

Manual of Petroleum Measurement Standards

Chapter 11 – Physical Properties Data

Section 2, Part 4 – Temperature Correction for the Volume NGL and LPG

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Foreword

For custody transfer purposes, natural gas liquid (NGL) and liquefied petroleum gas (LPG) volumes are generally stated at a fixed base temperature and saturation pressure. As most volume transfers occur at temperatures and pressures other than standard conditions, these volumes are adjusted to standard conditions through the use of correction factors.

This document presents a new method to calculate temperature correction factors. With the publication of this document, previous API, ASTM and GPA documents containing NGL and LPG temperature correction factors should no longer be used. The document is specifically titled as being suitable for NGL and LPG liquids. Light hydrocarbon mixtures containing significant quantities of methane, carbon dioxide and nitrogen which have density ranges which overlap those contained in these tables can be encountered. However, the two-fluid correlation which is the basis of these tables was not calibrated for such mixtures.

The actual Standard represented by this report consists of the explicit implementation procedures. Sample tables and other examples created from a computerized version of these implementation procedures are presented within. However, these are for examples only and do not represent the Standard.

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Summary of Changes from Chapter 11.2.4, 1st edition to Chapter 11.2.4, 2nd edition.

This 2nd edition revision addressed several editorial errors and issues that needed clarification. There are no changes in the 2nd edition which would change the implementation guidelines.

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Nomenclature

A, B, C	parameters in Section 5.1.2 quadratic equation
C_{TL}	temperature correction factor
h_2	scaling factor
k_1, k_2, k_3, k_4	parameters in saturation density equation
T_B	base temperature (60°F, 15°C, or 20°C)
T_{BK}	base temperature (288.15 K, or 293.15 K)
T_c	fluid critical temperature (K)
$T_{c,ref}$	reference fluid critical temperature (K)
T_F	observed measurement temperature (°F or °C)
$T_{r,x}$	reduced observed temperature
T_x	observed temperature (K)
V_{60}/V_{Tx}	ratio of volume at 60°F to volume at temperature T_x . Is the basic definition of C_{TL}
X	interpolating factor
Z_c	critical compressibility factor
α, β, ϕ	parameters in Section 5.1.2 quadratic equation
δ	interpolation variable
τ	parameter in saturation density equation
τ_x	<u>parameter in saturation density equation at observed temperature</u>
γ_x	relative density at observed temperature
$\gamma_{x,high}$	relative density at the observed temperature corresponding to the upper boundary for the 60°F relative density
$\gamma_{x,low}$	relative density at the observed temperature corresponding to the lower boundary for the 60°F relative density
$\gamma_{x,mid}$	relative density at the observed temperature corresponding to the intermediate 60° relative density used in Section 5.1.2 iteration procedure
$\gamma_{x,trial}$	trial relative density at the observed temperature used in Section 5.1.2 iteration procedure
γ_{TB}	relative density at the base temperature, T_B
γ_{60}	relative density at a base temperature of 60°F
γ_{Tx}	relative density at the observed temperature, T_x
$\gamma_{60,high}$	upper bound for the observed fluid's 60°F relative density
$\gamma_{60,low}$	lower bound for the observed fluid's 60°F relative density
$\gamma_{60,mid}$	intermediate 60°F relative density value used in Section 5.1.2 iteration procedure
$\gamma_{60,trial}$	trial 60°F relative density value used in Section 5.1.2 iteration procedure
ρ_c	critical molar density (gram-mole/L)
ρ_{60}	density at a base temperature of 60°F (kg/m^3)
ρ_{15}	density at a base temperature of 15°C (kg/m^3)

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ρ_{20} density at a base temperature of 20°C (kg/m³)
 ρ^{sat} saturation molar density (gram-mole/L)
 ρ_{60}^{sat} saturation molar density at 60°F (gram-mole/L)
 ρ_T^{sat} saturation molar density at observed temperature (gram-mole/L)

ρ_{w60} density of water at 60°F (kg/m³)

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Temperature Correction for the Volume of NGL and LPG

Tables 23E, 24E, 53E, 54E, 59E, and 60E

0 Implementation Guidelines

This Revised Standard/~~Technical Publication~~ is effective upon the date of publication and supersedes the ASTM-IP 1952 Petroleum Measurement Tables, GPA 2142, GPA TP-16, Tables 33 and 34 of API MPMS Chapter 11.1-1980 Volumes XI/XII (Adjuncts to ASTM D1250-80 and IP 200/80), ~~API MPMS Chapter 11.2.2/11.2.2M~~, and API/ASTM/GPA 8217/8117. However, due to the nature of the changes in this Revised Standard/~~Technical Publication~~ and the fact that it is or may be incorporated by reference in various regulations, it is recognized that guidance concerning an implementation period may be needed in order to avoid disruptions within the industry and ensure proper application. ~~As a result, it is recommended that this Revised Standard/Technical Publication be utilized on all new and existing applications no later than TWO YEARS after the publication date.~~ An application, for this purpose, is defined as the point where the calculation is applied.

Once the Revised Standard/~~Technical Publication~~ is implemented in a particular application, the Previous Standard/~~Technical Publication~~ will no longer be used in that application.

However, the use of API standards ~~and ASTM and GPA technical publications~~ remains voluntary, and the decision on when to ~~utilize~~ a standard/technical publication is an issue that is subject to the negotiations between the parties involved in the transaction.

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1 Introduction

For custody transfer purposes, natural gas liquid (NGL) and liquefied petroleum gas (LPG) volumes are generally stated at a fixed base temperature and saturation pressure. As most volume transfers occur at temperatures and pressures other than standard conditions, these volumes are adjusted to standard conditions through the use of correction factors. Separate factors for temperature (C_{TL}) and pressure (C_{PL}) are used to make these corrections. This document presents a new method to calculate temperature correction factors. Pressure correction factors are not within the scope of this document, but can be calculated using American Petroleum Institute *Manual of Petroleum Measurement Standards (MPMS)* Chapter 11.1-2004^[1] (which superseded Chapter 11.2.1-1984^[2] and 11.2.1M-1984^[3]), Chapter 11.2.2-1986/GPA 8286-86^[4] or Chapter 11.2.2M-1986/GPA 8286-86^[5], depending on product type.

Previously, most NGL and LPG temperature correction factors have been obtained from a variety of sources:

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- ASTM-IP "Petroleum Measurement Tables"^[6], published in 1952. This publication is limited to a 60°F relative density range of 0.500 and higher.
- GPA Standard 2142, "Standard Factors for Volume Correction and Specific Gravity Conversion of Liquefied Petroleum Gases"^[7], published in 1957, also contains the same correction factors as the 1982 ASTM-IP document.
- GPA TP-16 "Composite Pressure and Temperature Volume Correction Factor Tables for Liquefied Petroleum Gas (LPG) and Natural Gasoline"^[8], published in 1988. It is limited to the following products: HD-5 Propane with a relative densities of 0.501, 0.505, and 0.510; iso-butane at a relative density of 0.565; normal butane at a relative density of 0.585; and natural gasoline (12-14 psia RVP) at a relative density of 0.664.
- API MPMS Chapter 11.1-1980/ASTM D1250-80 Volume XII, Table 33 "Specific Gravity Reduction to 60°F For Liquefied Petroleum Gases and Natural Gasoline"^[9].
- API MPMS Chapter 11.1-1980/ASTM D1250-80 Volume XII, Table 34 "Reduction of Volume to 60°F Against Specific Gravity 60/60°F For Liquefied Petroleum Gases"^[9].
- API/ASTM/GPA 8117 "Temperature Correction for the Volume of Light Hydrocarbons"^[10].
- [API/ASTM/GPA 8217 "Temperature Correction for the Volume of NGL and LPG"](#)^[14]

With the publication of this document, the above API, ASTM and GPA documents should no longer be used for NGL and LPG temperature correction factors. Text for **GPA 8217₅** as approved is included without technical change in this present document. Some edits have been made to align flow charts with examples shown so that they may be consistent.

2 Scope

The actual Standard represented by this report consists of the explicit implementation procedures. Sample tables, flow charts, and specific examples created from a computerized version of these implementation procedures are presented within. The examples are to provide guides and check points to those who wish to implement a computerized procedure to represent the Standard, however these are not a part of the actual Standard.

This Standard covers a 60°F relative density range of 0.3500 to 0.6880 which nominally equates to a density at 15°C of 351.7 to 687.8 kg/m³ and a density at 20°C of 331.7 to 683.6 kg/m³. The temperature range of this Standard is -50.8 to 199.4°F (-46 to 93°C). At all conditions, the

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pressure is assumed to be at saturation conditions (also known as bubble point or saturation vapor pressure).

Note that these are nominal ranges which are further refined within the standard by correlation limits to be the ranges bounded by the points in the following table:

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Table 1: MPMS 11.2.4 Correlation Limits

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<u>Relative Density</u> <u>(60°F/60°F)</u>	<u>Lower Temperatur e Limit</u> (<u>°F</u>)	<u>Upper Temperatur e Limit</u> (<u>°F</u>)	<u>Lower Temperatur e Limit</u> (<u>°C</u>)	<u>Upper Temperatur e Limit</u> (<u>°C</u>)	<u>Lower Temperatur e Limit</u> (<u>K</u>)	<u>Upper Temperatur e Limit</u> (<u>K</u>)
<u>0.35000</u>	<u>-50.8</u>	<u>87.4</u>	<u>-46.0</u>	<u>30.8</u>	<u>227.15</u>	<u>303.93</u>
<u>0.35599</u>	<u>-50.8</u>	<u>89.9</u>	<u>-46.0</u>	<u>32.2</u>	<u>227.15</u>	<u>305.32</u>
<u>0.42928</u>	<u>-50.8</u>	<u>140.9</u>	<u>-46.0</u>	<u>60.5</u>	<u>227.15</u>	<u>333.65</u>
<u>0.47038</u>	<u>-50.8</u>	<u>174.8</u>	<u>-46.0</u>	<u>79.3</u>	<u>227.15</u>	<u>352.48</u>
<u>0.49935</u>	<u>-50.8</u>	<u>199.4</u>	<u>-46.0</u>	<u>93.0</u>	<u>227.15</u>	<u>366.15</u>
<u>0.68800</u>	<u>-50.8</u>	<u>199.4</u>	<u>-46.0</u>	<u>93.0</u>	<u>227.15</u>	<u>366.15</u>

As shown in the following figure:

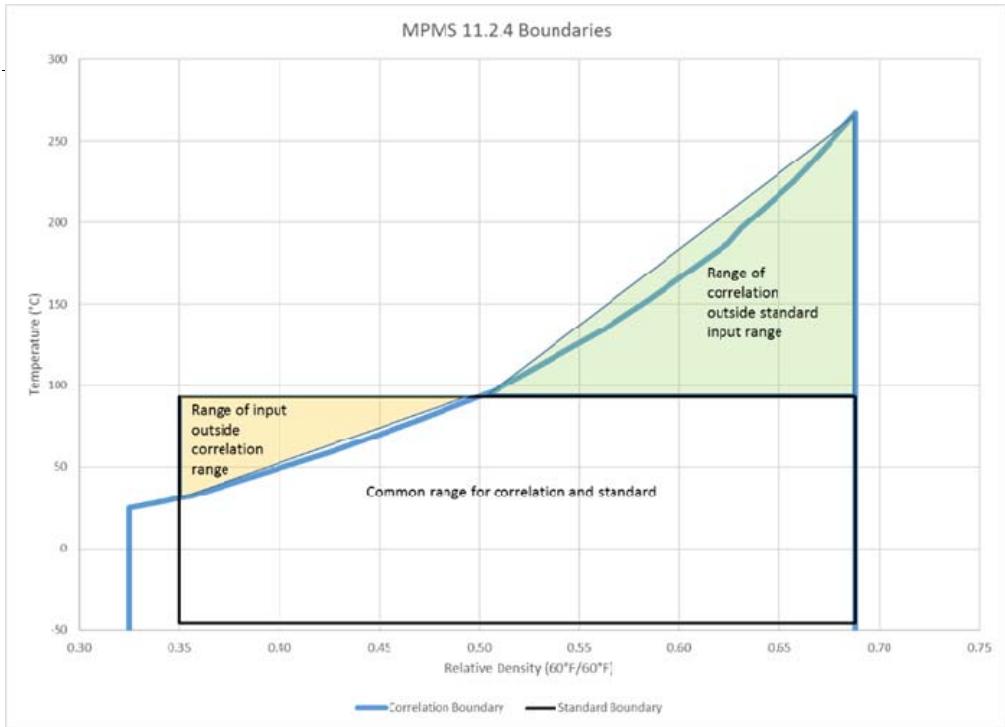


Figure 1: MPMS 11.2.4 Boundaries

Input range – the box defined in the scope of the standard as a ($60^{\circ}\text{F}/60^{\circ}\text{F}$) relative density of 0.35 to 0.688 and -46 to 93 °C.

Correlation range – the polygon defined by line segments connecting the relative densities and critical temperatures of the reference fluids in Table 1 of the standard for the upper boundary, -46 °C for the lower temperature boundary, the relative density of EE (68/32) for the lower relative density boundary and the relative density of n-heptane for the upper relative density boundary. See Figure 1 in this document for an illustration.

The calculation method was developed from GPA RR-148 “Volume Correction Factors for Natural Gas Liquids – Phase II”^[11] and API/ASTM/GPA Technical Publication, TP-25, September, 1998^[10]. The implementation procedures for Tables 23 and 24 are entirely consistent with those presented in API/ASTM/GPA Technical Publication, TP-275. Supporting data can be found in GPA RR-147 “Density Measurements on Natural Gas Liquids”^[12]. GPA RR-133 “Volume Correction Factors for Natural Gas Liquids – Phase I”^[13] should no longer be used, as GPA RR-148 completely replaced it.

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The implementation procedures describe how to:

- 1) calculate the C_{TL} given an appropriate density factor at the basis temperature and an observed temperature, and
- 2) calculate the appropriate density factor at basis temperature given a relative density at an observed temperature.

The implementation procedures are presented in pairs by base temperature. First the procedures for Tables 23 and 24 at a 60°F base temperature are given. The procedure for Table 23 makes use of the procedure described in Table 24 thus Table 24 is presented first. These are followed by procedures for Tables 54 and 53 at a base temperature of 15°C which themselves make use of procedures described in Tables 23 and 24; these in turn are followed by the procedures for Tables 60 and 59 at a base temperature of 20°C which also make use of procedures described in Tables 23 and 24.

It is important to note that this standard assumes all fluids covered by this standard are at a fixed base temperature and saturation pressure. When a RHO_{tp} is measured at an elevated pressure, an iterative procedure to solve for base density is required for fiscal purposes. The following expression shall be used to determine base density RHO_b)

$$|\delta p_o^{(m)}| < 0.000001 \text{ kg/m}^3 \quad \text{where} \quad \delta p_o^{(m)} = p_o - p_{60}^{(m)} \cdot C_{TPL}^{(m)}$$

The computation for correcting from density at flowing conditions (RHO_{tp}) to density at base conditions (RHO_b) may be carried out continuously if mutually agreed between the parties.

3 Significant Digits

It is intended that all future temperature correction factors be utilized used with five decimal digits (e.g., 0.xxxxx or 1.xxxxx). As a result, this document contains C_{TL} values with only five decimal digits. This is a departure from both the 1952 “ASTM-IP Petroleum Measurement Tables” and GPA TP-16, which give either 3 or 4 decimal digits.

4 Comparison to the Previous Standards

As the 1952 ASTM-IP standard is limited to a low-end relative density of 0.50, a comparison can only be made at higher relative densities. The following figures show how the standards compare. The calculations are performed at 10°F and 5°C increments. It can be noted that the deviation plots for the 0.50 to 0.59 relative densities (500 to 590 kg/m³ densities) are “ragged” in appearance, while the deviation plots for the higher relative densities are “smooth.” This can mostly be attributed to the 1952 ASTM-IP Standard's rounding method: C_{TL} values under relative density 0.60 contain 3 decimal digits while C_{TL} values greater than 0.600 contain 4 decimal digits.

Note: Negative deviations indicate that the new table C_{TL} is lower than the old (1952) ASTM table C_{TL} . Positive deviations indicate that the new table C_{TL} is higher than the old (1952) ASTM table C_{TL} .

Chart 1: C_{TL} Deviations of New Table 24 Values
Compared to Old Table 24 Values

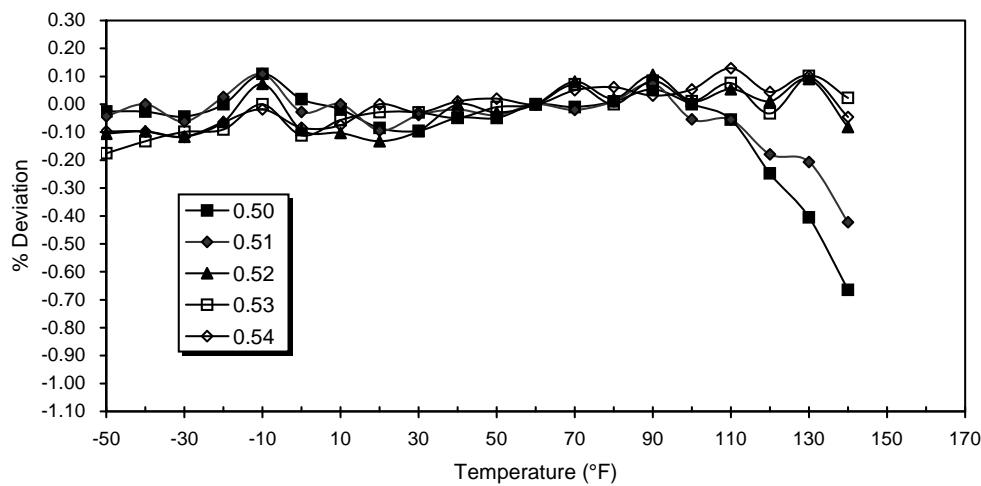
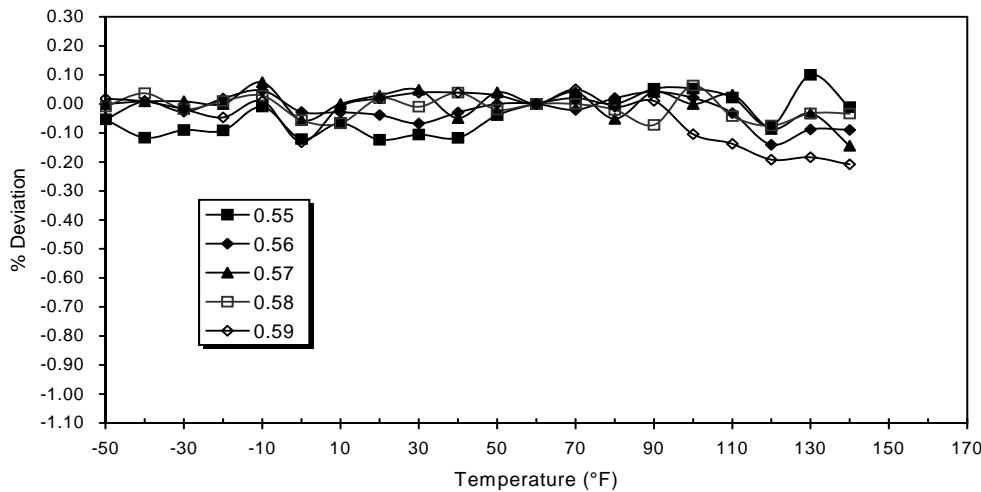


Chart 2: C_{TL} Deviations of New Table 24 Values
Compared to Old Table 24 Values



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Chart 3: C_{TL} Deviations of New Table 24 Values
Compared to Old Table 24 Values

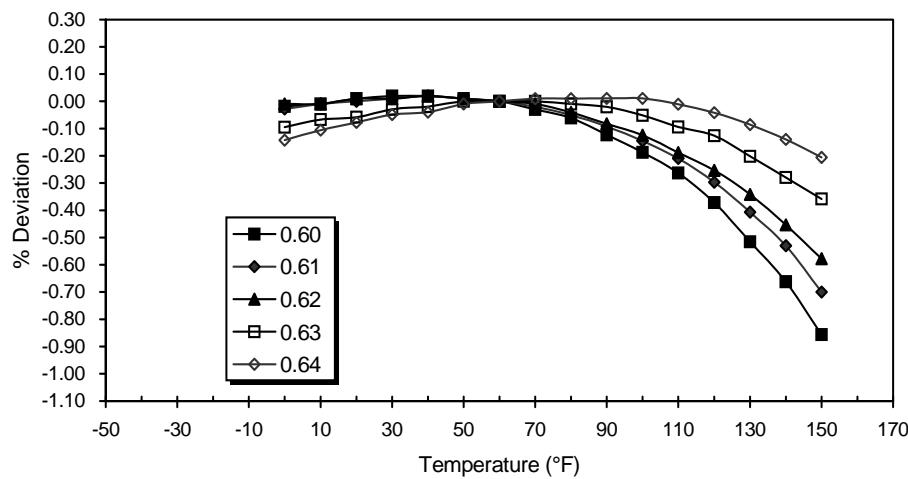
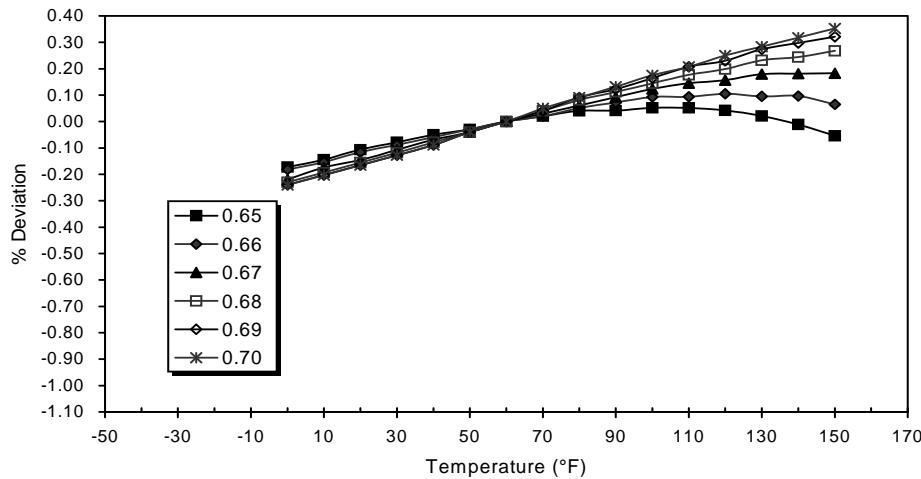


Chart 4: C_{TL} Deviations of New Table 24 Values
Compared to Old Table 24 Values



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Chart 5: C_{TL} Deviations of New Table 54 Values
Compared to Old Table 54 Values

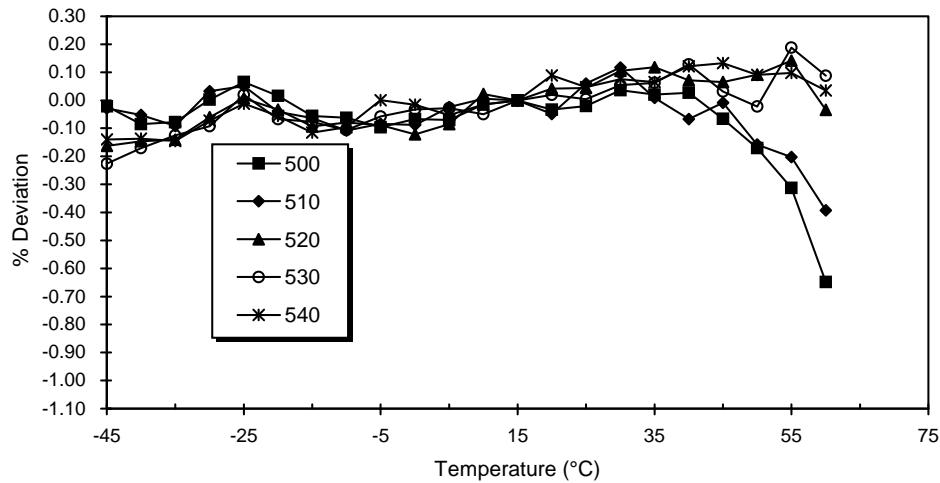
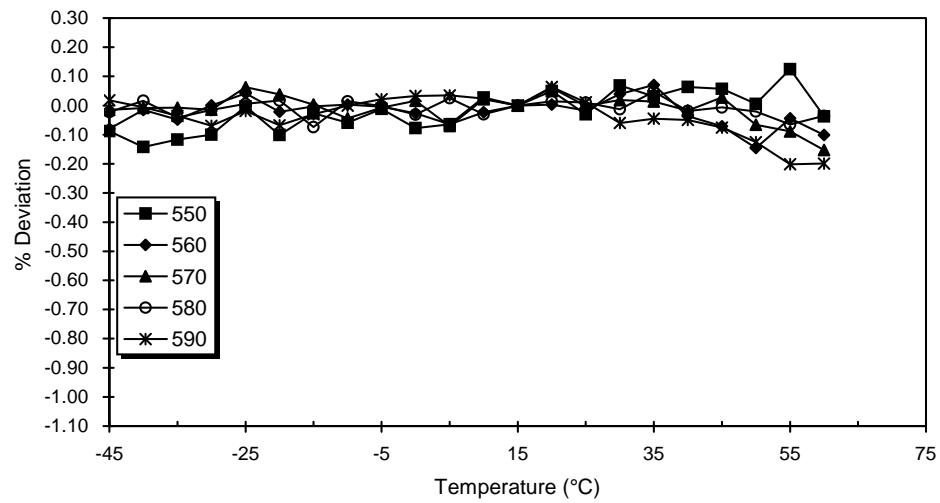


Chart 6: C_{TL} Deviations of New Table 54 Compared to
Old Table 54 Values



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Chart 7: C_{TL} Deviations of New Table 54 Values Compared to Old Table 54 Values

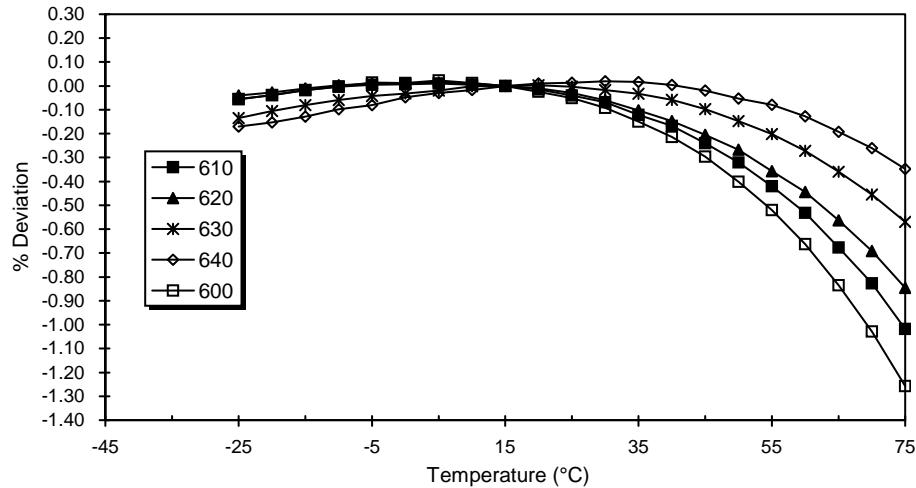
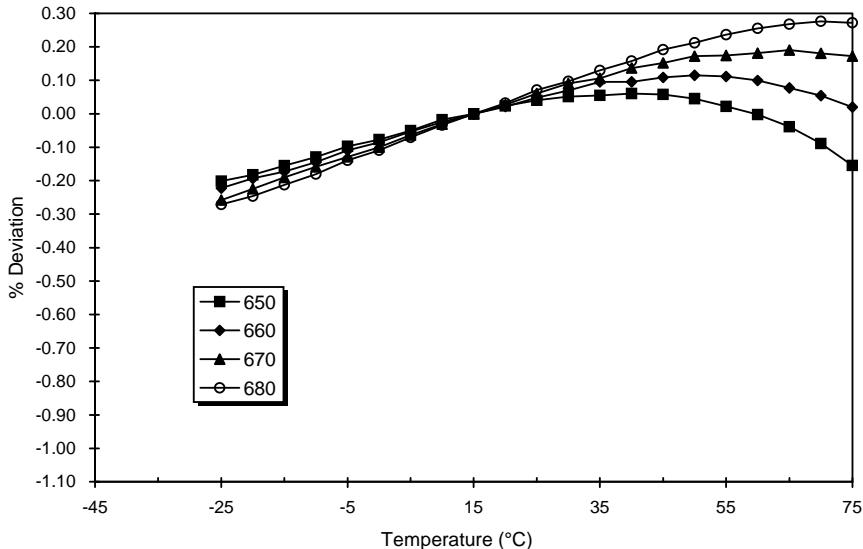


Chart 8: C_{TL} Deviations of New Table 54 Values Compared to Old Table 54 Values



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5 Implementation Procedures

The methods to calculate C_{TL} from Tables 24E, 54E, and 60E and relative density at the base temperature from Tables 23E, 53E and 59E follow. These methods are called implementation procedures, which are similar to the methods described and found in American Petroleum Institute MPMS Chapter 11.1. [The new API 11.1 2004 uses the Newton Iteration Method which is not employed or applicable for this standard.](#)

All calculations are to be performed using double precision (i.e., long floating point, eight byte, or 64-bit) arithmetic. This should allow the computer program to recognize the difference between 1.0 and $1.0 + \epsilon$ for absolute values of ϵ on the order of 10^{-16} . [This also means that approximately 16 decimal digits are used for all calculations.](#)

Examples are presented for each of the procedures described, they cover the range of the tables. Even though double precision was used for these example calculations only twelve decimal digits are printed here. If one uses these examples to test their own computer implementation of these procedures, it is suggested that at least eight of the significant digits be matched. The exceptions to this are for the variables α , β , A , B , and C of Table 23 (Section 5.1.2). These may show greater deviation, but the resulting $\gamma_{60,trial}$ and $\gamma_{x,trial}$ values should match within eight significant digits.

5.1 CTL (Table 24) and Relative Density (Table 23) for NGL and LPG using a 60°F Base Temperature

5.1.1 Implementation Procedure for Table 24E (60°F Basis)

This section presents the implementation procedure T24 for the computation of Temperature Correction Factor, C_{TL} . The C_{TL} is used to calculate volumes of fluid at the base temperature from volumes at some known measurement temperature. The fluids are characterized by the specification of relative density at the base temperature, 60°F.

5.1.1.1 Inputs and Outputs

Inputs: Relative density at 60°F, γ_{60}
 Observed temperature, T_F (°F)

Output: Temperature Correction Factor, C_{TL} (from T_F to T_B)

5.1.1.2 Outline of Calculations

The calculations are performed using an extended two-fluid corresponding states equation. By comparing densities at 60°F, two reference fluids are selected so that one is slightly more dense

and one is slightly less dense than the observed fluid. The densities of these reference fluids are then scaled to the observed reduced temperature (reduced by the critical temperature of the fluid of interest). The Temperature Correction Factor is then computed from the reference fluid densities. See Figure 1 for a general flow chart of the calculation procedure.

5.1.1.3 T24 Implementation Procedure

<u>T24/Step Number</u>	<u>Operation/Procedure at that step</u>
------------------------	---

T24/1: Round the relative density γ_{60} to the nearest 0.0001 and round the observed temperature T_F to the nearest 0.1°F.

Temperature rounding examples: -0.05 rounds to -0.1; -0.049 rounds to 0.0, -0.051 rounds to -0.1. Density rounding examples follow: 0.35555 rounds to 0.3556, [0.355549 rounds to 0.3555](#), 0.40289 rounds to 0.4029.

T24/2: Convert the rounded observed temperature to units of Kelvin, T_x :

$$T_x = \frac{T_F + 459.67}{1.8}$$

T24/3: The resultant temperature T_x and relative density γ_{60} must fall within the following [boundaries/ranges](#):

Temperature between 227.15 and 366.15 K, inclusive (equivalent to -46 to 93°C, or -50.8 to 199.4°F)

Relative density between 0.3500 and 0.6880, inclusive

If these values do not fall in these ranges, then the standard does not apply. Flag this result (possibly by returning a -1 for C_{TL}) and exit this procedure.

T24/4: Determine the two adjacent reference fluids to be used for the calculations. The rounded 60°F relative density γ_{60} will fit between two reference fluids' 60°F relative densities as listed in [Table 1](#)/[Table 2](#). Choose the lowest density reference fluid that has a density value greater than or equal to γ_{60} and refer to this fluid using the subscript "2." Also use the next lowest density reference fluid and refer to this fluid using the subscript "1."

T24/5: Using [Table 1](#)/[Table 2](#), 60°F relative densities, compute the interpolation variable, δ :

$$\delta = \frac{\gamma_{60} - \gamma_{60,1}}{\gamma_{60,2} - \gamma_{60,1}}$$

T24/6: From [Table 4](#)[Table 2](#) critical temperatures, calculate the fluid critical temperature, T_c :

$$T_c = T_{c,1} + \delta(T_{c,2} - T_{c,1})$$

T24/7: Compute the fluid's reduced observed temperature, $T_{r,x}$:

$$T_{r,x} = \frac{T_x}{T_c}$$

If the reduced temperature $T_{r,x}$ is greater than 1.0, then the fluid is at supercritical conditions and cannot exist as a liquid. Flag this result (possibly by returning a -1 for C_{TL}) and exit this procedure.

T24/8: Compute the reduced temperature at 60°F, $T_{r,60}$:

$$T_{r,60} = \frac{519.67}{1.8T_c}$$

T24/9: From [Table 4](#)[Table 2](#) critical compressibility factors, Z_c , and critical densities, ρ_c , calculate the scaling factor, h_2 :

$$h_2 = \frac{Z_{c,1} \times \rho_{c,1}}{Z_{c,2} \times \rho_{c,2}}$$

T24/10: Calculate the saturation density for both reference fluids at 60°F using the 60° reduced temperature, $T_{r,60}$. For each fluid, the equations to calculate the saturation density at any reduced temperature T_r are:

$$\tau = 1 - T_r$$

$$\rho^{sat} = \rho_c \left(1 + \frac{(k_1 \times \tau^{0.35}) + (k_3 \times \tau^2) + (k_4 \times \tau^3)}{1 + (k_2 \times \tau^{0.65})} \right)$$

where the k_1 , k_2 , k_3 , and k_4 parameters are different for each reference fluid and are listed in [Table 4](#)[Table 2](#). Refer to the calculated density for the first reference fluid as $\rho_{60,1}^{sat}$ and for the second reference fluid as $\rho_{60,2}^{sat}$.

