has to work

$$
\begin{aligned}
& H_{m}=\frac{p_{d}}{\omega}-\frac{p_{s}}{\omega}=h+h_{f}+\frac{V_{s}^{2}}{2 g} \\
& \frac{p_{s}}{\omega}=\frac{p_{a}}{\omega}-\frac{V_{s}^{2}}{2 g}-h_{s}-h_{f s} ;
\end{aligned}
$$

$$
\begin{aligned}
& =\mathrm{h}+\mathrm{h}_{\mathrm{f}}+\frac{V_{d}^{2}}{2 g}-\frac{V_{d}^{2}}{2 g}+\frac{V_{s}^{2}}{2 g} \\
& =\mathrm{H}_{\mathrm{e}}+\frac{V_{s}^{2}}{2 g}-\frac{V_{d}^{2}}{2 g}
\end{aligned}
$$

If diameter of suction and delivery pipe are same then $\mathrm{V}_{\mathrm{s}}=\mathrm{V}_{\mathrm{d}}$
Hence $\mathrm{H}_{\mathrm{m}}=\mathrm{H}_{\mathrm{e}}$
Even otherwise also $\mathrm{V}_{\mathrm{s}}$ and $\mathrm{V}_{\mathrm{d}}$ are very small such that kinetic energy associated with them are negligible.
Hence generally $H_{m}=H_{e}$ if manometric efficiency is not given
If losses are given
$H_{m}=H_{e}$-losses (ie loss of head in the impellor and casing)
4. A centrifugal pump lifts water under a static head of 36 m of water of which 4 m is suction lift. Suction and delivery pipes have both 150 mm in diameter. The head loss in suction pipe is 1.8 m and 7 m in delivery pipes. The impeller is 380 mm in diameter and 25 mm wide at mouth and revolves at 1200 rpm . The exit blade angle is $35^{\circ}$. If the manometric efficiency of the pump is $82 \%$, find the discharge and pressure at the suction and delivery branches of the pump. ( $7 \mathrm{c}, 08$, Dec12)

## Discharge

$h=36 m ; \quad h_{s}=4 m ; \quad h_{f s}=1.8 m ; \quad h_{f d}=7 m D_{2}=380 \mathrm{~mm}=0.38 \mathrm{~m} ;$
$B_{2}=25 \mathrm{~mm}=0.025 \mathrm{~m} ; ~ N=1200 \mathrm{rpm} ; \quad \beta_{2}=35^{\circ} ; \quad \eta_{m}=82 \% ; Q=? ; p_{s}=? ; p_{d}=?$;
$H_{m}=h+h_{f}+\frac{V_{s}^{2}}{2 g} ; \quad H_{m}=36+(1.8+7) \quad H_{m}=44.8 m$
$U_{2}=\frac{\pi D_{2} \mathrm{~N}}{60} ; \quad U_{2}=\frac{\pi * 0.38 * 1200}{60} ; \quad U_{2}=23.88 \mathrm{~m} / \mathrm{s}$
$\eta_{m}=\frac{g H_{m}}{\overrightarrow{V_{u 2}} U_{2}} ; \quad 0.82=\frac{9.81 * 44.8}{\overrightarrow{V_{u 2}} * 23.88} ; \quad \overrightarrow{V_{u 2}}=22.44 \mathrm{~m} / \mathrm{s}$
$\overrightarrow{V_{u 2}}=U_{2}-V_{f 2} \cot \beta_{2} ; \quad 22.44=23.88-V_{f 2} \cot 35 \quad V_{f 2}=1 \mathrm{~m} / \mathrm{s}$
$Q=C \pi D_{2} B_{2} V_{f 2}$ where $C=1$ since there is no blockage, Hence $Q=\pi D_{2} B_{2} V_{f 2}$
$Q=\pi * 0.38 * 025 * 1 ; \quad Q=0.029845 \mathrm{~m}^{3} / \mathrm{s}$
Suction pressure:

$$
Q=\frac{\pi d_{s}^{2}}{4} * V_{s} ; \quad 0.029845=\frac{\pi * 0.15^{2}}{4} * V_{S} \quad V_{S}=1.69 \mathrm{~m} / \mathrm{s}
$$

$\frac{p_{s}}{\omega}=\frac{p_{a}}{\omega}-\frac{V_{s}^{2}}{2 g}-h_{s}-h_{f s} ; \quad \frac{p_{s}}{\omega}=10.3-\frac{1.69^{2}}{2 * 9.81}-4-1.8 \quad \frac{p_{s}}{\omega}=4.35$ of water

## delivery pressure

$\frac{p_{d}}{\omega}=\frac{p_{a}}{\omega}+h_{d}+h_{f d} \quad \frac{p_{d}}{\omega}=10.3+32+7 \quad \frac{p_{d}}{\omega}=49.3 \mathrm{~m}$ of water
5. A centrifugal pump impeller has radial vanes from inner radius of 8 cm to outer radius 24 cm . The width of the impeller is constant and is 6 cm between the shrouds. If the speed is 1500 rpm and the discharge is 25 litres/s. Find i) Change in enthalpy ii) The outlet pressure if inlet pressure is 0.8 kPa and flow is outward ( $7 \mathrm{c}, 8$, June/July16)
radial vanes, $\beta_{2}=90^{\circ} ; \quad R_{1}=8 \mathrm{~cm} ; \quad D_{1}=16 \mathrm{~cm}=0.16 \mathrm{~m} ; \quad R_{2}=24 \mathrm{~cm}$;
$D_{2}=48 \mathrm{~cm}=0.48 \mathrm{~m} B_{1}=B_{2}=6 \mathrm{~cm}=0.06 \mathrm{~m} ; N=1500 \mathrm{rpm} ; Q=25 \mathrm{litrs} / \mathrm{s}=0.025 \mathrm{~m}^{3} / \mathrm{s}$
$U_{2}=\frac{\pi D_{2} N}{60} ; \quad U_{2}=\frac{\pi * 0.48 * 1500}{60} ; \quad U_{2}=37.7 \mathrm{~m} / \mathrm{s}$
$Q=C \pi D_{2} B_{2} V_{f 2}$ where $C=1$ since there is no blockage, Hence $Q=\pi D_{2} B_{2} V_{f 2}$ $0.025=\pi * 0.48 * 0.06 * V_{f 2} ; \quad V_{f 2}=0.2763 \mathrm{~m} / \mathrm{s}$
Change in enthalpy $=\frac{E}{\dot{m}^{\prime}}$;
radial vanes, $\beta_{2}=90^{\circ}$

$$
\begin{array}{lll}
\overrightarrow{V_{u 2}}=U_{2} ; & \frac{E}{\dot{m}}=\frac{\overrightarrow{V_{u 2}} U_{2}}{g_{c}} & \frac{E}{\dot{m}}=\frac{U_{2} U_{2}}{g_{c}} ; \quad \frac{E}{\dot{m}}=\frac{37.7 * 37.7}{1} \\
\frac{E}{\dot{m}}=1421.29 \mathrm{~J} / \mathrm{kg} &
\end{array}
$$

The outlet pressure if inlet pressure is 0.8 kPa and flow is outward

$$
\begin{array}{ll}
\frac{p_{d}}{\omega}=\frac{p_{s}}{\omega}+H_{e} & \\
H_{e}=\frac{V_{u 2} U_{2}}{g} ; & H_{e}=\frac{U_{2} U_{2}}{g} \quad H_{e}=\frac{37.7^{2}}{9.81} ; \quad H_{e}=144.88 \mathrm{~m} \text { of } \text { water } \\
\frac{p_{d}}{\omega}=\frac{800}{9810}+144.88 ; & \frac{p_{d}}{\omega}=144.96 \mathrm{~m} \text { of water } \quad \frac{p_{d}}{9810}=144.96 \\
p_{d}=144.96 * 9810 ; & p_{d}=1422057.6 \mathrm{~N} / \mathrm{m}^{2} \quad p_{d}=1.422 \mathrm{bar}
\end{array}
$$

6. A centrifugal pump is to discharge $0.118 \mathrm{~m}^{3} / \mathrm{s}$ of water at a speed of 1450 rpm against a head of 25 m . The impeller diameter is 25 cm and its width at the outlet is 5 cm and manometric efficiency is $75 \%$ Calculate the vane angle at outlet ( $7 \mathrm{~b}, 6, \mathrm{Dec} 14 / \mathrm{Jan} 15$ )
$Q=0.118 \mathrm{~m}^{3} / \mathrm{s} ; N=1450 \mathrm{rpm} ; H_{m}=25 \mathrm{~m} ; D_{2}=25 \mathrm{~cm}=0.25 \mathrm{~m} ; \quad B_{2}=5 \mathrm{~cm}=0.05 \mathrm{~m} ;$
$\eta_{m}=75 \% ; \quad \beta_{2}=$ ?

## vane angle at outlet $\beta_{2}$

$Q=C \pi D_{2} B_{2} V_{f 2}$ where $C=1$ since there is no blockage, Hence $Q=\pi D_{2} B_{2} V_{f 2}$
$0.118=\pi * 0.25 * 0.05 * V_{f 2} ; \quad V_{f 2}=3 \mathrm{~m} / \mathrm{s}$
$U_{2}=\frac{\pi D_{2} N}{60}$;
$U_{2}=\frac{\pi * 0.25 * 1450}{60} ;$
$U_{2}=18.98 \mathrm{~m} / \mathrm{s}$
$\eta_{m}=\frac{g H_{m}}{\overline{V u}_{u_{2}} U_{2}} ;$
$0.82=\frac{9.81 * 25}{\overrightarrow{V_{u 2}} * 18.98} ;$
$\overrightarrow{V_{u 2}}=15.76 \mathrm{~m} / \mathrm{s}$
$\overrightarrow{V_{u 2}}=U_{2}-V_{f 2} \cot \beta_{2} ;$
$15.76=18.98-3 \cot \beta_{2} ;$
$\cot \beta_{2}=1.074$
$\tan \beta_{2}=0.93$
$\beta_{2}=42.98^{\circ}$
7. A centrifugal pump working in dock pumps 1565 lit/s against ahead (mean lift) of 6.1 m when the impeller rotates at 200 rpm . The impeller diameter is 122 cm and the area at outlet periphery is $6450 \mathrm{~cm}^{2}$. If the vanes are set back at an angle of $26^{\circ}$ at the outlet, find i) hydraulic efficiency ii) Pump required to drive the pump. If the ratio of external to internal diameter is 2 , find the minimum speed to start pumping (9b, 8,Dec18/Jan19 15 scheme )
$Q=1565 \mathrm{lit} / \mathrm{s}=1565 * 10^{-3} \mathrm{~m}^{3} / \mathrm{s} ; H_{m}=6.1 \mathrm{~m} ; \quad \mathrm{N}=200 \mathrm{rpm} ; ~ ; ~ D_{2}=122 \mathrm{~cm}=1.22 \mathrm{~m}$;
$A_{f 2}=6450 \mathrm{~cm}^{2}=6450 * 100^{-2} ; \quad \beta_{2}=26^{\circ} \eta_{m}=? ;$
Pump required to drive the pump $E=$ ?
If the ratio of external to internal diameter is 2 ie $\frac{D_{2}}{D_{1}}=2 N_{\text {min }}=$ ?
hydraulic efficiency
$\begin{array}{ccc}Q=A_{f 2} V_{f 2} ; & 1565 * 10^{-3}=6450 * 10^{-4} * V_{f 2} ; & V_{f 2}=2.43 \mathrm{~m} / \mathrm{s} \\ U_{2}=\frac{\pi D_{2} N}{60} ; & U_{2}=\frac{\pi * 1.22 * 200}{60} ; & U_{2}=12.78 \mathrm{~m} / \mathrm{s}\end{array}$
$\overrightarrow{V_{u 2}}=U_{2}-V_{f 2} \cot \beta_{2} ; \quad \overrightarrow{V_{u 2}}=12.78-2.43 \cot 26 ; \quad \overrightarrow{V_{u 2}}=7.8 \mathrm{~m} / \mathrm{s}$

$$
\eta_{m}=\frac{g H_{m}}{\overrightarrow{V_{u 2}} U_{2}} ; \quad \quad \eta_{m}=\frac{9.81 * 6.1}{7.8 * 12.78} ; \quad \eta_{m}=0.6
$$

## minimum speed to start pumping

For minimum starting speed

$$
\begin{array}{lc}
\frac{D_{2}}{D_{1}}=2 ; & \frac{1.22}{D_{1}}=2 \\
N_{\text {min }}^{2}=\left(\frac{60}{\pi}\right)^{2}\left(\frac{2 g H_{m}}{D_{2}^{2}-D_{1}^{2}}\right) ; & N_{\min }^{2}=\left(\frac{60}{\pi}\right)^{2}\left(\frac{2 * 9.81 * 6.1}{1.22^{2}-0.61^{2}}\right) ; \\
N_{\min }=197.75 \mathrm{rpm} &
\end{array}
$$

8. A centrifugal pump with 1.2 diameter runs at 200 rpm and pumps $1.88 \mathrm{~m}^{3} / \mathrm{s}$, the average lift being 6 m . The angle which the vane makes at exit with the tangent to the impeller is $26^{\circ}$ and radial velocity of flow is $2.5 \mathrm{~m} / \mathrm{s}$. Find manometric efficiency and the least speed to start pumping if the inner diameter being 0.6 m ( $7 \mathrm{c}, 8, \mathrm{Dec} 14 / \mathrm{Jan} 15$ )
9. A centrifugal pump has its impeller diameter 30 cm and a constant area of flow $210 \mathrm{~cm}^{2}$. The pump runs at 1440 rpm and delivers 90LPS against a head of 25 m . If there is no whirl velocity at entry, compute the rise in pressure head across the impeller and hydraulic efficiency of pump (9b, 08,June/July18)

## Rise in pressure head across the impeller

$D_{2}=30 \mathrm{~cm}=0.3 \mathrm{~m} ;$ constant area of flow $210 \mathrm{~cm}^{2} . A_{f 1}=A_{f 2}=210 \mathrm{~cm}^{2}$;

$$
A_{f 1}=A_{f 2}=210 * 10^{-4} \mathrm{~m}^{2} ; N=1440 \mathrm{rpm} ; \quad Q=90 \text { lit } / \mathrm{s}=90 * 10^{-3} \mathrm{~m}^{3} / \mathrm{s} ; H_{m}=25 \mathrm{~m}
$$

$Q=A_{f 2} V_{f 2} ;$

$$
90 * 10^{-3}=210 * 10^{-4} * V_{f 2}
$$

$$
V_{f 2}=4.28 \mathrm{~m} / \mathrm{s}
$$

$U_{2}=\frac{\pi D_{2} N}{60} ;$
$U_{2}=\frac{\pi * 0.3 * 1440}{60} ;$

$$
U_{2}=22.61 \mathrm{~m} / \mathrm{s}
$$

Blade angle at outlet is missing Hence assume $\beta_{2}=30^{\circ}$
$\overrightarrow{V_{u 2}}=U_{2}-V_{f 2} \cot \beta_{2} ;$

$$
\begin{aligned}
& \overrightarrow{V_{u 2}}=22.61-4.28 \cot 30 \\
& V_{2}^{2}=15.19^{2}+4.28^{2}
\end{aligned}
$$

$$
\overrightarrow{V_{u 2}}=15.19 \mathrm{~m} / \mathrm{s}
$$

$V_{2}^{2}=V_{u 2}^{2}+V_{f 2}^{2} ;$
$V_{2}^{2}=249.05$

Assuming flow velocity is constant $V_{f 1}=V_{f 2} ; \quad$ ie $V_{f 1}=4.28 \mathrm{~m} / \mathrm{s} ; \quad V_{1}=V_{f 1}=4.28 \mathrm{~m} / \mathrm{s}$
$H_{e}=\frac{V_{u 2} U_{2}}{g} ; \quad H_{e}=\frac{15.19 * 22.61}{9.81} \quad H_{e}=35 \mathrm{~m}$ of water
$\frac{p_{1}}{\omega}+\frac{V_{1}^{2}}{2 g}+H_{e}=\frac{p_{2}}{\omega}+\frac{V_{2}^{2}}{2 g} ; \quad \quad \frac{p_{1}}{\omega}+\frac{V_{1}^{2}}{2 g}+\frac{V_{u 2} U_{2}}{g}=\frac{p_{2}}{\omega}+\frac{V_{2}^{2}}{2 g} ; \quad \frac{p_{2}}{\omega}-\frac{p_{1}}{\omega}=\frac{V_{u 2} U_{2}}{g}-\left(\frac{V_{2}^{2}}{2 g}-\frac{V_{1}^{2}}{2 g}\right)$
$\frac{p_{2}}{\omega}-\frac{p_{1}}{\omega}=35-\left(\frac{249.05}{2 * 9.81}-\frac{4.28^{2}}{2 * 9.81}\right) ; \quad \frac{p_{2}}{\omega}-\frac{p_{1}}{\omega}=23.24 \mathrm{~m}$ of water