T24/11: Calculate the interpolating factor X :

$$X = \frac{\rho_{60,1}^{\text{sat}}}{1 + \delta \left[\left(\frac{\rho_{60,1}^{\text{sat}}}{h_2 \times \rho_{60,2}^{\text{sat}}} \right) - 1 \right]}$$

T24/12: Obtain the saturation density for both reference fluids at reduced observed temperature $T_{r,x}$ using the procedure in Step T24/10. Refer to the calculated density for the first reference fluid as $\rho_{x,1}^{\text{sat}}$ and that for the second reference fluid as $\rho_{x,2}^{\text{sat}}$.

T24/13: Calculate the Temperature Correction Factor at the observed temperature, C_{TL} :

$$C_{TL} = \frac{\rho_{x,1}^{\text{sat}}}{X \left[1 + \delta \left(\frac{\rho_{x,1}^{\text{sat}}}{h_2 \times \rho_{x,2}^{\text{sat}}} - 1 \right) \right]}$$

T24/14: Round the Temperature Correction Factor C_{TL} to the nearest 0.00001. Exit this procedure.

Table 1**Table 2:** Reference Fluid Parameters

No.	Fluid Name	γ_{60}	T_c	Z_c	ρ_c	k_1	k_2	k_3	k_4
1	EE (68/32) ⁽¹⁾	0.325022	298.11	0.27998	6.250	2.54616855327	-0.058244177754	0.803398090807	-0.745720314137
2	Ethane	0.355994	305.33	0.28220	6.870	1.89113042610	-0.370305782347	-0.544867288720	0.337876634952
3	EP (65/35) ⁽²⁾	0.429277	333.67	0.28060	5.615	2.20970078464	-0.294253708172	-0.405754420098	0.319443433421
4	EP (35/65) ⁽³⁾	0.470381	352.46	0.27930	5.110	2.25341981320	-0.266542138024	-0.372756711655	0.384734185665
5	Propane	0.507025	369.78	0.27626	5.000	1.96568366933	-0.327662435541	-0.417979702538	0.303271602831
6	i-Butane	0.562827	407.85	0.28326	3.860	2.04748034410	-0.289734363425	-0.330345036434	0.291757103132
7	n-Butane	0.584127	425.16	0.27536	3.920	2.03734743118	-0.299059145695	-0.418883095671	0.380367738748
8	i-Pentane	0.624285	460.44	0.27026	3.247	2.06541640707	-0.238366208840	-0.161440492247	0.258681568613
9	n-Pentane	0.631054	469.65	0.27235	3.200	2.11263474494	-0.261269413560	-0.291923445075	0.308344290017
10	i-Hexane	0.657167	498.05	0.26706	2.727	2.02382197871	-0.423550090067	-1.152810982570	0.950139001678
11	n-Hexane	0.664064	507.35	0.26762	2.704	2.17134547773	-0.232997313405	-0.267019794036	0.378629524102
12	n-Heptane	0.688039	540.15	0.26312	2.315	2.19773533433	-0.275056764147	-0.447144095029	0.493770995799

Table Notes:

γ_{60} is the fluid relative density at 60°F and saturation pressure

T_c is the fluid critical temperature in Kelvin

Z_c is the fluid critical compressibility factor

ρ_c is the fluid critical density in gram-moles per liter

k_1 , k_2 , k_3 , and k_4 are saturation density fitting parameters

(1) EE (68/32) denotes a 68 mole % ethane + 32 % ethylene mixture

(2) EP (65/35) denotes a 65 mole % ethane + 35 % propane mixture

(3) EP (35/65) denotes a 35 mole % ethane + 65 % propane mixture



DRAFT

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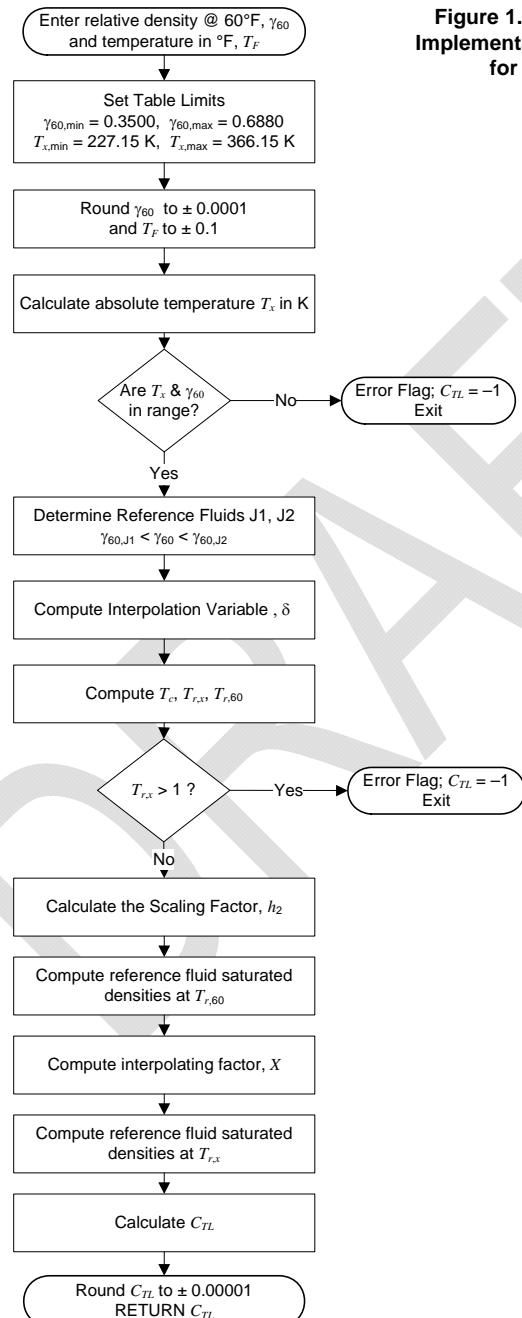


Figure 1. Flow Chart of Implementation Procedure for Table 24

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5.1.1.4 Examples for Section 5.1.1 (Table 24E)

(See [Table 1](#)[Table 2](#) for properties of the Reference Fluids)

Example 24/1 – Utilize EE (68/32) and Ethane

Input Data
 γ_{60} RD60 @ 60°F Relative density @ 60°F RD60 0.350130
 Observed temperature, T_{obs} 48.0200
 Computed Data – last digit is rounded
 T24/1
 Input Data – rounded
 γ_{60} RD60, rounded to 0.0001 0.3501
 T_{obs} , rounded to 0.1 48.0
 T24/2
 T_{ref} , Kelvin 228.705555555556
 T24/3
 Input data within range
 T24/4
 Reference Fluid 1 EE (68/32)
 Reference Fluid 2 Ethane
 T24/5
 Delta (δ) 0.809699083043
 T24/6
 Critical temperature (T_c) 303.956027379569
 T24/7
 Reduced observed temp. (T_{ref}) 0.752429742971
 T24/8
 Reduced temp. at 60°F ($T_{ref,60}$) 0.949826716859
 T24/9
 Scaling factor (λ) 0.902595741301
 T24/10
 Tau for fluid at 60°F (τ) 0.050173283141
 Sat den fluid 1 at 60°F ($\rho_{60,1}^{sat}$) 11.892882208216
 Sat den fluid 2 at 60°F ($\rho_{60,2}^{sat}$) 11.673968376914
 T24/11
 Interpolating factor (χ) 10.770572039296
 T24/12
 Tau for fluid at obs. temp. (τ_{obs}) 0.247570257029

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Sat den fluid 1 at obs. temp. $(\rho_{x,1}^{sat})$ 16.490243357324

Sat den fluid 2 at obs. temp. $(\rho_{x,2}^{sat})$ 16.012272020935

T24/13
 C_{TL} 1.374174158511

T24/14
CTL rounded C_{TL} (rounded) 1.37417

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Example 24/2 – Utilize Use Ethane and EP (65/35)

Input Data

Relative density @ 60°F (γ_{60}) Relative density @ 60°F RD60 0.399950
 Observed temperature, °F (T_F) Observed temperature T_F , °F 24.9500

Computed Data – last digit is rounded
T24/1

Input Data – rounded

γ_{60} rounded to 0.0001 RD60, rounded to 0.0001 0.4000
 T_F rounded to 0.1 T_F , °F, rounded to 0.1 25.0
T24/2

T_x , Kelvin T_x , Kelvin 269.261111111111

T24/3
Input data within range
T24/4

Reference Fluid 1 Ethane
Reference Fluid 2 Reference Fluid 2 EP (65/35)
T24/5

Delta (δ) Delta 0.600493975410

T24/6
Critical temperature (T_c) Critical temperature T_c 322.347999263131

T24/7
Reduced observed temp. ($T_{r,x}$) Reduced observed temp. $T_{r,x}$ 0.835311873276

T24/8
Reduced temp. at 60°F ($T_{r,60}$) Reduced temp. at 60°F $T_{r,60}$ 0.895633154899

T24/9
Scaling factor (h_1) Scaling factor h_1 1.230484986694

T24/10
Tau for fluid at 60°F (τ) Tau for fluid at 60°F 0.104366845101

Sat den fluid 1 at 60°F ($\rho_{60,1}^{sat}$) Sat den fluid 1 at 60°F 13.268022876946

Sat den fluid 2 at 60°F ($\rho_{60,2}^{sat}$) Sat den fluid 2 at 60°F 11.625034524899

T24/11
Interpolating factor (X) Interpolating factor X 13.871545440974

T24/12

Tau for fluid at obs. temp. (τ_x) Tau for fluid at obs. temp.
0.164688126724

Sat den fluid 1 at obs. temp. ($\rho_{x,1}^{sat}$) Sat den fluid 1 at obs. temp.
14. 572475327916

Sat den fluid 2 at obs. temp. ($\rho_{x,2}^{sat}$) Sat den fluid 2 at obs. temp.
12. 816926793350

T24/13
 C_{TL} CTL

T24/14
CTL rounded C_{TL} (rounded) 1. 10076

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Example 24/3 – Utilize Use EP (65/35) and EP (35/65)

Input Data

Relative density @ 60°F (γ_{60}) Relative density @ 60°F RD60 0.451530
Observed temperature, °F (T_f) Observed temperature Tf, °F 87.4200

Computed Data – last digit is rounded
T24/1

Input Data – rounded

γ_{60} rounded to 0.0001 RD60, rounded to 0.0001 0.451515
 T_f rounded to 0.1 Tf, °F, rounded to 0.1 87.4

T24/2

T_x , Kelvin T_x , Kelvin
303.92777777778

T24/3

Input data within range

T24/4

Reference Fluid 1 Reference Fluid 1
Reference Fluid 2 Reference Fluid 2

T24/5

Delta (δ) Delta
0.540652977812

T24/6

Critical temperature (T_c) Critical temperature Tc
343.828869453095

T24/7

Reduced observed temp. ($T_{r,x}$) Reduced observed temp. Tr, x
0.883950723106

T24/8

Reduced temp. at 60°F ($T_{r,60}$) Reduced temp. at 60°F Tr, 60
0.839678052674

T24/9

Scaling factor (h_1) Scaling factor h2
1.103940309258

T24/10

Tau for fluid at 60°F (τ) Tau for fluid at 60°F
0.160321947326

Sat den fluid 1 at 60°F ($\rho_{60,1}^{sat}$) Sat den fluid 1 at 60°F
12.739470807395

Sat den fluid 2 at 60°F ($\rho_{60,2}^{sat}$) Sat den fluid 2 at 60°F
11.668538966703

T24/11

Interpolating factor (X) Interpolating factor X
12.815798776833

T24/12

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<u>Tau for fluid at obs. temp. (τ_x)</u>	<u>Tau for fluid at obs. temp.</u>
0.116049276894	
<u>Sat den fluid 1 at obs. temp. ($\rho_{x,1}^{sat}$)</u>	<u>Sat den fluid 1 at obs. temp.</u>
11.880371290411	
<u>Sat den fluid 2 at obs. temp. ($\rho_{x,2}^{sat}$)</u>	<u>Sat den fluid 2 at obs. temp.</u>
10.885682581443	
T24/13	
<u>C_{TL}</u>	<u>CTL</u>
0.932749411288	
T24/14	
<u>CTL rounded</u>	<u>C_{TL} (rounded)</u>
	0.93275

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Example 24/4 – Utilize Use EP (35/65) and Propane

Input Data

Relative density @ 60°F (γ_{60}) Relative density @ 60°F RD60 0.490400
Observed temperature, °F (T_F) Observed temperature T_F , °F 184.9700

Computed Data – last digit is rounded
T24/1

Input Data – rounded

γ_{60} rounded to 0.0001 RD60, rounded to 0.0001 0.4904
 T_F rounded to 0.1 T_F , °F, rounded to 0.1 185.0
T24/2

T_x , Kelvin T_x , Kelvin 358.150000000000

T24/3
Input data within range
T24/4

Reference Fluid 1 Reference Fluid 1
Reference Fluid 2 Reference Fluid 2
T24/5

Delta (δ) Delta
0.546310446458

T24/6
Critical temperature (T_c) Critical temperature T_c
361.922096932649

T24/7
Reduced observed temp. ($T_{r,x}$) Reduced observed temp. $T_{r,x}$
0.989577599808

T24/8
Reduced temp. at 60°F ($T_{r,60}$) Reduced temp. at 60°F $T_{r,60}$
0.797700825682

T24/9
Scaling factor (h_2) Scaling factor h_2
1.033246217331

T24/10
Tau for fluid at 60°F (τ) Tau for fluid at 60°F
0.202299174318

Sat den fluid 1 at 60°F ($\rho_{60,1}^{sat}$) Sat den fluid 1 at 60°F
12.309519597134

Sat den fluid 2 at 60°F ($\rho_{60,2}^{sat}$) Sat den fluid 2 at 60°F
11.272394278161

T24/11
Interpolating factor (X) Interpolating factor X
11.938610116810

T24/12

<u>Tau for fluid at obs. temp. (τ_x)</u>	<u>Tau for fluid at obs. temp.</u>
0.010422400192	
<u>Sat den fluid 1 at obs. temp. ($\rho_{x,1}^{sat}$)</u>	<u>Sat den fluid 1 at obs. temp.</u>
7.473276954765	
<u>Sat den fluid 2 at obs. temp. ($\rho_{x,2}^{sat}$)</u>	<u>Sat den fluid 2 at obs. temp.</u>
7.023541210265	
T24/13	
<u>C_{TL}</u>	<u>CTL</u>
0.615949186930	
T24/14	
<u>CTL rounded</u>	<u>C_{TL} (rounded)</u>
	0.61595

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Example 24/5 – Utilize Use Propane and i-Butane

Input Data

Relative density @ 60°F (γ_{60}) Relative density @ 60°F RD60 0.540020
Observed temperature, °F (T_F) Observed temperature T_F , °F 155.0400

Computed Data – last digit is rounded
T24/1

Input Data – rounded

γ_{60} rounded to 0.0001 RD60, rounded to 0.0001 0.5400
 T_F rounded to 0.1 T_F , °F, rounded to 0.1 155.0
T24/2

T_x , Kelvin T_x , Kelvin
341.483333333333

T24/3
Input data within range
T24/4

Reference Fluid 1 Reference Fluid 1
Reference Fluid 2 Reference Fluid 2
T24/5

Delta (δ) Delta
0.590928640551

T24/6
Critical temperature (T_c) Critical temperature T_c
392.276653345758

T24/7
Reduced observed temp. ($T_{r,x}$) Reduced observed temp. $T_{r,x}$
0.870516586753

T24/8
Reduced temp. at 60°F ($T_{r,60}$) Reduced temp. at 60°F $T_{r,60}$
0.735974351502

T24/9
Scaling factor (h_2) Scaling factor h_2
1.263326064155

T24/10
Tau for fluid at 60°F (τ) Tau for fluid at 60°F
0.264025648498

Sat den fluid 1 at 60°F ($\rho_{60,1}^{sat}$) Sat den fluid 1 at 60°F
12.016437691588

Sat den fluid 2 at 60°F ($\rho_{60,2}^{sat}$) Sat den fluid 2 at 60°F
9.429772887863

T24/11
Interpolating factor (X) Interpolating factor X
11.955024717591

T24/12

<u>Tau for fluid at obs. temp. (τ_x)</u>	<u>Tau for fluid at obs. temp.</u>
0.129483413247	
<u>Sat den fluid 1 at obs. temp. ($\rho_{x,1}^{sat}$)</u>	<u>Sat den fluid 1 at obs. temp.</u>
10.227566043346	
<u>Sat den fluid 2 at obs. temp. ($\rho_{x,2}^{sat}$)</u>	<u>Sat den fluid 2 at obs. temp.</u>
8.025028872910	
T24/13	
<u>C_{TL}</u>	<u>CTL</u>
0.851071799690	
T24/14	
<u>CTL rounded</u>	<u>C_{TL} (rounded)</u>
	0.85107

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Example 24/6 – Utilize Use i-Butane and n-Butane

Input Data

Relative density @ 60°F (γ_{60}) Relative density @ 60°F RD60 0.569980
Observed temperature, °F (T_F) Observed temperature T_F , °F 3.0330

Computed Data – last digit is rounded
T24/1

Input Data – rounded

γ_{60} rounded to 0.0001 RD60, rounded to 0.0001 0.5700
 T_F rounded to 0.1 T_F , °F, rounded to 0.1 3.0

T24/2

T_x , Kelvin T_x , Kelvin
257.03888888889

T24/3

Input data within range

T24/4

Reference Fluid 1 Reference Fluid 1
Reference Fluid 2 Reference Fluid 2

T24/5

Delta (δ) Delta
0.336760563380

T24/6

Critical temperature (T_c) Critical temperature T_c
413.679325352113

T24/7

Reduced observed temp. ($T_{r,x}$) Reduced observed temp. $T_{r,x}$
0.621348163025

T24/8

Reduced temp. at 60°F ($T_{r,60}$) Reduced temp. at 60°F $T_{r,60}$
0.697896988954

T24/9

Scaling factor (h_1) Scaling factor h_2
1.01294464538

T24/10

Tau for fluid at 60°F (τ) Tau for fluid at 60°F
0.302103011046

Sat den fluid 1 at 60°F ($\rho_{60,1}^{sat}$) Sat den fluid 1 at 60°F
9.757836502218

Sat den fluid 2 at 60°F ($\rho_{60,2}^{sat}$) Sat den fluid 2 at 60°F
9.883346486657

T24/11

Interpolating factor (X) Interpolating factor X
9.841741258063

T24/12

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<u>Tau for fluid at obs. temp. (τ_x)</u>	<u>Tau for fluid at obs. temp.</u>
0. 378651836975	
<u>Sat den fluid 1 at obs. temp. ($\rho_{x,1}^{sat}$)</u>	<u>Sat den fluid 1 at obs. temp.</u>
10. 367065629858	
<u>Sat den fluid 2 at obs. temp. ($\rho_{x,2}^{sat}$)</u>	<u>Sat den fluid 2 at obs. temp.</u>
10. 496815949474	
T24/13	
<u>C_{TL}</u>	<u>CTL</u>
1. 062314380669	
T24/14	
<u>CTL rounded</u>	<u>C_{TL} (rounded)</u>
	1. 06231

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Example 24/7 – Utilize Use n-Butane and i-Pentane

Input Data

Relative density @ 60°F (γ_{60}) Relative density @ 60°F RD60 0.599970
 Observed temperature, °F (T_F) Observed temperature T_F , °F 110.0400

Computed Data – last digit is rounded
T24/1

Input Data – rounded

γ_{60} rounded to 0.0001 RD60, rounded to 0.0001 0.6000
 T_F rounded to 0.1 T_F , °F, rounded to 0.1 110.0

T24/2

T_x , Kelvin T_x , Kelvin
316.483333333333

T24/3

Input data within range

T24/4

Reference Fluid 1 Reference Fluid 1
 Reference Fluid 2 Reference Fluid 2

T24/5

Delta (δ) Delta
0.395263708352

T24/6

Critical temperature (T_c) Critical temperature T_c
439.104903630659

T24/7

Reduced observed temp. ($T_{r,x}$) Reduced observed temp. $T_{r,x}$
0.720746524843

T24/8

Reduced temp. at 60°F ($T_{r,60}$) Reduced temp. at 60°F $T_{r,60}$
0.657486521258

T24/9

Scaling factor (h_2) Scaling factor h_2
1.230050265162

T24/10

Tau for fluid at 60°F (τ) Tau for fluid at 60°F
0.342513478742

Sat den fluid 1 at 60°F ($\rho_{60,1}^{sat}$) Sat den fluid 1 at 60°F
10.214309417120

Sat den fluid 2 at 60°F ($\rho_{60,2}^{sat}$) Sat den fluid 2 at 60°F
8.446076234558

T24/11

Interpolating factor (X) Interpolating factor X
10.282689503192

T24/12

<u>Tau for fluid at obs. temp. (τ_x)</u>	<u>Tau for fluid at obs. temp.</u>
0.279253475157	
<u>Sat den fluid 1 at obs. temp. ($\rho_{x,1}^{sat}$)</u>	<u>Sat den fluid 1 at obs. temp.</u>
9.687510842155	
<u>Sat den fluid 2 at obs. temp. ($\rho_{x,2}^{sat}$)</u>	<u>Sat den fluid 2 at obs. temp.</u>
8.011335247961	
T24/13	
<u>C_{TL}</u>	<u>CTL</u>
0.948465346003	
T24/14	
<u>CTL rounded</u>	<u>C_{TL} (rounded)</u>
	0.94847

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Example 24/8 – Utilize Use i-Pentane and n-Pentane

Input Data

Relative density @ 60°F (γ_{60}) Relative density @ 60°F RD60 0.625020
Observed temperature, °F (T_F) Observed temperature T_F , °F 169.9700

Computed Data – last digit is rounded
T24/1

Input Data – rounded

γ_{60} RD60, rounded to 0.0001 0.6250
 T_F rounded to 0.1 T_F , °F, rounded to 0.1 170.0

T24/2

T_x , Kelvin T_x , Kelvin 349.81666666667

T24/3

Input data within range
T24/4

Reference Fluid 1 Reference Fluid 1
Reference Fluid 2 Reference Fluid 2

T24/5

Delta (δ) Delta
0.105628600975

T24/6

Critical temperature (T_c) Critical temperature T_c
461.412839414980

T24/7

Reduced observed temp. ($T_{r,x}$) Reduced observed temp. $T_{r,x}$
0.758142463288

T24/8

Reduced temp. at 60°F ($T_{r,60}$) Reduced temp. at 60°F $T_{r,60}$
0.625699007253

T24/9

Scaling factor (h_2) Scaling factor h_2
1.006900839912

T24/10

Tau for fluid at 60°F (τ) Tau for fluid at 60°F
0.374300992747

Sat den fluid 1 at 60°F ($\rho_{60,1}^{sat}$) Sat den fluid 1 at 60°F
8.652500418110

Sat den fluid 2 at 60°F ($\rho_{60,2}^{sat}$) Sat den fluid 2 at 60°F
8.668052899178

T24/11

Interpolating factor (X) Interpolating factor X
8.660400031891

T24/12

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<u>Tau for fluid at obs. temp. (τ_x)</u>	<u>Tau for fluid at obs. temp.</u>
0.241857536712	
<u>Sat den fluid 1 at obs. temp. ($\rho_{x,1}^{sat}$)</u>	<u>Sat den fluid 1 at obs. temp.</u>
7.734059015744	
<u>Sat den fluid 2 at obs. temp. ($\rho_{x,2}^{sat}$)</u>	<u>Sat den fluid 2 at obs. temp.</u>
7.744880148272	
T24/13	
<u>C_{TL}</u>	<u>CTL</u>
0.893815224960	
T24/14	
<u>CTL rounded</u>	<u>C_{TL} (rounded)</u>
	0.89382

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Example 24/9 – Utilize Use n-Pentane and i-Hexane

Input Data

Relative density @ 60°F (γ_{60}) Relative density @ 60°F RD60 0.640040
 Observed temperature, °F (T_F) Observed temperature T_F , °F 12.0200

Computed Data – last digit is rounded
T24/1

Input Data – rounded

γ_{60} rounded to 0.0001 RD60, rounded to 0.0001 0.6400
 T_F rounded to 0.1 T_F , °F, rounded to 0.1 12.0

T24/2

T_x , Kelvin T_x , Kelvin

248.70555555556

T24/3

Input data within range

T24/4

Reference Fluid 1 Reference Fluid 1
 Reference Fluid 2 Reference Fluid 2

T24/5

Delta (δ) Delta
 0.342587982997

T24/6

Critical temperature (T_c) Critical temperature T_c
 479.379498717114

T24/7

Reduced observed temp. ($T_{r,x}$) Reduced observed temp. $T_{r,x}$
 0.518807241906

T24/8

Reduced temp. at 60°F ($T_{r,60}$) Reduced temp. at 60°F $T_{r,60}$
 0.602248440595

T24/9

Scaling factor (h_2) Scaling factor h_2
 1.196694721271

T24/10

Tau for fluid at 60°F (τ) Tau for fluid at 60°F
 0.397751559405

Sat den fluid 1 at 60°F ($\rho_{60,1}^{sat}$) Sat den fluid 1 at 60°F
 8.816158414827

Sat den fluid 2 at 60°F ($\rho_{60,2}^{sat}$) Sat den fluid 2 at 60°F
 7.499847998980

T24/11

Interpolating factor (X) Interpolating factor X
 8.869948165069

T24/12

Tau for fluid at obs. temp. (τ_x) Tau for fluid at obs. temp.
0.481192758094

Sat den fluid 1 at obs. temp. ($\rho_{x,1}^{sat}$) Sat den fluid 1 at obs. temp.
9.321161815695

Sat den fluid 2 at obs. temp. ($\rho_{x,2}^{sat}$) Sat den fluid 2 at obs. temp.
7.929963121410

T24/13
C_L CTL

T24/14
CTL rounded . . . C_L (rounded) 1.05730

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Example 24/10 – Utilize Use i-Hexane and n-Hexane

Input Data

Relative density @ 60°F (γ_{60}) Relative density @ 60°F RD60 0.660033
 Observed temperature, °F (T_F) Observed temperature T_F , °F 177.0450

Computed Data – last digit is rounded
T24/1

Input Data – rounded

γ_{60} rounded to 0.0001 RD60, rounded to 0.0001 0.660000
 T_F rounded to 0.1 T_F , °F, rounded to 0.1 177.0

T24/2

T_x , Kelvin T_x , Kelvin 353.70555555556

T24/3

Input data within range
T24/4

Reference Fluid 1 Reference Fluid 1
 Reference Fluid 2 Reference Fluid 2

T24/5

Delta (δ) Delta
0.410758300710

T24/6

Critical temperature (T_c) Critical temperature T_c
501.870052196607

T24/7

Reduced observed temp. ($T_{r,x}$) Reduced observed temp. $T_{r,x}$
0.704775178370

T24/8

Reduced temp. at 60°F ($T_{r,60}$) Reduced temp. at 60°F $T_{r,60}$
0.575259580228

T24/9

Scaling factor (h_2) Scaling factor h_2
1.006395599121

T24/10

Tau for fluid at 60°F (τ) Tau for fluid at 60°F
0.424740419772

Sat den fluid 1 at 60°F ($\rho_{60,1}^{sat}$) Sat den fluid 1 at 60°F
7.641170665754

Sat den fluid 2 at 60°F ($\rho_{60,2}^{sat}$) Sat den fluid 2 at 60°F
7.665708531720

T24/11

Interpolating factor (X) Interpolating factor X
7.671217510578

T24/12

<u>Tau for fluid at obs. temp. (τ_x)</u>	<u>Tau for fluid at obs. temp.</u>
0.295224821630	
<u>Sat den fluid 1 at obs. temp. ($\rho_{x,1}^{sat}$)</u>	<u>Sat den fluid 1 at obs. temp.</u>
6.925133823039	
<u>Sat den fluid 2 at obs. temp. ($\rho_{x,2}^{sat}$)</u>	<u>Sat den fluid 2 at obs. temp.</u>
6.945363609083	
T24/13	
<u>C_{TL}</u>	<u>CTL</u>
0.906185214223	
T24/14	
<u>CTL rounded</u>	<u>C_{TL} (rounded)</u>
	0.90619

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Example 24/11 – Utilize n-Hexane and n-Heptane

Input Data

Relative density @ 60°F (γ_{60}) Relative density @ 60°F RD60 0.670042
 Observed temperature, °F (T_F) Observed temperature T_F , °F 181.0300

Computed Data – last digit is rounded
T24/1

Input Data – rounded

γ_{60} rounded to 0.0001 RD60, rounded to 0.0001 0.6700
 T_F rounded to 0.1 T_F , °F, rounded to 0.1 181.0
T24/2

T_x , Kelvin T_x , Kelvin 355.92777777778

T24/3
Input data within range
T24/4

Reference Fluid 1 Reference Fluid 1
 Reference Fluid 2 Reference Fluid 2
T24/5

Delta (δ) Delta
0.247591240876

T24/6
Critical temperature (T_c) Critical temperature T_c
515.470992700730

T24/7
Reduced observed temp. ($T_{r,x}$) Reduced observed temp. $T_{r,x}$
0.690490411328

T24/8
Reduced temp. at 60°F ($T_{r,60}$) Reduced temp. at 60°F $T_{r,60}$
0.560081090195

T24/9
Scaling factor (h_1) Scaling factor h_1
1.188010824747

T24/10
Tau for fluid at 60°F (τ) Tau for fluid at 60°F
0.439918909805

Sat den fluid 1 at 60°F ($\rho_{60,1}^{sat}$) Sat den fluid 1 at 60°F
7.744857153990

Sat den fluid 2 at 60°F ($\rho_{60,2}^{sat}$) Sat den fluid 2 at 60°F
6.743069361289

T24/11
Interpolating factor (X) Interpolating factor X
7.809053198722

T24/12

<u>Tau for fluid at obs. temp. (τ_x)</u>	<u>Tau for fluid at obs. temp.</u>
0.309509588672	
<u>Sat den fluid 1 at obs. temp. ($\rho_{x,1}^{sat}$)</u>	<u>Sat den fluid 1 at obs. temp.</u>
7.030188106398	
<u>Sat den fluid 2 at obs. temp. ($\rho_{x,2}^{sat}$)</u>	<u>Sat den fluid 2 at obs. temp.</u>
6.111938115029	
T24/13	
<u>C_{TL}</u>	<u>CTL</u>
0.907404360428	
T24/14	
<u>CTL rounded</u>	<u>C_{TL} (rounded)</u>
	0.90740

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Example 24/12 – Reduced Temperature ($T_{r,x}$) Greater Than 1.0

Input Data

Relative density @ 60°F (γ_{60}) Relative density @ 60°F RD60 0.350180
Observed temperature, °F (T_F) Observed temperature T_F , °F 195.0250

Computed Data – last digit is rounded
T24/1

Input Data – rounded

γ_{60} rounded to 0.0001 RD60, rounded to 0.0001 0.3502
 T_F rounded to 0.1 T_F , °F, rounded to 0.1 195.0

T24/2

T_x , Kelvin T_x , Kelvin
363.70555555556

T24/3

Input data within range

T24/4

Reference Fluid 1 Reference Fluid 1
Reference Fluid 2 Reference Fluid 2

T24/5

Delta (δ) Delta
0.812927805760

T24/6

Critical temperature (T_c) Critical temperature T_c
303.979338757587

T24/7

Reduced observed temp. ($T_{r,x}$) Reduced observed temp. $T_{r,x}$
1.196481172181

Reduced temperature Input data $T_{r,x}$ greater than 1.0, is no solution outside the correlation range of the standard

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Example 24/13 – Observed Temperature (T_f) < Lower Range Limit

Input Data

Relative density @ 60°F (γ_{60}) Relative density @ 60°F RD60 0.500000
Observed temperature, °F (T_f) Observed temperature T_f , °F 50.8500

Computed Data – last digit is rounded

T24/1

Input Data – rounded

γ_{60} rounded to 0.0001 RD60, rounded to 0.0001 0.5000

T_f rounded to 0.1 T_f , °F, rounded to 0.1 -50.9

T24/2

T_x , Kelvin T_x , Kelvin

227.09444444444

T24/3

T_x , °F less than 227.15, is outside the input range of the standard no solution

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Example 24/14 – Relative Density @ 60°F (γ_{60}) RD60 < Lower Range Limit

Input Data

<u>Relative density @ 60°F (γ_{60})</u>	<u>Relative density @ 60°F RD60</u>	0.349940
<u>Observed temperature, °F (T_F)</u>	<u>Observed temperature Tf, °F</u>	40.0000

Computed Data – last digit is rounded

T24/1

Input Data – rounded

<u>γ_{60} rounded to 0.0001</u>	<u>RD60, rounded to 0.0001</u>	0.3499
<u>T_F rounded to 0.1</u>	<u>Tf, °F, rounded to 0.1</u>	40.0

T24/2

<u>T_x, Kelvin</u>	<u>T_x, Kelvin</u>
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277.594444444444

T24/3

γ_{60} RD60 is less than 0.3500, outside the input range of the standard no solution

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Example 24/15 – Observed Temperature (T_F) T_F > Upper Range Limit

Input Data

Relative density @ 60°F (γ_{60}) Relative density @ 60°F RD60 0.450000
Observed temperature, °F (T_F) Observed temperature T_F , °F 199.4600

Computed Data – Last digit is rounded
T24/1

Input Data – rounded

γ_{60} rounded to 0.0001 RD60, rounded to 0.0001 0.4500
 T_F rounded to 0.1 T_F , °F, rounded to 0.1 199.5

T24/2

T_x , Kelvin T_x , Kelvin
366.205555555556

T24/3

T_x , °F greater than 366.15, is outside the input range of the standard no solution

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Example 24/16 – Relative Density @ 60°F (γ_{60}) RD60 > Upper Range Limit

Input Data

<u>Relative density @ 60°F (γ_{60})</u>	<u>Relative density @ 60°F RD60</u>	0.688070
<u>Observed temperature, °F (T_F)</u>	<u>Observed temperature T_F, °F</u>	0.0000

Computed Data – last digit is rounded

T24/1

Input Data – rounded

<u>γ_{60} rounded to 0.0001</u>	<u>RD60, rounded to 0.0001</u>	0.6881
<u>T_F rounded to 0.1</u>	<u>T_F, °F, rounded to 0.1</u>	0.0

T24/2

<u>T_x, Kelvin</u>	<u>T_x, Kelvin</u>
---------------------------------------	---------------------------------------

255.372222222222

T24/3

γ_{60} RD60 is greater than 0.6880, outside the input range of the standard no solution

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Example 24/17 – Observed Temperature (T_f/T_F) and Relative Density @ 60°F (γ_{60}) RD60 = Upper Range Limits

Input Data

Relative density @ 60°F (γ_{60})	Relative density @ 60°F RD60	0.688000
Observed temperature, °F (T_f)	Observed temperature T_f , °F	199.4400
Computed Data – Last digit is rounded		
T24/1		
Input Data – rounded		
γ_{60} rounded to 0.0001	RD60, rounded to 0.0001	0.6880
T_f rounded to 0.1	T_f , °F, rounded to 0.1	199.4
T24/2		
T_x , Kelvin	T_x , Kelvin	
366.1500000000000		
T24/3		
Input data within range		
T24/4		
Reference Fluid 1	Reference Fluid 1	
Reference Fluid 2	Reference Fluid 2	
T24/5		
Delta (δ)	Delta	
0.998373305527		
T24/6		
Critical temperature (T_c)	Critical temperature T_c	
540.096644421272		
T24/7		
Reduced observed temp. ($T_{r,x}$)	Reduced observed temp. $T_{r,x}$	
0.677934224887		
T24/8		
Reduced temp. at 60°F ($T_{r,60}$)	Reduced temp. at 60°F $T_{r,60}$	
0.534544249696		
T24/9		
Scaling factor (h_2)	Scaling factor h_2	
1.188010824747		
T24/10		
Tau for fluid at 60°F (τ)	Tau for fluid at 60°F	
0.465455750304		
Sat den fluid 1 at 60°F ($\rho_{60,1}^{sat}$)	Sat den fluid 1 at 60°F	
7.876480858049		
Sat den fluid 2 at 60°F ($\rho_{60,2}^{sat}$)	Sat den fluid 2 at 60°F	
6.859355371549		
T24/11		
Interpolating factor (X)	Interpolating factor X	
8.148529834765		
T24/12		

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[20]

[21]

TEMPERATURE CORRECTION FOR THE VOLUME OF NGL AND LPG TABLES 23E, 24E, 53E, 54E, 59E, AND 60E

47

Tau for fluid at obs. temp. (τ_x) Tau for fluid at obs. temp.
0.322065775113

Sat den fluid 1 at obs. temp. ($\rho_{x,1}^{sat}$) Sat den fluid 1 at obs. temp.
7.103375621618

Sat den fluid 2 at obs. temp. ($\rho_{x,2}^{sat}$) Sat den fluid 2 at obs. temp.
6.176601533604

T24/13
C_T CTL
0.900466171184

T24/14
CTL rounded . . . C_T (rounded) 0.90047

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Example 24/18 – Observed Temperature (T_F) aTf &nd Relative Density @ 60°F (γ_{60})RD60 = Lower Range Limits

Input Data

Relative density @ 60°F (γ_{60})..... Relative density @ 60°F RD60..... 0.35000
Observed temperature, °F (T_F)..... Observed temperature Tf, °F..... 50.8000

Computed Data – last digit is rounded
T24/1

Input Data – rounded

γ_{60} rounded to 0.0001..... RD60, rounded to 0.0001..... 0.3500
 T_F rounded to 0.1..... T_F , °F, rounded to 0.1..... 50.8

T24/2

 T_x , Kelvin..... T_x , Kelvin.....

227.1500000000000

T24/3

Input data within range

T24/4

Reference Fluid 1..... Reference Fluid 1.....Reference Fluid 2..... Reference Fluid 2.....

T24/5

Delta (δ)..... Delta.....

0.806470360325

T24/6

Critical temperature (T_c)..... Critical temperature T_c
303.932716001550

T24/7

Reduced observed temp. ($T_{r,x}$)..... Reduced observed temp. $T_{r,x}$
0.747369361839

T24/8

Reduced temp. at 60°F ($T_{r,60}$)..... Reduced temp. at 60°F $T_{r,60}$
0.949899567752

T24/9

Scaling factor (h_2)..... Scaling factor h_2
0.902595741301

T24/10

Tau for fluid at 60°F (τ)..... Tau for fluid at 60°F.....
0.050100432248Sat den fluid 1 at 60°F ($\rho_{60,1}^{sat}$)..... Sat den fluid 1 at 60°F.....
11.889940226938Sat den fluid 2 at 60°F ($\rho_{60,2}^{sat}$)..... Sat den fluid 2 at 60°F.....
11.671295077352

T24/11

Interpolating factor (λ)..... Interpolating factor λ
10.772124448866

T24/12

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TEMPERATURE CORRECTION FOR THE VOLUME OF NGL AND LPG TABLES 23E, 24E, 53E, 54E, 59E, AND 60E

49

Tau for fluid at obs. temp. (τ_x) Tau for fluid at obs. temp.
0.252630638161

Sat den fluid 1 at obs. temp. ($\rho_{x,1}^{sat}$) Sat den fluid 1 at obs. temp.
16. 573069193167

Sat den fluid 2 at obs. temp. ($\rho_{x,2}^{sat}$) Sat den fluid 2 at obs. temp.
16. 091771523334

T24/13
 C_{T_L} CTL
1. 381375977418

T24/14
CTL rounded C_{T_L} (rounded)
1. 38138

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5.1.2 Implementation Procedure for Table 23E (60°F Basis)

This section presents the implementation procedure T23 for calculating the relative densities of NGLs and LPGs at [a base condition](#) of 60°F from known temperatures and densities.

In the past, a hydrometer correction option was allowed [so as to be able](#) to correct for the expansion of the glass comprising a hydrometer stem. The hydrometer correction previously took the following form:

Observed densities determined by a glass hydrometer require correction for the effect of temperature on the instrument. Readings from most density meters do not. If the density was determined with a glass hydrometer, then a correction for the expansion or contraction of the glass must be made. Call the rounded observed relative density the uncorrected relative density γ_x^* .

Calculate the corrected relative density, γ_x , from:

$$\gamma_x = [1 - 0.00001278(T_F - 60) - 0.000000062(T_F - 60)^2] \gamma_x^*$$

The value of γ_x was not rounded prior to use^[10].

Density readings must be corrected for the effect of temperature on the instrument prior to entering the density into the following implementation procedure.

5.1.2.1 Inputs and Outputs

Inputs: Relative density at observed temperature, γ_x
 Observed temperature, T_F (°F)

Output: Relative density at 60°F, γ_{60}

5.1.2.2 Outline of Calculations

The calculations are performed using an extended two-fluid corresponding states equation. Two reference fluids are found that are slightly denser and slightly less dense than the observed fluid by comparing their densities at the observed temperature. Iteration must be performed to determine the value of the fluid's relative density at 60°F such that when the Temperature Correction Factor is applied, the observed relative density is obtained. The "guessed" value for the fluid's relative density at 60°F is constrained to lie between the relative densities at 60°F of these two reference fluids (as upper and lower bounds). As the iterations progress, these upper and lower bounds are "brought together" based upon intermediate calculations.

See Figure 2 for a general flow chart of the calculation procedure.

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5.1.2.3 T23 Implementation Procedure

T23/Step Number Operation/Procedure at that step

T23/1: Round the relative density γ_x to the nearest 0.0001 and round the observed temperature T_F to the nearest 0.1°F.

Temperature rounding examples follow: -0.05 rounds to -0.1; -0.049 rounds to 0.0, -0.051 rounds to -0.1. Density rounding examples follow: 0.35555 rounds to 0.3556, [0.355549 rounds to 0.3555](#), 0.40289 rounds to 0.4029.

T23/2: Convert the rounded observed temperature to units of Kelvin, T_x :

$$T_x = \frac{T_F + 459.67}{1.8}$$

T23/3: Check the values of temperature and relative density to ensure that they are in the proper range. The observed temperature T_x and relative density γ_x must fall within the following [boundariesranges](#):

Temperature between 227.15 and 366.15 K, inclusive (equivalent to -46 to 93°C, or -50.8 to 199.4°F)

Relative density between 0.2100 and 0.7400 inclusive.

If these values do not fall in these ranges, then the standard does not apply. Flag this result (possibly by returning a -1 for γ_{60}) and exit this procedure.

T23/4: Reference fluids must be chosen to perform the density calculations. As written here, this is done in two separate steps: T23/4 to compute the density for each reference fluid at the observed temperature and T23/5 to determine which two reference fluids are to be used. However, Steps 4 and 5 could be combined into a single step (e.g., using a binary search technique).

The reference fluids' densities are to be calculated at the observed temperature, T_x . Use the reference fluids' parameter values from [Table 4](#)[Table 2](#). First, use each reference fluid's critical temperature, $T_{c,ref}$, to compute its reduced observed temperature, $T_{r,x}$:

$$T_{r,x} = \frac{T_x}{T_{c,ref}}$$

If $T_{r,x} \leq 1$, calculate the saturation density for this reference fluid at this reduced temperature $T_{r,x}$. Use the procedure as described in Section 5.1.1.3 Step T24/10. Refer to this calculated density for the reference fluid as $\rho_{x,ref}^{sat}$. Repeat this for 60°F using the reduced temperature $T_{r,60}$:

$$T_{r,60} = \frac{519.67}{1.8T_{c,ref}}$$

Refer to this calculated density as $\rho_{60,ref}^{sat}$. Finally, calculate its relative density at the observation temperature, $\gamma_{x,ref}$, as:

$$\gamma_{x,ref} = \gamma_{60,ref} \left(\frac{\rho_{x,ref}^{sat}}{\rho_{60,ref}^{sat}} \right)$$

where $\gamma_{60,ref}$ is the reference fluid's relative density at 60°F

If $T_{r,x} > 1$, this reference fluid will not be a liquid at this observed temperature and no value of $\gamma_{x,ref}$ can be calculated. It is suggested that this type of “no value” case be flagged by returning a—any negative value for $\gamma_{x,ref}$, such as the additive inverse of $\gamma_{60,ref}$ (by multiplying $\gamma_{60,ref}$ by -1).

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- | T23/5: Determine the two adjacent reference fluids to be used for the calculations. Choose the lowest density reference fluid that has a density value greater than γ_x and refer to this fluid using the subscript “2”. AlsoAlso, use the next lowest density reference fluid and refer to this fluid using the subscript “1” (even though this reference fluid may not exist as a liquid at the observation temperature). If γ_x is below that for “EE 68/32” (the least dense reference fluid), then set “EE 68/32” as fluid “1” and “ethane” as fluid “2”. If γ_x is above that for “n-heptane” (the most dense reference fluid), then set “n-hexane” as fluid “1” and “n-heptane” as fluid “2”.
- | T23/6: Initialize the boundaries on the iteration for the observed fluid’s 60°F relative density. For most cases, the observed fluid’s 60°F relative density should be between the two reference fluids “1” and “2”, $\gamma_{60,1}$ and $\gamma_{60,2}$.

Initialize the upper boundary for the observed fluid’s 60°F relative density, $\gamma_{60,high}$, as:

$$\gamma_{60,high} = \gamma_{60,2}$$

and the corresponding relative density at the observed temperature, $\gamma_{x,high}$, as:

$$\gamma_{x,high} = \gamma_{x,2}$$

However, if the relative density γ_x is greater than the reference fluid “2” relative density at the observed temperature $\gamma_{x,2}$, then no answer exists. If this is the case, then $\gamma_{x,60}$ should be flagged (perhaps by being set to -1) and exit this procedure.

Initialize the lower boundary for the observed fluid’s 60°F relative density, $\gamma_{60,low}$, as:

$$\gamma_{60,low} = \gamma_{60,1}$$

and the corresponding relative density at the observed temperature, $\gamma_{x,low}$, as:

$$\gamma_{x,low} = \gamma_{x,1}$$

However, if reference fluid “1” is not a liquid at the observed temperature (i.e., $T_{r,x} > 1$ for the reference fluid), then set the lower boundary convergence 60°F relative density by the following equation:

$$\gamma_{60,low} = \left[\frac{T_x - T_{c,1}}{T_{c,2} - T_{c,1}} \right] (\gamma_{60,2} - \gamma_{60,1}) + \gamma_{60,1}$$

Note that this equation was derived from equations in Section 5.1 at a reduced temperature of 1.0.

If $\gamma_{60,low}$ is less than 0.3500, then set it equal to 0.3500.

If $\gamma_{60,low}$ has been reset using the preceding technique then recalculate the corresponding $\gamma_{x,low}$ value. Use the procedure in Section 5.1.1.3 Steps T24/4 through T24/13 to calculate its Temperature Correction Factor, CTL. Skip Step 24/14 to avoid rounding the output CTL. The relative density at the observed temperature will be:

$$\gamma_{x,low} = C_{TL} \times \gamma_{60,low}$$

At this point, upper and lower convergence boundaries have been set. After one more check, the iterative process to determine a 60°F relative density γ_{60} can begin. If the observed relative density γ_x is less than the lower limit $\gamma_{x,low}$, then no answer exists. If this is the case, then γ_{60} should be flagged (perhaps by being set to -1) and exit this procedure.

- T23/7: Calculate an intermediate 60°F relative density value, $\gamma_{60,mid}$. If a value for $\gamma_{60,low}$ exists, then calculate $\gamma_{60,mid}$ from:

$$\delta = \frac{\gamma_x - \gamma_{x,low}}{\gamma_{x,high} - \gamma_{x,low}}$$

If δ is less than 0.001 then set it equal to 0.001; if δ is greater than 0.999 then set it equal to 0.999. Calculate the intermediate 60°F relative density value:

$$\gamma_{60,mid} = \gamma_{60,low} + \delta (\gamma_{60,high} - \gamma_{60,low})$$

However, if a value for $\gamma_{x,low}$ does not exist, then calculate $\gamma_{60,mid}$ from:

$$\gamma_{60,mid} = \frac{\gamma_{60,high} + \gamma_{60,low}}{2}$$

Calculate the Temperature Correction Factor, C_{TL} , using this value of $\gamma_{60,mid}$ and T_x , unrounded, and the procedure from Section 5.1.1.3 Steps T24/5 to T24/13. (Do not round this C_{TL} value.) The relative density, $\gamma_{x,mid}$, at observed temperature, T_x , will be:

$$\gamma_{x,mid} = C_{TL} \times \gamma_{60,mid}$$

T23/8: Check for convergence of the 60°F relative density. The calculations will be considered converged if either occurs:

- If γ_x is between $\gamma_{x,low}$ and $\gamma_{x,mid}$ and the difference between $\gamma_{60,low}$ and $\gamma_{60,mid}$ is less than 0.00000001 (10^{-8}).
- If γ_x is between $\gamma_{x,high}$ and $\gamma_{x,mid}$ and the difference between $\gamma_{60,high}$ and $\gamma_{60,mid}$ is less than 0.00000001 (10^{-8}).

If convergence has been achieved, set:

$$\gamma_{60} = \gamma_{60,mid}$$

and skip to Step T23/12.

T23/9: There are three pairs of relative density values: $(\gamma_{x,low}, \gamma_{60,low})$, $(\gamma_{x,mid}, \gamma_{60,mid})$ and $(\gamma_{x,high}, \gamma_{60,high})$. A quadratic equation can be fit through these three points. This quadratic equation should be a good approximation to the actual relationship between γ_x and γ_{60} . Using the value of the observed relative density γ_x in the quadratic equation should give a very good estimate to γ_{60} .

Calculate the parameters for the quadratic equation by:

$$\alpha = (\gamma_{60,high} - \gamma_{60,low})$$

$$\beta = \gamma_{x,high}^2 - \gamma_{x,low}^2$$

$$\phi = \frac{\gamma_{x,high} - \gamma_{x,low}}{\gamma_{x,mid} - \gamma_{x,low}}$$

$$A = \frac{\alpha - \phi(\gamma_{60,mid} - \gamma_{60,low})}{\beta - \phi(\gamma_{x,mid}^2 - \gamma_{x,low}^2)}$$

$$B = \frac{\alpha - A\beta}{\gamma_{x,high} - \gamma_{x,low}}$$

$$C = \gamma_{60,low} - B\gamma_{x,low} - A\gamma_{x,low}^2$$

Using these values of A , B , and C , calculate the associated value $\gamma_{60,trial}$ using:

$$\gamma_{60,trial} = A\gamma_x^2 + B\gamma_x + C$$

This value of $\gamma_{60,trial}$ may have to be adjusted if it goes outside of the range of $\gamma_{60,low}$ or $\gamma_{60,high}$. If $\gamma_{60,trial} < \gamma_{60,low}$, then reset the value as:

$$\gamma_{60,trial} = \gamma_{60,low} + \frac{(\gamma_{60,mid} - \gamma_{60,low})(\gamma_x - \gamma_{x,low})}{(\gamma_{x,mid} - \gamma_{x,low})}$$

If $\gamma_{60,trial} > \gamma_{60,high}$ then reset the value as:

$$\gamma_{60,trial} = \gamma_{60,mid} + \frac{(\gamma_{60,high} - \gamma_{60,mid})(\gamma_x - \gamma_{x,mid})}{(\gamma_{x,high} - \gamma_{x,mid})}$$

Finally, calculate the Temperature Correction Factor, C_{TL} , using the value of $\gamma_{60,trial}$ and the procedure from Section 5.1.1.3 Steps T24/4 to T24/13. Skip Step 24/14 to avoid rounding the output C_{TL} . The relative density at observed temperature, $\gamma_{x,trial}$, will be:

$$\gamma_{x,trial} = C_{TL} \times \gamma_{60,trial}$$

T23/10: Check for convergence of the 60°F relative density. The calculations will be considered converged if the absolute difference between $\gamma_{x,trial}$ and γ_x is less than $0.00000001 (10^{-8})$. If converged, set:

$$\gamma_{60} = \gamma_{60,trial}$$

and skip to Step T23/12.

T23/11: The calculation has not yet converged, so the iteration bound~~aries~~ must be updated.

If $\gamma_{x,trial} > \gamma_x$ then reset the upper boundary~~aries~~ to:

$$\gamma_{x,high} = \gamma_{x,trial}$$

$$\gamma_{60,high} = \gamma_{60,trial}$$

DRAFT

Also, if $\gamma_{x,mid} < \gamma_x$ then reset the lower boundaries to:

$$\gamma_{x,low} = \gamma_{x,mid}$$

$$\gamma_{60,low} = \gamma_{60,mid}$$

Or if $\gamma_{x,trial} < \gamma_x$ then reset the lower boundaries to:

$$\gamma_{x,low} = \gamma_{x,trial}$$

$$\gamma_{60,low} = \gamma_{60,trial}$$

Also, if $\gamma_{x,mid} > \gamma_x$ then reset the upper boundaries to:

$$\gamma_{x,high} = \gamma_{x,mid}$$

$$\gamma_{60,high} = \gamma_{60,mid}$$

Return to Step T23/7 and continue iterations. Do at most 10 iterations. If 10 iterations are reached, then no solution can be found. Flag this result (possibly by returning a -1 for γ_{60}) and exit this procedure.

Note: At this time, all known cases have been found to require less than 10 iterations.

- T23/12: Round the 60°F relative density value γ_{60} to the nearest 0.0001. If the value is less than 0.3500 or greater than 0.6880, then the result is outside the scope of this standard. Flag result (possibly by returning a -1 for γ_{60}). Exit this procedure.

Comment [KF1]: Update Figure Number for addition of Figure 1

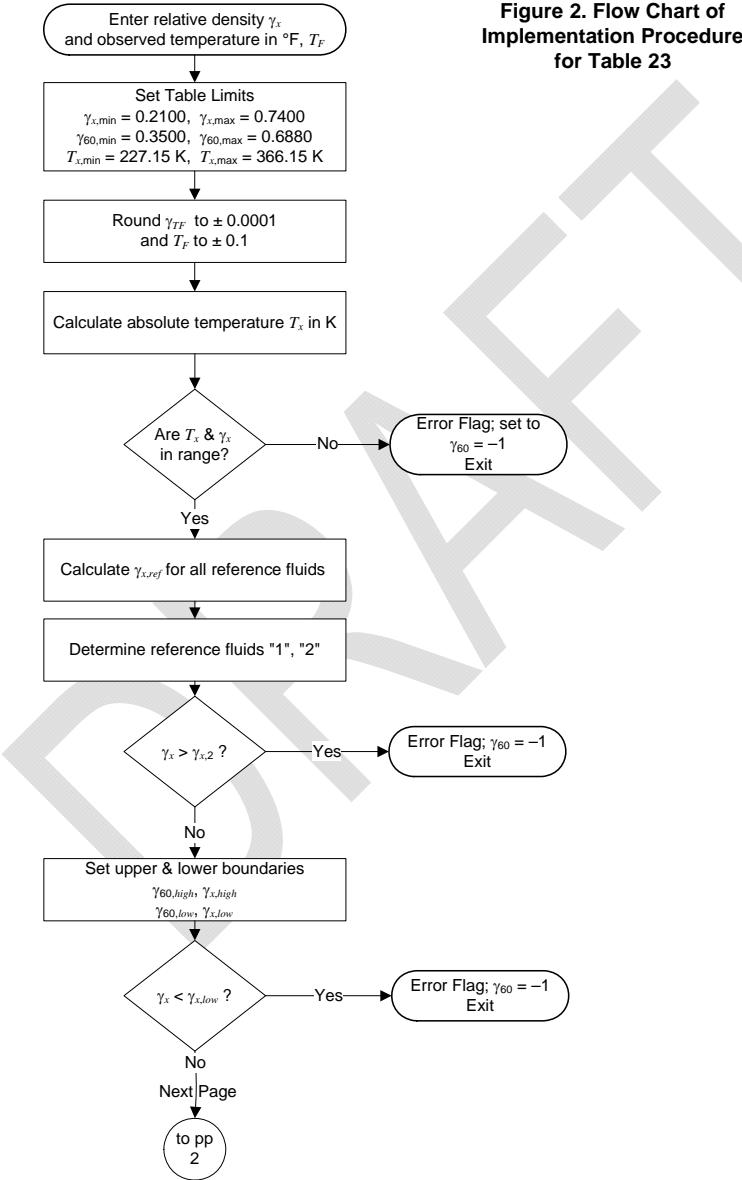
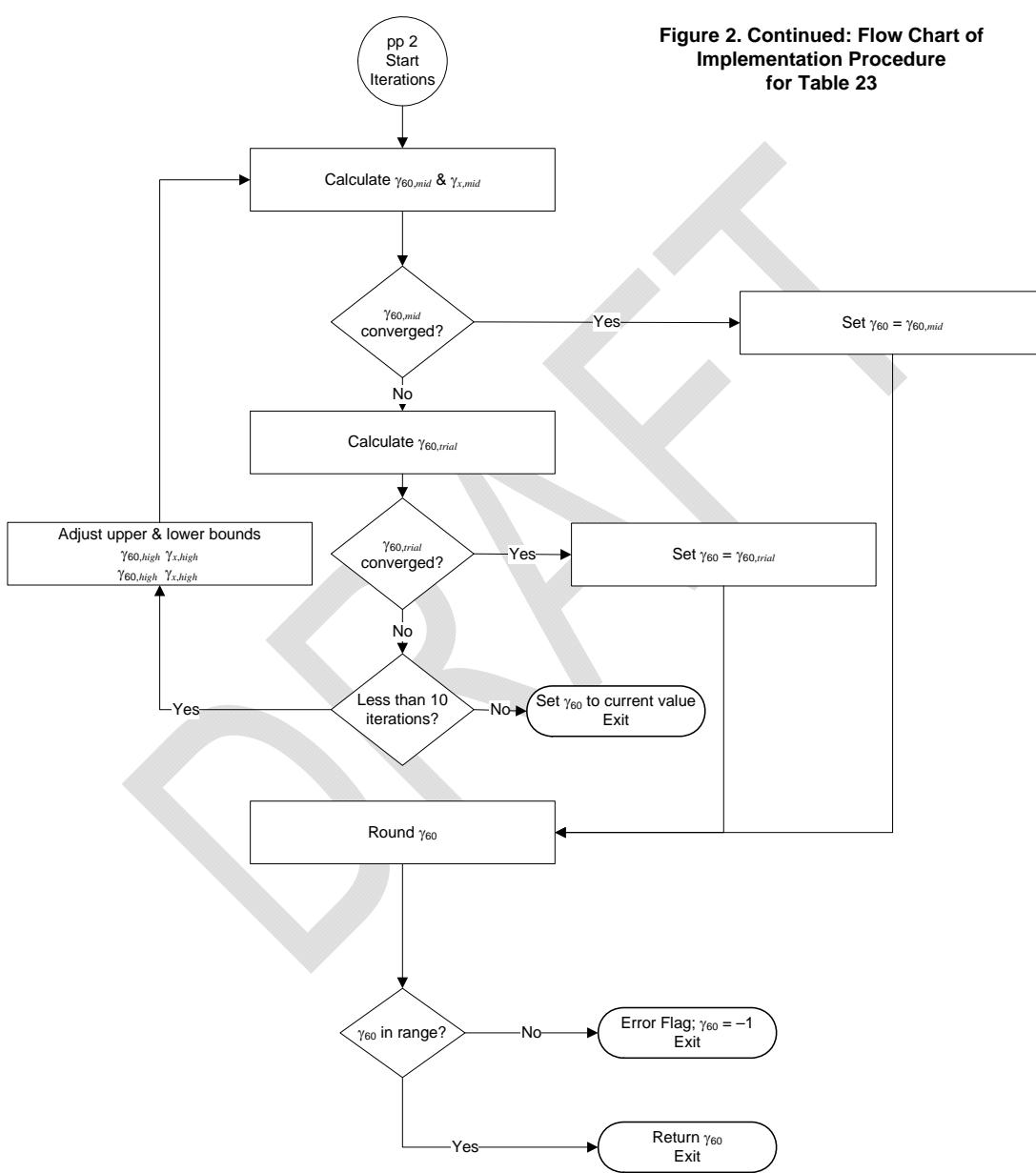


Figure 2. Flow Chart of Implementation Procedure for Table 23

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Figure 2. Continued: Flow Chart of Implementation Procedure for Table 23



Comment [KF2]: Update Figure Number for addition of Figure 1

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5.1.2.4 Examples for Section 5.1.2 (Table 23E)

(See [Table 1](#)[Table 2](#) for properties of the Reference Fluids)

Example 23/1 – Utilize Use i-Pentane and n-Pentane

```

Input Data
Relative density @ obs. temp. ( $\gamma_{20}$ ) ... Relative density @ obs. temp. ... 0.67432
Observed temperature, °F ( $T_o$ ) ... Observed temperature, °F ( $T_f$ ) ... 23.33
Computed Data - last digit is rounded
T23/1
Input Data - rounded
RDTF observed rel. density ... 0.6743
TTF, °F ... 23.3
T23/2
Tfx, Kel vi n ... 242.42777777778
T23/3
RDTF and Tf are within range, continue, and Tf are within range, continue
T23/4
RDTF for Fluid 1 ... 0.668992076725
RDTF w/ for Fluid 2 ... 0.674300900334
T23/5
Reference Fluid 1 ..... Reference Fluid 1 ..... i -Pentane
Reference Fluid 2 ..... n -Pentane
Reference Fluid 2 ..... n -Pentane
Tfx, Tf - for Fluid 1 ... 0.526513286808
Tfx, Tf - for Fluid 2 ... 0.516188177958
TTF_60 for Fluid 1 ... 0.627021013716
TTF_60 for Fluid 2 ... 0.614724913352
T23/6
Upper boundary  $\gamma_{60,high}$  ... 0.631054000000
Upper boundary  $\gamma_{60,high}$  ... 0.674300900334
Lower boundary  $\gamma_{60,low}$  ... 0.624285000000
Lower boundary  $\gamma_{60,low}$  ... 0.668992076725
Iteration steps
T23/7
Delta ( $\Delta$ ) Delta ... Pass 1
0.999000000000
T23/8
RDTF (m) ... 0.631047231000
C1G1T1 ... 1.068534241176
RDTF (m) ... 0.674295574123
Continue
T23/9
Alpha ( $\alpha$ ) Alpha ... -0.006769000000
Beta ( $\beta$ ) ... 0.07131305470
Phi ( $\phi$ ) ... 1.001004282842
A ... -0.784857658731
B ... 2.329340853270
C ... -0.582762216726
T60,trial ... 0.631052855782
C1G1T1 ... 1.068531730459
RDTF (trial) ... 0.674300000000
Converged
T23/10
T23/11 not needed, convergence already achieved
T23/12
 $\gamma_{60, RD60}$  ( $\gamma_{60, trial}$ , RD60, Ttrial rounded) ... 0.6311

```

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Example 23/2 – Steps 9 & 11, Adjust $y_{60, \text{high}}$ Trials, Reset High and Low/Hight Boundaries

Input Data
 γ_x at obs. temp. (T_x) ... Relative density at obs. temp. ... 0.24573
 Observed temperature, °F (T_x) ... Observed temperature Tf, °F ... 189.98
 Computed Data - last digit is rounded
 T23/1
 Input Data - rounded
 γ_x , observed rel. density ... RDtf, observed rel. density ... 0.2457
 T_x , °F ... Tf, °F ... 190.0
 T23/2
 T_x , Kelvin ... Tx, Kelvin ... 360.927777777778
 T23/3
 $RDTf$ and Tf are within range, continue y_x and T_f are within range, continue
 T23/4
 y_x for Fluid 1 RDtf for Fluid 1 0.470381000000
 y_x for Fluid 2 RDtf for Fluid 2 0.341646473673
 T23/5
 Reference Fluid 1 Reference Fluid 1 EP (35/65)
 Reference Fluid 2 Reference Fluid 2 Propane
 $T_{r,x}$ for Fluid 1 $T_{r,x}$ for Fluid 1 1.024024790835
 $T_{r,x}$ for Fluid 2 $T_{r,x}$ for Fluid 2 0.976060840981
 $T_{r,60}$ for Fluid 1 $T_{r,60}$ for Fluid 1 0.819115801951
 $T_{r,60}$ for Fluid 2 $T_{r,60}$ for Fluid 2 0.780749514726
 T23/6
 Upper boundary $y_{60, \text{high}}$ Upper boundary RD60, high 0.507025000000
 Upper boundary $y_{x, \text{high}}$ Upper boundary RDtf, high 0.341646473673
 Lower boundary $y_{60, \text{low}}$ Lower boundary RD60, low 0.488296314601
 Lower boundary $y_{x, \text{low}}$ Lower boundary RDtf, low 0.209990106855
 Iteration steps
 T23/7
 Delta (Δ) Delta 0.271235596182 271235596182 0.6017964345840 126556348248 0.004138210954
 $RD60, m_6^6 y_{60, \text{mid}}$ 0.493376200751 493376200751 0.489664201999 48966454518 0.488882034911 488882034911 0.488850690456
 $C_{n,\text{GTL}}$ 0.587375829009 587375829009 0.5293454548 5293454548 529645859070 504021249568 502607558267
 $RDTF y_{x, \text{mid}}$ 0.289797254929 0.289797254929 0.259348434199 259348434199 0.246406934127 246406934127 0.245700051887
 T23/8
 Continue Continue Continue Continue Continue
 T23/9
 $\text{Alpha} (\alpha)$ Alpha 0.018728685399 0.002273006817 0.002273006817 0.0008-95498051064e-04 0.0003-14747042172e-05
 $\text{Beta} (\beta)$ Beta 0.072626467996 0.072626467996 0.072626467996 0.028442228403 0.007860987453 0.000-3-49330714383e-04
 $\text{Phi} (\phi)$ Phi 1.649681388134 1.202204934943 5.820815799273 237.456099384553
 A 1.515978266954 1.061284960315 1.061284960315 1.166129963841 1.088675802961
 B -0.694014759007 0.470388528249 -0.529337816619 -0.491403133721

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<i>C</i>	0.548511356689	0.543866723826	0.567184205356	0.540274994825	
<i>y₆₀ Trial</i>	<i>RD60, Trial</i>	0.488182097917	0.488768703948		
<i>y₆₀ Trial RD60, Trial adj usted</i>	<i>RD60, Trial</i>	0.490569321418	not changed	not	
<i>changed</i>	<i>not changed</i>				
<i>Gu trial</i>	<i>CTL, Trial</i>	0.549012993292	0.498645735699		
0.502601576844	0.502607454450				
<i>RDTF_{yx} Trial</i>	<i>Trial</i>	0.269328931569	0.243722429967		
0.245697062401	0.				
T23/10 Converged	Continue	e	Continue	C	Continue
T23/11 Reset boundaries					
<i>RDTF_{yx} hi gh</i>		0.269328931569	0.259348434199	0.	0.246406984127
<i>y₆₀ hi gh RD60, hi gh</i>		0.490569321418	0.	0.489664201999	0.
0.488882034911					
<i>RDTF_{yx} low</i>	<i>low</i>	0.	not changed	0.	0.243722429967
<i>y₆₀ low</i>	<i>RB60, low</i>	0.	not changed	0.	0.488768703948
T23/12					
<i>y₆₀ (y₆₀ Trial rounded)</i>	<i>RD60 (RD60, Trial rounded)</i>	0.4889			

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Example 23/3 – T23/11, Reset Upper Boundary Only