## hydraulic efficiency of pump

$\eta_{m}=\frac{g H_{m}}{V_{u 2} U_{2}}$;

$$
\eta_{m}=\frac{9.81 * 25}{15.19 * 22.61} ; \quad \eta_{m}=0.7140
$$

10. A centrifugal designed to run at 1450rpm, with a maximum discharge of 1800litrres $/ \mathrm{min}$ against a total head of 20 m . The suction and delivery pipes are designed such that they are equal in size of 100 mm . If the inner diameter and outer diameters of the impeller are 12 cm and 24 cm respectively. Determine the blade angles $\beta_{1}$ and $\beta_{2}$ for radial entry. Neglect friction and other losses (7c,10,Dec13/Jan14)
$N=1450 \mathrm{rpm} ; Q=1800 \mathrm{lit} / \mathrm{min}=1800 * 10^{-3} \mathrm{~m}^{3} / \mathrm{min}$ $Q=\frac{1800}{60} 10^{-3} \mathrm{~m}^{3} / \mathrm{s} ; Q=30 * 10^{-3} \mathrm{~m}^{3} / \mathrm{s} ; H_{m}=30 \mathrm{~m} ; d_{s}=d_{d}=100 \mathrm{~mm} d_{s}=d_{d}=0.1 \mathrm{~m}$
$D_{1}=12 \mathrm{~cm}=0.12 \mathrm{~m} ; D_{2}=24 \mathrm{~cm}=0.24 \mathrm{~m}$
Neglect friction and other losses ie $\eta_{m}=1$
i) $\quad \beta_{1}=$ ?
li) $\beta_{2}=$ ?
$Q=\frac{\pi d_{s}^{2}}{4} V_{f 1} ; \quad$ Also $Q=\frac{\pi d_{d}^{2}}{4} V_{f 2}$
$Q=\frac{\pi d_{S}^{2}}{4} V_{f 1} ;$
$30 * 10^{-3}=\frac{\pi * 0.1^{2}}{4} V_{f 1}$
$V_{f 1}=3.82 \mathrm{~m} / \mathrm{s}$
$Q=\frac{\pi d_{d}^{2}}{4} V_{f 2} ;$
$30 * 10^{-3}=\frac{\pi * 0.1^{2}}{4} V_{f 2}$
$V_{f 2}=3.82 \mathrm{~m} / \mathrm{s}$
$U_{1}=\frac{\pi D_{1} N}{60}$;

$$
U_{2}=\frac{\pi * 0.12 * 1450}{60} \text {; }
$$

$$
U_{1}=9.11 \mathrm{~m} / \mathrm{s}
$$

$U_{2}=\frac{\pi D_{2} N}{60}$;
$U_{2}=\frac{\pi * 0.24 * 1440}{60}$;
$U_{2}=18.22 \mathrm{~m} / \mathrm{s}$
$1=\frac{9.81 * 30}{\overrightarrow{V_{u 2}} * 18.22}$;
$\overrightarrow{V_{u 2}}=16.15 \mathrm{~m} / \mathrm{s}$
$\overrightarrow{V_{u 2}}=U_{2}-V_{f 2} \cot \beta_{2} ;$
$16.15=18.22-3.82 \cot \beta_{2} ;$
$\cot \beta_{2}=0.54$
$\tan \beta_{2}=1.85 ; \quad \beta_{2}=61.54^{\circ}$
$\tan \beta_{1}=\frac{V_{f 1}}{U_{1}} ; \quad \quad \tan \beta_{1}=\frac{3.82}{9.11} ;$

$$
\beta_{1}=22.74^{\circ}
$$

11. A 3 stage centrifugal pump has impeller each of 38 cm diameter and 1.9 cm wide at outlet. The vane are curved at anangle is $45^{\circ}$ at the outlet and reduced the circumferential area by $10 \%$. The manometric efficiency is $90 \%$ and overall efficiency is $0.8 \%$. Find the total head generated by the pump when running at 1000 rpm delivering 50 litres $/ \mathrm{s}$. Also calculate the power required to drive the pump(7c, 10, June July 17)*
12. A centrifugal pump having outer diameter equal to two times the inner diameter and running at 1000rpm works against a total head of 40 m . The velocity of flow through the impeller is constant and equal to $2.5 \mathrm{~m} / \mathrm{s}$. The vanes are set back at an angle of $40^{\circ}$ at outlet. Of the outer diameter of the impeller is 500 mm and width at outlet is 50 mm , determine i) vane angle at inlet ii) Work done by impeller on water /s iii) manometric efficiency (7c, 8,Dec16/Jan 17)
outer diameter equal to two times the inner diameter ie $D_{2}=2 D_{1}$;
$N=1000 \mathrm{rpm} ; H_{m}=40 \mathrm{~m} ; V_{f 1}=V_{f 2}=2.5 \mathrm{~m} / \mathrm{s} ; \beta_{2}=40^{\circ} ; D_{2}=500 \mathrm{~mm}=0.5 \mathrm{~m} ;$
$B_{2}=50 \mathrm{~mm}=0.05 \mathrm{~m} ;$ i) $\beta_{1}=$ ? ii) $E=$ ? iii) $\eta_{m}=$ ?
vane angle at inlet
$D_{2}=2 D_{1}$;

$$
0.5 m=2 D_{1}
$$

$$
D_{1}=0.25 m
$$

$U_{1}=\frac{\pi D_{1} N}{60}$;
$U_{2}=\frac{\pi * 0.25 * 1000}{60}$;
$U_{1}=13.09 \mathrm{~m} / \mathrm{s}$

$$
\tan \beta_{1}=\frac{V_{f 1}}{U_{1}} ; \quad \tan \beta_{1}=\frac{2.5}{13.09^{\prime}} ; \quad \beta_{1}=10.81^{\circ}
$$

## Work done by impeller on water/s

$$
Q=C \pi D_{2} B_{2} V_{f 2} \text { where } C=1 \text { since there is no blockage, Hence } Q=\pi D_{2} B_{2} V_{f 2}
$$

$$
\begin{array}{llr}
Q=\pi * 0.5 * 0.05 * 2.5 ; & & Q=0.1963 \mathrm{~m}^{3} / \mathrm{s} \\
\quad \dot{m}=\rho Q ; & & \\
\quad \dot{m}=1000 * 0.1963 & \dot{m}=196.3 \mathrm{~kg} / \mathrm{s} \\
U_{2}=\frac{\pi D_{2} N}{60} ; & U_{2}=\frac{\pi * 0.5 * 1000}{60} ; & U_{2}=26.17 \mathrm{~m} / \mathrm{s} \\
\overrightarrow{V_{u 2}}=U_{2}-V_{f 2} \cot \beta_{2} ; & \overrightarrow{V_{u 2}}=26.17-2.5 \cot 40 ; & \overrightarrow{V_{u 2}}=23.19 \mathrm{~m} / \mathrm{s} \\
\frac{E}{\dot{m}}=\frac{V_{u 2} U_{2}}{g_{c}} ; & \frac{E}{196.3}=\frac{23.19 * 26.17}{1} & E=119134.16 \mathrm{Watts}
\end{array}
$$

13. A centrifugal pump having outer diameter equal to two times the inner diameter and running at 1200 rpm works against a total head of 75 m . The velocity of flow through the impeller is constant and equal to $3 \mathrm{~m} / \mathrm{s}$. The vanes are set back at an angle of $30^{\circ}$ at outlet. Of the outer diameter of the impeller is 60 cm and width at outlet is 5 cm , determine i) vane angle at inlet ii) Work done by impeller on water /s iii) manometric efficiency (7b,08,June/July14)
14. The outer diameter of a pump is 50 cm and inner diameter is 25 cm and runs at 1000 rpm against a head of 40 m . Velocity of flow is constant and is equal to $2.5 \mathrm{~m} / \mathrm{s}$. Vanes are set back an angle $40^{\circ}$ at the outlet. Width at outlet is 5 cm Find i) Vane angle at inlet ii) Work done by impeller iii) Manometric efficiency ( 6b, 10,June July 13)
15. The outer diameter of the impeller of a centrifugal pump is 40 cm and Width of the impeller at outlet is 5 cm The pump is running at 800 rpm and working against a total head of 1.5 m . The Vanes angle at outlet $40^{\circ}$ and manometric efficiency is $75 \%$. Determine i) velocity of flow at outlet ii) velocity of water leaving the vane iii) Angle made by the absolute velocity at outlet with the direction of motion at outlet iv) Discharge ( 7b, 08,Dec18/Jan19) (7b, 10,Dec17/Jan18)

$$
D_{2}=40 \mathrm{~cm}=0.4 \mathrm{~m} ; B_{2}=5 \mathrm{~cm}=0.05 \mathrm{~m} ; \quad N=800 \mathrm{rpm} ; H_{m}=15 \mathrm{~m} ; \beta_{2}=40^{\circ} ; \eta_{m}=75 \%
$$

$$
\text { i) } V_{f 2}=\text { ? } \text { ii) } V_{2}=\text { ? ii) } \alpha_{2}=\text { ? iii) } Q=\text { ? }
$$

## i) velocity of flow at outlet

$U_{2}=\frac{\pi D_{2} N}{60} ;$
$U_{2}=\frac{\pi * 0.4 * 800}{60} ;$

$$
U_{2}=16.76 \mathrm{~m} / \mathrm{s}
$$

$$
\eta_{m}=\frac{g H_{m}}{\overline{V_{u 2} U_{2}}}
$$

$$
0.75=\frac{9.81 * 15}{\overrightarrow{V_{u 2}} * 16.76}
$$

$$
\overrightarrow{V_{u 2}}=11.71 \mathrm{~m} / \mathrm{s}
$$

$\overrightarrow{V_{u 2}}=U_{2}-V_{f 2} \cot \beta_{2} ; \quad \quad 11.71=16.76-V_{f 2} \cot 40 ; \quad V_{f 2}=4.23 \mathrm{~m} / \mathrm{s}$
ii) velocity of water leaving the vane
$V_{2}^{2}=V_{u 2}^{2}+V_{f 2}^{2} ; \quad V_{2}^{2}=11.71^{2}+4.23^{2} ; \quad V_{2}^{2}=155.08$
$V_{2}=12.45 \mathrm{~m} / \mathrm{s}$
iii) Angle made by the absolute velocity at outlet with the direction of motion at outlet
$\tan \alpha_{2}=\frac{V_{f 2}}{U_{2}} ; \quad \quad \tan \alpha_{2}=\frac{4.23}{16.76} \quad \alpha_{2}=14.16^{\circ}$
iv) Discharge
$Q=C \pi D_{2} B_{2} V_{f 2}$ where $C=1$ since there is no blockage, Hence $Q=\pi D_{2} B_{2} V_{f 2}$
$Q=\pi * 0.4 * 0.05 * 4.23 ; \quad Q=0.266 \mathrm{~m}^{3} / \mathrm{s}$
16. A three stage centrifugal pump has impeller of 40 cm diameter and 2.5 cm wide at the outlet. The vanes are curved back at outlet at $30^{\circ}$ and reduce the circumferential area by $15 \%$. The manometric efficiency is $85 \%$ and overall efficiency is $75 \%$. Determine the head generated by the pump when running at 12000 rpm , and discharging the water at $0.06 \mathrm{~m}^{3} / \mathrm{s}$. Find the shaft power also
17. A 4 stage centrifugal pump has impellers each of 38 cms diameter and 1.9 cm wide at outlet. The outlet vane angle is $49^{\circ}$ and vanes occupy $8 \%$ of outlet area. The manometric efficiency is $84 \%$ and overall efficiency is $75 \%$. Determine the head generated by the pump when running at 900rpm discharging 59litres per sec
18. A centrifugal pump is running at 1000 rpm , the output vane angle of the impeller is $45^{\circ}$ and the velocity of flow at outlet is $2.5 \mathrm{~m} / \mathrm{s}$. The discharge through the pump is 200lit/s, when the pump is working against the total head of 20 m . If the manometric efficiency of the pump is $80 \%$, determine : i) Diameter of the impeller ii) width of the impeller at outlet
19. The diameters of the impeller of a centrifugal pump are 30 cm and 60 cm respectively. The velocity of flow at outlet is $2 \mathrm{~m} / \mathrm{s}$ and the vanes are set back at an angle of $45^{\circ}$ at outlet. Determine the minimum starting speed of the pump if its manometric efficiency is $70 \%$
20. A centrifugal pump with impeller outer diameter 1.5 m runs at 180 rpm and pumps $1.9 \mathrm{~m}^{3} / \mathrm{s}$. The average lift is 8.0 m . The angle which the vane makes at exit with the tangent to the impeller is
$24^{\circ}$ and the radial velocity is $2.8 \mathrm{~m} / \mathrm{s}$. Determine the manometric efficiency of the centrifugal pump
21. A centrifugal pump delivers 50 lit/s against a total head of 24 m when running at 1500 rpm . The velocity of the flow is maintained constant at $2.4 \mathrm{~m} / \mathrm{s}$. and blades are curved back at $30^{\circ}$ to the tangent at outlet. The inner diameter is half the outer diameter. If the manometric efficiency is $80 \%$, determine i) Blade angle at inlet ii) Power required to drive the pump)(7b, 10,June/July 18)*
$Q=50 \mathrm{lit} / \mathrm{s} ; H_{m}=24 \mathrm{~m} ; N=1500 \mathrm{rpm} ; \quad V_{f 1}=V_{f 2}=2.4 \mathrm{~m} / \mathrm{s} ; \beta_{2}=30^{\circ}$;
The inner diameter is half the outer diameter ie $D_{1}=\frac{1}{2} D_{2} ; \eta_{m}=80 \%$ i) $\beta_{1}=$ ? ; ii) $E=$ ?
i) Blade angle at inlet
$\overrightarrow{V_{u 2}}=U_{2}-V_{f 2} \cot \beta_{2} ; \quad \overrightarrow{V_{u 2}}=U_{2}-2.4 \cot 40 \quad \overrightarrow{V_{u 2}}=U_{2}-2.86$
$\eta_{m}=\frac{g H_{m}}{\bar{V}_{u 2} U_{2}} ; \quad 0.8=\frac{9.81 * 24}{\left(U_{2}-2.86\right) U_{2}} ; \quad 0.8\left(U_{2}-2.86\right) U_{2}=235.44$
$\left(U_{2}-2.86\right) U_{2}=294.3 ;$
$U_{2}^{2}-2.86 U_{2}=294.3 \quad U_{2}^{2}-2.86 U_{2}-294.3=0$
$U_{2}=\frac{-b \pm \sqrt{b^{2}-4 a c}}{2 a} ; \quad U_{2}=\frac{+2.86 \pm \sqrt{2.86^{2}-(4 * 1 *[-294.3])}}{2 * 1} ;$
$U_{2}=\frac{\pi D_{2} N}{60} ;$
$18.64=\frac{\pi * D_{2} * 1500}{60} ;$
$D_{2}=0.237 m$
$D_{1}=\frac{1}{2} D_{2} ;$
$D_{1}=\frac{1}{2} * 0.237 ; \quad D_{1}=0.119 m$
$U_{1}=\frac{\pi D_{1} N}{60} ;$