Input Data
 γ_x at obs. temp. (T_x) ... Relative density at obs. temp. ... 0.50004
 Observed temperature, °F (T_x) ... Observed temperature T_f , °F ... 190.04
 Computed Data – last digit is rounded
 T23/1
 Input Data – rounded
 γ_x observed rel. density ... RD f , observed rel. density ... 0.5000
 T_f , °F ... T_f , °F ... 190.0
 T23/2
 T_x , Kelvin ... T_x , Kelvin ... 360.927777777778
 T23/3
 $RDTf$ and T_f are within range, continue γ_x and T_f are within range, continue
 T23/4
 γ_x for Fluid 1 RD f for Fluid 1 0.488812742534
 γ_x for Fluid 2 RD f for Fluid 2 0.543932948655
 T23/5
 Reference Fluid 1 Reference Fluid 1 n-Butane
 Reference Fluid 2 Reference Fluid 2 i-Pentane
 $T_{r,x}$ for Fluid 1 $T_{r,x}$ for Fluid 1 0.848922235812
 $T_{r,x}$ for Fluid 2 $T_{r,x}$ for Fluid 2 0.783875809612
 $T_{r,60}$ for Fluid 1 $T_{r,60}$ for Fluid 1 0.679051546607
 $T_{r,60}$ for Fluid 2 $T_{r,60}$ for Fluid 2 0.627021013716
 T23/6
 $\gamma_{60,high}$ Upper boundary RD $60,high$ 0.624285000000
 $\gamma_{x,high}$ Upper boundary RD $f,high$ 0.543932948655
 $\gamma_{60,low}$ Lower boundary RD $60,low$ 0.584127000000
 $\gamma_{x,low}$ Lower boundary RD f,low 0.488812742534

Iteration steps	Pass 1	Pass 2	Iteration steps
Pass 2			
T23/7			
Δ ta (Δ) Delta 0.202961096368	0	0	0.999000000000
$\gamma_{60,mid}$ RD $60,mid$ 0.592277511708	0	0	0.591706929263
$C_{L,GT}$ 0.845587965896	0	0	0.845005240854
$RDTf_{\gamma_{x,mid},mid}$ 0.500822736371	0	0	0.499990386246
T23/8		Continue	Continue
T23/9			
α (α) Alpha 0.040158000000	0	0	-0.007581510774
β (β) Beta 0.056925155369	0	0	-0.011064449627
ϕ (φ) Phi 4.589528260128			589528260128
A 1.260826338621	A 1.157707890490	157707890490	
B 0	B -0.467064681900	-0	-0.569112796362
C 0	C -0.535813879101	0	-0.561057392636
$\gamma_{60,Trial}$ RD $60,Trial$ 0.591708510774	0	0	0.591707579111
$C_{L,Trial}$ CTL,Trial 0.845012937594	0	0	0.845014991820

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<u>RDTF_{Tx_Trial}</u>	<u>Trial</u>	0. 500001346888	0.	0.-500000000000
T23/10	_____ Continue	Converged		
T23/11				
Reset boundaries				
<u>RDTF_{Tx_high}</u>	<u>high</u>	0. 500001346888		
<u>y60_high</u>	<u>RD60_high</u>	0. 591708510774		
T23/12				
<u>y60_(y60_Trial rounded)</u>	<u>RD60_(RD60_Trial rounded)</u>	0. 5917		

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Example 23/4 – Calculated Relative Density @ 60°F (γ_{60}) RD60 equals 0.3500, T23/11 lo/hi, T23/8 detects = Lower Rate Limit

Input Data
 γ_x relative density @ obs. temp. (γ_x) ... Relative density @ obs. temp. ... 0.22238
 Observed temperature, °F (T_o) Observed temperature Tf, °F 87.25
 Computed Data – last digit is rounded
 T23/1
 Input Data – rounded
 γ_x , observed rel. density RDtf, observed rel. density 0.2224
 T_o , °F Tf, °F 87.3
 T23/2
 T_x , Kelvin T_x , Kelvin 303.872222222222
 T23/3
 $RDTf$ and Tf are within range, continue γ_x and T_f are within range, continue
 T23/4
 γ_x for Fluid 1 RDtf for Fluid 1 0.325022000000
 γ_x for Fluid 2 RDtf for Fluid 2 0.267719237662
 T23/5
 Reference Fluid 1 Reference Fluid 1 EE (68/32)
 Reference Fluid 2 Reference Fluid 2 Ethane
 $T_{r,x}$ for Fluid 1 $T_{r,x}$ for Fluid 1 1.019329181249
 $T_{r,x}$ for Fluid 2 $T_{r,x}$ for Fluid 2 0.995225566509
 $T_{r,60}$ for Fluid 1 $T_{r,60}$ for Fluid 1 0.968453106422
 $T_{r,60}$ for Fluid 2 $T_{r,60}$ for Fluid 2 0.945552535144
 T23/6
 Upper boundary $\gamma_{60,high}$ Upper boundary RD60, high 0.355994000000
 Upper boundary $\gamma_{x,high}$ Upper boundary RDtf, high 0.267719237662
 Lower boundary $\gamma_{60,low}$ Lower boundary RD60, low 0.350000000000
 Lower boundary $\gamma_{x,low}$ Lower boundary RDtf, low 0.222390762498
 Iteration steps
 Pass 2 Pass 1 Pass 2 Iteration steps
 T23/7
 Δt Δt 0.001000000000 0 0 0.001000000000
 $\gamma_{60,mid}$ RD60, mid 0.350005994000 0 0 0.350000328926
 $C_{tL,GT}$ 0.635875915052 0 0 0.635428359299
 $RDTf_{\gamma_x,mid}$ 0.222560381708 0 0 0.222400134764
 T23/8 Continue Converged
 T23/9
 α 0.005994000000
 β 0.022215938970
 ϕ 267.236683329960
 A A 2.145687234871
 B B 0.919388011785
 C C 0.448342750031
 $\gamma_{60,Trial}$ RD60, Trial 0.350000323256
 $C_{tL,Trial}$ CTL, Trial 0.635427908123

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<u>RDTF_{y_x, Trial}</u>	<u>Trial</u>	0. 222399973249
T23/10	_____ Continue	
T23/11		
Reset boundaries		
<u>RDTF_{y_x, high}</u>	<u>high</u>	0. 222560381708
<u>y₆₀, high</u>	<u>RD60, high</u>	0. 350005994000
<u>RDTF_{y_x, low}</u>	<u>low</u>	0. 222399973249
<u>y₆₀, low</u>	<u>RD60, low</u>	0. 350000323256
T23/12		
<u>y₆₀ (y₆₀, Trial rounded)</u>	<u>RD60 (RD60, Trial rounded)</u>	0. 3500

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Example 23/5 – Relative Density at Observed Temperature (T23/6, γ_x) RDtf < Lower Boundary

Input Data
 γ_{x_0} relative density @ obs. temp. (γ_x) ... Relative density @ obs. temp. 0.34006
 Observed temperature, °F (T_o) Observed temperature Tf, °F 64.63

Computed Data – last digit is rounded
 T23/1
 Input Data – rounded
 γ_{x_0} observed rel. density RDtf, observed rel. density 0.3401
 T_o , °F Tf, °F 64.6

T23/2
 T_{x_0} Kelvin T_x , Kelvin 291.261111111111

T23/3
RDtf and Tf are within range, continue
 γ_x and T_f are within range, continue
 T23/4
 γ_x for Fluid 1 RDtf for Fluid 1 0.310026832478
 γ_x for Fluid 2 RDtf for Fluid 2 0.346752475914

T23/5
 Reference Fluid 1 Reference Fluid 1 EE (68/32)
 Reference Fluid 2 Reference Fluid 2 Ethane
 $T_{r,x}$ for Fluid 1 $T_{r,x}$ for Fluid 1 0.977025631851
 $T_{r,x}$ for Fluid 2 $T_{r,x}$ for Fluid 2 0.953922349953
 $T_{r,60}$ for Fluid 1 $T_{r,60}$ for Fluid 1 0.968453106422
 $T_{r,60}$ for Fluid 2 $T_{r,60}$ for Fluid 2 0.945552535144

T23/6
 $\gamma_{x_0,high}$ Upper boundary RD60, high 0.355994000000
 $\gamma_{x_0,high}$ Upper boundary RDtf, high 0.346752475914
 $\gamma_{x_0,low}$ Lower boundary RD60, low 0.350000000000
 $\gamma_{x_0,low}$ Lower boundary RDtf, low 0.340112938057

γ_x observed RDtf observed is less than lower boundary RDtf, no solution outside the boundary of the standard
 γ_x observed is outside the correlation range of the standard

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Example 23/6 – T23/6, Relative Density at Observed Temperature (y_x) RD_{tf}> Upper Boundary

Input Data
 Relative density @ obs. temp. (y_x) Relative density @ obs. temp. 0.72858
 Observed temperature, °F (T_x) Observed temperature Tf, °F 27.53
 Computed Data – Last digit is rounded
 T23/1
 Input Data – rounded
 y_x , observed rel. density RD_{tf}, observed rel. density 0.7286
 T_x , °F Tf, °F 27.5
 T23/2
 T_x , Kelvin Tx, Kelvin 240.094444444444
 T23/3
 RD_{tf} and Tf are within range, continue y_x and Tf are within range, continue
 T23/4
 y_x for Fluid 1 RD_{tf} for Fluid 1 0.706219967989
 y_x for Fluid 2 RD_{tf} for Fluid 2 0.728360741594
 T23/5
 Reference Fluid 1 Reference Fluid 1 n-Hexane
 Reference Fluid 2 Reference Fluid 2 n-Heptane
 $T_{r,x}$ for Fluid 1 Tr_x for Fluid 1 0.473232373006
 $T_{r,x}$ for Fluid 2 Tr_x for Fluid 2 0.444495870489
 $T_{r,60}$ for Fluid 1 Tr₆₀ for Fluid 1 0.569046132957
 $T_{r,60}$ for Fluid 2 Tr₆₀ for Fluid 2 0.534491447849
 T23/6
 y_x observed is outside the boundary of the standard
 y_x observed is outside the correlation range of the standard
 RD_{tf} observed is greater than Fluid 2 RD_{tf}, no solution

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Example 23/7 – Test Binary Search Routine ~~at~~ At Low End

Input Data
~~Relative density @ obs. temp. (γ_x) . . . Relative density @ obs. temp. 0.45572~~
~~Observed temperature, °F (T_f) Observed temperature T_f, °F 24.67~~
 Computed Data – last digit is rounded
 T23/1
 Input Data – rounded
 ~~γ_x , observed rel. density RD_{TF}, observed rel. density 0.4557~~
~~T_f, °F T_f, °F 24.7~~
 T23/2
~~T_x, Kelvin T_x, Kelvin 241.650000000000~~
 T23/3
~~RD_{TF} and T_f are within range, continue γ_x and T_f are within range, continue~~
 T23/4
 ~~γ_x for Fluid 1 RD_{TF} for Fluid 1 0.455790716298~~
 ~~γ_x for Fluid 2 RD_{TF} for Fluid 2 0.462651655172~~
 T23/5
~~Reference Fluid 1 Reference Fluid 1 EE (68/32)~~
~~Reference Fluid 2 Reference Fluid 2 Ethane~~
~~T_{r,x} for Fluid 1 T_{r,x} for Fluid 1 0.810606822985~~
~~T_{r,x} for Fluid 2 T_{r,x} for Fluid 2 0.791438771166~~
~~T_{r,60} for Fluid 1 T_{r,60} for Fluid 1 0.968453106422~~
~~T_{r,60} for Fluid 2 T_{r,60} for Fluid 2 0.945552535144~~
 T23/6
~~Upper boundary $\gamma_{60,high}$ Upper boundary RD_{60,high} 0.355994000000~~
~~Upper boundary $\gamma_{x,high}$ Upper boundary RD_{TF,high} 0.462651655172~~
~~Lower boundary $\gamma_{60,low}$ Lower boundary RD_{60,low} 0.350000000000~~
~~Lower boundary $\gamma_{x,low}$ Lower boundary RD_{TF,low} 0.459877928850~~
 ~~γ_x observed is outside the boundary of the standard RD_{TF} observed is less than lower boundary RD_{TF}, no solution~~
 ~~γ_x observed is outside the correlation range of the standard~~

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Example 23/8 – Relative Density at Observed Temperature (γ_x) RD_{tf} near $\gamma_{x,low}$ RD_{low}T_f, T23/11 Reset Lower/Upper Boundaries

Input Data
 Relative density @ obs. temp. (γ_x) ... Relative density @ obs. temp. ... 0.25776
 Observed temperature, °F (T_f) ... Observed temperature, °F ... 179.28
 Computed Data – Last digit is rounded
 T23/1
 Input Data – rounded
 γ_x observed rel. density RD_{tf} observed rel. density 0.2578
 T_f , °F Tf, °F 179.3
 T23/2
 T_x , Kelvin Tx, Kelvin 354.983333333333
 T23/3
 RD_{tf} and Tf are within range, continue γ_x and Tf are within range, continue
 T23/4
 γ_x for Fluid 1 RD_{tf} for Fluid 1 0.470381000000
 γ_x for Fluid 2 RD_{tf} for Fluid 2 0.367118287562
 T23/5
 Reference Fluid 1 Reference Fluid 1 EP (35/65)
 Reference Fluid 2 Reference Fluid 2 Propane
 $T_{r,x}$ for Fluid 1 Tr_x for Fluid 1 1.007159204827
 $T_{r,x}$ for Fluid 2 Tr_x for Fluid 2 0.959985216435
 $T_{r,60}$ for Fluid 1 Tr₆₀ for Fluid 1 0.819115801951
 $T_{r,60}$ for Fluid 2 Tr₆₀ for Fluid 2 0.780749514726
 T23/6
 Upper boundary $\gamma_{60,high}$ Upper boundary RD_{60,high} 0.507025000000
 Upper boundary $\gamma_{x,high}$ Upper boundary RD_{tf,high} 0.367118287562
 Lower boundary $\gamma_{60,low}$ Lower boundary RD_{60,low} 0.475719627406
 Lower boundary $\gamma_{x,low}$ Lower boundary RD_{tf,low} 0.203205649078
 Iteration steps
 Pass 1 Pass 2 Pass 3 Iteration steps
 T23/7
 Delta (Δ) Delta 0.333069807351 0 0.203517533920
 $\gamma_{60,mid}$ RD_{60,mid} 0.486146501825 0 0.478475881642
 $C_{T,CTL}$ 0.636706579940 0 0.560060148072 0
 Δ 0.540064021350
 RD_{tf} $\gamma_{x,mid}$ 0.309532676527 0 0.267975273121 0
 Δ 0.257851552201
 T23/8
 Continue Continue Continue
 T23/9
 Δ 0.001061240214 0.031305372594 0 0.009630620270
 Δ 0.005510968782 0.093483301245 0 0.035990492538
 Φ 1.541589588429 541589588429
 Δ 2.776410749513 776410749513 28.803325550048
 Δ 1.551880192561 551880192561 1.415113489360

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TEMPERATURE CORRECTION FOR THE VOLUME OF NGL AND LPG TABLES 23E, 24E, 53E, 54E, 59E, AND 60E

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<u>B.....</u>	<u>B.....</u>	0. 729324366880	-0.....	0-711644239073
<u>0.....</u>	<u>0.....</u>	0-642401682060		
<u>C.....</u>	<u>C.....</u>	0. 557290084813	0.....	0-557737265084
<u>0.....</u>	<u>0.....</u>	0-549003291079		
<u>y60_Trial.....</u>	<u>RD60_Trial.....</u>	0. 476515881554	0.....	0-477414641428
<u>0.....</u>	<u>0.....</u>	0-477441768642		
<u>Ctrl_Trial.....</u>	<u>CTL_Trial.....</u>	0. 513269870440	0.....	0-539337110326
<u>0.....</u>	<u>0.....</u>	0-539961117999		
<u>RDTF_yx_Trial.....</u>	<u>Trial.....</u>	0. 244581244788	0.....	0-257487433135
<u>0.....</u>	<u>0.....</u>	0-257799991175		
<u>T23/10</u>	<u>Continue</u>			
<u>T23/10</u>	<u>Continue</u>			
<u>T23/11</u>	<u>Converged</u>			
Reset boundaries				
<u>RDTF_yx_high.....</u>	<u>high.....</u>	0. 309532676527	0.....	0-267975273121
<u>y60_high.....</u>	<u>RD60_high.....</u>	0. 486146501825	0.....	0-48475881642
<u>RDTF_yx_low.....</u>	<u>low.....</u>	0. 244581244788	0.....	0-257487433135
<u>y60_low.....</u>	<u>RD60_low.....</u>	0. 476515881554	0.....	0-477414641428
T23/12				
<u>y60_(y60_Trial rounded).....</u>	<u>RD60_(RD60_Trial rounded).....</u>			

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Example 23/9 – T23/11, rReset Upper/Lower Boundaries Using Ethane &And EP (65/35)

```

Input Data
Relative density @ obs. temp. ( $\gamma_x$ ) ..... Relative density @ obs. temp. .... 0.39548
Observed temperature, °F ( $T_x$ ) ..... Observed temperature, °F ..... 59.78
    Computed Data - last digit is rounded
T23/1
    Input Data - rounded
 $\gamma_x$ , observed rel. density ..... RDtf, observed rel. density ..... 0.3955
 $T_x$ , °F ..... TF, °F ..... 59.8
T23/2
 $T_x$ , Kelvin ..... Tx, Kelvin ..... 288.5944444444444

T23/3
RDtf and Tf are within range, continue $\gamma_x$  and  $T_x$  are within range, continue
T23/4
 $\gamma_x$  for Fluid 1 ..... RDtf for Fluid 1 ..... 0.356376967243
 $\gamma_x$  for Fluid 2 ..... RDtf for Fluid 2 ..... 0.429505267826

T23/5
Reference Fluid 1 ..... Reference Fluid 1 ..... Ethane
Reference Fluid 2 ..... Reference Fluid 2 ..... EP (65/35)
 $T_{r,x}$  for Fluid 1 ..... Tr_x for Fluid 1 ..... 0.945188630152
 $T_{r,x}$  for Fluid 2 ..... Tr_x for Fluid 2 ..... 0.864909774461
 $T_{r,60}$  for Fluid 1 ..... Tr_60 for Fluid 1 ..... 0.945552535144
 $T_{r,60}$  for Fluid 2 ..... Tr_60 for Fluid 2 ..... 0.865242771467

T23/6
Upper boundary  $\gamma_{60,high}$  ..... Upper boundary RD60, high ..... 0.429277000000
Upper boundary  $\gamma_x,high$  ..... Upper boundary RDtf, high ..... 0.429505267826
Lower boundary  $\gamma_{60,low}$  ..... Lower boundary RD60, low ..... 0.355994000000
Lower boundary  $\gamma_x,low$  ..... Lower boundary RDtf, low ..... 0.356376967243

Iteration steps
Pass 1           Pass 2           Iteration steps
Pass 2
T23/7
Delta ( $\delta$ ) ..... Delta ..... 0.534991685093 0 ..... 0.999000000000
 $\gamma_{60,mid}$  ..... RD60, mid ..... 0.395199795659 0 ..... 0.395230790997
CnCTL ..... 1.000681275169 1.000681092670
RDtf( $\gamma_x,mid$ )mid ..... 0.395469035466 0 ..... 0.395499979792
T23/8
Continue ..... Continue ..... T23/8
Continue
T23/9
Alpha ( $\alpha$ )Alpha ..... 3.10263646086e-05 ..... 0.073283000000 073283000000
Beta ( $\beta$ )Beta ..... 2.45005041712e-05 ..... 0.057470232309 057470232309
Phi ( $\phi$ )Phi ..... 1.001001001559 ..... 1.870668498940 870668498940
A ..... -0.023321269027 -0 ..... 0.018033364749
B ..... 1.015912364749 ..... 1.020443223123 020443223123
C ..... -0.004706553990 -0 ..... 0.003741745597
 $\gamma_{60,Trial}$  ..... RD60, Trial ..... 0.395230822023 0 ..... 0.395230811239
CnCTL,Trial ..... CTL, Trial ..... 1.000681092487 000681092487 1.00068109

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TEMPERATURE CORRECTION FOR THE VOLUME OF NGL AND LPG TABLES 23E, 24E, 53E, 54E, 59E, AND 60E

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<u>RDTE_{y_x} Trial</u>	<u>Trial</u>	0.395500010767	0.	0.3955000000000000
<u>T23/10</u>	<u>Continue</u>	<u>Converged</u>	<u>T23/10</u>	<u>Converged</u>
T23/11				
Reset boundaries				
<u>RDTE_{y_x} high</u>	<u>high</u>	0.395500010767		
<u>y₆₀ high</u>	<u>RD60, high</u>	0.395230822023		
<u>RDTE_{y_x} low</u>	<u>low</u>	0.395469035466		
<u>y₆₀ low</u>	<u>RD60, low</u>	0.395199795659		
T23/12				
<u>y₆₀ (y₆₀ trial rounded)</u>	<u>RD60 (RD60, Trial rounded)</u>	0.3952		

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Example 23/10 – T23/9 & 11, Adjust $\gamma_{60, RD60, Trial}$, Reset High and Low/High+low/Hi Boundaries

Input Data
 $\text{Relative density @ obs. temp. } (\gamma_x) \dots \text{Relative density @ obs. temp.} \dots 0.21056$
 $\text{Observed temperature, } ^\circ\text{F } (T_x) \dots \text{Observed temperature, } ^\circ\text{F } (T_F) \dots 87.46$
 Computed Data – last digit is rounded
 T23/1
 Input Data – rounded
 $\gamma_x, \text{observed rel. density} \dots \text{RDtf, observed rel. density} \dots 0.2106$
 $T_x, ^\circ\text{F} \dots T_F, ^\circ\text{F} \dots 87.5$
 T23/2
 $T_x, \text{Kelvin} \dots T_F, \text{Kelvin} \dots 303.983333333333$
 T23/3
 $\text{RDtf and } T_F \text{ are within range, continue } \gamma_x \text{ and } T_F \text{ are within range, continue}$
 T23/4
 $\gamma_x \text{ for Fluid 1} \dots \text{RDtf for Fluid 1} \dots 0.325022000000$
 $\gamma_x \text{ for Fluid 2} \dots \text{RDtf for Fluid 2} \dots 0.266017434379$
 T23/5
 $\text{Reference Fluid 1} \dots \text{Reference Fluid 1} \dots \text{EE (68/32)}$
 $\text{Reference Fluid 2} \dots \text{Reference Fluid 2} \dots \text{Ethane}$
 $T_{r,x} \text{ for Fluid 1} \dots T_{r,x} \text{ for Fluid 1} \dots 1.019701899746$
 $T_{r,x} \text{ for Fluid 2} \dots T_{r,x} \text{ for Fluid 2} \dots 0.995589471501$
 $T_{r,60} \text{ for Fluid 1} \dots T_{r,60} \text{ for Fluid 1} \dots 0.968453106422$
 $T_{r,60} \text{ for Fluid 2} \dots T_{r,60} \text{ for Fluid 2} \dots 0.945552535144$
 T23/6
 $\text{Upper boundary } \gamma_{60, \text{high}} \dots \text{Upper boundary RD60, high} \dots 0.355994000000$
 $\text{Upper boundary } \gamma_x, \text{high} \dots \text{Upper boundary RDtf, high} \dots 0.266017434379$
 $\text{Lower boundary } \gamma_{60, \text{low}} \dots \text{Lower boundary RD60, low} \dots 0.350217135734$
 $\text{Lower boundary } \gamma_x, \text{low} \dots \text{Lower boundary RDtf, low} \dots 0.201957415331$

Iteration steps	Pass 1	Pass 2	Pass 3	Pass 4	Pass 5
steps	Pass 1	Pass 2	Pass 3	Pass 4	Pass 5
T23/7					
Delta (Δ)	0.285572535939	0.045507746482	0.134913863553	0.442156617893	
$\gamma_{60, \text{mid}}$	0.350250911268	0.350238857349	0.350996514811	0.350315978649	
C_{GETL}	0.605460325548	0.601336301107	0.663001877090	0.618306878199	0.
$RDtf(\gamma_{x, \text{mid}}, \text{mid})$	0.212063030760	0.210611338982	0.232711348172	0.216601542528	0.
T23/8	Continue	Continue	Continue	Continue	T23/8
α	0.0002-19024009957e-04	0.00008-82768152069e-05	0.00001-26286194162e-05	0.005776864266	0.005776864266
β	0.-0.003568550978	0.0006-47744349018e-04	0.029978477786	0.-0.008277157180	
ϕ	1.334762574159	334762574159	2.175177227878	175177227878	18.901668137223
A	0.-0.877145829125	0.-0.793585193044	1.946686690732	0.-0.936748950385	
B	0.-0.362105293706	0.-0.327124761330	0.820821476963	0.-0.385474575544	

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TEMPERATURE CORRECTION FOR THE VOLUME OF NGL AND LPG TABLES 23E, 24E, 53E, 54E, 59E, AND 60E

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<i>C</i>	<i>C</i>	0. 436589003610	0.	0. 389856988966	
.....	0.	0. 387594169917	0.	0. 383933874925			
<i>y₆₀, Trial</i>	<i>RD60, Trial</i>	0. 350064149476	0.	0. 350225701834	Formatted: Tab stops: 2.3", Right,Leader: ... + 2.6", Decimal aligned + 3.7", Decimal aligned + 4.8", Decimal aligned + 5.9", Decimal aligned
.....	0.	0. 350238282649	0.	0. 350238776362			
<i>y₆₀, Trial, adjusted</i>	<i>RD60, Trial, adjusted</i>	<i>RD60, Trial</i>	0. 350436159743	not changed	Formatted: Tab stops: 2.3", Right,Leader: ... + 2.6", Decimal aligned + 3.7", Decimal aligned + 4.8", Decimal aligned + 5.9", Decimal aligned + Not at 2.5" + 3" + 4" + 5" + 6"
<i>changed</i>	<i>not changed</i>				
<i>CTL, trial</i>	<i>CTL, Trial</i>	0. 632080457699	0.	0. 594476787322	Formatted: Tab stops: 2.3", Right,Leader: ... + 2.6", Decimal aligned + 3.7", Decimal aligned + 4.8", Decimal aligned + 5.9", Decimal aligned + Not at 2.5" + 3" + 4" + 5" + 6"
.....	0.	0. 601105752483	0.	0. 601304054034			
<i>RTDF_{fx, Trial}</i>	<i>Trial</i>	0. 221503848245	0.	0. 208201050064	Formatted: Tab stops: 2.3", Right,Leader: ... + 2.6", Decimal aligned + 3.7", Decimal aligned + 4.8", Decimal aligned + 5.9", Decimal aligned
.....	0.	0. 210530246440	0.	0. 210599996106			
T23/10	Continue	Continue	Converged	
T23/10	Continue	Continue	Converged	
T23/11						
Reset boundaries						
<i>RTDF_{fx, high}</i>	<i>high</i>	0. 221503848245	0.	0. 212063030760	Formatted: Tab stops: 2.3", Right,Leader: ... + 2.6", Decimal aligned + 3.7", Decimal aligned + 4.8", Decimal aligned + 5.9", Decimal aligned + Not at 2.5" + 3" + 4" + 5" + 6"
.....	0.	0. 212063030760					
<i>y₆₀, high</i>	<i>RD60, high</i>	0. 350436159743	0.	0. 350319978649	Formatted: Tab stops: 2.3", Right,Leader: ... + 2.6", Decimal aligned + 3.7", Decimal aligned + 4.8", Decimal aligned + 5.9", Decimal aligned
.....	0.	0. 350250911268					
<i>RTDF_{fx, low}</i>	<i>low</i>	not changed	0.	0. 208201050064	Formatted: Tab stops: 2.3", Right,Leader: ... + 2.6", Decimal aligned + 3.7", Decimal aligned + 4.8", Decimal aligned + 5.9", Decimal aligned
.....	0.	0. 210530246440					
<i>y₆₀, low</i>	<i>RD60, low</i>	not changed	0.	0. 350225701834	Formatted: Tab stops: 2.3", Right,Leader: ... + 2.6", Decimal aligned + 3.7", Decimal aligned + 4.8", Decimal aligned + 5.9", Decimal aligned
.....	0.	0. 350238282649					
T23/12						
<i>y₆₀ (y₆₀, trial rounded)</i>	<i>RD60, (RD60, Trial rounded)</i>	0. 3502			Formatted: Tab stops: 2.3", Right,Leader: ... + 2.6", Decimal aligned + 3.7", Decimal aligned + 4.8", Decimal aligned + 5.9", Decimal aligned + Not at 2.5" + 3" + 4" + 5" + 6"
.....							

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Example 23/11 – T23/11, Reset Upper Boundary Only

```

Input Data
Relative density @ obs. temp. ( $\gamma_x$ ) ..... Relative density @ obs. temp. .... 0.45003
Observed temperature, °F ( $T_x$ ) ..... Observed temperature, °F ( $T_F$ ) ..... 199.43
    Computed Data - last digit is rounded
T23/1
    Input Data - rounded
 $\gamma_x$ , observed rel. density ..... RDtf, observed rel. density ..... 0.4500
 $T_F$ , °F ..... °F ..... 199.4
T23/2
 $T_x$ , Kelvin .....  $T_x$ , Kelvin ..... 366.150000000000
T23/3
RDtf and  $T_F$  are within range, continue  $\gamma_x$  and  $T_F$  are within range, continue
T23/4
 $\gamma_x$  for Fluid 1 ..... RDtf for Fluid 1 ..... 0.445396160533
 $\gamma_x$  for Fluid 2 ..... RDtf for Fluid 2 ..... 0.480129616454
T23/5
Reference Fluid 1 ..... Reference Fluid 1 ..... i-Butane
Reference Fluid 2 ..... Reference Fluid 2 ..... n-Butane
 $T_{r,x}$  for Fluid 1 .....  $T_{r,x}$  for Fluid 1 ..... 0.897756528135
 $T_{r,x}$  for Fluid 2 .....  $T_{r,x}$  for Fluid 2 ..... 0.861205193339
 $T_{r,60}$  for Fluid 1 .....  $T_{r,60}$  for Fluid 1 ..... 0.707871902797
 $T_{r,60}$  for Fluid 2 .....  $T_{r,60}$  for Fluid 2 ..... 0.679051546607
T23/6
Upper boundary  $\gamma_{60,high}$  ..... Upper boundary RD60, high ..... 0.584127000000
Upper boundary  $\gamma_x,high$  ..... Upper boundary RDtf, high ..... 0.480129616454
Lower boundary  $\gamma_{60,low}$  ..... Lower boundary RD60, low ..... 0.562827000000
Lower boundary  $\gamma_x,low$  ..... Lower boundary RDtf, low ..... 0.445396160533

Iteration steps
Pass 1           Pass 2           Iteration steps
Pass 2
T23/7
Delta (Δ) ..... Delta ..... 0.132547693417 0 ..... 0.999000000000
 $\gamma_{60,mid}$  ..... RD60, mid ..... 0.565650265870 0 ..... 0.565462936534
CnCTL ..... 0.796107835259 0 ..... 0.795800434708
RDtf( $\gamma_x,mid$ ,mid) ..... 0.450318608675 0 ..... 0.449995650705
T23/8
Continue Continue
T23/8
Continue Continue
T23/9
Alpha (α)Alpha ..... 0.021300000000 0 ..... 0.002638575109
Beta (β)Beta ..... 0.032146708779 0 ..... 0.004124443006
Phi (φ)Phi ..... 7.056134451304 056134451304
..... 1.000989768898
A ..... A ..... 1.331470032321 331470032321
..... 1.412580442222
B ..... B ..... 0.619068238574 0 ..... 0.691719762248
C ..... C ..... 0.574423600922 0 ..... 0.590694810831
 $\gamma_{60,Trial}$  ..... RD60, Trial ..... 0.565465575109 0 ..... 0.565465457370
CnTrial ..... CTL, Trial ..... 0.795804772113 0 ..... 0.795804578573

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TEMPERATURE CORRECTION FOR THE VOLUME OF NGL AND LPG TABLES 23E, 24E, 53E, 54E, 59E, AND 60E

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<u>RDTF_{y_x, Trial}</u>	<u>Trial</u>	0. 450000203137	0.	0. 450000600000
<u>T23/10</u>	<u>Continue</u>	<u>Converged</u>		
<u>T23/10</u>	<u>Continue</u>	<u>Converged</u>		
T23/11				
Reset boundaries				
<u>RDTF_{y_x, high}</u>	<u>high</u>	0. 450000203137		
<u>y₆₀, high</u>	<u>RD60, high</u>	0. 565465575109		
T23/12				
<u>y₆₀ (y₆₀, Trial rounded)</u>	<u>RD60 (RD60, Trial rounded)</u>	0. 5655		

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Example 23/12 – T23/10 dDetects Solution In One Pass, Using I-Hexane

```

Input Data
Relative density @ obs. temp. ( $\gamma_x$ ) ..... Relative density @ obs. temp. .... 0.60133
Observed temperature, °F ( $T_e$ ) ..... Observed temperature, °F ..... 177.17
    Computed Data – last digit is rounded
T23/1
    Input Data – rounded
 $\gamma_x$ , observed rel. density ..... RDtf, observed rel. density ..... 0.6013
 $T_e$ , °F ..... TF, °F ..... 177.2
T23/2
 $T_e$ , Kelvin ..... Tx, Kelvin ..... 353.816666666667

T23/3
RDtf and Tf are within range, continue $\gamma_x$  and  $T_e$  are within range, continue
T23/4
 $\gamma_x$  for Fluid 1 ..... RDtf for Fluid 1 ..... 0.594442903364
 $\gamma_x$  for Fluid 2 ..... RDtf for Fluid 2 ..... 0.602928497317

T23/5
Reference Fluid 1 ..... Reference Fluid 1 ..... i-Hexane
Reference Fluid 2 ..... Reference Fluid 2 ..... n-Hexane
 $T_{r,x}$  for Fluid 1 ..... Tr,x for Fluid 1 ..... 0.710403908577
 $T_{r,x}$  for Fluid 2 ..... Tr,x for Fluid 2 ..... 0.697381820571
 $T_{r,60}$  for Fluid 1 ..... Tr,60 for Fluid 1 ..... 0.579671831253
 $T_{r,60}$  for Fluid 2 ..... Tr,60 for Fluid 2 ..... 0.569046132957

T23/6
Upper boundary  $\gamma_{60,high}$  ..... Upper boundary RD60, high ..... 0.664064000000
Upper boundary  $\gamma_x,high$  ..... Upper boundary RDtf, high ..... 0.602928497317
Lower boundary  $\gamma_{60,low}$  ..... Lower boundary RD60, low ..... 0.657167000000
Lower boundary  $\gamma_x,low$  ..... Lower boundary RDtf, low ..... 0.594442903364

Iteration steps
Iteration steps
Pass 1
T23/7
Delta (Δ) ..... Delta ..... 0.808086820333
 $\gamma_{60,mid}$  ..... RD60,mid ..... 0.662740374800
CnCTL ..... 0.907329937112
RDtf $\gamma_{x,mid}$ ,mid ..... 0.601324182589

T23/8
T23/8
Continue
T23/9
Alpha (α)Alpha ..... 0.006897000000
Beta (β)Beta ..... 0.010160407517
Phi (φ)Phi ..... 1.233141931306
A ..... A ..... 1.780418160509
B ..... B ..... 1.319032483022
C ..... C ..... 0.812123726312
 $\gamma_{60,Trial}$  ..... RD60,Trial ..... 0.662720493291
CnTrial ..... CTL,Trial ..... 0.907320672201
RDtf $\gamma_{x,Trial}$  ..... Trial ..... 0.601300003454

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TEMPERATURE CORRECTION FOR THE VOLUME OF NGL AND LPG TABLES 23E, 24E, 53E, 54E, 59E, AND 60E

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T23/10 Converged
T23/11 not needed, convergence already achieved
T23/12
 γ_{60} (γ_{60} trial rounded) RD60 (RD60, Trial rounded) 0.6627

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Example 23/13 – Calculated Relative Density @ 60°F (γ_{60}) RD60 equals 0.6880 = Upper Range Limit

Input Data
Relative density @ obs. temp. (γ_x) Relative density @ obs. temp. 0.73592
Observed temperature, °F (T_x) Observed temperature T_F, °F 44.13
 Computed Data – Last digit is rounded
 T23/1
 Input Data – rounded
 γ_x , observed rel. density RDT_F, observed rel. density 0.7359
T_x, °F T_F, °F 44.1
 T23/2
 γ_x , Kelvin T_x, Kelvin 230.872222222222
 T23/3
RDT_F and T_F are within range, continue
 γ_x and T_x are within range, continue
 T23/4
 γ_x for Fluid 1 RDT_F for Fluid 1 0.714077137643
 γ_x for Fluid 2 RDT_F for Fluid 2 0.735959630678
 T23/5
Reference Fluid 1 Reference Fluid 1 n-Hexane
Reference Fluid 2 Reference Fluid 2 n-Heptane
 $T_{r,x}$ for Fluid 1 $T_{r,x}$ for Fluid 1 0.455055133975
 $T_{r,x}$ for Fluid 2 $T_{r,x}$ for Fluid 2 0.427422423812
 $T_{r,60}$ for Fluid 1 $T_{r,60}$ for Fluid 1 0.569046132957
 $T_{r,60}$ for Fluid 2 $T_{r,60}$ for Fluid 2 0.534491447849
 T23/6
Upper boundary $\gamma_{60,high}$ Upper boundary RD60, high 0.688039000000
Upper boundary $\gamma_x,high$ Upper boundary RDT_F, high 0.735959630678
Lower boundary $\gamma_{60,low}$ Lower boundary RD60, low 0.664064000000
Lower boundary γ_x,low Lower boundary RDT_F, low 0.714077137643
 Iteration steps
 Pass 1 Iteration steps Pass 1
 T23/7
Delta (Δ) Delta 0.997274959562
 $\gamma_{60,mid}$ RD60,mid 0.687973667156
C_TL CTL 1.069661466437
RDT_{F,x,mid} mid 0.735898921680
 T23/8
Continue
 T23/9
Alpha (α) Alpha 0.023975000000
Beta (β) Beta 0.031730419484
Phi (ϕ) Phi 1.002782036454
A A 0.891797542956
B B 2.388763933252
C C 0.586964652669
 $\gamma_{60,Trial}$ RD60,Trial 0.687974827662
C_TL,Trial CTL,Trial 1.069661229476
RDT_{F,x,Trial} Trial 0.735900000006
 T23/10 Converged

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T23/11 not needed, convergence already achieved
T23/12

$\gamma_{60} (\gamma_{60, \text{trial, rounded}}) \dots \dots \dots \text{RD60 - (RD60, Trial - rounded)} \dots \dots \dots 0.6880$

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Example 23/14 – Rd-Lower Boundary Reset Test=lower RD limit

Input Data
 γ_x relative density @ obs. temp. (γ_x) ... Relative density @ obs. temp. 0.21
 Observed temperature, °F (T_e) Observed temperature Tf, °F 189.4
 Computed Data – Last digit is rounded
 T23/1
 Input Data – rounded
 γ_x , observed rel. density RDtf, observed rel. density 0.2100
 T_e , °F Tf, °F 189.4
 T23/2
 T_e , Kelvin Tx, Kelvin 360.594444444444
 T23/3
 RDtf and Tf are within range, continue γ_x and T_e are within range, continue
 T23/4
 γ_x for Fluid 1 RDtf for Fluid 1 0.470381000000
 γ_x for Fluid 2 RDtf for Fluid 2 0.343306875586
 T23/5
 Reference Fluid 1 Reference Fluid 1 EP (35/65)
 Reference Fluid 2 Reference Fluid 2 Propane
 $T_{r,x}$ for Fluid 1 $T_{r,x}$ for Fluid 1 1.023079057040
 $T_{r,x}$ for Fluid 2 $T_{r,x}$ for Fluid 2 0.975159404090
 $T_{r,60}$ for Fluid 1 $T_{r,60}$ for Fluid 1 0.819115801951
 $T_{r,60}$ for Fluid 2 $T_{r,60}$ for Fluid 2 0.780749514726
 T23/6
 $\gamma_{60,high}$ Upper boundary RD60, high 0.507025000000
 $\gamma_{x,high}$ Upper boundary RDtf, high 0.343306875586
 $\gamma_{60,low}$ Lower boundary RD60, low 0.487591079805
 $\gamma_{x,low}$ Lower boundary RDtf, low 0.209600629464
 Iteration steps

Pass 1	Pass 2	Pass 3		Iteration steps
T23/7				
Delta (Δ) 0. -0.362651574654	Delta 0.002986925048	0. -0.090629503273		Formatted
$\gamma_{60,mid}$ 0. -0.487591089742	$\gamma_{60,mid}$ 0.487649127468	0. -0.487591210267		Formatted
Cn 0. -0.431453309175	CTL 0.462843318636	0. -0.433769342155		Formatted
RDtf $\gamma_{x,mid}$ 0. -0.210372789193	$\gamma_{x,mid}$ 0.225705140487	0. -0.211502118518		Formatted
T23/8	Continue	Continue	-T23/8	
Continue	Continue	Converged		
T23/9				
Alpha (α) 0.019433920195	Alpha 1.43950513215e-06			Formatted
Beta (β) 0.073927186953	Beta 0. -0.001866682512			Formatted
Phi (φ) 8.302409550559	Phi 302409550559.2.31746183			Formatted
A 1.205283669609	A 0. -0.103014400791			Formatted
B -0.521062500820	B 0. -0.043309773699			Formatted
C 0.543855074908	C 0. -0.492140295111			Formatted
$\gamma_{60,Trial}$ RD60, Trial 0.487584959566	$\gamma_{60,Trial}$ 0. -0.487591045409			Formatted

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<i>y₆₀.Trial adjusted RD60, Trial adjusted</i>	<i>RD60, Trial</i>	0.487592519310	0.	487591107206	net
<i>CTL, trial</i>	<i>CTL, Trial</i>	0.438905949758	0.	0.432126227318	
<i>RDTF_{ix}, Trial</i>	<i>Trial</i>	0.214007257783	0.	0.210701880813	
<u>T23/10</u>	Continue	Continue			
<u>T23/10</u>	Continue	Continue			
<u>T23/11</u>					
Reset boundaries					
<i>RDTF_{ix}, high</i>	<i>high</i>	0.214007257783	0.	0.210701880813	+ 6"
<i>y₆₀, high</i>	<i>RD60, high</i>	0.487592519310	0.	0.487591107206	
T23/12					
<i>y₆₀ (y₆₀, Trial rounded)</i>	<i>RD60 - (RD60, Trial rounded)</i>				

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Example 23/15 – Relative Density at Observed Temperature ($T_{23/3}$, y_x) $RDtf <$ Lower Range Limit

Input Data
Relative density @ obs. temp. (y_x) Relative density @ obs. temp. 0.20993
Observed temperature, °F (T_x) Observed temperature, °F 187.94
 Computed Data – Last digit is rounded
 T23/1
 Input Data – rounded
 y_x , observed rel. density $RDtf$, observed rel. density 0.2099
 T_x , °F TF , °F 187.9
 T23/2
 T_x , Kelvin T_K , Kelvin 359.761111111111

T23/3
 $RDtf_{in}$ is outside the input range of the standard less than 0.2100, no solution

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Example 23/16 – T23/3, Relative Density at Observed Temperature (γ_x) RDtf > Upper Range Limit

Input Data
 γ_{x_0} relative density @ obs. temp. (γ_x) ... Relative density @ obs. temp. 0.74005
 Observed temperature, °F (T_f) Observed temperature Tf, °F 28.48
 Computed Data – last digit is rounded
 T23/1
 Input Data – rounded
 γ_{x_0} observed rel. density RDtf, observed rel. density 0.7401
 T_f , °F Tf, °F 28.5
 T23/2
 T_x , Kelvin Tx, Kelvin 239.538888888889
 T23/3
 RDtf_x is outside the input range of the standard greater than 0.7400, no solution

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Example 23/17 – Relative Density at Observed Temperature (γ_x) - RD_{tf} => Upper range Boundary Limit, fails T23/6

Input Data
Relative density @ obs. temp. (γ_x) Relative density @ obs. temp. 0.74
Observed temperature, °F (T_x) Observed temperature Tf, °F 50
 Computed Data – Last digit is rounded
 T23/1
 Input Data – rounded
 γ_x , observed rel. density RD_{tf}, observed rel. density 0.7400
 T_x , °F Tf, °F 50.0
 T23/2
 T_x , Kelvin T_f, Kelvin 227.594444444444
 T23/3
RD_{tf} and Tf are within range, continue
 γ_x and T_x are within range, continue
 T23/4
 γ_x for Fluid 1 RD_{tf} for Fluid 1 0.716864897522
 γ_x for Fluid 2 RD_{tf} for Fluid 2 0.738661816297
 T23/5
Reference Fluid 1 Reference Fluid 1 n-Hexane
Reference Fluid 2 Reference Fluid 2 n-Heptane
 $T_{r,x}$ for Fluid 1 $T_{r,x}$ for Fluid 1 0.448594549018
 $T_{r,x}$ for Fluid 2 $T_{r,x}$ for Fluid 2 0.421354150596
 $T_{r,60}$ for Fluid 1 $T_{r,60}$ for Fluid 1 0.569046132957
 $T_{r,60}$ for Fluid 2 $T_{r,60}$ for Fluid 2 0.534491447849
 T23/6
 γ_x observed is outside the boundary of the standard
 γ_x observed is outside the correlation range of the standard
RD_{tf} observed is greater than Fluid 2 RD_{tf}, no solution

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Example 23/18 – Observed Temperature ($T_{23/3}, T_f$) T_f = Lower Range Limit

Input Data

Relative density @ obs. temp. (γ_x) ..	Relative density @ obs. temp.	0.5
Observed temperature, °F (T_o) ..	Observed temperature T_f , °F	50.8

Computed Data – last digit is rounded

T23/1	Input Data – rounded	
γ_x , observed rel. density	RD f , observed rel. density	0.5000
T_o , °F	T_f , °F	50.8

T23/2

T_x , Kelvin	T_x , Kelvin	227.15000000000
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T23/3

RD f and T_f are within range, continue γ_x and T_f are within range, continue

T23/4

γ_x for Fluid 1	RD f for Fluid 1	0.485962637468
γ_x for Fluid 2	RD f for Fluid 2	0.528232774666

T23/5

Reference Fluid 1	Reference Fluid 1	Ethane
Reference Fluid 2	Reference Fluid 2	EP (65/35)
$T_{r,x}$ for Fluid 1	$T_{r,x}$ for Fluid 1	0.743949169751
$T_{r,x}$ for Fluid 2	$T_{r,x}$ for Fluid 2	0.680762429946
$T_{r,60}$ for Fluid 1	$T_{r,60}$ for Fluid 1	0.945552535144
$T_{r,60}$ for Fluid 2	$T_{r,60}$ for Fluid 2	0.865242771467

T23/6

Upper boundary $\gamma_{60,high}$	Upper boundary RD $60,high$	0.429277000000
Upper boundary $\gamma_{x,high}$	Upper boundary RD $f,high$	0.528232774666
Lower boundary $\gamma_{60,low}$	Lower boundary RD $60,low$	0.355994000000
Lower boundary $\gamma_{x,low}$	Lower boundary RD f,low	0.485962637468

Iteration steps

Pass 1	Pass 2	Pass 3	Iteration steps
Pass 1	Pass 2	Pass 3	
T23/7			
Delta (δ)	Delta	0.332086987697	0
0	0	0.996676046418	0
$\gamma_{60,mid}$	RD $60,mid$	0.380330330719	0
0	0	0.389195295035	0
Ctl	CTL	1.301530344004	1.284969011460
1.284702066298			
RD $f_{\gamma_{x,mid}}$	mid	0.495011466176	0
0	0	0.499999999725	0
T23/8	Continue	Continue	Continue – T23/8
Continue	Continue	Continue	

T23/9

Alpha (α)	Alpha	0.073283000000	0
0.000	1.515307654763e-04	0	0.011401775368
Beta (β)	Beta	0.042870179217	0
0.0000	9.04641913088e-05	0	0.006504743146
Phi (φ)	Phi	4.671337977889	671337977889.1.33253945
1.003338101716			
A	A	-28.769572088869	-769572088869
16.984940231986		-19.740869990631	-740869990631
B	B	30.911650589439	911650589439
21.419561059033	419561059033	18.658299106732	

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<i>C</i>	<i>C</i>	7. 871700166414	871700166414	-
5. 385367233142	385367233142-4.	693719199874		
<i>y₆₀.Trial</i>	<i>RD60, Trial</i>	0. 391732106088	0	0. 389195798716
0	0	0	0	0
<i>C_L.Trial</i>	<i>GTL, Trial</i>	1. 280310496169	280310496169	1. 280310496171
284701177082	1. 284702065485			
<i>RDTE_{fx}.Trial</i>	<i>Trial</i>	0. 501538727110	0	0. 500000300726
0	0	0	0	0
T23/10	Continue	Continue	Converged	
T23/10	Continue	Continue	Converged	
T23/11	Reset boundaries			
<i>RDTE_{fx}.high</i>	<i>high</i>	0. 501538727110	0	0. 500000300726
<i>y₆₀.high</i>	<i>RD60, high</i>	0. 391732106088	0	0. 389195798716
<i>RDTE_{fx}.low</i>	<i>low</i>	0. 495011466176	0	0. 499900828404
<i>y₆₀.low</i>	<i>RD60, low</i>	0. 380330330719	0	0. 38904167951
T23/12				
<i>y₆₀ (y₆₀.Trial rounded)</i>	<i>RD60 - (RD60, Trial rounded)</i>			

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Example 23/19 – Observed Temperature ($T_{23/3}$, T_f) $T_f <$ Lower Range Limit

Input Data
 γ_x , relative density @ obs. temp. (γ_x) ... Relative density @ obs. temp. 0.5
 Observed temperature, °F (T_f) Observed temperature T_f , °F 50.9
 Computed Data – last digit is rounded
 T23/1
 Input Data – rounded
 γ_x , observed rel. density RD T_f , observed rel. density 0.5000
 T_f , °F T_f , °F 50.9
 T23/2
 T_x , Kelvin T_x , Kelvin 227.094444444444

T23/3
 T_x is outside the input range of the standard less than 227.15, no solution

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5.2 CTL (Table 54) and Density (Table 53) for NGL and LPG using a 15°C Base Temperature

5.2.1 Implementation Procedure for Table 54E (15°C Basis)

This section presents the implementation procedure T54 for the computation of Temperature Correction Factor, C_{TL} . The C_{TL} is used to calculate volumes of fluid at the base temperature from volumes at some known temperature. The fluids are characterized by the specification of density at the base temperature, 15°C.

5.2.1.1 Inputs and Outputs

Inputs: Density at 15°C, ρ_{15} (kg/m^3)
Observed temperature, T_F ($^\circ\text{C}$)

Output: Temperature Correction Factor, C_{TL} (from T_F to T_B)

5.2.1.2 Outline of Calculations

The calculations are performed using an extended two-fluid corresponding states equation. By comparing densities at 60°F, two reference fluids are selected so that one is slightly more dense and one that is slightly less dense than the observed fluid. The densities of these reference fluids are then scaled to the observed reduced temperature (reduced by the critical temperature of the fluid of interest). The Temperature Correction Factor is then computed from the reference fluid densities. See Figure 3 for a general flow chart of the calculation procedure.

5.2.1.3 T54 Implementation Procedure

<u>T54/Step Number</u>	<u>Operation/Procedure at that step</u>
T54/1:	Round the density ρ_{15} to the nearest 0.1 and round the observed temperature T_F to the nearest 0.05°C.
T54/2:	Convert the rounded observed temperature to units of Kelvin, T_x :
$T_x = T_F + 273.15$	
T54/3:	The resultant temperature T_x and density ρ_{15} must fall within the following boundariesranges :
Temperature between 227.15 and 366.15 K, inclusive (equivalent to -46 to 93°C, or -50.8 to 199.4°F)	

Density between 351.7 and 687.8 kg/m³ inclusive

If these values do not fall in these ranges, then the standard does not apply. Flag this result (return a -1 for C_{TL}) and exit this procedure.

Note: The density boundaries_ranges tested in this step slightly exceed the boundaries_ranges used within the T24 implementation procedure (0.3500 to 0.6880 relative density at 60°F) that act as the true limits for this method.

- T54/4: Convert the 15°C density to relative density, relative to the density of water at 60°F

$$\gamma_{TB} = \frac{\rho_{15}}{\rho_{w60}}$$

At the time of the writing of this standard, the value for the relative absolute density of water at 60°F (ρ_{w60}) was 999.016 kg/m³. This was the value used for ρ_{w60} in the examples. Refer to API MPMS Chapter 11.4.1 for the most current value of ρ_{w60} .

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- T54/5: Use the procedure described in Section 5.1.2 for Table 23 to compute a relative density at 60°F from the known relative density at 15°C. Enter the procedure at Step T23/4 so as to avoid additional rounding of the input values. Inputs to implementation procedure T23 are the values of T_{BK} and γ_{TB} , where T_{BK} is the base temperature 15°C in Kelvin (288.15 K) and γ_{TB} is the density at the base temperature 15°C. Implementation procedure T23 is exited after Step T23/11 so as not to round the output values. The converged output from Step T23/11 is γ_{60} .

- T54/6: The resultant density γ_{60} , if it were rounded to the nearest 0.0001, must fall within 0.3500 and 0.6880 inclusive. Test γ_{60} to ensure it is within the following boundaries:

Relative density greater than or equal to 0.34995 and less than 0.68805

If the relative density does not fall in this range, then the standard does not apply. Flag this result (return a -1 for C_{TL}) and exit this procedure.

- T54/7: Use the procedure described in Section 5.1.1 for Table 24 to compute the Temperature Correction Factor (C_{TL1}) from 60°F to the observed temperature, T_x . This step provides the factor used to reduce an observed volume at T_x to a volume at 60°F when the relative density at 60°F, γ_{60} , is known. Enter implementation procedure T24 with T_x and γ_{60} at Step T24/4 to avoid double rounding of the inputs. On exit skip Step T24/14 to avoid rounding the output, C_{TL1} .

By definition:

$$C_{TL1} = \frac{V_{60}}{V_{Tx}} = \frac{\gamma_{Tx}}{\gamma_{60}}$$

- T54/8: Use the procedure described in Section 5.1.1 for Table 24 to compute the Temperature Correction Factor (C_{TL2}) from 60°F to the new base temperature 15°C. This step provides the factor used to reduce an observed volume at 15°C to a volume at 60°F if the relative density at 60°F, γ_{60} , is known. Enter implementation procedure T24 at Step T24/4 to avoid double rounding of the inputs. The inputs are T_{BK} and γ_{60} , where T_{BK} is the base temperature 15°C in Kelvin (288.15 K). On exit skip Step T24/14 to avoid rounding of the output C_{TL2} .

By definition:

$$C_{TL2} = \frac{V_{60}}{V_{15}} = \frac{\gamma_{TB}}{\gamma_{60}}$$

- T54/9: Compute the desired C_{TL} to reduce volume from the observed temperature, T_F , to the base condition of 15°C. The defining formulas show that the calculation is made by computing the ratio C_{TL1}/C_{TL2} .

$$\frac{C_{TL1}}{C_{TL2}} = \frac{\left(\frac{V_{60}}{V_{Tx}} \right)}{\left(\frac{V_{60}}{V_{15}} \right)} = \frac{V_{15}}{V_{Tx}}$$

$$C_{TL} = \frac{V_{15}}{V_{Tx}} = \frac{\gamma_{Tx}}{\gamma_{15}}$$

- T54/10: Perform error check to ascertain that only positive C_{TL} is used. If C_{TL} is less than or equal to 0, set an error flag (such as $C_{TL} = -1$) and quit.

- T54/11: Round the Temperature Correction Factor C_{TL} to the nearest 0.00001.

Enter density in kg/m³ @ 15°C, ρ_{15}
and observed temperature in °C, T_F

Set Table Limits
 $\rho_{15,\min} = 351.7 \text{ kg/m}^3$ $\rho_{15,\max} = 687.8 \text{ kg/m}^3$
 $T_{x,\min} = 227.15 \text{ K}$ $T_{x,\max} = 366.15 \text{ K}$
 $\gamma_{60,\min} = 0.34995$ $\gamma_{60,\max} = 0.68805$

Round ρ_{15} to ± 0.1
and T_F to ± 0.05

Calculate absolute temperature T_x in K

Are T_F & ρ_{15} in range?

No → Error Flag; $C_{TL} = -1$
Exit

Yes

Convert the 15°C density, ρ_{15}
to relative density, γ_{TB}

Compute relative density at 60°F from
known relative density at 15°C using
procedure T23 starting at step T23/4

Is γ_{60} in range?

No → Error Flag; $C_{TL} = -1$
Exit

Yes

Compute C_{TL1} from 60°F to T_x using
procedure T24 starting at step T24/4

Compute C_{TL2} from 60°F to 15°C using
procedure T24 starting at step T24/4

Compute $C_{TL} = C_{TL1}/C_{TL2}$

Is $C_{TL} > 0$?

No → Error Flag; $C_{TL} = -1$
Exit

Yes

Round C_{TL} to ± 0.00001

RETURN C_{TL}

Figure 3. Flow Chart of Implementation Procedure for Table 54

Comment [KF3]: Update Figure Number for addition of Figure 1

5.2.1.4 Examples for Section 5.2.2 (Table 54E)

(See [Table 1](#)[Table 2](#) for properties of the Reference Fluids)

Example 54/1 – Utilize Use EE (68/32) and Ethane

Input Data to Implementation Procedure T54

Density (kg/m^3) @ 15°C ($\rho_{15}\text{Den15}$) 352.59
Observed temperature ($T_x\text{TF}$, $^\circ\text{C}$) -45.020

Computed Data – last digit is rounded

T54/1

Input Data – rounded

$\rho_{15}\text{Den15}$, rounded to 0.1 352.6
 $T_x\text{TF}$, $^\circ\text{C}$, rounded to 0.05 -45.00

T54/2

$T_x\text{TK}$, Kelvin 228.15

T54/3

$T_x\text{TK}$ and $\rho_{15}\text{Den15}$ are within range, continue

T54/4

$\rho_{15}\text{Den15}$ relative to 60°F water 0.352947300143

T54/5, Call Table 23 procedure to obtain relative density at 60°F

$\gamma_{60}\text{RD60}$ from Table 23 0.350947981104

T54/6

$\gamma_{60}\text{RD60}$ is within range, continue

T54/7, Call Table 24 Procedure with $T_x\text{TK}$ and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 EE (68/32)

Reference Fluid 2 Reference Fluid 2 Ethane

C_{TL} , $T_x\text{TK}$ to 60°F 1.374246650548

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T54/8, Call Table 24 Procedure with 15°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 EE (68/32)

Reference Fluid 2 Reference Fluid 2 Ethane

C_{TL} , 15°C to 60°F 1.005696910034

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T54/9 $C_{TL\text{CTL}} = C_{TL1\text{CTL1}}/C_{TL2\text{CTL2}}$

C_{TL} , $T_x\text{TK}$ to 15°C 1.366462039245

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T54/10

$C_{TL\text{CTL}}$ is positive, continue

T54/11 $C_{TL\text{CTL}}$ rounded

$C_{TL\text{CTL}}$ (rounded) 1.36646

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Example 54/2 – Utilize Use Ethane and EP (65/35)

Input Data to Implementation Procedure T54

Density (kg/m³) @ 15°C ($\rho_{15}\text{Den15}$) . 399.55
Observed temperature T_{xT} , °C -3.920

Computed Data – last digit is rounded

T54/1

Input Data – rounded

$\rho_{15}\text{Den15}$, rounded to 0.1 399.6
 T_{xT} , °C, rounded to 0.05 -3.90

T54/2
 T_{xT} , Kelvin 269.25
T54/3

T_{xT} and $\rho_{15}\text{Den15}$ are within range, continue
T54/4

$\rho_{15}\text{Den15}$ relative to 60°F water 0.399993593696

T54/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60}\text{RD60}$ from Table 23 0.398679750427

T54/6

$\gamma_{60}\text{RD60}$ is within range, continue

T54/7, Call Table 24 Procedure with T_{xT} and $\gamma_{60}\text{RD60}$
Reference Fluid 1 Reference Fluid 1 Ethane
Reference Fluid 2 Reference Fluid 2 EP (65/35)
 $C_{TL}\text{CTL}_1$, T_{xT} to 60°F 1.101743247711

T54/8, Call Table 24 Procedure with 15°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 Ethane
Reference Fluid 2 Reference Fluid 2 EP (65/35)
 $C_{TL}\text{CTL}_2$, 15°C to 60°F 1.003295485330

T54/9 $C_{TL}\text{CTL} = C_{TL}\text{CTL}_1 / C_{TL}\text{CTL}_2$
 $C_{TL}\text{CTL}$, T_{xT} to 15°C 1.098124394877

T54/10

$C_{TL}\text{CTL}$ is positive, continue

T54/11 $C_{TL}\text{CTL}$ rounded
 $C_{TL}\text{CTL}$ (rounded) 1.09812

Example 54/3 – Utilize Use EP (65/35) and EP (35/65)

Input Data to Implementation Procedure T54

Density (kg/m^3) @ 15°C ($\rho_{15}\text{Den15}$) . 451.09
Observed temperature T_{xTx} , $^\circ\text{C}$ 30.774

Computed Data – last digit is rounded

T54/1

Input Data – rounded

$\rho_{15}\text{Den15}$, rounded to 0.1 451.1
 T_{xTx} , $^\circ\text{C}$, rounded to 0.05 30.75

T54/2

T_{xTx} , Kelvin 303.90

T54/3

T_{xTx} and $\rho_{15}\text{Den15}$ are within range, continue

T54/4

$\rho_{15}\text{Den15}$ relative to 60°F water 0.451544319610

T54/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60}\text{RD60}$ from Table 23 0.450522856945

T54/6

$\gamma_{60}\text{RD60}$ is within range, continue

T54/7, Call Table 24 Procedure with T_{xTx} and $\gamma_{60}\text{RD60}$

Reference Fluid 1	Reference Fluid 1	EP (65/35)
Reference Fluid 2	Reference Fluid 2	EP (35/65)

$C_{T1}\text{CTL1}$, T_{xTx} to 60°F 0.932384171290

T54/8, Call Table 24 Procedure with 15°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1	Reference Fluid 1	EP (65/35)
Reference Fluid 2	Reference Fluid 2	EP (35/65)

$C_{T2}\text{CTL2}$, 15°C to 60°F 1.002267286478

T54/9 $C_{T1}\text{CTL} = C_{T1}\text{CTL1}/C_{T2}\text{CTL2}$
 $C_{T1}\text{CTL}$, T_{xTx} to 15°C 0.930274971427

T54/10

$C_{T1}\text{CTL}$ is positive, continue

T54/11 $C_{T1}\text{CTL}$ rounded
 $C_{T1}\text{CTL}$ (rounded) 0.93027

Example 54/4 – Utilize Use EP (35/65) and Propane

Input Data to Implementation Procedure T54

Density (kg/m³) @ 15°C ($\rho_{15}\text{Den15}$) . 489.92

Observed temperature T_{xT^F} , °C 84.975

Computed Data – last digit is rounded

T54/1

Input Data – rounded

$\rho_{15}\text{Den15}$, rounded to 0.1 489.9

T_{xT^F} , °C, rounded to 0.05 85.00

T54/2

T_{xT^K} , Kelvin 358.15

T54/3

T_{xT^K} and $\rho_{15}\text{Den15}$ are within range, continue

T54/4

$\rho_{15}\text{Den15}$ relative to 60°F water 0.490382536416

T54/5, Call Table 23 procedure to obtain relative density at 60°F

$\gamma_{60}\text{RD60}$ from Table 23 0.489511777456

T54/6

$\gamma_{60}\text{RD60}$ is within range, continue

T54/7, Call Table 24 Procedure with T_{xT^K} and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 EP (35/65)

Reference Fluid 2 Reference Fluid 2 Propane

$C_{TL}\text{CTL1}$, T_{xT^K} to 60°F 0.608584025858

T54/8, Call Table 24 Procedure with 15°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 EP (35/65)

Reference Fluid 2 Reference Fluid 2 Propane

$C_{TL}\text{CTL2}$, 15°C to 60°F 1.001778832207

T54/9 $C_{TL}\text{CTL} = C_{TL}\text{CTL1}/C_{TL}\text{CTL2}$

$C_{TL}\text{CTL}$, T_{xT^K} to 15°C 0.607503379281

T54/10

$C_{TL}\text{CTL}$ is positive, continue

T54/11 $C_{TL}\text{CTL}$ rounded

$C_{TL}\text{CTL}$ (rounded) 0.60750

Example 54/5 – Utilize Use Propane and i-Butane

Input Data to Implementation Procedure T54

Density (kg/m³) @ 15°C ($\rho_{15}\text{Den15}$) . 539.49
Observed temperature T_{xTx} , °C 68.360

Computed Data – last digit is rounded

T54/1

Input Data – rounded

$\rho_{15}\text{Den15}$, rounded to 0.1 539.5
 T_{xTx} , °C, rounded to 0.05 68.35
T54/2
 T_{xTx} , Kelvin 341.50
T54/3
 T_{xTx} and $\rho_{15}\text{Den15}$ are within range, continue
T54/4

$\rho_{15}\text{Den15}$ relative to 60°F water 0.540031390889

T54/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60}\text{RD60}$ from Table 23 0.539309445177

T54/6

$\gamma_{60}\text{RD60}$ is within range, continue

T54/7, Call Table 24 Procedure with T_{xTx} and $\gamma_{60}\text{RD60}$
Reference Fluid 1 Reference Fluid 1 Propane
Reference Fluid 2 Reference Fluid 2 i-Butane
 $C_{TL1}\text{CTL1}$, T_{xTx} to 60°F 0.850308225942

T54/8, Call Table 24 Procedure with 15°C and $\gamma_{60}\text{RD60}$
Reference Fluid 1 Reference Fluid 1 Propane