$$
U_{2}=\frac{\pi * 0.119 * 1500}{60} ;
$$

$$
U_{1}=9.32 \mathrm{~m} / \mathrm{s}
$$

$\tan \beta_{1}=\frac{V_{f 1}}{U_{1}} ;$
$\tan \beta_{1}=\frac{2.4}{9.32} ;$
$\beta_{1}=13.43^{\circ}$
Power required to drive the pump
$\overrightarrow{V_{u 2}}=U_{2}-2.86 ; \quad \overrightarrow{V_{u 2}}=18.64-2.86 ; \quad \overrightarrow{V_{u 2}}=15.78 \mathrm{~m} / \mathrm{s}$
$Q=C \pi D_{2} B_{2} V_{f 2}$ where $C=1$ since there is no blockage, Hence $Q=\pi D_{2} B_{2} V_{f 2}$
$Q=\pi * 0.237 * 0.05 * 2.4 ; \quad Q=0.0893 \mathrm{~m} / \mathrm{s}$
$\dot{m}=\rho Q ; \quad \dot{m}=1000 * 0.0893 \quad \dot{m}=89.3 \mathrm{~kg} / \mathrm{s}$
$\frac{E}{\dot{m}}=\frac{V_{u 2} U_{2}}{g_{c}} ;$
$\frac{E}{89.3}=\frac{15.78 * 26.17}{1}$
$E=36877.56 \mathrm{Watts}$
22. The outer diameter of the impeller of a centrifugal pump is 40 cm and width of the impeller at outlet is 5 cm . The pump is running at 800 rpm and is working against a total head of 15 m . The vane angle at outlet is $40^{\circ}$ and manometric efficiency is $75 \%$. Determine i) Velocity of flow at outlet ii) Velocity of water leaving the vane iii) Angle made by the absolute velocity at outlet with the direction of motion at outlet iv) Discharge
23. A backward swept centrifugal fan develops a pressure of 75 mm W.G. It has an impeller diameter of 89 cm and runs at 720 rpm . The blade angle at the tip is $39^{\circ}$ and the width of the impeller 10 cm . Assuming a constant radial velocity of $9.15 \mathrm{~m} / \mathrm{s}$ and density of $1.2 \mathrm{~kg} / \mathrm{m}^{3}$, determine the fan efficiency , discharge, power required, stage reaction and pressure coefficient
24. A centrifugal pump discharges $0.15 \mathrm{~m}^{3} / \mathrm{s}$ of water against a head of 12.5 m , the speed of the impeller being 600 rpm . The outer and inner diameter of the impeller are 50 cm and 20 cm respectively and the vanes are bent back at $35^{\circ}$ to the tangential at the exit. If the area of flow remains $0.07 \mathrm{~m}^{2}$ from inlet to outlet, calculate i) manometric efficiency of the pump ii) vane angle at inlet iii) loss of head at inlet to the impeller when the discharge is reduced by $40 \%$ without changing the speed
25. The following data refers to a Centrifugal pump: Pump being single stage radial bladed. i)impeller diameter $=120 \mathrm{~mm}$ ii) Discharge gauge reading $=1.5$ bar iii) Suction gauge reading $=150 \mathrm{~mm}$ of Hg below atmosphere iv) RPM $=1440 \mathrm{v}$ ) Flow rate $=240 \mathrm{lit} / \mathrm{min}$ vi) Power required $=1 \mathrm{~kW}$ vii) Impeller width at tip= 10 mm . Find Overall efficiency and specific speed
26. A centrifugal pump has its impeller diameter 30 cm and a constant area of flow $210 \mathrm{~cm}^{2}$. The pump runs at 1440 rpm and delivers 90 lps against a head of 25 m . If there is no whirl velocity at entry, compute the rise in pressure head across the impeller and hydraulic efficiency of pump. The vanes at exit are bent back at $22^{\circ}$ wrt tangential speed
27. A centrifugal pump with an impeller outer diameter of 1.05 m runs at 1000RPM. The blades are backward curved and they makes an angle of $20^{\circ}$ with the wheel tangent at the blade tip. If the radial velocity of flow at the tip is $8 \mathrm{~m} / \mathrm{s}$ and the slip coefficient is 0.86 . Find i) The actual work input /kg of water flow ii) the absolute velocity of fluid at the impeller tip and iii) hydraulic efficiency.If the pump is fitted with diffusion chamber with an efficiency of 0.75 , so that the exit velocity is reduced to $5 \mathrm{~m} / \mathrm{s}$. Find the new efficiency
28. A single stage centrifugal pump with a impeller of diameter of 30 cm rotates at 2000 rpm and lifts $3 \mathrm{~m}^{3} / \mathrm{s}$ water to a height of 40 m with a manometric efficiency of $75 \%$. Find the number of stages
and diameter of each impeller of a multistage pump to lift $5 \mathrm{~m}^{3} / \mathrm{s}$ of water to height of 200 m when rotating at 1500 rpm
29. Explain the phenomenon of surging, stalling and choking in centrifugal compressor stage (7a, 5June July 17)

## Module 5 compressors

1. With neat schematic diagram, explain an axial flow compressor, Also sketch the general velocity triangles for an axial flow compressor(8a, 10, Dec18/19)
2. With a neat sketch, explain the axial flow compressor (8b, 6, Dec16/Jan17)
3. What are the types of diffuser ? Explain any two (10b, 08 Dec18/Jan19CBCS)
4. What is a function of diffuser? Name the different types of diffusers and explain them with neat sketch (8a,10,June/July 18)
5. Draw the velocity triangles at the entry and exit for the axial compressor stage (8b,6,June/July14) (
6. Explain the working principle of axial flow compressor along with a neat sketch of compressor (10a, 10,June/July18)
7. For axial flow compressor show that $E=V_{f} U\left(\frac{\tan \beta_{2}-\tan \beta_{1}}{\tan \beta_{1} \tan \beta_{2}}\right)(10 a, 08$ Dec18/Jan19CBCS $)$
8. Derive an expression for overall pressure ratio for a centrifugal compressor in terms of impeller tip speed, slip . power input factor and isentropic efficiency of compressor(8a,12,Dec 13/Jan14 )
9. With the help of H-Q plot explain the phenomenon of surging in centrifugal compressor(8a, 10,June/July13)
10. Define the following terms of centrifugal compressor i) slip factor, ii) Power factor and iii) Pressure coefficient (8a,6,June/July 16)
11. Explain slip and slip coefficient (8a,5,June/July17) and slip factor (8a, 06,Dec14/Jan15)
12. Define the following terms of centrifugal compressor:i) overall pressure ratio i) slip factor, ii) Power factor and iii) Pressure coefficient (8a, 08,Dec12)
13. Explain surging and choking of compressor (8b,5June/July17) (8b,4,June/July 16)(8b, 04,Dec14/Jan15) (8b, 08,Dec12)
14. Explain surging , stalling and Slip factor with reference a compressor (8a, 8,Dec15/Jan16)(8a,6,June/July14)
15. Explain the phenomenon of surging and stalling in centrifugal compressor(8a, 6, Dec16/Jan17) and Choking(8a,6,June/July14)
16. What is radial equilibrium in an axial flow compressor? Derive an expression for radial equilibrium in terms of flow velocity and whirl velocity of fluid (8a,10, Dec17/Jan18)
17. What is a function of diffuser? Name the different types of diffusers and explain them with neat sketch (8a,10,June/July 18)

## Axial flow compressor

An axial flow compressor is essentially an axial flow turbine driven the reverse direction. The turning angle is very small preferably lower than $30^{\circ}$ to avoid flow separation.

It consists of number of fixed blades which are attached to the casing and alternative rows of moving blades on to the shaft which is mounted on bearings. Air progresses from one blade row to the next blade rows guided through the fixed blades. Fixed blades serves the function of diffuser and hence the pressure of air increases when it comes out of it. Air flows in the compressor parallel to the shaft.

The usual type of compressor is of $50 \%$ degree of reaction in which static enthalpy change in rotor is half the stage static enthalpy change (total head). In 50\% Reaction compressor velocity triangle at inlet and outlet are symmetrical as in the case of $50 \%$ reaction turbine. It is necessary to achieve prewhirl at inlet so as to maintain the Mach number below 0.9 as it required for high efficiency.

Because of low turning angle the pressure rise per stage is very small. However, the large axial velocity of flow at the exit can cause more losses and hence it leads to a low total to static efficiency.

For ideal condition diffuser inlet angle $\alpha_{1}$ is same as the fluid angle at inlet of the rotor
If the fluid enters axially, no guide vane blades are required ie $\alpha_{1}=90^{\circ}$, the static pressure rise in the rotor blades is much larger than in the stator blades. Because of the large relative velocities compared to $50 \%$ reaction, the stage efficiency is lower than that of symmetrical stage.

If the fluid leaves axially $\alpha_{2}=90^{\circ}$ the static pressure rise occurs entirely in the rotor blades, the stator blades causing only a small pressure rise. The degree of reaction is therefore greater than $100 \%$. The energy transfer per stage is low and hence stage efficiency also . But due to low exit velocity, the overall efficiency is likely to be larger than the other types of compressors with $\mathrm{R}<0.5, \mathrm{R}=0.5, \mathrm{R}<1$

With neat schematic diagram, explain an axial flow compressor, Also sketch the general velocity triangles for an axial flow compressor(8a, 10, Dec18/19)

A single stage axial flow compressor consisting one row of inlet guide vanes, one row of rotor blades (moving blades) and one row of diffusers (fixed blades) as shown in figure 4.1(a). The main function of the inlet guide vane is to control the direction of fluid flow at the rotor inlet. The rotor blades exert a torque on the fluid, its pressure and velocity increases. The diffuser blades increase the fluid pressure further by decreasing fluid velocity. The pressure and velocity variations through an axial flow compressor stage are shown in the figure


Fig. 4.1 The pressure and velocity variations through an axial flow compressor stage
The general velocity triangles for an axial flow compressor are shown in the figure For axial flow compressors the mean tangential rotor velocity remains constant ( $U_{1}=U_{2}=U$ ). If the flow is repeated in another stage of axial flow compressor, then $V_{I}=V_{3}$ and $\alpha_{1}=\alpha_{3}$.


Velocity triangles for an axial flow compressor

## Work Input and Efficiencies in Compressor

All are centrifugal turbo machines are radial flow power absorbing turbo machines In axial flow power absorbing turbo machine $U_{1}=U_{2}=U$

In radial flow power absorbing turbo machine $U_{1} \neq U_{2}$
In power absorbing turbo machine
$\frac{E}{\dot{m}}=\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right)$ is negative ie $\overrightarrow{V_{u 2}} U_{2}>\overrightarrow{V_{u 1}} U_{1}$
Turning angle of fluid from inlet to outlet is small

## Axial flow Compressor

General Inlet velocity triangle


General outlet velocity triangle


In axial flow power absorbing turbomachine, since $U_{1}=U_{2}$ outlet and inlet velocity triangles can be drawn with common base

$\gamma$ are called air angles
$\gamma_{1}$ is called air angle at inlet, $\gamma_{2}$ is called as air angle at outlet
output per unit mass $\frac{E}{\dot{m}}=\frac{1}{\mathrm{~g}_{\mathrm{c}}}\left(\overrightarrow{V_{u 1}} U_{1}-\overrightarrow{V_{u 2}} U_{2}\right)$
output per unit mass $\frac{E}{\dot{m}}=\frac{1}{\mathrm{~g}_{\mathrm{c}}}\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) U \quad$ since $U_{1}=U_{2}=U$
This expression will have negative value in power absorbing machine since $\overrightarrow{V_{u 2}}>\overrightarrow{V_{u 1}}$ therefore, generally In power absorbing we express Input/per unit mass

Input/per unit mass ie $-\frac{E}{\dot{m}}=\frac{1}{\mathrm{gc}_{\mathrm{c}}}\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right) U$

## le negative of output =Input

## When the kinetic energy is neglected

The actual work Input, $\quad W_{a}=h_{2}-h_{1}$;

$$
W_{a}=C_{P}\left(T_{2}-T_{1}\right)
$$

The Ideal work, $\quad W_{s}=h_{2 s}-h_{1}$

$$
W_{s}=C_{P}\left(T_{2 s}-T_{1}\right)
$$

$\eta_{s-s}=\frac{W_{s}}{W_{a}} ;$
$\eta_{s-s}=\frac{C_{P}\left(T_{2 s}-T_{1}\right)}{C_{P}\left(T_{2}-T_{1}\right)} ;$
$\eta_{s-s}=\frac{\left(T_{2 s}-T_{1}\right)}{\left(T_{2}-T_{1}\right)}$
$\eta_{s-s}=\frac{T_{1}\left(\frac{T_{2 s}}{T_{1}}-1\right)}{T_{2}-T_{1}}$
But $\frac{T_{2 s}}{T_{1}}=\left(\frac{p_{2}}{p_{1}}\right)^{\frac{\gamma-1}{\gamma}} ; \quad \frac{T_{2 s}}{T_{1}}=\left(p_{r}\right)^{\frac{\gamma-1}{\gamma}} \quad$ where $p_{r}$ is the static pressure ratio
$\eta_{\text {stage } s-s}=\frac{T_{1}\left(p_{r}^{\gamma-1}-1\right)}{T_{2}-T_{1}} ;$
$\eta_{s}=\frac{W_{S}}{W_{a}} ;$
$W_{a}=\frac{C_{P}\left(T_{2 s}-T_{1}\right)}{\eta_{s-s}} ;$
$W_{a}=\frac{C_{P} T_{1}\left(\frac{T_{2 s}}{T_{1}}-1\right)}{\eta_{s-s}}$
$W_{a}=\frac{C_{P} T_{1}\left(\frac{T_{2 s}}{T_{1}}-1\right)}{\eta_{s-s}} ; \quad W_{a}=\frac{C_{P} T_{1}\left(\left(\frac{p_{2}}{p_{1}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\eta_{s-s}} ; \quad W_{a}=\frac{C_{P} T_{1}\left(p_{r}^{\frac{\gamma-1}{\gamma}}-1\right)}{\eta_{s}}$ where $p_{r}$ is the
static pressure ratio
For more general case, when the kinetic energy is significant then, the actual work required is
$\eta_{s}=\frac{W_{S}}{W_{a}} ;$
$\eta_{\text {stage } t-t}=\frac{W_{S t-t}}{W_{a t-t}} ;$
$W_{\text {a stage } t-t}=\frac{W_{S t-t}}{\eta_{t-t}}$
$W_{\text {astage } t-t}=\frac{C_{P}\left(T_{02 s}-T_{01}\right)}{\eta_{s-s}} ; \quad W_{\text {astage } t-t}=\frac{C_{P} T_{01}\left(\frac{T_{02 s}}{T_{01}}-1\right)}{\eta_{t-t}} ; \quad W_{\text {at }-t}=\frac{C_{P} T_{01}\left(\left(\frac{p_{02}}{p_{01}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\eta_{t-t}}$
$W_{\text {astage } t-t}=\frac{C_{P} T_{01}\left(p_{r}^{\frac{\gamma-1}{\gamma}}-1\right)}{\eta_{t-t}} ; \quad p_{r}^{\frac{\gamma-1}{\gamma}}-1=\frac{\eta_{t-t} W_{a t-t}}{C_{P} T_{01}} ; \quad p_{r 0}=\left(\frac{\eta_{t-t} W_{a t-t}}{C_{P} T_{01}}+1\right)^{\frac{\gamma}{\gamma-1}}$
$p_{r 0}=\left(\frac{\eta_{t-t} C_{P}\left(T_{02}-T_{01}\right)}{C_{P} T_{01}}+1\right)^{\frac{\gamma}{\gamma-1}} ; \quad p_{r 0}=\left(\frac{\eta_{t-t}\left(T_{02}-T_{01}\right)}{T_{01}}+1\right)^{\frac{\gamma}{\gamma-1}} ;$
$\eta_{t-t}$ and $\eta_{s-s}$ are not differ much for compressor and generally both are same. Hence, isentropic efficiency of compressor is generally based on static values

## Work Done factor:

Due to the growth of boundary layers on the hub and casing of the axial flow compressor, the axial velocity along the blade height is not uniform. This effect is not so significant in the first stage of a multi-stage machine but is quite significant in the subsequent stages.


Fig :Axial velocity profile along blade height in an axial flow compressor
Figure shows the axial velocity distribution in the first and last stages of a multi-stage axial flow compressor. The degree of distortion in the axial velocity distribution will depend on the number of the stages. On account of this, axial velocity in the hub and tip regions is much less than the mean value, whereas in the central region its value is higher than the mean.

In cascade design, generally the value of $\alpha_{1}, \beta_{1}$ and $U$ will be kept constant. It may be the work absorption capacity decreases with an increase in the axial velocity and vice versa. Therefore, the work absorbing capacity of the stage is reduced in the central region of the annulus and increased in the hub and tip region. However, the expected increase in the work at the tip and hub is not obtained in actual practice on account of higher losses. Therefore stage work is less than that given by the Euler's equation based on a constant value of the axial velocity along the blade height. This reduction in the work absorbing capacity of the stage is taken into account by a "work done factor".

The work done factor $(\Omega)$ is defined as the ratio of stage work to Euler's work. It can also be defined as the ratio of actual work absorbing capacity to ideal work absorbing capacity

## Diffuser

Diffuser is a set of stationary vanes that surround the impeller. The purpose of diffuser is to increase the efficiency by allowing a more gradual expansion and less turbulent area for the liquid and convert the velocity energy at the exit of the the rotor to pressure energy,

Diffusers can be vaneless, vaned or an alternating combination. High efficiency vaned diffusers are also designed over a wide range of solidities from less than 1 to over 4 . Hybrid versions of vaned diffusers include: wedge, channel, and pipe diffusers. Some turbochargers have no diffuser.

Bernoulli's fluid dynamic principle plays an important role in understanding diffuser perform
Vaneless diffusers have a wider flow range but lower pressure recovery and efficiency, whereas vaned diffusers have higher pressure recovery and efficiency, but narrower flow range. ...

The diffuser with the constant area diffuser has a slightly lower efficiency but the operation range was larger.


1. For axial flow compressor show that $E=V_{f} U\left(\frac{\tan \beta_{2}-\tan \beta_{1}}{\tan \beta_{1} \tan \beta_{2}}\right)(10 a, 08 \operatorname{Dec} 18 / J a n 19 C B C S)$

$\frac{E}{\dot{m}}=\frac{1}{\mathrm{~g}_{\mathrm{c}}}\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) \mathrm{U}$;
$-\frac{E}{\dot{m}}=\frac{1}{\mathrm{~g}_{\mathrm{c}}}\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) \mathrm{U}$
$\tan \gamma_{0}=\frac{\overrightarrow{V_{u 1}}}{V_{a}} ; \quad \overrightarrow{V_{u 1}}=V_{a} \tan \gamma_{o} ; \quad \tan \gamma_{3}=\frac{\overrightarrow{V_{u 2}}}{V_{a}} ; \quad \overrightarrow{V_{u 2}}=V_{a} \tan \gamma_{3}$
$-\frac{E}{\dot{m}}=\frac{1}{\mathrm{~g}_{\mathrm{c}}}\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right) \mathrm{U}$
$-\frac{E}{\dot{m}}=\frac{1}{\mathrm{~g}_{\mathrm{c}}}\left(V_{a} \tan \gamma_{3}-V_{a} \tan \gamma_{o}\right) \mathrm{U} ;$

$$
\begin{aligned}
& -\frac{E}{\dot{m}}=\frac{V_{a}}{\mathrm{~g}_{\mathrm{c}}}\left(\tan \gamma_{3}-\tan \gamma_{o}\right) \mathrm{U} \\
& \text { also } U=V_{a}\left(\tan \gamma_{2}+\tan \gamma_{3}\right) \\
& \quad \tan \gamma_{0}+\tan \gamma_{1}=\tan \gamma_{2}+\tan \gamma_{3}
\end{aligned}
$$

$U=V_{a}\left(\tan \gamma_{0}+\tan \gamma_{1}\right) ;$
$V_{a}\left(\tan \gamma_{0}+\tan \gamma_{1}\right)=V_{a}\left(\tan \gamma_{2}+\tan \gamma_{3}\right)$;
$\tan \gamma_{3}-\tan \gamma_{o}=\tan \gamma_{1}-\tan \gamma_{2}$
Hence, $-\frac{E}{\dot{m}}=\frac{V_{a}}{\mathrm{~g}_{\mathrm{c}}}\left(\tan \gamma_{1}-\tan \gamma_{2}\right) \mathrm{U}$
$\gamma_{1}=180-\beta_{1} ; \tan \gamma_{1}=\tan \left(180-\beta_{1}\right) ; \tan \gamma_{1}=\cot \beta_{1}$
$\gamma_{2}=180-\beta_{1} ; \tan \gamma_{2}=\tan \left(180-\beta_{2}\right) ; \tan \gamma_{2}=\cot \beta_{2}$
$-\frac{E}{\dot{m}}=\frac{V_{a}}{\mathrm{~g}_{\mathrm{c}}}\left(\cot \beta_{1}-\cot \beta_{2}\right) \mathrm{U} ; \quad-\frac{E}{\dot{m}}=\frac{V_{a}}{\mathrm{~g}_{\mathrm{c}}}\left(\frac{1}{\tan \beta_{1}}-\frac{1}{\tan \beta_{2}}\right) \mathrm{U} ;-\frac{E}{\dot{m}}=\frac{V_{a}}{\mathrm{~g}_{\mathrm{c}}} U\left(\frac{\tan \beta_{2}-\tan \beta_{1}}{\tan \beta_{1} \tan \beta_{2}}\right)$
Power Input in axial flow compressor is $\frac{V_{a}}{\mathrm{~g}_{c}}\left(\frac{\tan \beta_{2}-\tan \beta_{1}}{\tan \beta_{1} \tan \beta_{2}}\right) U$
2. Define degree of reaction for an axial flow machine. Prove that degree of reaction for an axial flow device (assuming constant velocity of flow ) is given by $R=\frac{V_{f}}{2 U}\left(\frac{\tan \beta_{1}+\tan \beta_{2}}{\tan \beta_{1} * \tan \beta_{2}}\right)$ where $\beta_{1}$ and $\beta_{2}$ are the angles made with tangent to the blades (4a. 10, Dec13/Jan 14)( 4a. 10, Dec18/Jan 19) (4a. 10 Dec17/Jan 2018)

$R=\frac{\frac{U_{1}^{2}-U_{2}^{2}}{2}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2}}{\frac{V_{1}^{2}-V_{2}^{2}}{2}+\frac{U_{1}^{2}-U_{2}^{2}}{2}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2}}=\frac{\frac{U_{1}^{2}-U_{2}^{2}}{2}-\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2}}{\frac{E}{\dot{m}}}$
$U_{1}=U_{1}=U ;$

$$
\frac{E}{\dot{m}}=\frac{1}{\mathrm{~g}_{\mathrm{c}}}\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) \mathrm{U}
$$

Hence, $\quad R=\frac{-\left(\frac{V_{r 1}^{2}-V_{r 2}^{2}}{2 \mathrm{~g}_{c}}\right)}{\frac{1}{\mathrm{gc}}\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) \mathrm{U}}$;
$R=\frac{-\left(V_{r 1}^{2}-V_{r 2}^{2}\right)}{2\left(\overrightarrow{V_{u 1}}-\overrightarrow{V_{u 2}}\right) U}$
$V_{r 1}^{2}=V_{a}^{2}+X^{2} ; \quad V_{r 1}^{2}=V_{a}^{2}+\left(V_{a} \tan \gamma_{1}\right)^{2}$
$V_{r 2}^{2}=V_{a}^{2}+Y^{2} ; \quad V_{r 2}^{2}=V_{a}^{2}+\left(V_{a} \tan \gamma_{2}\right)^{2}$
$\tan \gamma_{0}=\frac{\overrightarrow{V_{u 1}}}{V_{a}} ; \quad \overrightarrow{V_{u 1}}=V_{a 1} \tan \gamma_{o} ; \quad \tan \gamma_{3}=\frac{\overrightarrow{V_{u 2}}}{V_{a}} ; \quad \overrightarrow{V_{u 2}}=V_{a} \tan \gamma_{3}$
$R=\frac{-\left(\left(V_{a}^{2}+\left(V_{a} \tan \gamma_{1}\right)^{2}\right)-\left(V_{a}^{2}+\left(V_{a} \tan \gamma_{2}\right)^{2}\right)\right)}{2\left(V_{a} \tan \gamma_{0}-V_{a} \tan \gamma_{3}\right) U} ; \quad \quad R=\frac{V_{a}^{2}\left(\tan ^{2} \gamma_{2}-\tan ^{2} \gamma_{1}\right)}{2 V_{a}\left(\tan \gamma_{0}-\tan \gamma_{3}\right) U}$
$R=\frac{V_{a}\left(\tan ^{2} \gamma_{2}-\tan ^{2} \gamma_{1}\right)}{2\left(\tan \gamma_{2}-\tan \gamma_{1}\right) U} \quad$ since, $\tan \gamma_{1}-\tan \gamma_{2}=\tan \gamma_{3}-\tan \gamma_{0}$
$R=\frac{V_{a}\left(\tan \gamma_{1}+\tan \gamma_{2}\right)}{2 \mathrm{U}}$
$\gamma_{1}=180-\beta_{1} ; \tan \gamma_{1}=\tan \left(180-\beta_{1}\right) ; \tan \gamma_{1}=\cot \beta_{1}$
$\gamma_{2}=180-\beta_{1} ; \tan _{2}=\tan \left(180-\beta_{2}\right) ; \tan \gamma_{2}=\cot \beta_{2}$
Hence , $R=\frac{V_{a}\left(\cot \beta_{1}+\cot \beta_{2}\right)}{2 \mathrm{U}}$;
$R=\frac{V_{a}\left(\frac{1}{\tan \beta_{1}}+\frac{1}{\tan \beta_{2}}\right)}{2 \mathrm{U}} ; ; R=\frac{V_{a}\left(\tan \beta_{2}+\tan \beta_{1}\right)}{2 \mathrm{U}\left(\tan \beta_{1} * \tan \beta_{2}\right)}$

## The effect of axial velocity:

$$
\frac{U}{g_{c}}\left(V_{u 2}-V_{u 1}\right)
$$

From Inlet and outlet velocity triangle
$V_{u 2}=U-V_{a} \cot \beta_{2}$ and $V_{u 1}=U-V_{a} \cot \beta_{1}$
Hence, $\mathrm{W}=U\left(\left(U-V_{a} \cot \beta_{2}\right)-\left(U-V_{a} \cot \beta_{1}\right)\right)$
$\mathrm{W}=U\left(V_{a} \cot \beta_{1}-V_{a} \cot \beta_{2}\right)$

Adding and subtracting $\cot \alpha_{1}$ to the above equation
$\mathrm{W}=U\left(V_{a}\left(\cot \beta_{1}+\cot \alpha_{1}\right)-V_{a}\left(\cot \beta_{2}+\cot \alpha_{1}\right)\right)$
But $\mathrm{U}=\cot \beta_{1}+\cot \alpha_{1}$
Hence, $W=U\left(U-V_{a}\left(\cot \beta_{2}+\cot \alpha_{1}\right)\right)$
From above equation fit is seen that if $U, \beta_{2}$ and $\alpha_{1}$ are kept constant in axial flow compressor Work absorbed by the compressor to raise the pressure depends only axial velocity

Variation of $V_{a}$ alters $U$

As $V_{a}$ increases $U$ decreases Hence $W$ decreases as $U$ is +ve and $V_{a}$ have-ve sign in Work absorbing equation Hence Work absorption capacity decreases. Therefore, the work absorbing capacity of the stage is reduced in the central region of the annulus and increased in the work at the hub and tip region

Therefore stage work is less than that given by the Eulers equation based on a constant value of the axial velocity along the blade height. This reduction in the work absorbing capacity of the stage is taken into account by Work Done Factor

Work done factor is defined as the ratio of stage work input to Eulers work Input
Also degined as the ratio of actual absorbing capacity to Ideal work absorbing capacity

Radial Equilibrium Condition:

Assumptions:

1) The rate of radial pressure gradient $\frac{d p}{d r}$ is assumed
2) There is no flow in radial direction ie flow in axial direction only
3) Stream lines do not experience any shift in radial direction and therefore lie on cylindrical surface coaxially

In axial flow machines the stream lines in a flow do not experience any radial shift and therefore flow is assumed along coaxial cylinders. Such a flow in an annulus is known as radial equilibrium.

Equation of motion for three dimensional flow in cylindrical co-ordinate is therefore given as

$$
V_{r d} \frac{d V_{r d}}{d r}+V_{a} \frac{d V_{a}}{d r}-\frac{V_{u}^{2}}{r}=-\frac{1}{\rho} \frac{d p}{d r}
$$

There is no flow in radial direction $V_{r d}=0$
Flow velocity is constant $V_{a}=$ constant ie $\frac{d V_{a}}{d r}=0$
Hence above equation becomes
$0+0-\frac{V_{u}^{2}}{d r}=-\frac{1}{\rho} \frac{d p}{d r}$
$\frac{V_{u}^{2}}{r}=\frac{1}{\rho} \frac{d p}{d r}$ $\qquad$
Stagnation pressure $p_{0}=p+\rho \frac{1}{2} V^{2}$
But $V^{2}=V_{r d}^{2}+V_{a}^{2}+V_{u}^{2} ; \quad V^{2}=V_{a}^{2}+V_{u}^{2}$ as $V_{r d}=0$
Hence, $\quad p_{0}=p+\rho \frac{1}{2}\left(V_{a}^{2}+V_{u}^{2}\right)$
$\frac{d p_{0}}{d r}=\frac{d p}{d r}+\rho \frac{1}{2} \frac{d\left(V_{a}^{2}+V_{u}^{2}\right)}{d r}$
$\frac{1}{\rho} \frac{d p_{0}}{d r}=\frac{1}{\rho} \frac{d p}{d r}+\frac{1}{2} 2 V_{u} \frac{d V_{u}}{d r}+\frac{1}{2} 2 V_{a} \frac{d V_{a}}{d r}$
$\frac{1}{\rho} \frac{d p}{d r}=\frac{1}{\rho} \frac{d p_{0}}{d r}-V_{u} \frac{d V_{u}}{d r}-V_{a} \frac{d V_{a}}{d r}$

From $1 \frac{V_{u}^{2}}{r}=\frac{1}{\rho} \frac{d p}{d r}$
$\frac{d p}{d r}=\rho \frac{V_{u}^{2}}{r}$ $\qquad$

Substituting 3 in 2
$\frac{1}{\rho} \rho \frac{V_{u}^{2}}{r}=\frac{1}{\rho} \frac{d p_{0}}{d r}-V_{u} \frac{d V_{u}}{d r}-V_{a} \frac{d V_{a}}{d r}$
$\frac{V_{u}^{2}}{r}=\frac{1}{\rho} \frac{d p_{0}}{d r}-V_{u} \frac{d V_{u}}{d r}-V_{a} \frac{d V_{a}}{d r}$
This is known as radial equilibrium equation for axisymmetric unsteady flow in turbomachine
The pressure coefficient $\varphi_{p}$ is defined is the ratio of the actual stagnation enthalpy change to kinetic energy of a fluid which has the same speed as the blades.
$\varphi_{p}=\frac{\Delta h_{o}}{\frac{U^{2}}{2}} ; \quad \quad \varphi_{p}=\frac{\Delta V_{u} U}{\frac{U^{2}}{2}} ; \quad \varphi_{p}=\frac{2 \Delta V_{u} U}{U^{2}}$
If Fluid is incompressible $\Delta h_{o}=\frac{\Delta p_{o}}{\rho}$
Then for Incompressible fluid , $\varphi_{p}=\frac{2 \Delta p_{o}}{\rho U^{2}}$

Pressure coefficient usually ranges between 0.4 and 0.7

The flow coefficient $\psi$ is defined as is the ratio of flow velocity to the blade speed
$\psi=\frac{V_{a x}}{U}$