Reference Fluid 2 Reference Fluid 2 i-Butane
 $C_{TL2}\text{CTL2}$, 15°C to 60°F 1.001338650108

T54/9 $C_{TL}\text{CTL} = C_{TL1}\text{CTL1}/C_{TL2}\text{CTL2}$
 $C_{TL}\text{CTL}$, T_{xTx} to 15°C 0.849171482446

T54/10

$C_{TL}\text{CTL}$ is positive, continue

T54/11 $C_{TL}\text{CTL}$ rounded
 $C_{TL}\text{CTL}$ (rounded) 0.84917

Example 54/6 – Utilize Use i-Butane and n-Butane

Input Data to Implementation Procedure T54

Density (kg/m³) @ 15°C ($\rho_{15}\text{Den15}$) . 569.42

Observed temperature T_{Tx} , °C -16.090

Computed Data – last digit is rounded

T54/1

Input Data – rounded

$\rho_{15}\text{Den15}$, rounded to 0.1 569.4

T_{Tx} , °C, rounded to 0.05 -16.10

T54/2

T_{Tx} , Kelvin 257.05

T54/3

T_{Tx} and $\rho_{15}\text{Den15}$ are within range, continue

T54/4

$\rho_{15}\text{Den15}$ relative to 60°F water 0.569960841468

T54/5, Call Table 23 procedure to obtain relative density at 60°F

$\gamma_{60}\text{RD60}$ from Table 23 0.569305082960

T54/6

$\gamma_{60}\text{RD60}$ is within range, continue

T54/7, Call Table 24 Procedure with T_{Tx} and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 i-Butane

Reference Fluid 2 Reference Fluid 2 n-Butane

$C_{T1}\text{CTL1}$, T_{Tx} to 60°F 1.062511014737

T54/8, Call Table 24 Procedure with 15°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 i-Butane

Reference Fluid 2 Reference Fluid 2 n-Butane

$C_{T2}\text{CTL2}$, 15°C to 60°F 1.001151857830

T54/9 $C_{T1}\text{CTL} = C_{T1}\text{CTL1}/C_{T2}\text{CTL2}$

$C_{T1}\text{CTL}$, T_{Tx} to 15°C 1.061288561198

T54/10

$C_{T1}\text{CTL}$ is positive, continue

T54/11

$C_{T1}\text{CTL}$ rounded

$C_{T1}\text{CTL}$ (rounded) 1.06129

Example 54/7 – Utilize Use n-Butane and i-Pentane

Input Data to Implementation Procedure T54

Density (kg/m³) @ 15°C ($\rho_{15}\text{Den15}$) . 599.37
Observed temperature T_{xTx} , °C 43.360

Computed Data – last digit is rounded

T54/1

Input Data – rounded

$\rho_{15}\text{Den15}$, rounded to 0.1 599.4
 T_{xTx} , °C, rounded to 0.05 43.35

T54/2

T_{xTx} , Kelvin 316.50

T54/3

T_{xTx} and $\rho_{15}\text{Den15}$ are within range, continue

T54/4

$\rho_{15}\text{Den15}$ relative to 60°F water 0.599990390544

T54/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60}\text{RD60}$ from Table 23 0.599396660576

T54/6

$\gamma_{60}\text{RD60}$ is within range, continue

T54/7, Call Table 24 Procedure with T_{xTx} and $\gamma_{60}\text{RD60}$

Reference Fluid 1	Reference Fluid 1	n-Butane
Reference Fluid 2	Reference Fluid 2	i-Pentane

$C_{TL1}\text{CTL1}$, T_{xTx} to 60°F 0.948276855780

T54/8, Call Table 24 Procedure with 15°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1	Reference Fluid 1	n-Butane
Reference Fluid 2	Reference Fluid 2	i-Pentane

$C_{TL2}\text{CTL2}$, 15°C to 60°F 1.000990546173

T54/9 $C_{TL}\text{CTL} = C_{TL1}\text{CTL1}/C_{TL2}\text{CTL2}$
 $C_{TL}\text{CTL}$, T_{xTx} to 15°C 0.947338473281

T54/10

$C_{TL}\text{CTL}$ is positive, continue

T54/11 $C_{TL}\text{CTL}$ rounded
 $C_{TL}\text{CTL}$ (rounded) 0.94734

Example 54/8 – Utilize Use i-Pentane and n-Pentane

Input Data to Implementation Procedure T54

Density (kg/m³) @ 15°C ($\rho_{15}\text{Den15}$) . 624.42
Observed temperature T_{TF} , °C 76.650

Computed Data – last digit is rounded

T54/1

Input Data – rounded

$\rho_{15}\text{Den15}$, rounded to 0.1 624.4
 T_{TF} , °C, rounded to 0.05 76.65

T54/2

T_{Tx} , Kelvin 349.80

T54/3

T_{Tx} and $\rho_{15}\text{Den15}$ are within range, continue

T54/4

$\rho_{15}\text{Den15}$ relative to 60°F water 0.625015014775

T54/5, Call Table 23 procedure to obtain relative density at 60°F

$\gamma_{60}\text{RD60}$ from Table 23 0.624458073820

T54/6

$\gamma_{60}\text{RD60}$ is within range, continue

T54/7, Call Table 24 Procedure with T_{Tx} and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 i -Pentane

Reference Fluid 2 Reference Fluid 2 n-Pentane

$C_{TL}\text{CTL1}$, T_{Tx} to 60°F 0.893460003018

T54/8, Call Table 24 Procedure with 15°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 i -Pentane

Reference Fluid 2 Reference Fluid 2 n-Pentane

$C_{TL}\text{CTL2}$, 15°C to 60°F 1.000891878859

T54/9 $C_{TL}\text{CTL} = C_{TL}\text{CTL1}/C_{TL}\text{CTL2}$

$C_{TL}\text{CTL}$, T_{Tx} to 15°C 0.892663854998

T54/10

$C_{TL}\text{CTL}$ is positive, continue

T54/11 $C_{TL}\text{CTL}$ rounded

$C_{TL}\text{CTL}$ (rounded) 0.89266

Example 54/9 – Utilize n-Pentane and i-Hexane

Input Data to Implementation Procedure T54

Density (kg/m³) @ 15°C ($\rho_{15}\text{Den15}$) . 639.41
Observed temperature T_{xTx} , °C -24.460

Computed Data – last digit is rounded

T54/1

Input Data – rounded

$\rho_{15}\text{Den15}$, rounded to 0.1 639.4
 T_{xTx} , °C, rounded to 0.05 -24.45

T54/2

T_{xTx} , Kelvin 248.70

T54/3

T_{xTx} and $\rho_{15}\text{Den15}$ are within range, continue

T54/4

$\rho_{15}\text{Den15}$ relative to 60°F water 0.640029789313

T54/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60}\text{RD60}$ from Table 23 0.639504496457

T54/6

$\gamma_{60}\text{RD60}$ is within range, continue

T54/7, Call Table 24 Procedure with T_{xTx} and $\gamma_{60}\text{RD60}$

Reference Fluid 1	Reference Fluid 1	n-Pentane
Reference Fluid 2	Reference Fluid 2	i-Hexane

$C_{T1}\text{CTL1}$, T_{xTx} to 60°F 1.057426821739

T54/8, Call Table 24 Procedure with 15°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1	Reference Fluid 1	n-Pentane
Reference Fluid 2	Reference Fluid 2	i-Hexane

$C_{T2}\text{CTL2}$, 15°C to 60°F 1.000821406041

T54/9 $C_{T1}\text{CTL} = C_{T1}\text{CTL1}/C_{T2}\text{CTL2}$
 $C_{T1}\text{CTL}$, T_{xTx} to 15°C 1.056558957827

T54/10

$C_{T1}\text{CTL}$ is positive, continue

T54/11 $C_{T1}\text{CTL}$ rounded
 $C_{T1}\text{CTL}$ (rounded) 1.05656

Example 54/10 – Utilize Use i-Hexane and n-Hexane

Input Data to Implementation Procedure T54

Density (kg/m³) @ 15°C ($\rho_{15}\text{Den15}$) . 659.38

Observed temperature $T_{15^{\circ}\text{F}}$, °C 80.580

Computed Data – last digit is rounded

T54/1

Input Data – rounded

$\rho_{15}\text{Den15}$, rounded to 0.1 659.4

$T_{15^{\circ}\text{F}}$, °C, rounded to 0.05 80.60

T54/2

$T_{15^{\circ}\text{F}}$, Kelvin 353.75

T54/3

$T_{15^{\circ}\text{F}}$ and $\rho_{15}\text{Den15}$ are within range, continue

T54/4

$\rho_{15}\text{Den15}$ relative to 60°F water 0.660049488697

T54/5, Call Table 23 procedure to obtain relative density at 60°F

$\gamma_{60}\text{RD60}$ from Table 23 0.659551831579

T54/6

$\gamma_{60}\text{RD60}$ is within range, continue

T54/7, Call Table 24 Procedure with $T_{15^{\circ}\text{F}}$ and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 i-Hexane

Reference Fluid 2 Reference Fluid 2 n-Hexane

$C_{TL}\text{CTL1}$, $T_{15^{\circ}\text{F}}$ to 60°F 0.905892081483

T54/8, Call Table 24 Procedure with 15°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 i-Hexane

Reference Fluid 2 Reference Fluid 2 n-Hexane

$C_{TL}\text{CTL2}$, 15°C to 60°F 1.000754538301

T54/9 $C_{TL}\text{CTL} = C_{TL}\text{CTL1}/C_{TL}\text{CTL2}$

$C_{TL}\text{CTL}$, $T_{15^{\circ}\text{F}}$ to 15°C 0.905209066572

T54/10

$C_{TL}\text{CTL}$ is positive, continue

T54/11 $C_{TL}\text{CTL}$ rounded

$C_{TL}\text{CTL}$ (rounded) 0.90521

Example 54/11 – Utilize n-Hexane and n-Heptane

Input Data to Implementation Procedure T54

Density (kg/m³) @ 15°C ($\rho_{15}\text{Den15}$) . 669.38
Observed temperature T_{xTx} , °C 82.790

Computed Data – last digit is rounded

T54/1

Input Data – rounded

$\rho_{15}\text{Den15}$, rounded to 0.1 669.4
 T_{xTx} , °C, rounded to 0.05 82.80

T54/2

T_{xTx} , Kelvin 355.95

T54/3

T_{xTx} and $\rho_{15}\text{Den15}$ are within range, continue

T54/4

$\rho_{15}\text{Den15}$ relative to 60°F water 0.670059338389

T54/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60}\text{RD60}$ from Table 23 0.669573371528

T54/6

$\gamma_{60}\text{RD60}$ is within range, continue

T54/7, Call Table 24 Procedure with T_{xTx} and $\gamma_{60}\text{RD60}$

Reference Fluid 1	Reference Fluid 1	n-Hexane
Reference Fluid 2	Reference Fluid 2	n-Heptane

$C_{TL1}\text{CTL1}$, T_{xTx} to 60°F 0.907185481500

T54/8, Call Table 24 Procedure with 15°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1	Reference Fluid 1	n-Hexane
Reference Fluid 2	Reference Fluid 2	n-Heptane

$C_{TL2}\text{CTL2}$, 15°C to 60°F 1.000725785828

T54/9 $C_{TL}\text{CTL} = C_{TL1}\text{CTL1}/C_{TL2}\text{CTL2}$
 $C_{TL}\text{CTL}$, T_{xTx} to 15°C 0.906527536662

T54/10

$C_{TL}\text{CTL}$ is positive, continue

T54/11 $C_{TL}\text{CTL}$ rounded

$C_{TL}\text{CTL}$ (rounded) 0.90653

Example 54/12 – Reduced Temperature (T_{rx}) Greater Than 1.0

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Input Data to Implementation Procedure T54

Density (kg/m³) @ 15°C ($\rho_{15}Den15$) . 399.83Observed temperature T_{rx} , °C 90.570

Computed Data – last digit is rounded

T54/1

Input Data – rounded

 $\rho_{15}Den15$, rounded to 0.1 399.8 T_{rx} , °C, rounded to 0.05 90.55

T54/2

 T_{rx} , Kelvin 363.70

T54/3

 T_{rx} and $\rho_{15}Den15$ are within range, continue

T54/4

 $\rho_{15}Den15$ relative to 60°F water 0.400193790690

T54/5, Call Table 23 procedure to obtain relative density at 60°F

 $\gamma_{60}RD60$ from Table 23 0.398881468881

T54/6

 $\gamma_{60}RD60$ is within range, continueT54/7, Call Table 24 Procedure with T_{rx} and $\gamma_{60}RD60$

Reference Fluid 1 Reference Fluid 1 Ethane

Reference Fluid 2 Reference Fluid 2 EP (65/35)

Reduced temperature T_{rx} input data greater than 1.0, no solution is outside the correlation range of the standard $C_{TL}CTL4$, T_{rx} to 60°F -1.0

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Value from Table 24 not valid, no solution is outside the correlation range of the standard

Example 54/13 – Observed Temperature (T_{FT}) < Lower Range Limit**Formatted:** Font: Bold

Input Data to Implementation Procedure T54

Density (kg/m³) @ 15°C ($\rho_{15}Den15$) . 449.56
Observed temperature T_{FT} , °C -46.030

Computed Data – Last digit is rounded

T54/1

Input Data – rounded

$\rho_{15}Den15$, rounded to 0.1 449.6
 T_{FT} , °C, rounded to 0.05 -46.05

T54/2

T_{FK} , Kelvin 227.10

T54/3

~~Tx – Input data is outside the range of the standard less than 227.15, no solution~~

Example 54/14 – Density at 15°C (ρ_{15}) < Lower Range Limit

Input Data to Implementation Procedure T54

Density (kg/m³) @ 15°C (ρ_{15}) . 349.59

Observed temperature T_{TF} , °C 4.440

Computed Data – last digit is rounded

T54/1

Input Data – rounded

ρ_{15} , rounded to 0.1 349.6

T_{TF} , °C, rounded to 0.05 4.45

T54/2

T_{TK} , Kelvin 277.60

T54/3

Density input data is outside the range of the standard less than 351.7, no solution

Example 54/15 – Observed Temperature (T_{FT}) > Upper Range Limit**Formatted:** Font: Bold

Input Data to Implementation Procedure T54
Density (kg/m³) @ 15°C ($\rho_{15}Den15$) . 449.56
Observed temperature T_{FT} , °C 93.030
Computed Data – last digit is rounded
T54/1
Input Data – rounded
 $\rho_{15}Den15$, rounded to 0.1 449.6
 T_{FT} , °C, rounded to 0.05 93.05
T54/2
 T_{FK} , Kelvin 366.20
T54/3
~~| Tx-Input data is outside the range of the standard greater than 366.15, no solution~~

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Example 54/16 – Density at 15°C (ρ_{15}) > Upper Range Limit

Input Data to Implementation Procedure T54

Density (kg/m³) @ 15°C (ρ_{15}) . 687.85

Observed temperature T_{TF} , °C -17.780

Computed Data – last digit is rounded

T54/1

Input Data – rounded

ρ_{15} , rounded to 0.1 687.9

T_{TF} , °C, rounded to 0.05 -17.80

T54/2

T_{TK} , Kelvin 255.35

T54/3

ρ_{15} input data is outside the range of the standard greater than 687.8, no solution

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Example 54/17 – Observed Temperature (T_{FTF}) &and Density at 15°C ($\rho_{15}Den15$) = Upper range Boundary Limits

Input Data to Implementation Procedure T54

Density (kg/m³) @ 15°C ($\rho_{15}Den15$) . 687.84
Observed temperature T_{FTF} , °C 93.020

Computed Data – Last digit is rounded

T54/1

Input Data – rounded

$\rho_{15}Den15$, rounded to 0.1 687.8
 T_{FTF} , °C, rounded to 0.05 93.00

T54/2

T_{FTF} , Kelvin 366.15

T54/3

T_{FTF} and $\rho_{15}Den15$ are within range, continue

T54/4

$\rho_{15}Den15$ relative to 60°F water 0.688477461822

T54/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60}RD60$ from Table 23 0.688010661267

T54/6

$\gamma_{60}RD60$ is within range, continue

T54/7, Call Table 24 Procedure with T_{FTF} and $\gamma_{60}RD60$

Reference Fluid 1	Reference Fluid 1 n-Hexane
Reference Fluid 2	Reference Fluid 2 n-Heptane

$C_{TL1}CTL1$, T_{FTF} to 60°F 0.900470590102

T54/8, Call Table 24 Procedure with 15°C and $\gamma_{60}RD60$

Reference Fluid 1	Reference Fluid 1 n-Hexane
Reference Fluid 2	Reference Fluid 2 n-Heptane

$C_{TL2}CTL2$, 15°C to 60°F 1.000678478666

T54/9 $C_{TL}CTL = C_{TL1}CTL1 / C_{TL2}CTL2$ 0.899860054252
 $C_{TL}CTL$, T_{FTF} to 15°C 0.899860054252

T54/10

$C_{TL}CTL$ is positive, continue

T54/11 $C_{TL}CTL$ rounded 0.89986

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Example 54/18 – Observed Temperature (T_{TF}) &and Density at 15°C (ρ_{15}) ρ_{15} = Lower range Boundary Limits

Input Data to Implementation Procedure T54

Density (kg/m³) @ 15°C (ρ_{15}) . 351.67
Observed temperature T_{TF} , °C -46.020

Computed Data – last digit is rounded

T54/1

Input Data – rounded

ρ_{15} ρ_{15} , rounded to 0.1 351.7
 T_{TF} , °C, rounded to 0.05 -46.00

T54/2

T_{TF} , Kelvin 227.15

T54/3

T_{TF} and ρ_{15} ρ_{15} are within range, continue

T54/4

ρ_{15} ρ_{15} relative to 60°F water 0.352046413671

T54/5, Call Table 23 procedure to obtain relative density at 60°F

γ_{60} γ_{60} from Table 23 0.350027377993

T54/6

γ_{60} γ_{60} is within range, continue

T54/7, Call Table 24 Procedure with T_{TF} and γ_{60} γ_{60}

Reference Fluid 1 Reference Fluid 1 EE (68/32)

Reference Fluid 2 Reference Fluid 2 Ethane

C_{TL} C_{TL} , T_{TF} to 60°F 1.381296917892

T54/8, Call Table 24 Procedure with 15°C and γ_{60} γ_{60}

Reference Fluid 1 Reference Fluid 1 EE (68/32)

Reference Fluid 2 Reference Fluid 2 Ethane

C_{TL} C_{TL} , 15°C to 60°F 1.005768222160

T54/9 C_{TL} C_{TL} = C_{TL} C_{TL} 1/ C_{TL} C_{TL} 2

C_{TL} C_{TL} , T_{TF} to 15°C 1.373374985865

T54/10

C_{TL} C_{TL} is positive, continue

T54/11 C_{TL} C_{TL} rounded

C_{TL} C_{TL} (rounded) 1.37337

5.2.2 Implementation Procedure for Table 53E (15°C Basis)

This section presents the implementation procedure T53 for calculating the densities of NGLs and LPGs at [a base condition](#) of 15°C from known measurement temperatures and densities.

Density readings must be corrected for the effect of temperature on the instrument prior to entering the density into the following implementation procedure.

5.2.2.1 Inputs and Outputs

Inputs: Density at observed temperature, ρ_x (kg/m³)
Observed temperature, T_F (°C)

Output: Density at 15°C, ρ_{15} (kg/m³)

5.2.2.2 Outline of Calculations

The calculations are done using an extended two-fluid corresponding states equation. Two reference fluids are found that are slightly denser and slightly less dense than the observed fluid by comparing their densities at the observed temperature. Iteration must be performed to determine the value of the fluid's relative density at 60°F such that when the Temperature Correction Factor is applied, the observed relative density is obtained. The "guessed" value for the fluid's relative density at 60°F is constrained to lie between the relative densities at 60°F of these two reference fluids (as upper and lower bounds). As the iterations progress, these upper and lower bounds are "brought together" based upon intermediate calculations. The relative density at 15°C is then computed from the 60°F relative density by using scaling factors between the properties of the two reference fluids.

See Figure 4 for a general flow chart of the calculation procedure.

5.2.2.3 T53 Implementation Procedure

T53/Step Number Operation/Procedure at that step

T53/1: Round the density ρ_x to the nearest 0.1 and round the observed temperature T_F to the nearest 0.05°C.

T53/2: Convert the rounded observed temperature to units of Kelvin, T_x :

$$T_x = T_F + 273.15$$

T53/3: Convert the density, ρ_x , to relative density, γ_x , relative to the density of water at 60°F:

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$$\gamma_x = \frac{\rho_x}{\rho_{w60}} -$$

At the time of the writing of this standard, the value for the absolute relative density of water at 60°F ($\rho_{w60}\rho_{w60}$) was 999.016 kg/m³. This was the value used for $\rho_{w60}\rho_{w60}$ in the examples. Refer to API MPMS Chapter 11.4.1 for the most current value of $\rho_{w60}\rho_{w60}$.

T53/4: Check the values of temperature and relative density to ensure that they are in the proper range. The observed temperature T_x and relative density γ_x must fall within the following boundariesranges:

Temperature between 227.15 and 366.15 K, inclusive (equivalent to -46 to 93°C, or -50.8 to 199.4°F)

Relative density, if it were rounded to the nearest 0.0001, must fall within 0.2100 and 0.7400 inclusive. Test γ_x to ensure it is within the following boundariesranges:

Relative density greater than or equal to 0.20995 and less than 0.74005

If these values do not fall in these ranges, then the standard does not apply. Flag this result (possibly by returning -1 for the density) and exit this procedure.

T53/5: Compute the relative density at 60°F, γ_{60} , from the temperature and the relative density at the measurement condition, γ_x . Use the procedure described in Section 5.2.1 for Table 23 to perform this step. Enter the procedure with γ_x and T_x at Step T23/4 so as to avoid additional rounding of the input values. Exit after Step T23/11 to avoid rounding the result.

T53/6: Compute the relative density at 15°C, γ_{15} , from the relative density at 60°F. This is performed by using the procedure described in Section 5.1.1 for Table 24. Enter implementation procedure T24 with γ_{60} and $T_x = 288.15$ (e.g. 273.15 + 15.00). Enter at Step T24/4 to avoid double rounding of the inputs. The C_{TL} for the conversion between γ_{60} and γ_{15} will be returned without rounding from Step T24/13. Compute γ_{15} :

$$\gamma_{15} = C_{TL} \times \gamma_{60}$$

T53/7: Insure that only valid values came from Steps T53/5 and T53/6. If the γ_{60} obtained from Section 5.2.1 for Table 23 is greater than -1, then proceed. If not, set the fluid density at 15°C to some flag value such as -1 and quit. If the C_{TL} from Step T53/6 is negative, then set the fluid density at 15°C to the error flag condition and exit this procedure.

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T53/8: Calculate the fluid density at 15°C from the relative density at 15°C.

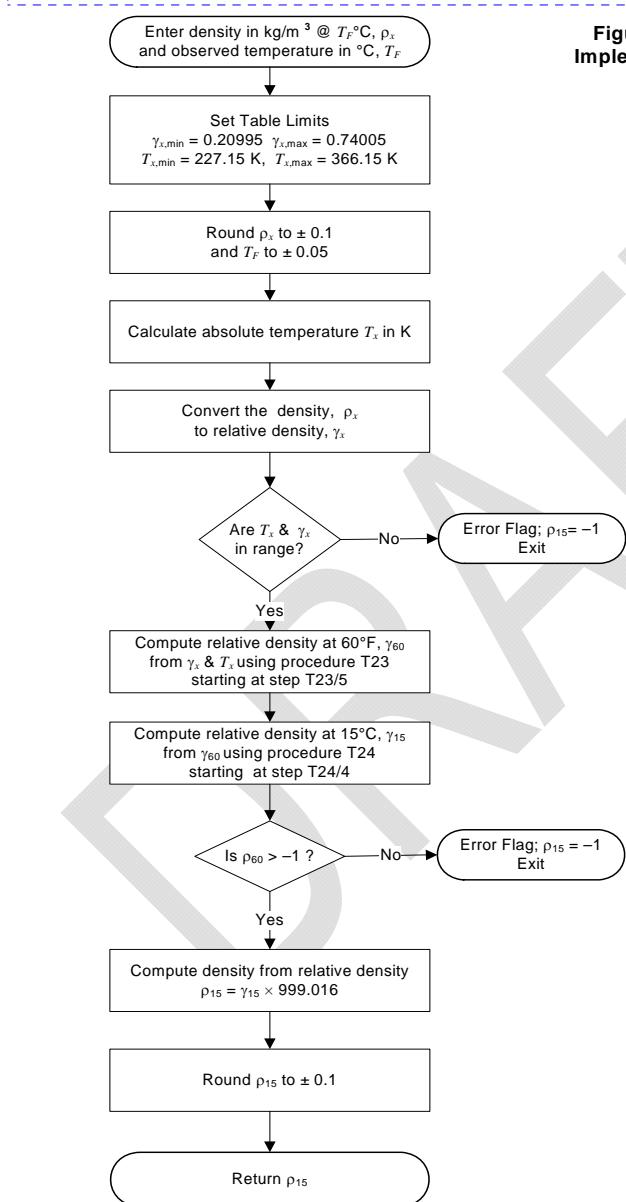
$$\rho_{15} = \gamma_{15} \times 999.016$$

T53/9: Round the fluid density, ρ_{15} , to the nearest 0.1. Exit this procedure.

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Figure 4. Flow Chart of Implementation Procedure for Table 53

Comment [KF4]: Update Figure Number for addition of Figure 1



5.2.2.4 Examples for Section 5.2.2 (Table 53E)

(See [Table 1](#)[Table 2](#) for properties of the Reference Fluids)

Example 53/1 – Utilize Use EP (65/35) & and EP (35/65)

Input Data to Implementation Procedure T53
 Density @ obs. temp. (kg/m^3) 532.57
 Observed Temperature T_{obs} ($^{\circ}\text{C}$) -44.120
 Computed Data – last digit is rounded
 T53/1
 Input Data – rounded
 Density, rounded to 0.1 532.6
 Temperature rounded to 0.05 -44.10
 T53/2
 T_{obs} , Kelvin 229.05
 T53/3
 Density relative to 60° water 0.533124594601
 T53/4
 T_{obs} and relative density are within range, continue
 T53/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60\text{RD60}}$ from Table 23 0.440515294609
 T53/6, Call Table 24 Procedure to obtain $C_{\text{L}, \text{GTI}}$ from 60°F to 15°C
 $C_{\text{L}, \text{GTI}}$ from Table 24 1.002432483838
 Relative density at 15°C 0.441586840944
 T53/7, Values returned from Tables 23 & and 24 valid, continue
 T53/8
 Density at 15 °C (kg/m^3) 441.152319492337
 T53/9
 Density at 15°C (rounded) 441.2

Example 53/2 – Utilize Use n-Pentane &and i-Hexane

Input Data to Implementation Procedure T53
Density @ obs. temp. (kg/m³) 673.66
Observed Temperature T_{obs} (°C) -23.330
Computed Data – last digit is rounded
T53/1
Input Data – rounded
Density, rounded to 0.1 673.7
Temperature rounded to 0.05 -23.35
T53/2
 T_{obs} , Kelvin 249.80
T53/3
Density relative to 60° water 0.674363573757
T53/4
 T_{obs} and relative density are within range, continue
T53/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60\text{RD60}}$ from Table 23 0.638538685930
T53/6, Call Table 24 Procedure to obtain C_L , C_{TL} from 60°F to 15°C
 C_L , C_{TL} from Table 24 1.000825081981
Relative density at 15°C 0.639065532694
T53/7, Values returned from Tables 23 &and 24 valid, continue
T53/8
Density at 15 °C (kg/m³) 638.436692209971
T53/9
Density at 15°C (rounded) 638.4

Example 53/3 – Utilize Use EP (35/65) &and Propane

Input Data to Implementation Procedure T53
Density @ obs. temp. (kg/m³) ... 245.49
Observed Temperature T_{obs} (°C) ... 87.770
Computed Data – last digit is rounded
T53/1
Input Data – rounded
Density, rounded to 0.1 245.5
Temperature rounded to 0.05 87.75
T53/2
 T_{Tx} , Kelvin 360.90
T53/3
Density relative to 60° water ... 0.245741809941
T53/4
 T_{Tx} and relative density are within range, continue
T53/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60\text{RD60}}$ from Table 23 0.488795025411
T53/6, Call Table 24 Procedure to obtain $C_{L\text{ CTL}}$ from 60°F to 15°C
 $C_{L\text{ CTL}}$ from Table 24 1.001786178364
Relative density at 15°C 0.489668100510
T53/7, Values returned from Tables 23 &and 24 valid, continue
T53/8
Density at 15 °C (kg/m³) 489.186267098922
T53/9
Density at 15°C (rounded) 489.2

Example 53/4 – Utilize Use n-Butane &and i-Pentane

Input Data to Implementation Procedure T53
Density @ obs. temp. (kg/m³) 499.55
Observed Temperature T_{obs} (°C) 87.820
Computed Data – last digit is rounded
T53/1
Input Data – rounded
Density, rounded to 0.1 499.6
Temperature rounded to 0.05 87.80
T53/2
 T_{obs} , Kelvin 360.95
T53/3
Density relative to 60° water 0.500092090617
T53/4
 T_{obs} and relative density are within range, continue
T53/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60\text{RD60}}$ from Table 23 0.591794896225
T53/6, Call Table 24 Procedure to obtain C_L , C_{TL} from 60°F to 15°C
 C_L , C_{TL} from Table 24 1.001026475488
Relative density at 15°C 0.592402359180
T53/7, Values returned from Tables 23 &and 24 valid, continue
T53/8
Density at 15 °C (kg/m³) 591.819435258795
T53/9
Density at 15°C (rounded) 591.8

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Example 53/5 – Utilize Use Ethane &and EP (65/35)

Input Data to Implementation Procedure T53
Density @ obs. temp. (kg/m³) ... 395.09
Observed Temperature T_{obs} (°C) ... 15.430
Computed Data – last digit is rounded
T53/1
Input Data – rounded
Density, rounded to 0.1 395.1
Temperature rounded to 0.05 15.45
T53/2
 T_{Tx} , Kelvin 288.60
T53/3
Density relative to 60° water ... 0.395489161335
T53/4
 T_{Tx} and relative density are within range, continue
T53/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60\text{RD60}}$ from Table 23 0.395233433716
T53/6, Call Table 24 Procedure to obtain $C_{L\text{ CTL}}$ from 60°F to 15°C
 $C_{L\text{ CTL}}$ from Table 24 1.003392579214
Relative density at 15°C 0.396574294447
T53/7, Values returned from Tables 23 &and 24 valid, continue
T53/8
Density at 15 °C (kg/m³) 396.184065341566
T53/9
Density at 15°C (rounded) 396.2

Example 53/6 – Utilize Use i-Butane &and n-Butane

Input Data to Implementation Procedure T53
Density @ obs. temp. (kg/m³) 449.59
Observed Temperature T_{obs} (°C) 93.020
Computed Data – last digit is rounded
T53/1
Input Data – rounded
Density, rounded to 0.1 449.6
Temperature rounded to 0.05 93.00
T53/2
 T_{obs} , Kelvin 366.15
T53/3
Density relative to 60° water 0.450042842157
T53/4
 T_{obs} and relative density are within range, continue
T53/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60\text{RD60}}$ from Table 23 0.565490291365
T53/6, Call Table 24 Procedure to obtain C_L , C_{TL} from 60°F to 15°C
 C_L , C_{TL} from Table 24 1.001176265550
Relative density at 15°C 0.566155458114
T53/7, Values returned from Tables 23 &and 24 valid, continue
T53/8
Density at 15 °C (kg/m³) 565.598361142720
T53/9
Density at 15°C (rounded) 565.6

Example 53/7 – Utilize Use i-Hexane &and n-Hexane

Input Data to Implementation Procedure T53
Density @ obs. temp. (kg/m³) ... 600.74
Observed Temperature T_{obs} (°C) ... 80.650
Computed Data – last digit is rounded
T53/1
Input Data – rounded
Density, rounded to 0.1 600.7
Temperature rounded to 0.05 80.65
T53/2
 T_{Tx} , Kelvin 353.80
T53/3
Density relative to 60° water ... 0.601291671004
T53/4
 T_{Tx} and relative density are within range, continue
T53/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60\text{RD60}}$ from Table 23 0.662699711760
T53/6, Call Table 24 Procedure to obtain $C_{L\text{ CTL}}$ from 60°F to 15°C
 $C_{L\text{ CTL}}$ from Table 24 1.000745797303
Relative density at 15°C 0.663193951418
T53/7, Values returned from Tables 23 &and 24 valid, continue
T53/8
Density at 15 °C (kg/m³) 662.541368569934
T53/9
Density at 15°C (rounded) 662.5

Example 53/8 – Calculated Relative Density @ 60°F (γ_{60}) RD60 Near 0.6880 Upper Boundary Limit Using N-Hexane &and N-Heptane

Input Data to Implementation Procedure T53
Density @ obs. temp. (kg/m³) 736.80
Observed Temperature T_{obs} (°C) -44.230
Computed Data – last digit is rounded
T53/1
Input Data – rounded
Density, rounded to 0.1 736.8
Temperature rounded to 0.05 -44.25
T53/2
 T_{obs} , Kelvin 228.90
T53/3
Density relative to 60° water 0.737525725314
T53/4
 T_{obs} and relative density are within range, continue
T53/5, Call Table 23 procedure to obtain relative density at 60°F
 γ_{60} RD60 from Table 23 0.687974688885
T53/6, Call Table 24 Procedure to obtain C_{TL} CTL from 60°F to 15°C
 C_{TL} CTL from Table 24 1.000678561307
Relative density at 15°C 0.688441521889
T53/7, Values returned from Tables 23 &and 24 valid, continue
T53/8
Density at 15 °C (kg/m³) 687.764095431267
T53/9
Density at 15°C (rounded) 687.8

Example 53/9 – Calculated Relative Density @ 60°F (γ_{60}) RD60 Near 0.3500 Lower Boundary Limit Using EE (68/32) and Ethane

Input Data to Implementation Procedure T53

Density @ obs. temp. (kg/m³) ... 224.56
Observed Temperature T_{obs} (°C) ... 30.680

Computed Data – last digit is rounded

T53/1

Input Data – rounded

Density, rounded to 0.1 224.6
Temperature rounded to 0.05 30.70

T53/2

T_{obs} , Kelvin 303.85

T53/3

Density relative to 60° water 0.224821224084

T53/4

T_{obs} and relative density are within range, continue

T53/5, Call Table 23 procedure to obtain relative density at 60°F

γ_{60} RD60 from Table 23 0.350001829424