Numericals

1. An axial flow compressor of $50 \%$ reaction design has blades with inlet and outlet angles with respect of axial directions of $45^{\circ}$ and $10^{\circ}$ repectively. The compressor is to produce a pressure ratio of $6: 1$ with a overall isentropic efficiency of 0.85 . When the inlet static temperature of $37^{\circ} \mathrm{C}$. The blade speed and axial velocity are constant throughout the compressor. Assuming a value of $200 \mathrm{~m} / \mathrm{s}$ for blade speed. Find the number of stages required if the work done factor is i) unity and ii) 0.87 for all stages ( $8 \mathrm{c}, 10$, June/July17)(8b,08,Dec13/Jan14)
$R=50 \% ; \gamma_{2}=45^{\circ} ; \gamma_{3}=10^{\circ} ;$
The compressor is to produce a pressure ratio of $6: 1$ ie $\frac{p_{k+1}}{p_{1}}=6 ; \eta_{0}=0.85 ; T_{1}=37^{\circ} \mathrm{C}$ The blade speed and axial velocity are constant throughout the compressor.
ie $U_{1}=U_{2}=U$ and $V_{a 1}=V_{a 2}=V_{a 2}$
$U=200 \mathrm{~m} / \mathrm{s} ; k=$ ? when i) $\Omega=1 \mathrm{ii}) \Omega=0.87$


## the number of stages for work done factor is unity

$R=\frac{V_{a}\left(\tan \gamma_{1}+\tan \gamma_{2}\right)}{2 U} ; \quad 0.5=\frac{V_{a}(\tan 45+\tan 10)}{2 * 200}$
$\tan _{2}=\frac{Y}{V_{a}} ; \quad Y=\overrightarrow{V_{u 1}} ; \quad \quad \tan \gamma_{2}=\frac{V_{u 1}}{V_{a}} ; \quad \tan 10=\frac{\overrightarrow{V_{u 1}}}{170} ; \quad \overrightarrow{V_{u 1}}=29.97 \mathrm{~m} / \mathrm{s}$
$\overrightarrow{V_{u 2}}=U-Y$;
$\overrightarrow{V_{u 2}}=200-29.97$
$\overrightarrow{V_{u 2}}=170.03 \mathrm{~m} / \mathrm{s}$
$-\frac{E}{\dot{m}}=\frac{\Omega\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right) U}{g_{c}} ; \quad \quad$ Increase in entalphy $\Delta h_{o} /$ stage $=\frac{1(170.03-29.97) 200,}{1}$
$\Delta h_{o} /$ stage $=28012 \mathrm{~J} / \mathrm{kg}$
$\eta_{0}=\frac{\Delta h_{0 s}}{\Delta h_{0}} ;$

$$
\eta_{0}=\frac{C_{p}\left(T_{o s k+1}-T_{01}\right)}{\Delta h_{0}} ; \quad \eta_{0}=\frac{C_{p} T_{01}\left(\frac{T_{o s k+1}}{T_{01}}-1\right)}{\Delta h_{0}}
$$

$\eta_{0}=\frac{C_{p} T_{01}\left(\left(\frac{p_{k+1}}{p_{1}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\Delta h_{0}} ;$
$\Delta h_{0}=\frac{C_{p} T_{01}\left(\left(\frac{p_{k+1}}{p_{1}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\eta_{0}} ;$
$V_{1}^{2}=V_{u 1}^{2}+V_{a}^{2} ;$
$V_{1}^{2}=29.97^{2}+170^{2} ;$
$V_{1}^{2}=29798.2$
$T_{01}=T_{1}+\frac{V_{1}^{2}}{2 * C_{p}} ;$
$T_{01}=310+\frac{29798.2}{2 * 1005} ;$
$T_{01}=324.82 \mathrm{~K}$
$\Delta h_{0}=\frac{C_{p} T_{01}\left(\left(\frac{p_{k+1}}{p_{1}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\eta_{0}} ;$
$\left(\Delta h_{0}\right)_{\text {total }}=\frac{1005 * 324.82\left[(6)^{0.286}-1\right]}{0.85} ; \quad\left(\Delta h_{0}\right)_{\text {total }}=257070.82 \mathrm{~J} / \mathrm{kg}$
Number of stages, $k,=\frac{\left(\Delta h_{0}\right)_{\text {total }}}{\Delta h_{o} / \text { stage }} ; \quad k=\frac{257070.82}{28012} ; \quad k=9.18 \quad$ say 10 stages
the number of stages for work done factor is 0.87
$-\frac{E}{\dot{m}}=\frac{\Omega\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right) U}{g_{c}} ; \quad \quad$ Increase in entalphy $\Delta h_{o} /$ stage $=\frac{0.87(170.03-29.97) 200}{1}$,
$\Delta h_{o} /$ stage $=23810.2 \mathrm{~J} / \mathrm{kg} ;$
$\eta_{0}=\frac{C_{p} T_{01}\left(\left(\frac{p_{k+1}}{p_{1}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\Delta h_{0}} ; \quad \Delta h_{0}=\frac{C_{p} T_{01}\left(\left(\frac{p_{k+1}}{p_{1}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\eta_{0}} ; \quad\left(\Delta h_{0}\right)_{\text {total }}=\frac{1005 * 324.82\left[(6)^{0.286}-1\right]}{0.85}$
$\left(\Delta h_{0}\right)_{\text {total }}=257070.82 \mathrm{~J} / \mathrm{kg}$
Number of stages, $k,=\frac{\left(\Delta h_{0}\right)_{\text {total }}}{\Delta h_{o} / \text { stage }} ; \quad k=\frac{257070.82}{23810.2} ; \quad k=10.79 \quad$ say 11 stages
2. The axial flow compressor with $50 \%$ reaction is having a flow coefficient of 0.54 . Air enters the compressor at stagnation condition of 1 bar and $30^{\circ} \mathrm{C}$. The total to total efficiency across the rotor is 0.88 . The total to pressure ratio across the rotor is 1.26 . The pressure coefficient is 0.45 and workdone factor is 0.88 . The mass flow rate is 15 kgs . Calculate i) The mean rotor blade speed ii) Rotor blade angles at inlet and exit iii) Power input to the system (8b,10,Dec 12)
$R=0.5 ;$ flow coefficient $\psi=0.54 ; p_{01}=1$ bar; $T_{01}=30^{\circ} C ; \eta_{t t}=0.88 ; p_{r o}=1.26$;
Pressure coefficient $\varphi_{p}=0.45$; work done factor $\Omega=0.88$; $\dot{m}=15 \mathrm{~kg} / \mathrm{s}$
i) $\quad U=$ ?
ii) $\beta_{1}=$ ?, $\beta_{2}=$ ?;
iii) Power input $E=$ ?
$\psi=\frac{V_{a}}{U}=0.54 ; \varphi_{p}=\frac{\Delta h_{0}}{\frac{u^{2}}{2}}=0.45$

## i) The mean rotor blade speed

$\eta_{t t}=\frac{\Delta h_{0 s}}{\Delta h_{0}} ; \quad \quad \eta_{0}=\frac{C_{p}\left(T_{o s k+1}-T_{01}\right)}{\Delta h_{0}} ; \quad \eta_{0}=\frac{C_{p} T_{01}\left(\frac{T_{o s k+1}}{T_{01}}-1\right)}{\Delta h_{0}}$

$$
\begin{gathered}
\eta_{0}=\frac{C_{p} T_{01}\left(\left(\frac{p_{k+1}}{p_{1}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\Delta h_{0}} ; \quad \Delta h_{0}=\frac{1005 * 303\left((1.26)^{0.286}-1\right)}{0.88} ; \quad \Delta h_{0}=23645.37 \mathrm{~J} / \mathrm{kg} \\
\varphi_{p}=\frac{2 \Delta h_{0}}{u^{2}}=0.45 ; \quad 0.45=\frac{2 * 23645.37}{u^{2}} ; \quad u^{2}=105.090 .52 \quad U=324.17 \mathrm{~m} / \mathrm{s}
\end{gathered}
$$

## ii) Rotor blade angles at inlet and exit

$\psi=\frac{V_{a}}{U}=0.54 ; \quad \frac{V_{a}}{324.17}=0.54 ; \quad V_{a}=175.05 \mathrm{~m} / \mathrm{s}$

$-\frac{E}{\dot{m}}=\frac{\Omega\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right) U}{g_{c}} ; \quad \Delta h_{0}=\frac{\Omega \Delta \mathrm{V}_{\mathrm{u}} U}{g_{c}} ; \quad 23645.37=\frac{0.88 * \Delta \mathrm{~V}_{\mathrm{u}} * 324.17}{1} \quad \Delta \mathrm{~V}_{\mathrm{u}}=82.89 \mathrm{~m} / \mathrm{s}$
$Y=\overrightarrow{V_{u 1}}$ since $R=0.5$ ie triangles are symmetrical
$U=\Delta \mathrm{V}_{\mathrm{u}}+\overrightarrow{V_{u 1}}+Y ; \quad U=\Delta \mathrm{V}_{\mathrm{u}}+2 \overrightarrow{V_{u 1}} ; \quad 324.17=82.89+2 \overrightarrow{V_{u 1}} ; \quad \overrightarrow{V_{u 1}}=120.64$
$\tan \alpha_{1}=\frac{V_{a}}{\overrightarrow{V_{u 1}}} ;$
$\tan \alpha_{1}=\frac{175.05}{120.64} ;$
$\alpha_{1}=55.42^{0} ;$

For $R=0.5$
$\beta_{2}=\alpha_{1} ;$
$\beta_{2}=55.42^{0}$
$\Delta \mathrm{V}_{\mathrm{u}}=\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}} ;$
$82,89=\overrightarrow{V_{u 2}}-120.64$
$\overrightarrow{V_{u 2}}=203.53 \mathrm{~m} / \mathrm{s}$
$\tan \alpha_{2}=\frac{V_{a}}{\overrightarrow{V_{u 2}} ;}$
$\tan \alpha_{2}=\frac{175.05}{203.53} ;$
$\alpha_{2}=40.69^{0}$

For $R=0.5$
$\beta_{1}=\alpha_{2} ;$
$\beta_{1}=40.69^{0}$
iii) Power input to the system
$-\frac{E}{\dot{m}}=\frac{\Omega\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right) U}{g_{c}} ; \quad-\frac{E}{\dot{m}}=\Delta h_{0} ; \quad \frac{-E}{15}=23645.37 \quad-E=354680.55 \mathrm{~W}$
3. An axial flow compressor has the following data entry condition 1 bar, $20^{\circ} \mathrm{C}$, degree of reaction $50 \%$ mean blade ring diameter 36 cm . Rotational speed 18000 rpm bade height at entry 6 cm . Blade angle at rotor and stator exit $65^{\circ}$ axial velocity $180 \mathrm{~m} / \mathrm{s}$ mechanical efficiency 0.967. Find i) Guide blade angle at outlet ii) Power required to drive the compressor (8c, 8, Dec16/Jan17)
$p_{01}=1 \mathrm{bar} ; T_{01}=20^{\circ} \mathrm{C}=293 \mathrm{~K} ; R=0.5 ; D=36 \mathrm{~cm}=0.36 \mathrm{~m} ; N=18000 \mathrm{rpm} ;$
bade height at entry $6 \mathrm{~cm} h=6 \mathrm{~cm}=0.06 \mathrm{~m}$;
Blade angle at rotor and stator exit $65^{\circ}$ axial velocity $180 \mathrm{~m} / \mathrm{s} ; \alpha_{1}=\beta_{2}=65^{\circ}$
$V_{a 1}=V_{a 2}=V_{a}=180 \mathrm{~m} / \mathrm{s} ; \quad \eta_{\text {mech }}=0.967$
i)
ii) $E=$ ?
$U=\frac{\pi D N}{60} ;$
$U=\frac{\pi * 0.36 * 18000}{60}$
$U=339.3 \mathrm{~m} / \mathrm{s}$

$\tan \alpha_{1}=\frac{V_{a}}{\overrightarrow{V_{u 1}}} ;$

$$
\tan 65=\frac{180}{\overrightarrow{V_{u 1}}}
$$

$$
\overrightarrow{V_{u 1}}=83.93 \mathrm{~m} / \mathrm{s}
$$

Since, $R=0.5$,

$$
Y=\overrightarrow{V_{u 1}}
$$

$$
Y=83.93 \mathrm{~m} / \mathrm{s}
$$

$\overrightarrow{V_{u 2}}=U-Y ;$
$\overrightarrow{V_{u 2}}=339.3-83.94$
$\tan \alpha_{2}=\frac{V_{a}}{\overline{V_{u 2}}} ;$
$\tan \alpha_{2}=\frac{180}{255.36} ;$

$$
\overrightarrow{V_{u 2}}=255.36 \mathrm{~m} / \mathrm{s}
$$

$$
\alpha_{2}=35.17^{0}
$$

For $R=0.5$
$\beta_{1}=\alpha_{2} ;$
$\beta_{1}=35.17^{0}$
ii) Power required to drive the compressor
$-\frac{E}{\dot{m}}=\frac{\Omega\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right) U}{g_{c}} ;$
$\dot{m}=\rho A_{f} V_{a} ;$

$$
\rho=\frac{p_{1}}{R T} \quad \rho=\frac{1 * 10^{5}}{287 * 293} ;
$$

$$
\rho=1.189 \mathrm{~kg} / \mathrm{m}^{3}
$$

$A_{f}=\pi D h ;$
$A_{f}=\pi * 0.36 * 0.06$
$A_{f}=0.068 m^{2}$
$\dot{m}=14.34 \mathrm{~kg} / \mathrm{s}$
$\dot{m}=\rho A_{f} V_{a} ;$
$\dot{m}=1.189 * 0.067 * 180$
$-\frac{E}{\dot{m}}=\frac{\Omega\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right) U}{g_{c}} ; \quad \quad \frac{-E}{14.34}=\frac{1(255.36-83.93) 339.3}{1} ; \quad-E=834103.3 \mathrm{~W}$
Power input to the impeller $=834103.3 \mathrm{~W}$
Power Required to drive the shaft of Impeller $=\frac{\text { Power Input to blades }}{\eta_{\text {mech }}}$
Power Required to drive the shaft of Impeller $=\frac{834103.3}{0.967}$ ie $862568 \mathrm{~W} P=862568 \mathrm{~W}$
4. The speed of an axial flow compressor is 15000 rpm . The mean diameter is 0.6 m . The axial velocity is constant and is $225 \mathrm{~m} / \mathrm{s}$. The velocity of whirl at inlet is $85 \mathrm{~m} / \mathrm{s}$. The work done is $45 \mathrm{~kJ} / \mathrm{kg}$ of air. The inlet conditions are 1 bar and 300 K . Assume a stage efficiency of
0.89. Calculate i) Fluid deflection angle ii) Pressure ratio iii) Degree of reaction iv) Mass flow rate of air . Power developed is $425 k W$ ( $8 \mathrm{c}, 10$,June/July 16)
$N=15000 \mathrm{rpm} ; D=0.6 \mathrm{~m} ; V_{a}=225 \mathrm{~m} / \mathrm{s} ; \overrightarrow{V_{u 1}}=85 \mathrm{~m} / \mathrm{s} ;-\frac{E}{\dot{m}}=45 \mathrm{~kJ} / \mathrm{kg}$;
$p_{1}=1 \mathrm{bar} ; T_{1}=300 \mathrm{~K} ; \eta_{s}=0.89$
i) Fluid deflection angle ii) Pressure ratio $\frac{p_{2}}{p_{1}}=$ ?; iii) $R=$ ? iv) $\dot{m}=$ ? $E=425 \mathrm{~kW}$

$$
U=\frac{\pi D N}{60}
$$

$U=\frac{\pi * 0.6 * 15000}{60}$
$U=471.24 \mathrm{~m} / \mathrm{s}$


| $-\frac{E}{\dot{m}}=\frac{\Omega\left(\overrightarrow{V_{u 2}}-\overrightarrow{V_{u 1}}\right) U}{g_{c}} ;$ | Assume $\Omega=1$ | $45000=\frac{1\left(\overrightarrow{V_{u 2}}-85\right) 471.24}{1} ;$ |
| :--- | ---: | :--- |
| $\overrightarrow{V_{u 2}}-85=95.49 ;$ | $\overrightarrow{V_{u 2}}=180.49 \mathrm{~m} / \mathrm{s} ;$ |  |
| $\tan \alpha_{1}=\frac{V_{a}}{\overrightarrow{V_{u 1}} ;}$ | $\tan \alpha_{1}=\frac{225}{85} ;$ | $\alpha_{1}=69.3^{0}$ |
| $\tan \alpha_{2}=\frac{V_{a}}{\overrightarrow{V_{u 2}} ;}$ | $\tan \alpha_{2}=\frac{225}{180.49^{\prime}} ;$ | $\alpha_{2}=51.26^{0}$ |
| $\tan \beta_{1}=\frac{V_{a}}{U-\overrightarrow{V_{u 1}}} ;$ | $\tan \beta_{1}=\frac{225}{471.21-85}$ | $\beta_{1}=30.22^{\circ}$ |
| $\tan \beta_{2}=\frac{V_{a}}{U-\overrightarrow{V_{u 2}}} ;$ | $\tan \beta_{2}=\frac{225}{471.21-180.49}$ | $\beta_{2}=37.73^{\circ}$ |

## Pressure ratio $\frac{p_{2}}{p_{1}}$

$\eta_{s}=\frac{\Delta h_{0 s}}{\Delta h_{0}} ;$

$$
\eta_{0}=\frac{C_{p}\left(T_{o 2 s}-T_{01}\right)}{\Delta h_{0}} ; \quad \eta_{0}=\frac{C_{p} T_{01}\left(\frac{T_{02 s}}{T_{01}}-1\right)}{\Delta h_{0}}
$$

$$
\eta_{s}=\frac{C_{p} T_{01}\left(\left(\frac{p_{02}}{p_{01}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\Delta h_{0}} ; \quad \Delta h_{0}=-\frac{E}{\dot{m}}=45 \mathrm{~kJ} / \mathrm{kg} ; \quad \Delta h_{0}=45000 \mathrm{~J} / \mathrm{kg}
$$

$$
0.89=\frac{1005 * 300\left(\left(\frac{p_{02}}{p_{01}}\right)^{0.286}-1\right)}{45000} ; \quad 0.133=\left(\frac{p_{02}}{p_{01}}\right)^{0.286}-1 ; \quad \frac{p_{02}}{p_{01}}=1.546
$$

iii) Degree of reaction
$R=\frac{\frac{E}{\dot{m}}-\left(\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}\right)}{\frac{E}{\dot{m}}} ; \quad \quad R=1-\frac{\left(V_{1}^{2}-V_{2}^{2}\right)}{2 g_{c} \frac{E}{\dot{m}}} ;$
$\begin{array}{lll}V_{1}^{2}=V_{u 1}^{2}+V_{a}^{2} ; & V_{1}^{2}=85^{2}+225^{2} ; & V_{1}^{2}=57850 \\ V_{2}^{2}=V_{u 2}^{2}+V_{a}^{2} ; & V_{2}^{2}=180.49^{2}+225^{2} ; & V_{2}^{2}=83201.64 \\ -\frac{E}{\dot{m}}=45 \mathrm{~kJ} / \mathrm{kg} ; & \frac{E}{\dot{m}}=-45000 \mathrm{~J} / \mathrm{kg} & \end{array}$
$R=1-\frac{\left(V_{1}^{2}-V_{2}^{2}\right)}{2 g_{c} \frac{E}{\dot{m}}} ; \quad R=1-\frac{(57850-83201.64)}{2 * 1 *(-45000)} \quad R=1-0.282 \quad R=0.718$
$R=\frac{V_{a}}{2 U}\left(\frac{\tan \beta_{1}+\tan \beta_{2}}{\tan \beta_{1} * \tan \beta_{2}}\right) ; \quad R=\frac{225}{2 * 471.24}\left(\frac{\tan 30.22+\tan 37.73}{\tan 30.22 * \tan 37.73}\right) ; \quad R=0.718$
$R=\frac{V_{a}}{2 U}\left(\frac{\tan \beta_{1}+\tan \beta_{2}}{\tan \beta_{1} * \tan \beta_{2}}\right)-$ this formula can be used only when workdone factor is 1

## iv) Mass flow rate of air .

$-E=425 \mathrm{~kW}$
$-\frac{E}{\dot{m}}=45 \mathrm{~kJ} / \mathrm{kg} ; \quad \frac{-E}{\dot{m}}=45 \mathrm{~kJ} / \mathrm{kg} ; \quad \frac{425 \mathrm{~kW}}{\dot{m}}=45 \mathrm{~kJ} / \mathrm{kg}$
$\dot{m}=9.44 \mathrm{~kg} / \mathrm{s}$
5. The mean diameter of rotor of an axial flow compressor is 0.5 m , and it rotates at 15000 rpm . The velocity of flow $220 \mathrm{~m} / \mathrm{s}$, is constant and the velocity of whirl at the inlet is $80 \mathrm{~m} / \mathrm{s}$. The inlet pressure and temperature are 1 bar and 300 K . The stage efficiency is 0.88 . The pressure ratio through the stage is 1.5 . Calculate i) Fluid deflection angle ii) The degree of reaction if work done factor is 0.8 ( $8 \mathrm{c}, 10$,Dec14/Jan15)
$D=0.5 \mathrm{~m} ; \quad N=15000 \mathrm{rpm} ; \quad V_{a}=220 \mathrm{~m} / \mathrm{s} ; \quad \overrightarrow{V_{u 1}}=80 \mathrm{~m} / \mathrm{s} ; \quad p_{1}=1 \mathrm{bar} ; \quad T_{1}=300 \mathrm{~K}$ $\eta_{s}=0.88 ; \quad \frac{p_{2}}{p_{1}}=1.5 ;$ work done factor is $0.8 \Omega=0.8$
$U=\frac{\pi D N}{60} ;$
$U=\frac{\pi * 0.5 * 15000}{60}$
$U=392.69 \mathrm{~m} / \mathrm{s}$

$\eta_{s}=\frac{\Delta h_{0 S}}{\Delta h_{0}} ;$
$\eta_{s}=\frac{\left.C_{p} T_{01}\left(\frac{p_{02}}{p_{01}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\Delta h_{0}} ;$
$\frac{-E}{\dot{m}}=\Delta h_{0} ;$
$-\frac{E}{\dot{m}}=\frac{\Omega\left(\overrightarrow{\left(\overrightarrow{u_{2}}\right.}-\overrightarrow{V_{u 1}}\right) U}{g_{c}}$;
$\tan \alpha_{1}=\frac{V_{a}}{V_{u 1}} ;$
$\tan \alpha_{2}=\frac{V_{a}}{V_{u 2}} ;$
$\tan \beta_{1}=\frac{V_{a}}{U-\overline{V_{u 1}}} ;$
$\tan \beta_{1}=\frac{220}{392.69-80}$
$\beta_{1}=35.12^{\circ}$
$\tan \beta_{2}=\frac{V_{a}}{U-\overline{V_{u 2}}} ; \quad \quad \tan \beta_{2}=\frac{220}{392.69-214.09}$

$$
\beta_{2}=50.92^{\circ}
$$

## iii) Degree of reaction

$R=\frac{\frac{E}{\dot{m}}-\left(\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}\right)}{\frac{E}{\dot{m}}} ;$
$V_{1}^{2}=V_{u 1}^{2}+V_{a}^{2} ;$

$$
V_{2}^{2}=V_{u 2}^{2}+V_{a}^{2} ;
$$

$$
-\frac{E}{\dot{m}}=42125.83 \mathrm{~J} / \mathrm{kg} ;
$$

$$
\begin{array}{rlr}
R & =1-\frac{\left(V_{1}^{2}-V_{2}^{2}\right)}{2 g_{c} \underline{\underline{E}}} ; & \\
V_{1}^{2}= & 80^{2}+220^{2} ; & V_{1}^{2}=54800 \\
V_{2}^{2}= & 214.09^{2}+220^{2} ; & V_{2}^{2}=94234.53 \\
& \frac{E}{\dot{m}}=-42125.83 \mathrm{~J} / \mathrm{kg} &
\end{array}
$$

$R=1-\frac{\left(V_{1}^{2}-V_{2}^{2}\right)}{2 g_{c}^{E} \underline{\tilde{m}}} ;$

$$
R=1-\frac{(54800-94234.53)}{2 * 1 *(-42125.83)}
$$

$$
R=1-0.468
$$

$$
R=0.531
$$

$R=\frac{V_{a}}{2 U}\left(\frac{\tan \beta_{1}+\tan \beta_{2}}{\tan \beta_{1} * \tan \beta_{2}}\right) ;-\quad$ this formula cannot be used since work done factor is not 1

## Centrifugal Power absorbing machine

Power absorbing tubomachines are classified into
i) Fans,
ii) Blowers and
iii) compressors

## Difference between fan, blower and compressor

A fan consists of single rotor with or without a stator which causes only small pressure rise as low as few centimeters of water column ( 70 cm of water). In analysis of fan fluid considered as incompressible fluid as the density change is very small due to small pressure rise.

Blowers may consist of one or multistage of compression with rotor mounted on a common shaft. The air is compressed in a series of successive stages and passed through a diffuser located near the exit to recover the pressure energy from the large kinetic energy. The overall pressure rise may be in the range of 1.5 bars to 2 . Bars. Blowers are used in ventilation, power station, workshops etc

Compressors is used to produce large pressure rise ranging from 2.5 bars to 10bars or more. A single stage compressor can generally produce a pressure rise upto 4 bar.

## Important elements of centrifugal compressor

i) Nozzle
ii) Impeller
iii) diffuser
iv) casing

Functions
i) Inlet casing with convergent nozzle: is to accelerate the entering fluid to the impeller inlet which direct the flow in the desired direction at the inlet of the impeller from state 0 to 1
ii) Impeller converts the supplied mechanical energy into fluid energy wherein the fluid kinetic energy converted into static pressure rise. Impeller consists of radial vane fitted to shrouds and has two portion inducer and a large radial portion. The inducer receives the flow between hub and tip diameter of the impeller eye and passes onto the radial portion of the impeller blades. The impeller may be single sided or double sided. Double sided impeller may be used where for the given size the compressor has to handle more flow
iii) The diffuser receives the flow from the impeller through a vane less space and raises the static pressure of the fluid further an account of conversion of exit high energy to pressure energy
iv) Spiral casing: The flow at the outer periphery of the diffuser is collected by a spiral casing known as volute, which discharges the flow into the delivery pipe.


Inducer casing with nozzle

Variation of Pressure and Velocity.
As the fluid approaches the impeller, it is subjected to centrifugal effect thereby the kinetic energy and pressures of the fluid both increases along the radial direction.

When the impeller discharges the fluid into the diffuser, the static pressure of the fluid rises due to the deceleration of the flow results in reduction in velocity and increase in pressure further due to conversion of kinetic energy into pressure energy.

## Energy Transfer

Velocity triangle at Inlet


Velocity triangle at Outlet

$\frac{E}{m}=\frac{V_{u 1} U_{1}-V_{u 2} U_{2}}{g_{c}} ; \quad \quad \frac{E}{m}=\frac{-V_{u 2} U_{2}}{g_{c}}$ as $V_{u 1}=0 ; \quad-\frac{E}{m}=\frac{+V_{u 2} U_{2}}{g_{c}}$
Energy Input $==\frac{+V_{u 2} U_{2}}{g_{c}}$ where $g_{c}=1$
Eulers Head
For maximum Efficiency vanes are assumed to be radial $\boldsymbol{\beta}_{2}=90^{0}$
le $V_{u 2}=U_{2}$
Outlet velocity triangle
Energy Input $=\frac{U_{2} U_{2}}{g_{c}} ; \quad$ vvEnergy Input $=\frac{U_{2}^{2}}{g_{c}}$

## Slip and Slip coefficienct:

In Euler's equation, it is assumed that the velocities in turbomachine is constant across the given area. But in actual machine, velocities vary across the given area. This results in change of pressure across the vane, with high pressure at the leading face and a low pressure at the trailing face. As a result, the fluid leaves tangentially only at the high pressure face and nowhere else. The lower pressure at the trailing face results in a lower speed of fluid flow compared with that of leading face and the mean vane exit angle $\beta_{2}$ is less than the vane exit angle $\beta_{2}^{\prime}$

Hence the actual tangential component of absolute velocity at the exit $\left(\mathrm{V}_{\mathrm{u}_{2}}\right)$ will be less than the tangential component of absolute velocity for the ideal condition ( $\mathrm{V}_{\mathrm{u} 2}{ }^{\prime}$ ) . Hence, Eulers head developed in actual condition is less than the actual condition The difference between Eulers head developed for actual case and ideal condition is called slip

Slip $=H_{e}^{\prime}-H_{e}$
The ratio of actual Eulers head developed (with pre-rotation) to the ideal Eulers head developed (with out pre-rotation) is called as slip coefficient

Slip coefficient $\mu=\frac{H_{e}}{H_{e}^{\prime}}=\frac{V_{u 2}}{V_{u z}^{\prime}}$

Actual Eulers head developed $=\mu \frac{V_{u 2} U_{2}}{g}$


With slip for radial curved vane

Energy Input $=\frac{\mu U_{2}^{2}}{g_{c}}$

## Power Input Factor or Work done factor

Power Input factor is defined as the ratio of actual power to be supplied to theoretical work supplied

In real fluid, some part of the power supplied by the impeller on the air is used to overcome the losses like windage, disc friction and losses. Therefore the power required is greater than the actual power to be supplied on the air and hence the actual power to be supplied is taken care by the term power Input factor
$\varphi=\frac{\text { actual power to be supplied }}{\text { theortical work supplied }}=\frac{E}{\frac{\mu U_{2}^{2}}{g_{c}}}$
$E=\varphi \frac{\mu U_{2}^{2}}{g_{c}}$
The typical value of $\varphi$ ranging from 1.035 to 1.04

## Overall pressure ratio ( $p_{r o}$ )

$E=h_{02}-h_{01}=\psi \frac{\mu U_{2}^{2}}{g_{c}}$
As there is no work transfer in the diffuser, by energy balance we can write,
$h_{03}-h_{02}=h_{02}-h_{01}$ as in diffuser enthalpy remains constant ie $h_{03}=h_{02}$
$\eta_{t t}=\frac{C_{P}\left(T_{03}^{\prime}-T_{01}\right)}{C_{P}\left(T_{03}-T_{01}\right)} ; \quad\left(T_{03}^{\prime}-T_{01}\right)=\eta_{t t}\left(T_{03}-T_{01}\right)$
Dividing both sides by $T_{01}$
$\frac{T_{03}^{\prime}}{T_{01}}-1=\frac{\eta_{t t}\left(T_{03}-T_{01}\right)}{T_{01}} ; \quad\left(\frac{p_{03}}{p_{01}}\right)^{\frac{\gamma-1}{\gamma}}-1=\frac{\eta_{t t}\left(T_{03}-T_{01}\right)}{T_{01}} ; \quad \frac{p_{03}}{p_{01}}=\left(1+\frac{\eta_{t t}\left(T_{03}-T_{01}\right)}{T_{01}}\right)^{\frac{\gamma}{\gamma-1}}$
$\frac{p_{03}}{p_{01}}=\left(1+\frac{\eta_{t t} C_{P}\left(T_{03}-T_{01}\right)}{C_{P} T_{01}}\right)^{\frac{\gamma}{\gamma-1}} ; \quad \frac{p_{03}}{p_{01}}=\left(1+\frac{\eta_{t t} \psi \mu U_{2}^{2}}{C_{P} T_{01}}\right)^{\frac{\gamma}{\gamma-1}}$

## Pressure coefficient /Loading Coefficient

Because of compressor losses as well as the kinetic energy, the actual pressure rise is less than theoretical specified by the impeller speed. This is expressed by a quantity is called pressure coefficient

It is defined as the ratio of isentropic work input across the impeller to the Eulers work input
$\phi_{P}=\frac{\text { isentropic work input across the impeller }}{\text { Max Eulers work input }}$
$\phi_{P}=\frac{C_{P}\left(T_{02}^{\prime}-T_{01}\right)}{U_{2}^{2}} ; \quad \quad \eta_{c}=\frac{C_{P}\left(T_{02}^{\prime}-T_{01}\right)}{C_{P}\left(T_{02}-T_{01}\right)} ; \quad \eta_{c} C_{P}\left(T_{02}-T_{01}\right)=C_{P}\left(T_{02}^{\prime}-T_{01}\right)$
Hence, $\quad \phi_{P}=\frac{\eta_{c} C_{P}\left(T_{02}-T_{01}\right)}{U_{2}^{2}}$
$E=h_{02}-h_{01}$

$$
E=\psi \frac{\mu U_{2}^{2}}{g_{c}}
$$

$C_{P}\left(T_{02}-T_{01}\right)=\psi \frac{\mu U_{2}^{2}}{g_{c}}$

$$
\phi_{P}=\frac{\psi \mu U_{2}^{2}}{U_{2}^{2}}
$$

The loading factor in terms of exit blade angle
$\phi_{P}=\frac{\text { isentropic work input across the impeller }}{\text { Max Eulers work input }}$
$\phi_{P}=\frac{V_{u 2} U_{2}}{U_{2}^{2}}$
$V_{u 2}=U_{2}-V_{f 2} \cot \beta_{2}$
$\phi_{P}=\frac{\left(U_{2}-V_{f 2} \cot \beta_{2}\right) U_{2}}{U_{2}^{2}}$
$\phi_{P}=\frac{U_{2}-V_{f 2} \cot \beta_{2}}{U_{2}}$
$\phi_{P}=1-\frac{V_{f 2}}{U_{2}} \cot \beta_{2}$

## Surging

Surge is a characteristic behavior of a centrifugal compressor that can occur when inlet flow is reduced such that the head developed by the compressor is insufficient to overcome the pressure at the discharge of the compressor. Once surge occurs, the output pressure of the compressor is drastically reduced, resulting in flow reversal within the compressor.