T53/6, Call Table 24 Procedure to obtain $C_{L, \text{CTL}}$ from 60°F to 15°C
 $C_{L, \text{CTL}}$ from Table 24 1.005770230278

Relative density at 15°C 0.352021420577

T53/7, Values returned from Tables 23 and 24 valid, continue

T53/8

Density at 15 °C (kg/m³) 351.675031499270

T53/9

Density at 15°C (rounded) 351.7

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Example 53/10 – Relative Density at Observed Temperature (γ_e , T_{23/6}, RD_{t,f}) < Lower Boundary Using EE (68/32) &and Ethane

Input Data to Implementation Procedure T53

Density @ obs. temp. (kg/m³) ... 339.63

Observed Temperature T_{obs} (°C) ... 18.130

Computed Data – last digit is rounded

T53/1

Input Data – rounded

Density, rounded to 0.1 339.6

Temperature rounded to 0.05 18.15

T53/2

T_{obs} , Kelvin 291.30

T53/3

Density relative to 60° water 0.339934495544

T53/4

T_{obs} and relative density are within range, continue

T53/5, Call Table 23 procedure to obtain relative density at 60°F

$\gamma_{60\text{RD}60}$ from Table 23 -1.0

Input data is outside the range correlation range of Table 23, no solution on the standard

Example 53/11 – Relative Density at Observed Temperature ($T_{23/6}$, $\gamma_{23/6}$) RD_{tf} > Upper Boundary Using n-Hexane &and n-Heptane

Input Data to Implementation Procedure T53

Density @ obs. temp. (kg/m³) ... 727.86
Observed Temperature $T_{23/6}$ (°C) ... -33.070

Computed Data – last digit is rounded

T53/1

Input Data – rounded

Density, rounded to 0.1 727.9
Temperature rounded to 0.05 -33.05
T53/2

$T_{23/6}$, Kelvin 240.10

T53/3

Density relative to 60° water ... 0.728616959088

T53/4

$T_{23/6}$ and relative density are within range, continue
T53/5, Call Table 23 procedure to obtain relative density at 60°F

$\gamma_{60}RD60$ from Table 23 -1.0

Input data is outside the range correlation range of Table 23, no solution on the standard

Example 53/12 – Density Input Density < Input Range Limit

Input Data to Implementation Procedure T53

Density @ obs. temp. (kg/m^3) ... 209.74

Observed Temperature T_{obs} ($^{\circ}\text{C}$) ... 11.530

Computed Data – last digit is rounded

T53/1

Input Data – rounded

Density, rounded to 0.1 209.7

Temperature rounded to 0.05 11.55

T53/2

T_{corr} , Kelvin 284.70

T53/3

Density relative to 60° water ... 0.209906548043

T53/4

Relative density is less than 0.210020995, no solution outside the input range of the standard

Example 53/13 – Input Density > Input Range Limit

Input Data to Implementation Procedure T53

Density @ obs. temp. (kg/m³) ... 739. 3235

Observed Temperature T_{4F} (°C) ... 11.530

Computed Data – last digit is rounded

T53/1

Input Data – rounded

Density, rounded to 0.1 739. 34

Temperature rounded to 0.05 11.55

T53/2

T_{4F}, Kelvin 284. 70

T53/3

Density relative to 60° water ... 0. 7401282862340-740028187737

T53/4

Relative density is outside the input range of the standard greater than or equal to 0.74005, no solution

Example 53/14 – Input Temperature < Input Range Limit

Input Data to Implementation Procedure T53

Density @ obs. temp. (kg/m^3) 645.62

Observed Temperature T_{obs} ($^{\circ}\text{C}$) -46.030

Computed Data – last digit is rounded

T53/1

Input Data – rounded

Density, rounded to 0.1 645.6

Temperature rounded to 0.05 -46.05

T53/2

T_{Tx} , Kelvin 227.10

T53/3

Density relative to 60° water 0.646235896122

T53/4

T_{Tx} less than 227.15, no solution is outside the input range of the standard

Example 53/15 – Input Temperature > Input Range Limit

Input Data to Implementation Procedure T53

Density @ obs. temp. (kg/m³) 645.62
Observed Temperature T_{fx} (°C) 93.070

Computed Data – last digit is rounded

T53/1

Input Data – rounded

Density, rounded to 0.1 645.6
Temperature rounded to 0.05 93.05
T53/2

T_{fx}, Kelvin 366.20

T53/3

Density relative to 60° water 0.646235896122

T53/4

T_{fx} is outside the input range of the standard ~~greater than 366.15, no solution~~

5.3 CTL (Table 60) and Density (Table 59) for NGL and LPG using a 20°C Base Temperature

5.3.1 Implementation Procedure for Table 60E (20°C Basis)

This section presents the implementation procedure T60 for the computation of Temperature Correction Factors, C_{TL} s. The C_{TL} s are used to calculate volumes of fluid at the base temperature from volumes at some known temperature. The fluids are characterized by the specification of density at the base temperature, 20°C.

5.3.1.1 Inputs and Outputs

Inputs: Density at 20°C, ρ_{20} (kg/m^3)
Observed temperature, T_F ($^\circ\text{C}$)

Output: Temperature Correction Factor, C_{TL} (from T_F to T_B)

5.3.1.2 Outline of Calculations

The calculations are performed using an extended two-fluid corresponding states equation. By comparing densities at 60°F, two reference fluids are selected so that one is slightly more dense and one that is slightly less dense than the observed fluid. The densities of these reference fluids are then scaled to the observed reduced temperature (reduced by the critical temperature of the fluid of interest). The Temperature Correction Factor is then computed from the reference fluid densities. See Figure 5 for a general flow chart of the calculation procedure.

5.3.1.3 T60 Implementation Procedure

<u>T60/Step Number</u>	<u>Operation/Procedure at that step</u>
------------------------	---

T60/1: Round the density ρ_{20} to the nearest 0.1 and round the observed temperature T_F to the nearest 0.05°C.

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T60/2: Convert the rounded observed temperature to units of Kelvin, T_x :

$$T_x = T_F + 273.15$$

T60/3: The resultant temperature T_x and ρ_{20} must fall within the following boundariesranges:

Temperature between 227.15 and 366.15 K, inclusive (equivalent to -46 to 93°C, or -50.8 to 199.4°F)

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Density between 331.7 and 683.6 kg/m³ inclusive

If these values do not fall in these ranges, then the standard does not apply. Flag this result (possibly by returning a -1 for C_{TL}) and exit this procedure.

Note: The density [boundaries ranges](#) tested in this step slightly exceed the [boundaries ranges](#) used within the T24 implementation procedure (0.3500 to 0.6880 relative density at 60°F) that act as the true limits for this method.

- T60/4: Convert the 20°C density to relative density, relative to the density of water at 60°F:

$$\gamma_{TB} = \frac{\rho_{20}}{999.016}$$

- T60/5: Use the procedure described in Section 5.1.2 for Table 23 to compute a relative density at 60°F from the known relative density at 20°C. Enter the procedure at Step T23/4 [so as to](#) avoid additional rounding of the input values. Inputs to Procedure T23 are the values of T_{BK} and γ_{TB} , where T_{BK} is the base temperature 20°C in Kelvin (293.15 K) and γ_{TB} is the density at the base temperature 20°C. Implementation procedure T23 is exited after Step T23/11 so as not to round the output values. The converged output from Step T23/11 is γ_{60} .

- T60/6: The resultant density γ_{60} , if it were rounded to the nearest 0.0001, must fall within 0.3500 and 0.6880 inclusive. Test γ_{60} to ensure it is within the following [boundariesranges](#):

Relative density greater than or equal to 0.34995 and less than 0.68805

If the relative density does not fall in this range, then the standard does not apply. Flag this result (return a -1 for C_{TL}) and exit this procedure.

- T60/7: Use the procedure described in Section 5.1.1 for Table 24 to compute the Temperature Correction Factor (C_{TL1}) from 60°F to the observed temperature, T_x . This step provides the factor used to reduce an observed volume at T_x to a volume at 60°F when the relative density at 60°F, γ_{60} , is known. Enter implementation procedure T24 with T_x and γ_{60} at Step T24/4 to avoid double rounding of the inputs. On exit skip Step T24/14 to avoid rounding the output C_{TL1} .

By definition:

$$C_{TL1} = \frac{V_{60}}{V_{T_x}} = \frac{\gamma_{T_x}}{\gamma_{60}}$$

- T60/8: Use the procedure described in Section 5.1.1 for Table 24 to compute the Temperature Correction Factor (C_{TL2}) from 60°F to the new base temperature 20°C. This step provides the factor used to reduce an observed volume at 20°C to a volume at 60°F when the relative density at 60°F, γ_{60} , is known. Enter implementation procedure T24 at Step T24/4 to avoid double rounding of the inputs. The inputs are T_{BK} and γ_{60} , where T_{BK} is the base temperature 20°C in Kelvin (293.15 K). On exit skip Step T24/14 to avoid double rounding of the output C_{TL1} .

By definition:

$$C_{TL2} = \frac{V_{60}}{V_{20}} = \frac{\gamma_{TB}}{\gamma_{60}}$$

- T60/9: Compute the desired C_{TL} to reduce volume from the observed temperature, T_x , to the base condition of 20°C. The defining formulas show that the calculation is made by computing the ratio C_{TL1}/C_{TL2} .

$$\frac{C_{TL1}}{C_{TL2}} = \frac{\left(\frac{V_{60}}{V_{Tx}} \right)}{\left(\frac{V_{60}}{V_{20}} \right)} = \frac{V_{20}}{V_{Tx}}$$

$$C_{TL1} = \frac{V_{20}}{V_{Tx}} = \frac{\rho_{Tx}}{\rho_{20}}$$

- T60/10: Perform error check to ascertain that only positive C_{TL} is used. If C_{TL} is less than or equal to 0, set an error flag (such as $C_{TL} = -1$) and exit this procedure.

- T60/11: Round the Temperature Correction Factor C_{TL} to the nearest 0.00001. Exit this procedure.

Comment [KF5]: Update Figure Number for addition of Figure 1

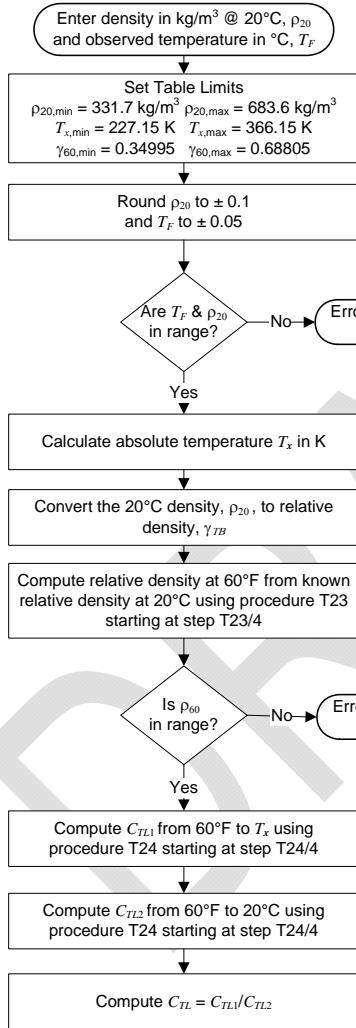


Figure 5. Flow Chart of Implementation Procedure for Table 60

5.3.1.4 Examples for Section 5.3.1 (Table 60)

(See [Table 1](#)[Table 2](#) for properties of the Reference Fluids)

Example 60/1 – Utilize EE (68/32) and Ethane

Input Data to Implementation Procedure T60

Density (kg/m^3) @ 20°C ($\rho_{20\text{Den}}$) 332.69

Observed temperature (T_{4F} , $^\circ\text{C}$) -5.020

Computed Data – last digit is rounded

T60/1

Input Data – rounded

$\rho_{20\text{Den20}}$, rounded to 0.1 332.7

T_{4F} , $^\circ\text{C}$, rounded to 0.05 -5.00

T60/2

T_{Tx} , Kelvin 268.15

T60/3

T_{Tx} and $\rho_{20\text{Den20}}$ are within range, continue

T60/4

$\rho_{20\text{Den20}}$ relative to 60°F water 0.333027699256

T60/5, Call Table 23 procedure

$\gamma_{60\text{RD60}}$ from Table 23 0.350810339452

T60/6

$\gamma_{60\text{RD60}}$ is within range, continue

T60/7, Call Table 24 Procedure with T_{Tx} and $\gamma_{60\text{RD60}}$

Reference Fluid 1 Reference Fluid 1 EE (68/32)

Reference Fluid 2 Reference Fluid 2 Ethane

$C_{TL1\text{CTL1}}$, T_{Tx} to 60°F 1.164305432161

T60/8, Call Table 24 Procedure with 20°C and $\gamma_{60\text{RD60}}$

Reference Fluid 1 Reference Fluid 1 EE (68/32)

Reference Fluid 2 Reference Fluid 2 Ethane

$C_{TL2\text{CTL2}}$, 20°C to 60°F 0.949309823927

T60/9 $C_{TL\text{CTL}} = \frac{C_{TL1\text{CTL1}}}{C_{TL2\text{CTL2}}}$

$C_{TL\text{CTL}}$, T_{Tx} to 20°C 1.226475701416

T60/10

$C_{TL\text{CTL}}$ is positive, continue

T60/11 $C_{TL\text{CTL}}$ rounded

$C_{TL\text{CTL}}$ (rounded) 1.22648

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Example 60/2 – Utilize Use Ethane and EP (65/35)

Input Data to Implementation Procedure T60

Density (kg/m^3) @ 20°C ($\rho_{20}\text{Den20}$) . 399.55
Observed temperature T_{xTx} , $^\circ\text{C}$ -3.920

Computed Data – last digit is rounded

T60/1

Input Data – rounded

$\rho_{20}\text{Den20}$, rounded to 0.1 399.6
 T_{xTx} , $^\circ\text{C}$, rounded to 0.05 -3.90
T60/2
 T_{xTx} , Kelvin 269.25
T60/3
 T_{xTx} and $\rho_{20}\text{Den20}$ are within range, continue
T60/4

$\rho_{20}\text{Den20}$ relative to 60°F water 0.399993593696
T60/5, Call Table 23 procedure

$\gamma_{60}\text{RD60}$ from Table 23 0.410257484971

T60/6

$\gamma_{60}\text{RD60}$ is within range, continue

T60/7, Call Table 24 Procedure with T_{xTx} and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 Ethane
Reference Fluid 2 Reference Fluid 2 EP (65/35)
 $C_{TL1}\text{CTL1}$, T_{xTx} to 60°F 1.094238548593

T60/8, Call Table 24 Procedure with 20°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 Ethane
Reference Fluid 2 Reference Fluid 2 EP (65/35)
 $C_{TL2}\text{CTL2}$, 20°C to 60°F 0.974981830112

T60/9 $C_{TL}\text{CTL} = C_{TL1}\text{CTL1}/C_{TL2}\text{CTL2}$
 $C_{TL}\text{CTL}$, T_{xTx} to 20°C 1.122316862527

T60/10

$C_{TL}\text{CTL}$ is positive, continue

T60/11 $C_{TL}\text{CTL}$ rounded
 $C_{TL}\text{CTL}$ (rounded) 1.12232

Example 60/3 – Utilize Use EP (65/35) and EP (35/65)

Input Data to Implementation Procedure T60

Density (kg/m^3) @ 20°C ($\rho_{20}\text{Den20}$) . 451.09

Observed temperature T_{Tx} , °C 30.774

Computed Data – last digit is rounded

T60/1

Input Data – rounded

$\rho_{20}\text{Den20}$, rounded to 0.1 451.1

T_{Tx} , °C, rounded to 0.05 30.75

T60/2

T_{Tx} , Kelvin 303.90

T60/3

T_{Tx} and $\rho_{20}\text{Den20}$ are within range, continue

T60/4

$\rho_{20}\text{Den20}$ relative to 60°F water 0.451544319610

T60/5, Call Table 23 procedure

$\gamma_{60}\text{RD60}$ from Table 23 0.459584427423

T60/6

$\gamma_{60}\text{RD60}$ is within range, continue

T60/7, Call Table 24 Procedure with T_{Tx} and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 EP (65/35)

Reference Fluid 2 Reference Fluid 2 EP (35/65)

$C_{T1}\text{CTL1}$, T_{Tx} to 60°F 0.936730755171

T60/8, Call Table 24 Procedure with 20°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 EP (65/35)

Reference Fluid 2 Reference Fluid 2 EP (35/65)

$C_{T2}\text{CTL2}$, 20°C to 60°F 0.982505700078

T60/9

$C_{T1}\text{CTL1} = C_{T1}\text{CTL1}/C_{T2}\text{CTL2}$

$C_{T1}\text{CTL1}$, T_{Tx} to 20°C 0.953409995582

T60/10

$C_{T1}\text{CTL1}$ is positive, continue

T60/11

$C_{T1}\text{CTL1}$ rounded

$C_{T1}\text{CTL1}$ (rounded) 0.95341

Example 60/4 – Utilize Use EP (35/65) and Propane

Input Data to Implementation Procedure T60

Density (kg/m³) @ 20°C ($\rho_{20}\text{Den20}$) . 489.92
Observed temperature T_{xTx} , °C 84.975

Computed Data – last digit is rounded

T60/1

Input Data – rounded

$\rho_{20}\text{Den20}$, rounded to 0.1 489.9
 T_{xTx} , °C, rounded to 0.05 85.00
T60/2
 T_{xTx} , Kelvin 358.15
T60/3
 T_{xTx} and $\rho_{20}\text{Den20}$ are within range, continue
T60/4

$\rho_{20}\text{Den20}$ relative to 60°F water 0.490382536416
T60/5, Call Table 23 procedure

$\gamma_{60}\text{RD60}$ from Table 23 0.497272599314

T60/6

$\gamma_{60}\text{RD60}$ is within range, continue

T60/7, Call Table 24 Procedure with T_{xTx} and $\gamma_{60}\text{RD60}$
Reference Fluid 1 Reference Fluid 1 EP (35/65)
Reference Fluid 2 Reference Fluid 2 Propane
 $C_{TL1}\text{CTL1}$, T_{xTx} to 60°F 0.659050245916

T60/8, Call Table 24 Procedure with 20°C and $\gamma_{60}\text{RD60}$
Reference Fluid 1 Reference Fluid 1 EP (35/65)
Reference Fluid 2 Reference Fluid 2 Propane
 $C_{TL2}\text{CTL2}$, 20°C to 60°F 0.986144294080

T60/9 $C_{TL}\text{CTL} = C_{TL1}\text{CTL1}/C_{TL2}\text{CTL2}$
 $C_{TL}\text{CTL}$, T_{xTx} to 20°C 0.668310154886

T60/10

$C_{TL}\text{CTL}$ is positive, continue

T60/11 $C_{TL}\text{CTL}$ rounded
 $C_{TL}\text{CTL}$ (rounded) 0.66831

Example 60/5 – Utilize Use Propane and i-Butane

Input Data to Implementation Procedure T60

Density (kg/m³) @ 20°C ($\rho_{20}\text{Den20}$) . 539.49

Observed temperature T_{TF} , °C 68.360

Computed Data – last digit is rounded

T60/1

Input Data – rounded

$\rho_{20}\text{Den20}$, rounded to 0.1 539.5

T_{TF} , °C, rounded to 0.05 68.35

T60/2

T_{Tx} , Kelvin 341.50

T60/3

T_{Tx} and $\rho_{20}\text{Den20}$ are within range, continue

T60/4

$\rho_{20}\text{Den20}$ relative to 60°F water 0.540031390889

T60/5, Call Table 23 procedure

$\gamma_{60}\text{RD60}$ from Table 23 0.545748636061

T60/6

$\gamma_{60}\text{RD60}$ is within range, continue

T60/7, Call Table 24 Procedure with T_{Tx} and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 Propane

Reference Fluid 2 Reference Fluid 2 i-Butane

$C_{T1}\text{CTL1}$, T_{Tx} to 60°F 0.856605931918

T60/8, Call Table 24 Procedure with 20°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 Propane

Reference Fluid 2 Reference Fluid 2 i-Butane

$C_{T2}\text{CTL2}$, 20°C to 60°F 0.989524032138

T60/9 $C_{T1}\text{CTL} = C_{T1}\text{CTL1}/C_{T2}\text{CTL2}$

$C_{T1}\text{CTL}$, T_{Tx} to 20°C 0.865674712384

T60/10

$C_{T1}\text{CTL}$ is positive, continue

T60/11 $C_{T1}\text{CTL}$ rounded

$C_{T1}\text{CTL}$ (rounded) 0.86567

Example 60/6 – Utilize Use i-Butane and n-Butane

Input Data to Implementation Procedure T60

Density (kg/m³) @ 20°C ($\rho_{20}\text{Den20}$) . 569.42
Observed temperature $T_x\text{Tx}$, °C -16.090

Computed Data – last digit is rounded

T60/1

Input Data – rounded

$\rho_{20}\text{Den20}$, rounded to 0.1 569.4
 $T_x\text{Tx}$, °C, rounded to 0.05 -16.10
T60/2
 $T_x\text{Tx}$, Kelvin 257.05
T60/3
 $T_x\text{Tx}$ and $\rho_{20}\text{Den20}$ are within range, continue
T60/4

$\rho_{20}\text{Den20}$ relative to 60°F water 0.569960841468
T60/5, Call Table 23 procedure

$\gamma_{60}\text{RD60}$ from Table 23 0.575142670956

T60/6

$\gamma_{60}\text{RD60}$ is within range, continue

T60/7, Call Table 24 Procedure with $T_x\text{Tx}$ and $\gamma_{60}\text{RD60}$
Reference Fluid 1 Reference Fluid 1 i-Butane
Reference Fluid 2 Reference Fluid 2 n-Butane
 $C_{TL1}\text{CTL1}$, $T_x\text{Tx}$ to 60°F 1.060732897657

T60/8, Call Table 24 Procedure with 20°C and $\gamma_{60}\text{RD60}$
Reference Fluid 1 Reference Fluid 1 i-Butane
Reference Fluid 2 Reference Fluid 2 n-Butane
 $C_{TL2}\text{CTL2}$, 20°C to 60°F 0.990990359414

T60/9 $C_{TL}\text{CTL} = C_{TL1}\text{CTL1}/C_{TL2}\text{CTL2}$
 $C_{TL}\text{CTL}$, $T_x\text{Tx}$ to 20°C 1.070376606170

T60/10

$C_{TL}\text{CTL}$ is positive, continue

T60/11 $C_{TL}\text{CTL}$ rounded
 $C_{TL}\text{CTL}$ (rounded) 1.07038

Example 60/7 – Utilize Use n-Butane and i-Pentane

Input Data to Implementation Procedure T60

Density (kg/m³) @ 20°C ($\rho_{20}\text{Den20}$) . 599.37
Observed temperature T_{Fx} , °C 43.360

Computed Data – last digit is rounded
T60/1

Input Data – rounded

$\rho_{20}\text{Den20}$, rounded to 0.1 599.4
 T_{Fx} , °C, rounded to 0.05 43.35

T60/2
 T_{Fx} , Kelvin 316.50
T60/3

T_{Fx} and $\rho_{20}\text{Den20}$ are within range, continue
T60/4

$\rho_{20}\text{Den20}$ relative to 60°F water 0.599990390544

T60/5, Call Table 23 procedure

$\gamma_{60}\text{RD60}$ from Table 23 0.604700215005

T60/6

$\gamma_{60}\text{RD60}$ is within range, continue

T60/7, Call Table 24 Procedure with T_{Fx} and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 n-Butane
Reference Fluid 2 Reference Fluid 2 i-Pentane
 $C_{TL1}\text{CTL1}$, T_{Fx} to 60°F 0.949609422686

T60/8, Call Table 24 Procedure with 20°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 n-Butane
Reference Fluid 2 Reference Fluid 2 i-Pentane
 $C_{TL2}\text{CTL2}$, 20°C to 60°F 0.992211317977

T60/9 $C_{TL}\text{CTL} = C_{TL1}\text{CTL1}/C_{TL2}\text{CTL2}$
 $C_{TL}\text{CTL}$, T_{Fx} to 20°C 0.957063687423

T60/10

$C_{TL}\text{CTL}$ is positive, continue

T60/11 $C_{TL}\text{CTL}$ rounded
 $C_{TL}\text{CTL}$ (rounded) 0.95706

Example 60/8 – Utilize Use i-Pentane and n-Pentane

Input Data to Implementation Procedure T60

Density (kg/m³) @ 20°C ($\rho_{20}\text{Den20}$) . 624.42
Observed temperature T_{xTx} , °C 76.650

Computed Data – last digit is rounded

T60/1

Input Data – rounded

$\rho_{20}\text{Den20}$, rounded to 0.1 624.4
 T_{xTx} , °C, rounded to 0.05 76.65
T60/2
 T_{xTx} , Kelvin 349.80
T60/3
 T_{xTx} and $\rho_{20}\text{Den20}$ are within range, continue
T60/4

$\rho_{20}\text{Den20}$ relative to 60°F water 0.625015014775
T60/5, Call Table 23 procedure

$\gamma_{60}\text{RD60}$ from Table 23 0.629388813227

T60/6

$\gamma_{60}\text{RD60}$ is within range, continue

T60/7, Call Table 24 Procedure with T_{xTx} and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 i -Pentane
Reference Fluid 2 Reference Fluid 2 n-Pentane
 $C_{TL1}\text{CTL1}$, T_{xTx} to 60°F 0.896907512500

T60/8, Call Table 24 Procedure with 20°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 i -Pentane
Reference Fluid 2 Reference Fluid 2 n-Pentane
 $C_{TL2}\text{CTL2}$, 20°C to 60°F 0.993050721018

T60/9 $C_{TL}\text{CTL} = C_{TL1}\text{CTL1}/C_{TL2}\text{CTL2}$
 $C_{TL}\text{CTL}$, T_{xTx} to 20°C 0.903183990019

T60/10

$C_{TL}\text{CTL}$ is positive, continue

T60/11 $C_{TL}\text{CTL}$ rounded
 $C_{TL}\text{CTL}$ (rounded) 0.90318

Example 60/9 – Utilize Use n-Pentane and i-Hexane

Input Data to Implementation Procedure T60

Density (kg/m³) @ 20°C ($\rho_{20}\text{Den20}$) . 639.41

Observed temperature T_{Tx} , °C -24.460

Computed Data – last digit is rounded

T60/1

Input Data – rounded

$\rho_{20}\text{Den20}$, rounded to 0.1 639.4

T_{Tx} , °C, rounded to 0.05 -24.45

T60/2

T_{Tx} , Kelvin 248.70

T60/3

T_{Tx} and $\rho_{20}\text{Den20}$ are within range, continue

T60/4

$\rho_{20}\text{Den20}$ relative to 60°F water 0.640029789313

T60/5, Call Table 23 procedure

$\gamma_{60}\text{RD60}$ from Table 23 0.644192277735

T60/6

$\gamma_{60}\text{RD60}$ is within range, continue

T60/7, Call Table 24 Procedure with T_{Tx} and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 n-Pentane

Reference Fluid 2 Reference Fluid 2 i-Hexane

$C_{T1}\text{CTL1}$, T_{Tx} to 60°F 1.056377254246

T60/8, Call Table 24 Procedure with 20°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 n-Pentane

Reference Fluid 2 Reference Fluid 2 i-Hexane

$C_{T2}\text{CTL2}$, 20°C to 60°F 0.993538437998

T60/9 $C_{T1}\text{CTL} = C_{T1}\text{CTL1}/C_{T2}\text{CTL2}$

$C_{T1}\text{CTL}$, T_{Tx} to 20°C 1.063247493850

T60/10

$C_{T1}\text{CTL}$ is positive, continue

T60/11 $C_{T1}\text{CTL}$ rounded

$C_{T1}\text{CTL}$ (rounded) 1.06325

Example 60/10 – Utilize Use i-Hexane and n-Hexane

Input Data to Implementation Procedure T60

Density (kg/m³) @ 20°C ($\rho_{20}\text{Den20}$) . 659.38
Observed temperature T_{xTx} , °C 80.580

Computed Data – last digit is rounded

T60/1

Input Data – rounded

$\rho_{20}\text{Den20}$, rounded to 0.1 659.4
 T_{xTx} , °C, rounded to 0.05 80.60
T60/2
 T_{xTx} , Kelvin 353.75
T60/3
 T_{xTx} and $\rho_{20}\text{Den20}$ are within range, continue
T60/4

$\rho_{20}\text{Den20}$ relative to 60°F water 0.660049488697
T60/5, Call Table 23 procedure
 $\gamma_{60}\text{RD60}$ from Table 23 0.664004852143

T60/6

$\gamma_{60}\text{RD60}$ is within range, continue

T60/7, Call Table 24 Procedure with T_{xTx} and $\gamma_{60}\text{RD60}$
Reference Fluid 1 Reference Fluid 1 i-Hexane
Reference Fluid 2 Reference Fluid 2 n-Hexane
 $C_{TL1}\text{CTL1}$, T_{xTx} to 60°F 0.908011926489

T60/8, Call Table 24 Procedure with 20°C and $\gamma_{60}\text{RD60}$
Reference Fluid 1 Reference Fluid 1 i-Hexane
Reference Fluid 2 Reference Fluid 2 n-Hexane
 $C_{TL2}\text{CTL2}$, 20°C to 60°F 0.994043170870

T60/9 $C_{TL}\text{CTL} = C_{TL1}\text{CTL1}/C_{TL2}\text{CTL2}$
 $C_{TL}\text{CTL}$, T_{xTx} to 20°C 0.913453211186

T60/10

$C_{TL}\text{CTL}$ is positive, continue

T60/11 $C_{TL}\text{CTL}$ rounded
 $C_{TL}\text{CTL}$ (rounded) 0.91345

Example 60/11 – Utilize n-Hexane and n-Heptane

Input Data to Implementation Procedure T60

Density (kg/m³) @ 20°C ($\rho_{20}\text{Den20}$) . 669.38

Observed temperature T_{Tx} , °C 82.790

Computed Data – last digit is rounded

T60/1

Input Data – rounded

$\rho_{20}\text{Den20}$, rounded to 0.1 669.4

T_{Tx} , °C, rounded to 0.05 82.80

T60/2

T_{Tx} , Kelvin 355.95

T60/3

T_{Tx} and $\rho_{20}\text{Den20}$ are within range, continue

T60/4

$\rho_{20}\text{Den20}$ relative to 60°F water 0.670059338389

T60/5, Call Table 23 procedure

$\gamma_{60}\text{RD60}$ from Table 23 0.673917506957

T60/6

$\gamma_{60}\text{RD60}$ is within range, continue

T60/7, Call Table 24 Procedure with T_{Tx} and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 n-Hexane

Reference Fluid 2 Reference Fluid 2 n-Heptane

$C_{T1}\text{CTL1}$, T_{Tx} to 60°F 0.909032061079

T60/8, Call Table 24 Procedure with 20°C and $\gamma_{60}\text{RD60}$

Reference Fluid 1 Reference Fluid 1 n-Hexane

Reference Fluid 2 Reference Fluid 2 n-Heptane

$C_{T2}\text{CTL2}$, 20°C to 60°F 0.994275014129

T60/9 $C_{T1}\text{CTL} = C_{T1}\text{CTL1}/C_{T2}\text{CTL2}$

$C_{T1}\text{CTL}$, T_{Tx} to 20°C 0.914266222283

T60/10

$C_{T1}\text{CTL}$ is positive, continue

T60/11 $C_{T1}\text{CTL}$ rounded

$C_{T1}\text{CTL}$ (rounded) 0.91427

Example 60/12 – Reduced Temperature (T_{rx}) Greater Than 1.0**Formatted:** Font: Italic**Formatted:** Font: Italic, Subscript

Input Data to Implementation Procedure T60

Density (kg/m³) @ 20°C ($\rho_{20}Den20$) . 399.83
Observed temperature T_{rx} , °C 90.570

Computed Data – last digit is rounded

T60/1

Input Data – rounded

$\rho_{20}Den20$, rounded to 0.1 399.8
 T_{rx} , °C, rounded to 0.05 90.55

T60/2

T_{rx} , Kelvin 363.70

T60/3

T_{rx} and $\rho_{20}Den20$ are within range, continue

T60/4

$\rho_{20}Den20$ relative to 60°F water 0.400193790690

T60/5, Call Table 23 procedure

$\gamma_{60}RD60$ from Table 23 0.410447384415

T60/6

$\gamma_{60}RD60$ is within range, continue

T60/7, Call Table 24 Procedure with T_{rx} and $\gamma_{60}RD60$

Reference Fluid 1 Reference Fluid 1 Ethane
Reference Fluid 2 Reference Fluid 2 EP (65/35)

Reduced temperature T_{rx} greater than 1.0, no solution is outside the range of the standard

$C_{T1}CTLE1$, T_{rx} to 60°F -1.0

Value from Table 24 is outside the correlation range of the standard not valid, no solution

Example 60/13 – Observed Temperature (T_f) $T_f <$ Lower Range Limit**Formatted:** Font: Times New Roman, Bold**Formatted:** Not Superscript/ Subscript

Input Data to Implementation Procedure T60

Density (kg/m³) @ 20°C (ρ_{20}^{Den20}) . 449.56

Observed temperature T_f , °C -46.030

Computed Data – last digit is rounded

T60/1

Input Data – rounded

ρ_{20}^{Den20} , rounded to 0.1 449.6

T_f , °C, rounded to 0.05 -46.05

T60/2

T_x , Kelvin 227.10

T60/3

T_x is outside the input range of the standard less than 227.15, no solution

Example 60/14 – Density at 20°C (ρ_{20}) < Lower Range Limit**Formatted:** Subscript

Input Data to Implementation Procedure T60

Density (kg/m³) @ 20°C (ρ_{20}) . 331.59
Observed temperature T_{obs} , °C 64.440

Computed Data – last digit is rounded

T60/1

Input Data – rounded

ρ_{20} , rounded to 0.1 331.6
 T_{obs} , °C, rounded to 0.05 64.45

T60/2

T_{corr} , Kelvin 337.60
T60/3

Density Density at 20°C is outside the input range of the standard less than 331.7, no solution

Example 60/15 – Observed Temperature (T_x) T_f > Upper Range Limit**Formatted:** Font: Times New Roman, Bold**Formatted:** Not Superscript/ Subscript

Input Data to Implementation Procedure T60

Density (kg/m³) @ 20°C (ρ_{20}) . 449.56Observed temperature T_f , °C 93.030

Computed Data – last digit is rounded

T60/1

Input Data – rounded

 ρ_{20} , rounded to 0.1 449.6 T_f , °C, rounded to 0.05 93.05

T60/2

 T_x , Kelvin 366.20

T60/3

 T_x is outside the input range of the standard greater than 366.15, no solution