Mass flow rate

At very high flow rates in machines with high pressure ratios, it possible for the flow to be chocked. In that case , the mass flow will be fixed no matter how low the delivery pressure. The charecterstic becomes nearly vertical

Consider the machine with an actual characteristic D-C-F-B-A. A stable operation at a point such as A implies that head developed by the machine $H_{A}$ at A equals the losses due to friction and other causes in delivery pipe when the flow rate is $Q_{A}$. At $A$, if due to an instantaneous disturbance is in the operating conditions the frictional losses are slightly increased, the flow rate tends to decrease. The operating point tends to move towards the left (ie, towards B) the delivery head developed by the machine increases. The rising head tends to compensate for the increased frictional losses and
increases the flow rate to push the operating point back to A. In a similar way , if instantaneously the exit pipe loss decreased due to small disturbance, the flow rate tend increase and the head developed by the machine tends increase and the head developed by the machine tends to drip as a consequence, trying to reduce the flow and to bring operating point back to its location at A. The machine thus tries to maintain a stable operating point. Thus machine maintain a stable operating point with a constant flow rate at a constant head

If the machine is initially operating at a point such as $C$ on the rising portion of the characteristic, any slight disturbance in the operating conditions tending to increase the frictional losses leads to a decrease in flow. However, since $C$ is on the rising portion of characteristic curve the head decreases (opposite to operating condition at A) Decreased head results in still decrease in flow and continues. The operating point tend move down still further along the curve CD in an unstable manner until the point D is reached. At D fluid cease to flow and loss of head due to friction is tends to zero since there is no flow. Then it starts to deliver suddenly. . Thus operating point moves up and down to cause a recurrence of unstable equilibrium. The periodic on and off operation of the machine in an unstable condition is referred to as surge.

Let C is the point at which compressor is operating. At C if the flow is reduced by gradual closing of control valve operating point will be shifted to $B$ and become stable. Further gradual closing of control valve at point $B$ pressure ratio increases and it reaches maximum pressure ratio at $A$. If flow decrease by gradual closing of control valve beyond the point A pressure ratio decreases. At this condition, at downstream pressure is higher than the upstream of control valve which results in momentary stop of flow of compressed air and even flow may be reversal. Due to momentary stop or reverse flow pressure in the downstream decreases which causes delivery of compressed air to the downstream of control valve. Again, the pressure at downstream increases, which causes again stoppage of flow or reverse flow. Due to this again after a moment pressure at downstream decreases causing flow from downstream to upstream. Likewise cycle gets repeated with high frequency. This Phenomenon is called Surging or Pumping

## Surge Mechanism

When a centrifugal compressor surges, there is an actual reversal of gas flow through the compressor impeller. The surge usually starts in one stage of a multistage compressor and can occur very rapidly.


Now we will see how the surge starts in a compressor. The surge is starting with the instant flow reverses, shown in the above figure. Consider the Point "A" is the actual flow developed by the compressor during normal operation. Due to the decrease in flow the operating point shift from "A" to "B". The compressed gas actually rushes backwards through the impeller from the discharge to the inlet. The release of compressed gas from the discharge side results in the pressure drop from " B " to " C ". The reduction in pressure allows the flow to be reestablished in the positive direction "C" to "D" and increase the discharge pressure from "D" to "A". If nothing in the system change, then the surge cycle will continuous. The increase in duration of the surge cycle results in damage to the compressor.

## How Surge takes place in Centrifugal Compressor

Now we will see the surge phenomena in centrifugal compressor with the example compressor performance curve

## Suction throttling

Now consider the inlet flow decreases due to the suction valve throttling (they are many reasons will cause the compressor inlet flow rate decreases). Consider the compressor operating at the following conditions

Flow rate $=5500 \mathrm{~kg} / \mathrm{hr}$

Discharge pressure $=20$ bar.

Speed $=6000 \mathrm{rpm}$


Due to suction valve throttling the inlet flow rate of the compressor is decreased from operating point (A) to the new operating point (B) (Refer above figure). At the new operating point (B) the compressor flow is reduced on the other hand the discharge pressure will rise further. Due to the rise of pressure and decrease flow will cause the Surge cycle.

## Discharge valve throttling

Similarly, if the discharge side system resistance will increase due to discharge valve throttling. The pressure developed by the compressor will increase and flow rate will start decreases. The same phenomena will happen, that is the operating point "A" shifted to the new operating point of "B". This will cause the surge in the centrifugal compressor.

## Change in Speed

An increase in operating speed of the compressor also causes compressor surge. Now consider the operating speed of the compressor is 6000 rpm . If the speed increase to 7500 rpm . The Operating point of the compressor will shift from "A" to "B". (Refer below figure)


At new operating point " $B$ ", the discharge pressure of the compressor will increase. Due to the increase in pressure. The point " B " fall in the surge line. Due to this surge phenomena will occur in the compressor.

Other reasons will cause Surge in Centrifugal Compressor

## Inlet Filter Chocking

Due to dirty particles present in inlet filter will decrease the flow rate and reduce the suction pressure. Due to the reduce flow rate, the operating point will move toward the surge line. Once the operating point touches the surge line then Surge occur in the compressor.

## Driver Input Speed

In the case of the compressor is driven by Turbine or Variable speed drives. Sometimes the increase in speed may cause operating will shift to surge limit line and surge will occur.

## Change in Compressed gas Property

The change in operating gas can cause compressor surge.

## Surge result in centrifugal compressor

As we seen the surge is due to the flow reversal in the compressor. As a result of the surge in the compressor, it may lead to damage of compressor or compressor system. The following are some of the resulting due to surging.

- During the surge, a significant mass gas will flow in the reverse direction. As a result of a large dynamic force act on the impeller or blading within the compressor. Due to this the components of the compressor (such as thrust bearings, bearing, casing) exposed to large changes in axial force on the rotor. If the surge is not controlled it may result in fatigue damage to compressor or piping components.
- During the surge, the reversal of flow within the compressor results in hot compressed gas returning to the compressor inlet. If the surge is not controlled, as a result the temperature at compressor inlet will increase and leads to a potential rubbing of close clearance components. Due to the differential thermal expansion of components within the compressor.

6. A centrifugal compressor delivers $20 \mathrm{~kg} / \mathrm{s}$ of air with a total head pressure ratio of $4: 1$. The speed of the compressor is $12,000 \mathrm{rpm}$. Inlet total temperature is $15^{\circ} \mathrm{C}$ stagnation pressure at inlet is 1.0 bar, slip factor is 0.9 , and power input is 1.04 . Efficiency is $80 \%$. Calculate the outer diameter of the impeller ( $8 \mathrm{~b}, 10, \mathrm{~J}$ une/July 18)

$$
\dot{m}=20 \mathrm{~kg} / \mathrm{s} ; \quad \frac{p_{0 k+1}}{p_{01}}=4 ; \quad N=12000 \mathrm{rpm} ; T_{01}=15^{\circ}=288 \mathrm{~K} ; p_{01}=1 \mathrm{bar} ;
$$

Slip factor , $\mu=0.9 ;$ Power Input factor $\varphi=1.04 ; \eta_{t t}=0.8 ; D_{2}=$ ?

## outer diameter of the impeller

$$
\begin{array}{lll}
\eta_{s}=\frac{\Delta h_{05} ;}{\Delta h_{0}} ; & \eta_{s}=\frac{C_{p}\left(T_{o 2}-T_{01}\right)}{\Delta h_{0}} ; & \eta_{s}=\frac{c_{p} T_{01}\left(\frac{T_{02}}{T_{01}}-1\right)}{\Delta h_{0}} \\
\eta_{s}=\frac{c_{p} T_{01}\left(\left(\frac{p_{02}}{p_{01}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\Delta h_{0}} ; & 0.80=\frac{1005 * 288\left(4^{0.286}-1\right)}{\Delta h_{0}} ; & \Delta h_{0}=176045.72 \mathrm{~J} / \mathrm{kg} \\
\frac{-E}{\dot{m}}=\Delta h_{0} ; & \frac{-E}{\dot{m}}=176045.72 \mathrm{~J} / \mathrm{kg} & \\
\frac{-E}{\dot{m}}=\varphi \frac{\mu U_{2}^{2}}{g_{c}} ; & 176045.72=1.04 * \frac{0.9 * U_{2}^{2}}{1} ; & U_{2}^{2}=188083.03 \\
U_{2}=m / s ; & &
\end{array}
$$

$$
U_{2}=\frac{\pi D_{2} N}{60} ; \quad 433.68=\frac{\pi * D_{2} * 12000}{60} \quad D_{2}=0.69 \mathrm{~m}
$$

7. A centrifugal compressor delivers $18.2 \mathrm{~kg} / \mathrm{s}$ of air with a total pressure ratio of $4: 1$. Speed is 15000 rpm . Inlet total temperature is $15^{\circ} \mathrm{C}$, slip coefficient is 0.9 , power input factor is 1.04 . Efficiency is 0.8 . calculate overall diameter of impeller(8b, 10,June/July13)
$\dot{m}=18.2 \mathrm{~kg} / \mathrm{s} ; \frac{p_{0 k+1}}{p_{01}}=4 ; \quad N=15000 \mathrm{rpm} ; T_{01}=15^{\circ}=288 \mathrm{~K} ; p_{01}=1 \mathrm{bar} ;$
Slip factor , $\mu=0.9 ;$ Power Input factor $\varphi=1.04 ; \eta_{t t}=0.8 ; \quad D_{2}=$ ?

## outer diameter of the impeller

$$
\begin{array}{lrl}
\eta_{s}=\frac{\Delta h_{0 S}}{\Delta h_{0}} ; & \eta_{s}=\frac{C_{p}\left(T_{o 2 s}-T_{01}\right)}{\Delta h_{0}} ; & \eta_{s}=\frac{C_{p} T_{01}\left(\frac{T_{02 s}}{T_{01}}-1\right)}{\Delta h_{0}} \\
\eta_{s}=\frac{C_{p} T_{01}\left(\left(\frac{p_{02}}{p_{01}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\Delta h_{0}} ; & 0.80=\frac{1005 * 288\left(4^{0.286}-1\right)}{\Delta h_{0}} ; & \Delta h_{0}=176045.72 \mathrm{~J} / \mathrm{kg} \\
\frac{-E}{\dot{m}}=\Delta h_{0} ; & \frac{-E}{\dot{m}}=176045.72 \mathrm{~J} / \mathrm{kg} \\
\frac{-E}{\dot{m}}=\varphi \frac{\mu U_{2}^{2}}{g_{c}} ; & 176045.72=1.04 * \frac{0.9 * U_{2}^{2}}{1} ; & U_{2}^{2}=188083.03 \\
U_{2}=m / s ; & & \\
U_{2}=\frac{\pi D_{2} N}{60} ; & 433.68=\frac{\pi * D_{2} * 15000}{60} & D_{2}=0.55 \mathrm{~m}
\end{array}
$$

8. A centrifugal compressor runs at a speed of 15000 rpm and delivers air at $20 \mathrm{~kg} / \mathrm{s}$. Exit radius is 0.35 m , relative velocity and vane angles at exit are $100 \mathrm{~m} / \mathrm{s}$ and $75^{\circ}$ respectively. Assuming axial inlet stagnation temperature and stagnation pressure as 300 K and 1 bar respectively. Calculate: i) the torque ii) the power required to drive the compressor iii) ideal head developed iv) the work done and v) the exit total pressure. Take $C_{p}$ of air= $1.005 \mathrm{~kJ} / \mathrm{kgK}(8 \mathrm{~b}, 10, \mathrm{Dec} 17 / J a n 18)$
$N=15000 \mathrm{rpm} ; \quad \dot{m}=20 \mathrm{~kg} / \mathrm{s} ; \quad R_{2}=0.35 \mathrm{~m} ; \quad V_{r 2}=100 \mathrm{~m} / \mathrm{s} ; \quad \beta_{2}=75^{\circ} ; \quad T_{01}=300 \mathrm{~K} ;$ $p_{01}=1$ bar
i) Torque $=?$ ii) $E=$ ? iii) $H_{\text {ideal }}=?$ iv) $E=?$ v) $p_{02}=? \quad C_{p}$ of air= $1.005 \mathrm{~kJ} / \mathrm{kgK}=1005 \mathrm{~J} / \mathrm{kgK}$
i) Torque=?
$U_{2}=\frac{\pi D_{2} N}{60} ;$

$$
U_{2}=\frac{\pi * 0.7 * 15000}{60}
$$

$$
U_{2}=549.77 \mathrm{~m} / \mathrm{s}
$$

$V_{r 2} \cos \beta_{2}=100 \cos 75 ; \quad V_{r 2} \cos \beta_{2}=25.88 \mathrm{~m} / \mathrm{s}$
$\overrightarrow{V_{u 2}}=U_{2}-V_{r 2} \cos \beta_{2} ;$

$$
\overrightarrow{V_{u 2}}=549.77-25.88
$$

$$
\overrightarrow{V_{u 2}}=523.88 \mathrm{~m} / \mathrm{s}
$$

Torque, $T=\dot{m}\left(\overrightarrow{V_{u 2}} R_{2}-\overrightarrow{V_{u 1}} R_{1}\right) ; \quad T=20(523.88 * 0.35-0) ; \quad T=3667.16 \mathrm{Nm}$
ii) the power required to drive the compressor
$\frac{-E}{\dot{m}}=\frac{\left(\overrightarrow{V_{22}} U_{2}-\overrightarrow{V_{11}} U_{1}\right)}{g_{c}} ;$

$$
\frac{-E}{20}=\frac{523.88 * 549.77-0}{1} ;
$$

$$
-E=5760270.15 \mathrm{~W}
$$

Power required to drive the compressor $=5.76 * 10^{6} \mathrm{~W}=5.76 \mathrm{MW}$

## iii) ideal head developed

$H_{\text {ideal }}=\frac{\overrightarrow{\overline{u 2} U_{2}}}{g} ; \quad H_{\text {ideal }}=\frac{523.88 * 549.77}{9.81} \quad H_{\text {ideal }}=29.359 * 10^{3} \mathrm{~m}$ of air

## iv) the work done

$\frac{-E}{\dot{m}}=\frac{\left(\overrightarrow{V_{u 2}} U_{2}-\overrightarrow{V_{1}} U_{1}\right)}{g_{c}} ; \quad \quad \frac{-E}{\dot{m}}=\frac{523.88 * 549.77-0}{1} \quad$ work Input per kg $=288.013 * 10^{3} \mathrm{~J} / \mathrm{kg}$

## v) the exit total pressure

$\eta_{t t}=\frac{\Delta h_{0 s}}{\Delta h_{0}} ; \quad \quad \eta_{t t}=\frac{C_{p}\left(T_{o 2 s}-T_{01}\right)}{\Delta h_{0}} ; \quad \eta_{t t}=\frac{C_{p} T_{01}\left(\frac{T_{02 s}}{T_{01}}-1\right)}{\Delta h_{0}}$
$\eta_{t t}=\frac{\left.C_{p} T_{01}\left(\frac{p_{02}}{p_{01}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\Delta h_{0}} ;$ Assuming $\eta_{t t}=100 \% \quad \Delta h_{0}=C_{p} T_{01}\left(\left(\frac{p_{02}}{p_{01}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)$

$$
\begin{aligned}
& \frac{-E}{\dot{m}}=\Delta h_{0} ; \quad \Delta h_{0}=288.013 * 10^{3} \mathrm{~J} / \mathrm{kg} \\
& 288.013 * 10^{3}=1005 * 300\left(\left(\frac{p_{02}}{p_{01}}\right)^{0.286}-1\right) ; \quad\left(\frac{p_{02}}{p_{01}}\right)^{0.286}=1.955 ; \quad \frac{p_{02}}{p_{01}}=10.42
\end{aligned}
$$

9. The impeller tip speed of a centrifugal compressor is $370 \mathrm{~m} / \mathrm{s}$, slip factor is 0.9 , and the radial component at the exit is $35 \mathrm{~m} / \mathrm{s}$. If the flow area at the exit is $0.18 \mathrm{~m}^{2}$ and compressor efficiency is $88 \%$. Determine the mass flow rate of air and the absolute Mach number at impeller tip. Assume air density $=1.57 \mathrm{~kg} / \mathrm{m}^{3}$ and inlet stagnation temperature 290 K . Neglect the work input factor. Also find the overall pressure ratio of the compressor ( $8 \mathrm{~b}, 12$, Dec15/Jan16)
$U_{2}=370 \mathrm{~m} / \mathrm{s} ; \quad$ slip factor $\mathrm{i} \mu=0.9 ;$
the radial component at the exit is $35 \mathrm{~m} / \mathrm{s}$ ie $V_{r d 2}=35 \mathrm{~m} / \mathrm{s}$;
flow area at the exit is $0.18 m^{2}$ ie $A_{f 2}=0.18 m^{2} ; \quad \eta_{t t}=0.88$
i) $\dot{m}=$ ? ii) absolute Mach number at impeller tip $M_{2}=$ ?; Assume $\rho=1.57 \mathrm{~kg} / \mathrm{m}^{3} ; T_{01}=290 \mathrm{~K}$

Neglect work input factor ie $\varphi=1$ iii) $\frac{p_{02}}{p_{01}}=$ ?

## the mass flow rate of air

$\dot{m}=\rho A_{f 2} V_{r d 2} ;$

$$
\dot{m}=1.57 * 0.18 * 35
$$

$$
\dot{m}=9.891 \mathrm{~kg} / \mathrm{s}
$$

## Absolute Mach number at impeller tip.

$\mu=\frac{\overrightarrow{V_{u 2}}}{V_{u 2}^{\prime}} ; \quad \overrightarrow{V_{u 2}}=\mu \overrightarrow{V_{u 2}^{\prime}}$ assuming radial vane at outlet ie $\overrightarrow{V_{u 2}^{\prime}}=U_{2} ; \quad \overrightarrow{V_{u 2}}=\mu U_{2}$
$\overrightarrow{V_{u 2}}=0.9 * 370 ; \quad \overrightarrow{V_{u 2}}=333 \mathrm{~m} / \mathrm{s}$
$V_{2}^{2}=V_{u 2}^{2}+V_{r d 2}^{2} ; \quad V_{2}^{2}=333^{2}+35^{2} ; \quad V_{2}^{2}=112114 \quad V_{2}=334.83$
$\frac{-E}{\dot{m}}=\frac{\overrightarrow{V_{u 2}} U_{2}}{g_{c}} ; \quad \frac{-E}{\dot{m}}=\frac{\mu U_{2} U_{2}}{g_{c}} ; \quad \frac{-E}{\dot{m}}=\frac{0.9 * 370^{2}}{1} ; \quad \frac{-E}{\dot{m}}=123210 \mathrm{~J} / \mathrm{kg} ;$
$\frac{-E}{\dot{m}}=\Delta h_{0} ; \quad \Delta h_{0}=123210 \mathrm{~J} / \mathrm{kg}$

$$
\begin{array}{lll}
\Delta h_{0}=C_{p}\left(T_{02}-T_{01}\right) ; & 123210=1005\left(T_{02}-290\right) & T_{02}=412.59 \mathrm{~K} \\
T_{02}=T_{2}+\frac{V_{2}^{2}}{2 g_{c} C_{p}} ; & 412.59=T_{2}+\frac{112114}{2 *!* 1005} ; & T_{2}=356.81 \mathrm{~K} \\
M_{2}=\frac{V_{2}}{\sqrt{\gamma R T_{2}} ;} ; & M_{2}=\frac{334.83}{\sqrt{1.4 * 287 * 356.81}} & M_{2}=0.884
\end{array}
$$

## overall pressure ratio of the compressor

$$
\eta_{t t}=\frac{\Delta h_{0 s}}{\Delta h_{0}} ; \quad \quad \eta_{t t}=\frac{C_{p}\left(T_{o 2 s}-T_{01}\right)}{\Delta h_{0}} ; \quad \eta_{t t}=\frac{c_{p} T_{01}\left(\frac{T_{02 s}}{T_{01}}-1\right)}{\Delta h_{0}}
$$

$$
\eta_{t t}=\frac{C_{p} T_{01}\left(\left(\frac{p_{02}}{p_{01}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\Delta h_{0}}
$$

$$
\Delta h_{0}=\frac{-E}{\dot{m}} ; \quad \frac{-E}{\dot{m}}=\frac{\overrightarrow{V_{u 2}} U_{2}}{g_{c}} ; \quad \frac{-E}{\dot{m}}=\frac{\mu U_{2} U_{2}}{g_{c}} ; \quad \frac{-E}{\dot{m}}=\frac{0.9 * 370^{2}}{1}
$$

$$
\frac{-E}{\dot{m}}=123210 \mathrm{~J} / \mathrm{kg} ; \quad \Delta h_{0}=123210 \mathrm{~J} / \mathrm{kg}
$$

$$
\eta_{t t}=\frac{C_{p} T_{01}\left(\left(\frac{p_{02}}{p_{01}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\Delta h_{0}} ; \quad 0.88=\frac{1005 * 290\left(\left(\frac{p_{02}}{p_{01}}\right)^{0.286}-1\right)}{123210} ; \quad\left(\frac{p_{02}}{p_{01}}\right)^{0.286}=1.372
$$

$$
\frac{p_{02}}{p_{01}}=3.02
$$

10. Backward swept centrifugal fan develops a pressure of 75 mm WG. It has an impeller diameter of 89 cm and runs at 720 rpm . The blade angle at the tip is $39^{\circ}$ and the width of the impeller is 10 cm . Assuming a constant velocity of flow of $9.15 \mathrm{~m} / \mathrm{s}$ and density of $1.2 \mathrm{~kg} / \mathrm{m}^{3}$, determine the fan efficiency, discharge, power required, stage reaction and pressure coefficient (8b, 10, Dec18/19)
pressure of 75 mm WG ie $\frac{p_{2}}{\rho g}=75 \mathrm{~mm} \mathrm{WG} ; D_{2}=89 \mathrm{~cm}=0.89 \mathrm{~m} ; \quad N=720 \mathrm{rpm}$;
The blade angle at the tip is $39^{\circ}$ ie $\beta_{2}=39^{\circ}$; width of the impeller is $10 \mathrm{~cm} H_{2}=0.1 \mathrm{~m}$
constant velocity of flow of $9.15 \mathrm{~m} / \mathrm{s}$ ie $V_{f 2}=9.15 \mathrm{~m} / \mathrm{s} ; \rho=1.2 \mathrm{~kg} / \mathrm{m}^{3}$
i) $\quad \eta_{t t}=$ ?;
ii) $\dot{m}=$ ?
iii) $-E=?$;
iv) $R=$ ? v) pressure coefficient $\varphi_{p}=$ ?

## fan efficiency

$U_{2}=\frac{\pi D_{2} N}{60} ;$

$$
U_{2}=\frac{\pi * 0.89 * 720}{60}
$$

$$
U_{2}=33.55 \mathrm{~m} / \mathrm{s}
$$

$V_{f 2} \cot \beta_{2}=9.15 \cot 39 ; \quad V_{f 2} \cot \beta_{2}=11.29 \mathrm{~m} / \mathrm{s}$
$\overrightarrow{V_{u 2}}=U_{2}-V_{f 2} \cot \beta_{2} ;$

$$
\overrightarrow{V_{u 2}}=33.55-11.29
$$

$$
\overrightarrow{V_{u 2}}=22.26 \mathrm{~m} / \mathrm{s}
$$

$\frac{-E}{\dot{m}}=\frac{\overrightarrow{V_{u 2}} U_{2}}{g_{c}} ;$

$$
\frac{-E}{\dot{m}}=\frac{22.26 * 33.55}{1}
$$

$$
\frac{-E}{\dot{m}}=746.89 \mathrm{~J} / \mathrm{kg}
$$

$\Delta h_{0}=\frac{-E}{\dot{m}} ;$

$$
\Delta h_{0}=746.89 \mathrm{~J} / \mathrm{kg}
$$

$\eta_{t t}=\frac{\Delta h_{0 s}}{\Delta h_{0}} ;$
$\eta_{t t}=\frac{C_{p} T_{01}\left(\left(\frac{p_{02}}{p_{01}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\Delta h_{0}}$
$\frac{p_{2}}{\omega}=75 \mathrm{~mm} \mathrm{WG}=0.075 \mathrm{~m}$ of water (guage);
$\frac{p_{02}}{\omega}($ absolute $)=$ guage pressure head + atm. Pressure head (generally 10.3 m of water)

$$
\begin{aligned}
\frac{p_{02(\text { guage })}^{9,81 * 1000}=0.075 \mathrm{~m} \text { of } \text { water } ;}{} & p_{02(\text { guage })}=735.75 \mathrm{~N} / \mathrm{m}^{2} \\
p_{02(\text { abs })}=p_{02(\text { guage })}+p_{\text {atm }} ; & \text { Assume } p_{\text {atm }}=1 \mathrm{bar}=10^{5} \mathrm{~N} / \mathrm{m}^{2} ; \\
p_{02(\text { abs })}=\left(735.75+10^{5}\right) \mathrm{N} / \mathrm{m}^{2} ; & p_{02(\text { abs })}=1.0074 \mathrm{bar}
\end{aligned}
$$

Assume $p_{01}=1$ bar $; T_{01}=300 \mathrm{~K}$
$\eta_{t t}=\frac{1005 * 300\left(\left(\frac{1.0074}{1}\right)^{0.286}-1\right)}{746.89} ; \quad \eta_{t t}=0.852$

## Discharge

$Q=A_{f 2} V_{f 2} ;$
$Q=\left(\pi D_{2} H_{2}\right) V_{f 2} ;$
$Q=\pi * 0.89 * 0.1 * 9.15 ;$
$Q=2.558 m^{3} / s$
$\dot{m}=\rho Q ;$
$\dot{m}=1.2 * 2.558 \mathrm{~kg} / \mathrm{s}$
$\dot{m}=3.07 \mathrm{~kg} / \mathrm{s}$

## power required

$-E=\frac{-E}{\dot{m}} \dot{m} ;$

$$
-E=746.89 * 3.07 W \quad \text { Power required }=2292.97 W
$$

stage reaction
$R=\frac{\frac{E}{\dot{m}}-\left(\frac{V_{1}^{2}-V_{2}^{2}}{2 g_{c}}\right)}{\frac{E}{\dot{m}}} ;$

$$
R=1-\frac{\left(V_{1}^{2}-V_{2}^{2}\right)}{2 g_{c}^{E}}
$$

$V_{2}^{2}=V_{u 2}^{2}+V_{f 2}^{2} ; \quad V_{2}^{2}=22.26^{2}+9.15^{2} ;$
$V_{1}^{2}=V_{u 1}^{2}+V_{f 1}^{2} ;$
$V_{1}^{2}=0+9.15^{2} ;$
$V_{2}^{2}=579.23$
$V_{1}^{2}=83.72$
$\frac{-E}{\dot{m}}=746.89 \mathrm{~J} / \mathrm{kg}$;
$\frac{E}{\dot{m}}=-746.89 \mathrm{~J} / \mathrm{kg}$
$R=1-\frac{\left(V_{1}^{2}-V_{2}^{2}\right)}{2 g_{c} \frac{E}{\dot{m}}} ;$
$R=1-\frac{(83.72-579.23)}{2 * 1 *(-746.89)} ;$
$R=0.668$
pressure coefficient $\varphi_{p}=\frac{\Delta h_{0}}{U_{2}^{2}}$
$\varphi_{p}=\frac{\Delta h_{0}}{U_{2}^{2}} ; \quad \varphi_{p}=\frac{746.89}{33.55^{2}} \quad \varphi_{p}=0.663$
11. An axial compressor / blower supplies air to furnace at the rate of $3 \mathrm{~kg} / \mathrm{s}$. The atmospheric conditions being 100 kPa and 310 K , the blower efficiency is $80 \%$. Mechanical efficiency is $85 \%$ The power supplied to 30 kW . Estimate the overall efficiency and pressure developed in mm WG(8c,8,June/July14)
$\dot{m}=3 \mathrm{~kg} / \mathrm{s} ; \quad p_{01}=100 \mathrm{kPa} ; \quad T_{01}=310 \mathrm{~K} \quad \eta_{t t}=0.8 \quad E=30 \mathrm{~kW}=3000 \mathrm{~W}$

## overall efficiency

$$
\eta_{o}=\eta_{t t} \eta_{\text {mech }} ; \quad \eta_{o}=0.8 * 0.85 \quad \eta_{o}=0.68
$$

## pressure developed in mm WG

$$
\begin{array}{llr}
\quad \frac{-E}{\dot{m}}=\frac{3000}{3} ; & \frac{-E}{\dot{m}}=1000 \mathrm{~J} / \mathrm{kg} ; & \frac{-E}{\dot{m}}=\Delta h_{0} ; \quad 1000 \mathrm{~J} / \mathrm{kg}=\Delta h_{0} \\
\eta_{t t}=\frac{\Delta h_{0 s}}{\Delta h_{0}} ; & \eta_{t t}=\frac{C_{p}\left(T_{02 s}-T_{01}\right)}{\Delta h_{0}} ; & \eta_{t t}=\frac{C_{p} T_{01}\left(\frac{T_{02 s}}{T_{01}}-1\right)}{\Delta h_{0}} \\
\eta_{t t}=\frac{C_{p} T_{01}\left(\left(\frac{p_{02}}{p_{01}}\right)^{\frac{\gamma-1}{\gamma}}-1\right)}{\Delta h_{0}} ; & 0.8=\frac{1005 * 310\left(\left(\frac{p_{02}}{p_{01}}\right)^{0.286}-1\right)}{1000} \\
\frac{p_{02}}{p_{01}}=1.009 ; & \frac{p_{02}}{100 * 10^{3}}=1.009 & \left(\frac{p_{02}}{p_{01}}\right)^{0.286}=1.00257 \\
& p_{02}=100901.48 \mathrm{~Pa}
\end{array}
$$

$p_{02}($ guage $)=100901.48-100000 ; \quad p_{02}($ guage $)=901.48 P a$
$\frac{p_{02}}{\omega}=\frac{901.48}{9810} ;$
$\frac{p_{02}}{\omega}=0.0918 \mathrm{~m}$ of water
$\frac{p_{02}}{\omega}=91.8 \mathrm{~mm} \mathrm{WG}$


[^0]:    Absolute Velocity at is to be resolved into two components ---

[^1]:    $V_{u 1}$ is $+v e$