Example 60/16 – Density at 20°C > Upper Range Limit

Input Data to Implementation Procedure T60

Density (kg/m³) @ 20°C ($\rho_{20}\text{Den20}$) . 683.65
Observed temperature T_{obs} , °C -17.780

Computed Data – last digit is rounded

T60/1

Input Data – rounded

$\rho_{20}\text{Den20}$, rounded to 0.1 683.7
 T_{obs} , °C, rounded to 0.05 -17.80

T60/2

T_{corr} , Kelvin 255.35

T60/3

| Density at 20°C is outside the input range of the standard greater than 683.6, no solution

Example 60/17 – Observed Temperature (T_{xTf}) &and Density at 20°C (ρ_{20}) = Upper Range Limits

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Input Data to Implementation Procedure T60

Density (kg/m³) @ 20°C ($\rho_{20}Den20$) . 683.64Observed temperature T_{xTf} , °C 93.020

Computed Data – last digit is rounded

T60/1

Input Data – rounded

 $\rho_{20}Den20$, rounded to 0.1 683.6 T_{xTf} , °C, rounded to 0.05 93.00

T60/2

 T_{xTx} , Kelvin 366.15

T60/3

 T_{xTx} and $\rho_{20}Den20$ are within range, continue

T60/4

 $\rho_{20}Den20$ relative to 60°F water 0.684273324952

T60/5, Call Table 23 procedure

 $\gamma_{60}RD60$ from Table 23 0.688015480920

T60/6

 $\gamma_{60}RD60$ is within range, continueT60/7, Call Table 24 Procedure with T_{xTx} and $\gamma_{60}RD60$

Reference Fluid 1 Reference Fluid 1 n-Hexane

Reference Fluid 2 Reference Fluid 2 n-Heptane

 $C_{TL}CTL$, T_{xTx} to 60°F 0.900472587577T60/8, Call Table 24 Procedure with 20°C and $\gamma_{60}RD60$

Reference Fluid 1 Reference Fluid 1 n-Hexane

Reference Fluid 2 Reference Fluid 2 n-Heptane

 $C_{TL}CTL$, 20°C to 60°F 0.994560942200

T60/9

 $C_{TL}CTL$ = $C_{TL}CTL1/C_{TL}CTL2$ $C_{TL}CTL$, T_{xTx} to 20°C 0.905397094707

T60/10

 $C_{TL}CTL$ is positive, continueT60/11 $C_{TL}CTL$ rounded $C_{TL}CTL$ (rounded) 0.90540

Example 60/18 – Observed Temperature ($T_{\text{F}} \text{ or } T_{\text{F}}$) & and Density at 20°C (ρ_{20}) = Lower Range Limits**Formatted:** Font: Times New Roman, Bold**Formatted:** Subscript

Input Data to Implementation Procedure T60

Density (kg/m³) @ 20°C ($\rho_{20}\text{Den20}$) . 331.67
Observed temperature T_{F} , °C -46.020

Computed Data – last digit is rounded

T60/1

Input Data – rounded

$\rho_{20}\text{Den20}$, rounded to 0.1 331.7
 T_{F} , °C, rounded to 0.05 -46.00

T60/2

T_{F} , Kelvin 227.15

T60/3

T_{F} and $\rho_{20}\text{Den20}$ are within range, continue

T60/4

$\rho_{20}\text{Den20}$ relative to 60°F water 0.332026714287

T60/5, Call Table 23 procedure

$\gamma_{60}\text{RD60}$ from Table 23 -1.0

Input data is outside the range of Table 23, no solution the standard

5.3.2 Implementation Procedure for Table 59E (20°C Basis)

This section presents the implementation procedure T59 for calculating the densities of NGLs and LPGs at [a base condition](#) of 20°C from known temperatures and densities.

Density readings must be corrected for the effect of temperature on the instrument prior to entering the density into the following implementation procedure.

5.3.2.1 Inputs and Outputs

Inputs: Density at observed temperature, ρ_x (kg/m³)
Observed temperature, T_F (°C)

Output: Density at 20°C, ρ_{20} (kg/m³)

5.3.2.2 Outline of Calculations

The calculations are done using an extended two-fluid corresponding states equation. Two reference fluids are found that are slightly denser and slightly less dense than the observed fluid by comparing their densities at the observed temperature. Iteration must be performed to determine the value of the fluid's relative density at 60°F such that when the Temperature Correction Factor is applied, the observed relative density is obtained. The "guessed" value for the fluid's relative density at 60°F is constrained to lie between the relative densities at 60°F of these two reference fluids (as upper and lower bounds). As the iterations progress, these upper and lower bounds are "brought together" based upon intermediate calculations. The relative density at 20°C is then computed from the 60°F relative density by using scaling factors between the properties of the two reference fluids.

See Figure 6 for a general flow chart of the calculation procedure.

5.3.2.3 T59 Implementation Procedure

T59/Step Number Operation/Procedure at that step

T59/1: Round the density ρ_x to the nearest 0.1 and round the observed temperature T_F to the nearest 0.05°C.

T59/2: Convert the rounded observed temperature to units of Kelvin, T_x :

$$T_x = T_F + 273.15$$

T59/3: Convert the density, ρ_x , to relative density, γ_x , relative to the density of water at 60°F.

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$$\gamma_x = \frac{\rho_x}{999.016}$$

DRAFT

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- T59/4: Check the values of temperature and relative density to ensure that they are in the proper range. The observed temperature T_x and relative density γ_x must fall within the following [boundariesranges](#):

Temperature between 227.15 and 366.15 K, inclusive (equivalent to -46 to 93°C, or -50.8 to 199.4°F)

Relative density, if it were rounded to the nearest 0.0001, must fall within 0.2100 and 0.7400 inclusive. Test γ_x to ensure it is within the following [boundariesranges](#):

Relative density greater than or equal to 0.20995 and less than 0.74005

If these values do not fall in these ranges, then the standard does not apply. Flag this result (possibly by returning -1 for the density) and exit this procedure.

- T59/5: Compute the relative density at 60°F, γ_{60} , from the temperature and the relative density at the measurement condition, γ_x . Use the procedure described in Section 5.1.2 for Table 23 to perform this step. Enter the implementation procedure with γ_x and T_x at Step T23/4 [so as to](#) avoid additional rounding of the input values. Exit after Step T23/11 to avoid rounding the result.

- T59/6: Compute the relative density at 20°C, γ_{20} , from the relative density at 60°F. This is performed by using the procedure described in Section 5.1.1 for Table 24. Enter implementation procedure T24 with γ_{60} and $T_x = 293.15$ (e.g. 273.15 + 20). Enter at Step T24/4 to avoid double rounding of the inputs. The C_{TL} for the conversion between γ_{60} and γ_{20} will be returned without rounding from Step T24/13. Compute γ_{20} :

$$\gamma_{20} = C_{TL} \times \gamma_{60}$$

- T59/7: Insure that only valid values came from Steps T59/5 and T59/6. If the γ_{60} obtained from Section 5.2.1 for Table 23 is greater than -1, then proceed. If not, set the fluid density at 20°C to some flag value such as -1 and quit. If the C_{TL} from Step T59/6 is negative, then set the fluid density at 20°C to the error flag condition and exit this procedure.

- T59/8: Calculate the fluid density at 20°C from the relative density at 20°C.

$$\rho_{20} = \gamma_{20} \times 999.016$$

- T59/9: Round the fluid density, ρ_{20} , to the nearest 0.1. Exit this procedure.

Comment [KF6]: Update Figure Number for addition of Figure 1

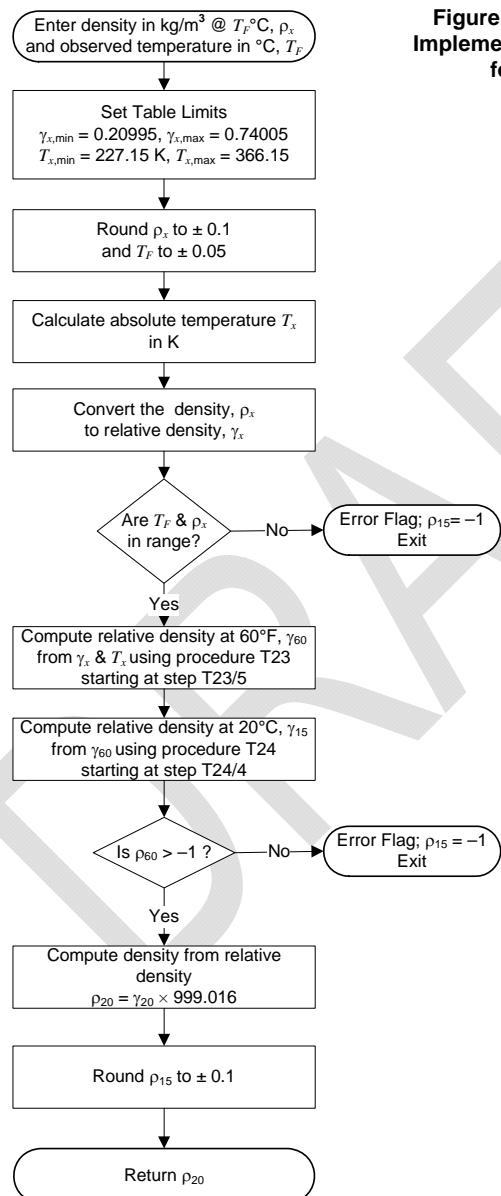


Figure 6. Flow Chart of Implementation Procedure for Table 59

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5.3.2.4 Examples for Section 5.3.2 (Table 59E)

(See [Table 4](#)[Table 2](#) for properties of the Reference Fluids)

Example 59/1 – Relative Density at Observed Temperature ($T_{23/6}$, γ_2) RD_{t,f} < Lower Boundary Using EP (35/65E (68/32) & and Propane/Ethane

Input Data to Implementation Procedure T59
Density at obs. temp. (kg/m³) ... 210.00

Observed Temperature $T_{23/6}$ (°C) ... -44.500
Computed Data – last digit is rounded

T59/1

Input Data – rounded

Density, rounded to 0.1 210.0
Temperature rounded to 0.05 -44.50

T59/2

$T_{23/6}$, Kelvin 228.65

T59/3

Density relative to 60° water ... 0.210206843534

T59/4

$T_{23/6}$ and relative density are within range, continue

T59/5, Call Table 23 procedure to obtain relative density at 60°F

$\gamma_{60}RD60$ from Table 23 -1.0

Input data is outside [the range correlation range of Table 23, no solution on the standard](#)

Example 59/2 – Utilize Use EP (65/35) &and EP (35/65)

Input Data to Implementation Procedure T59
Density at obs. temp. (kg/m^3) 532.57
Observed Temperature T_{obs} ($^{\circ}\text{C}$) -44.120
Computed Data – last digit is rounded
T59/1
Input Data – rounded
Density, rounded to 0.1 532.6
Temperature rounded to 0.05 -44.10
T59/2
 T_{obs} , Kelvin 229.05
T59/3
Density relative to 60° water 0.533124594601
T59/4
 T_{obs} and relative density are within range, continue
T59/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60\text{RD60}}$ from Table 23 0.440515294609
T59/6, Call Table 24 Procedure to obtain $C_{L\text{ CTL}}$ from 60°F to 20°C
 $C_{L\text{ CTL}}$ from Table 24 0.979997725752
20°C relative density 0.431703986876
T59/7, Values returned from Tables 23 &and 24 valid, continue
T59/8
Density at 20°C (kg/m^3) 431.279190152813
T59/9
Density at 20°C (rounded) 431.3

Example 59/3 – Utilize Use n-Pentane &and i-Hexane

Input Data to Implementation Procedure T59

Density at obs. temp. (kg/m^3) $\underline{\underline{\underline{673.66}}}$

Observed Temperature T_{obs} ($^{\circ}\text{C}$) $\underline{\underline{\underline{-23.330}}}$

Computed Data – last digit is rounded

T59/1

Input Data – rounded

Density, rounded to 0.1 $\underline{\underline{\underline{673.7}}}$

Temperature rounded to 0.05 $\underline{\underline{\underline{-23.35}}}$

T59/2

T_{obs} , Kelvin $\underline{\underline{\underline{249.80}}}$

T59/3

Density relative to 60° water $\underline{\underline{\underline{0.674363573757}}}$

T59/4

T_{obs} and relative density are within range, continue

T59/5, Call Table 23 procedure to obtain relative density at 60°F

$\gamma_{60\text{RD60}}$ from Table 23 $\underline{\underline{\underline{0.638538685930}}}$

T59/6, Call Table 24 Procedure to obtain C_L C_{TL} from 60°F to 20°C

C_L C_{TL} from Table 24 $\underline{\underline{\underline{0.993367912870}}}$

20°C 20 °C relative density $\underline{\underline{\underline{0.634303841729}}}$

T59/7, Values returned from Tables 23 &and 24 valid, continue

T59/8

Density at 20°C (kg/m^3) $\underline{\underline{\underline{633.679686748900}}}$

T59/9

Density at 20°C (rounded) $\underline{\underline{\underline{633.7}}}$

Example 59/4 – Utilize Use EP (35/65) &and Propane

Input Data to Implementation Procedure T59
Density at obs. temp. (kg/m^3) ... 245.49
Observed Temperature T_{obs} ($^{\circ}\text{C}$) ... 87.770
Computed Data – last digit is rounded
T59/1
Input Data – rounded
Density, rounded to 0.1 245.5
Temperature rounded to 0.05 87.75
T59/2
 T_{Tx} , Kelvin 360.90
T59/3
Density relative to 60° water ... 0.245741809941
T59/4
 T_{Tx} and relative density are within range, continue
T59/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60\text{RD60}}$ from Table 23 0.488795025411
T59/6, Call Table 24 Procedure to obtain $C_{L\text{ CTL}}$ from 60°F to 20°C
 $C_{L\text{ CTL}}$ from Table 24 0.985452958065
 20°C 20 °C relative density 0.481684503679
T59/7, Values returned from Tables 23 &and 24 valid, continue
T59/8
Density at 20°C (kg/m^3) 481.210526127346
T59/9
Density at 20°C (rounded) 481.2

Example 59/5 – Utilize Use n-Butane &and i-Pentane

Input Data to Implementation Procedure T59
Density at obs. temp. (kg/m^3) 499.55
Observed Temperature T_{obs} ($^{\circ}\text{C}$) 87.820
Computed Data – last digit is rounded
T59/1
Input Data – rounded
Density, rounded to 0.1 499.6
Temperature rounded to 0.05 87.80
T59/2
 T_{obs} , Kelvin 360.95
T59/3
Density relative to 60° water 0.500092090617
T59/4
 T_{obs} and relative density are within range, continue
T59/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60\text{RD60}}$ from Table 23 0.591794896225
T59/6, Call Table 24 Procedure to obtain C_L , C_U from 60°F to 20°C
 C_L , C_U from Table 24 0.991727237885
20°C 20 °C relative density 0.586899117828
T59/7, Values returned from Tables 23 &and 24 valid, continue
T59/8
Density at 20°C (kg/m^3) 586.321609095772
T59/9
Density at 20°C (rounded) 586.3

Example 59/6 – Utilize Use Ethane &and EP (65/35)

Input Data to Implementation Procedure T59
Density at obs. temp. (kg/m³) ... 395.09
Observed Temperature T_{obs} (°C) ... 15.430
Computed Data – last digit is rounded
T59/1
Input Data – rounded
Density, rounded to 0.1 395.1
Temperature rounded to 0.05 15.45
T59/2
 T_{Tx} , Kelvin 288.60
T59/3
Density relative to 60° water ... 0.395489161335
T59/4
 T_{Tx} and relative density are within range, continue
T59/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60\text{RD60}}$ from Table 23 0.395233433716
T59/6, Call Table 24 Procedure to obtain $C_{L\text{ CTL}}$ from 60°F to 20°C
 $C_{L\text{ CTL}}$ from Table 24 0.971608015812
 20°C 20 °C relative density 0.384011972315
T59/7, Values returned from Tables 23 &and 24 valid, continue
T59/8
Density at 20°C (kg/m³) 383.634104534331
T59/9
Density at 20°C (rounded) 383.6

Example 59/7 – Utilize Use i-Butane &and n-Butane

Input Data to Implementation Procedure T59
Density at obs. temp. (kg/m^3) $\underline{\underline{449.59}}$
Observed Temperature T_{obs} ($^{\circ}\text{C}$) $\underline{\underline{93.020}}$
Computed Data – last digit is rounded
T59/1
Input Data – rounded
Density, rounded to 0.1 $\underline{\underline{449.6}}$
Temperature rounded to 0.05 $\underline{\underline{93.00}}$
T59/2
 T_{obs} , Kelvin $\underline{\underline{366.15}}$
T59/3
Density relative to 60° water $\underline{\underline{0.450042842157}}$
T59/4
 T_{obs} and relative density are within range, continue
T59/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60\text{RD60}}$ from Table 23 $\underline{\underline{0.565490291365}}$
T59/6, Call Table 24 Procedure to obtain $C_{\text{L}} \text{, } C_{\text{T}}$ from 60°F to 20°C
 $C_{\text{L}} \text{, } C_{\text{T}}$ from Table 24 $\underline{\underline{0.990501113383}}$
20°C 20 °C relative density $\underline{\underline{0.560118763204}}$
T59/7, Values returned from Tables 23 &and 24 valid, continue
T59/8
Density at 20°C (kg/m^3) $\underline{\underline{559.567606341195}}$
T59/9
Density at 20°C (rounded) $\underline{\underline{559.6}}$

Example 59/8 – Utilize Use i-Hexane &and n-Hexane

Input Data to Implementation Procedure T59
Density at obs. temp. (kg/m^3) ... 600.74
Observed Temperature T_{obs} ($^{\circ}\text{C}$) ... 80.650
Computed Data – last digit is rounded
T59/1
Input Data – rounded
Density, rounded to 0.1 600.7
Temperature rounded to 0.05 80.65
T59/2
 T_{Tx} , Kelvin 353.80
T59/3
Density relative to 60° water ... 0.601291671004
T59/4
 T_{Tx} and relative density are within range, continue
T59/5, Call Table 23 procedure to obtain relative density at 60°F
 $\gamma_{60\text{RD60}}$ from Table 23 0.662699711760
T59/6, Call Table 24 Procedure to obtain $C_{L\text{ CTL}}$ from 60°F to 20°C
 $C_{L\text{ CTL}}$ from Table 24 0.994014419312
 20°C 20 °C relative density 0.658733069163
T59/7, Values returned from Tables 23 &and 24 valid, continue
T59/8
Density at 20°C (kg/m^3) 658.084875823243
T59/9
Density at 20°C (rounded) 658.1

**Example 59/9 – Calculated Relative Density @ 60°F (γ_{60})RD60 Near 0.6880Upper Boundary Using n-Hexane
&n-Heptane**

Input Data to Implementation Procedure T59
Density at obs. temp. (kg/m³) 736.80
Observed Temperature T_{4F} (°C) -44.230
Computed Data – last digit is rounded
T59/1
Input Data – rounded
Density, rounded to 0.1 736.8
Temperature rounded to 0.05 -44.25
T59/2
T_{4F}, Kelvin 228.90
T59/3
Density relative to 60° water 0.737525725314
T59/4
T_{4F} and relative density are within range, continue
T59/5, Call Table 23 procedure to obtain relative density at 60°F
 γ_{60} RD60 from Table 23 0.687974688885
T59/6, Call Table 24 Procedure to obtain C_L CTL from 60°F to 20°C
C_L CTL from Table 24 0.994560181470
20°C relative density 0.684232231424
T59/7, Values returned from Tables 23 &and 24 valid, continue
T59/8
Density at 20°C (kg/m³) 683.558946908054
T59/9
Density at 20°C (rounded) 683.6

**Example 59/10 – Calculated Relative Density @ 60°F (γ_{60})RD60 Near 0.3500Lower Boundary using EE
(68/32) &and Ethane**

Input Data to Implementation Procedure T59
 Density at obs. temp. (kg/m³) ... 224.56
 Observed Temperature T_{ATF} (°C) ... 30.680
 Computed Data – last digit is rounded
 T59/1
 Input Data – rounded
 Density, rounded to 0.1 224.6
 Temperature rounded to 0.05 30.70
 T59/2
T_{ATK}, Kelvin 303.85
 T59/3
 Density relative to 60° water 0.224821224084
 T59/4
T_{ATK} and relative density are within range, continue
 T59/5, Call Table 23 procedure to obtain relative density at 60°F
 γ_{60} RD60 from Table 23 0.350001829424
 T59/6, Call Table 24 Procedure to obtain C_LCTL from 60°F to 20°C
C_LCTL from Table 24 0.948659643284
 20°C relative density 0.332032610649
 T59/7, Values returned from Tables 23 &and 24 valid, continue
 T59/8
 Density at 20°C (kg/m³) 331.705890560614
 T59/9
 Density at 20°C (rounded) 331.7

Example 59/11 – Relative Density at Observed Temperature ($T_{23/6}$, γ_6) RD t_f < Lower Boundary Using EE (68/32) & Ethane

Input Data to Implementation Procedure T59

Density at obs. temp. (kg/m³) = 339.63

Observed Temperature $T_{23/6}$ (°C) = 18.130

Computed Data – last digit is rounded

T59/1

Input Data – rounded

Density, rounded to 0.1 339.6

Temperature rounded to 0.05 18.15

T59/2

$T_{23/6}$, Kelvin 291.30

T59/3

Density relative to 60° water = 0.339934495544

T59/4

$T_{23/6}$ and relative density are within range, continue

T59/5, Call Table 23 procedure to obtain relative density at 60°F

$\gamma_{60}RD60$ from Table 23 -1.0

Input data is outside the range correlation range of Table 23, no solution the standard

Example 59/12 – Relative Density at Observed Temperature ($T_{23/6}$, γ_2) RDtf > Upper Boundary Using n-Hexane & n-Heptane

Input Data to Implementation Procedure T59

Density at obs. temp. (kg/m³) ... 727.86
Observed Temperature $T_{23/6}$ (°C) ... -33.070

Computed Data – last digit is rounded

T59/1

Input Data – rounded

Density, rounded to 0.1 727.9
Temperature rounded to 0.05 -33.05
T59/2

$T_{23/6}$, Kelvin 240.10

T59/3

Density relative to 60° water ... 0.728616959088

T59/4

$T_{23/6}$ and relative density are within range, continue
T59/5, Call Table 23 procedure to obtain relative density at 60°F

γ_{60}^{RD60} from Table 23 -1.0

Input data is outside the range-correlation range of Table 23, no solution the standard

Example 59/13 – Density Input Density < Input Range Limit

Input Data to Implementation Procedure T59

Density at obs. temp. (kg/m^3) = 209.74

Observed Temperature T_{obs} ($^{\circ}\text{C}$) = 11.530

Computed Data – last digit is rounded

T59/1

Input Data – rounded

Density, rounded to 0.1 209.7

Temperature rounded to 0.05 11.55

T59/2

T_{corr} , Kelvin 284.70

T59/3

Density relative to 60° water = 0.209906548043

T59/4

Relative density is less than 0.2100, no solution outside the input range of the standard

Example 59/14 – Input Density > Input Range Limit

Input Data to Implementation Procedure T59

Density at obs. temp. (kg/m³) 739.3235

Observed Temperature T₄₄ (°C) 11.530

Computed Data – last digit is rounded

T59/1

Input Data – rounded

Density, rounded to 0.1 739.34

Temperature rounded to 0.05 11.55

T59/2

T₄₄X, Kelvin 284.70

T59/3

Density relative to 60° water 0.7401282862340-740028187737

T59/4

Relative density is greater than or equal to 0.74005, no solution outside the input range of the standard

Example 59/15 – Input Temperature < Input Range Limit

Input Data to Implementation Procedure T59

Density at obs. temp. (kg/m^3) 645.62

Observed Temperature T_{AT} ($^{\circ}\text{C}$) -46.030

Computed Data – last digit is rounded

T59/1

Input Data – rounded

Density, rounded to 0.1 645.6

Temperature rounded to 0.05 -46.05

T59/2

T_{AT} , Kelvin 227.10

T59/3

Density relative to 60° water 0.646235896122

T59/4

T_{AT} less than 227.15, no solution is outside the input range of the standard

Example 59/16 – Input Temperature > Input Range Limit

Input Data to Implementation Procedure T59

Density at obs. temp. (kg/m^3) 645.62
Observed Temperature T_{Tx} ($^{\circ}\text{C}$) 93.070

Computed Data – last digit is rounded

T59/1

Input Data – rounded

Density, rounded to 0.1 645.6
Temperature rounded to 0.05 93.05
T59/2

T_{Tx} , Kelvin 366.20

T59/3

Density relative to 60° water 0.646235896122

T59/4

T_{Tx} is outside the input range of the standard greater than 366.15, no solution

6 Sample Sections of Printed Tables

Sample tables based on all the implementation procedures are found on the following pages. These tables are representative of the format and appearance of the printed tables, but complete or partial sets of printed tables may be produced in any reasonable set of variable increments required. Note, these printed tables are not the Standard; the implementation procedures are the Standard.

Even though the implementation procedures are the standard, printed tables can be used. Interpolation should not be used with any printed table since the C_{TL} equations are not necessarily linear.

TABLE 23E - FOR NGL &AND LPG LIQUIDS
RELATIVE DENSITY REDUCTION TO 60°F

TEMP. (°F)	OBSERVED RELATIVE DENSITY								TEMP. (°F)
	0.5000	0.5001	0.5002	0.5003	0.5004	0.5005	0.5006	0.5007	
CORRESPONDING RELATIVE DENSITY 60/60°F									
100.0	0.5316	0.5316	0.5317	0.5318	0.5319	0.5320	0.5321	0.5322	0.5323
100.1	0.5316	0.5317	0.5318	0.5319	0.5320	0.5321	0.5322	0.5323	0.5323
100.2	0.5317	0.5318	0.5319	0.5320	0.5321	0.5322	0.5322	0.5323	0.5324
100.3	0.5318	0.5319	0.5320	0.5320	0.5321	0.5322	0.5323	0.5324	0.5325
100.4	0.5319	0.5319	0.5320	0.5321	0.5322	0.5323	0.5324	0.5325	0.5326
100.5	0.5319	0.5320	0.5321	0.5322	0.5323	0.5324	0.5325	0.5326	0.5326
100.6	0.5320	0.5321	0.5322	0.5323	0.5324	0.5324	0.5325	0.5326	0.5327
100.7	0.5321	0.5322	0.5323	0.5323	0.5324	0.5325	0.5326	0.5327	0.5328
100.8	0.5322	0.5322	0.5323	0.5324	0.5325	0.5326	0.5327	0.5328	0.5329
100.9	0.5322	0.5323	0.5324	0.5325	0.5326	0.5327	0.5328	0.5328	0.5329
101.0	0.5323	0.5324	0.5325	0.5326	0.5327	0.5327	0.5328	0.5329	0.5330
101.1	0.5324	0.5325	0.5326	0.5326	0.5327	0.5328	0.5329	0.5330	0.5331
101.2	0.5325	0.5325	0.5326	0.5327	0.5328	0.5329	0.5330	0.5331	0.5332
101.3	0.5325	0.5326	0.5327	0.5328	0.5329	0.5330	0.5331	0.5331	0.5332
101.4	0.5326	0.5327	0.5328	0.5329	0.5330	0.5330	0.5331	0.5332	0.5333
101.5	0.5327	0.5328	0.5329	0.5329	0.5330	0.5331	0.5332	0.5333	0.5334
101.6	0.5328	0.5328	0.5329	0.5330	0.5331	0.5332	0.5333	0.5334	0.5335
101.7	0.5328	0.5329	0.5330	0.5331	0.5332	0.5333	0.5334	0.5334	0.5335
101.8	0.5329	0.5330	0.5331	0.5332	0.5333	0.5333	0.5334	0.5335	0.5336
101.9	0.5330	0.5331	0.5331	0.5332	0.5333	0.5334	0.5335	0.5336	0.5337
102.0	0.5330	0.5331	0.5332	0.5333	0.5334	0.5335	0.5336	0.5337	0.5338
102.1	0.5331	0.5332	0.5333	0.5334	0.5335	0.5336	0.5336	0.5337	0.5338
102.2	0.5332	0.5333	0.5334	0.5335	0.5335	0.5336	0.5337	0.5338	0.5339
102.3	0.5333	0.5334	0.5334	0.5335	0.5336	0.5337	0.5338	0.5339	0.5340
102.4	0.5333	0.5334	0.5335	0.5336	0.5337	0.5338	0.5339	0.5340	0.5340
102.5	0.5334	0.5335	0.5336	0.5337	0.5338	0.5339	0.5339	0.5340	0.5341
102.6	0.5335	0.5336	0.5337	0.5338	0.5338	0.5339	0.5340	0.5341	0.5342
102.7	0.5336	0.5337	0.5337	0.5338	0.5339	0.5340	0.5341	0.5342	0.5343
102.8	0.5336	0.5337	0.5338	0.5339	0.5340	0.5341	0.5342	0.5343	0.5343
102.9	0.5337	0.5338	0.5339	0.5340	0.5341	0.5342	0.5342	0.5343	0.5344
103.0	0.5338	0.5339	0.5340	0.5341	0.5341	0.5342	0.5343	0.5344	0.5345
103.1	0.5339	0.5339	0.5340	0.5341	0.5342	0.5343	0.5344	0.5345	0.5346
103.2	0.5339	0.5340	0.5341	0.5342	0.5343	0.5344	0.5345	0.5345	0.5346
103.3	0.5340	0.5341	0.5342	0.5343	0.5344	0.5344	0.5345	0.5346	0.5347
103.4	0.5341	0.5342	0.5343	0.5343	0.5344	0.5345	0.5346	0.5347	0.5348
103.5	0.5342	0.5342	0.5343	0.5344	0.5345	0.5346	0.5347	0.5348	0.5349
103.6	0.5342	0.5343	0.5344	0.5345	0.5346	0.5347	0.5348	0.5348	0.5349
103.7	0.5343	0.5344	0.5345	0.5346	0.5347	0.5347	0.5348	0.5349	0.5350
103.8	0.5344	0.5345	0.5346	0.5346	0.5347	0.5347	0.5348	0.5349	0.5350
103.9	0.5345	0.5345	0.5346	0.5347	0.5348	0.5349	0.5350	0.5351	0.5352

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TABLE 24E - FOR NGL ~~& AND~~ LPG LIQUIDS
TEMPERATURE VOLUME CORRECTION TO 60°F

TEMP. (°F)	RELATIVE DENSITY 60/60 DEGREES °F								TEMP. (°F)
	0.4000	0.4001	0.4002	0.4003	0.4004	0.4005	0.4006	0.4007	
FACTOR FOR CORRECTING VOLUME TO 60°F									
50.0	1.03140	1.03137	1.03135	1.03133	1.03130	1.03128	1.03125	1.03123	50.0
50.1	1.03110	1.03107	1.03105	1.03102	1.03100	1.03098	1.03095	1.03093	50.1
50.2	1.03079	1.03077	1.03075	1.03072	1.03070	1.03068	1.03065	1.03063	50.2
50.3	1.03049	1.03047	1.03044	1.03042	1.03040	1.03037	1.03035	1.03033	50.3
50.4	1.03019	1.03017	1.03014	1.03012	1.03010	1.03007	1.03005	1.03003	50.4
50.5	1.02989	1.02986	1.02984	1.02982	1.02979	1.02977	1.02975	1.02973	50.5
50.6	1.02958	1.02956	1.02954	1.02952	1.02949	1.02947	1.02945	1.02942	50.6
50.7	1.02928	1.02926	1.02924	1.02921	1.02919	1.02917	1.02915	1.02912	50.7
50.8	1.02898	1.02896	1.02893	1.02891	1.02889	1.02887	1.02884	1.02882	50.8
50.9	1.02867	1.02865	1.02863	1.02861	1.02859	1.02856	1.02854	1.02852	50.9
51.0	1.02837	1.02835	1.02833	1.02830	1.02828	1.02826	1.02824	1.02822	51.0
51.1	1.02807	1.02804	1.02802	1.02800	1.02798	1.02796	1.02794	1.02791	51.1
51.2	1.02776	1.02774	1.02772	1.02770	1.02768	1.02765	1.02763	1.02761	51.2
51.3	1.02746	1.02744	1.02742	1.02739	1.02737	1.02735	1.02733	1.02731	51.3
51.4	1.02715	1.02713	1.02711	1.02709	1.02707	1.02705	1.02703	1.02701	51.4
51.5	1.02685	1.02683	1.02681	1.02679	1.02676	1.02674	1.02672	1.02670	51.5
51.6	1.02654	1.02652	1.02650	1.02648	1.02646	1.02644	1.02642	1.02640	51.6
51.7	1.02624	1.02622	1.02620	1.02618	1.02616	1.02614	1.02612	1.02610	51.7
51.8	1.02593	1.02591	1.02589	1.02587	1.02585	1.02583	1.02581	1.02579	51.8
51.9	1.02563	1.02561	1.02559	1.02557	1.02555	1.02553	1.02551	1.02549	51.9
52.0	1.02532	1.02530	1.02528	1.02526	1.02524	1.02522	1.02520	1.02518	52.0
52.1	1.02501	1.02499	1.02497	1.02495	1.02494	1.02492	1.02490	1.02488	52.1
52.2	1.02471	1.02469	1.02467	1.02465	1.02463	1.02461	1.02459	1.02457	52.2
52.3	1.02440	1.02438	1.02436	1.02434	1.02432	1.02430	1.02429	1.02427	52.3
52.4	1.02409	1.02407	1.02406	1.02404	1.02402	1.02400	1.02398	1.02396	52.4
52.5	1.02379	1.02377	1.02375	1.02373	1.02371	1.02369	1.02367	1.02366	52.5
52.6	1.02348	1.02346	1.02344	1.02342	1.02340	1.02339	1.02337	1.02335	52.6
52.7	1.02317	1.02315	1.02313	1.02312	1.02310	1.02308	1.02306	1.02304	52.7
52.8	1.02286	1.02284	1.02283	1.02281	1.02279	1.02277	1.02276	1.02274	52.8
52.9	1.02255	1.02254	1.02252	1.02250	1.02248	1.02247	1.02245	1.02243	52.9
53.0	1.02225	1.02223	1.02221	1.02219	1.02218	1.02216	1.02214	1.02212	53.0
53.1	1.02194	1.02192	1.02190	1.02188	1.02187	1.02185	1.02183	1.02182	53.1
53.2	1.02163	1.02161	1.02159	1.02158	1.02156	1.02154	1.02153	1.02151	53.2
53.3	1.02132	1.02130	1.02128	1.02127	1.02125	1.02123	1.02122	1.02120	53.3
53.4	1.02101	1.02099	1.02098	1.02096	1.02094	1.02093	1.02091	1.02089	53.4
53.5	1.02070	1.02068	1.02067	1.02065	1.02063	1.02062	1.02060	1.02059	53.5
53.6	1.02039	1.02037	1.02036	1.02034	1.02032	1.02031	1.02029	1.02028	53.6
53.7	1.02008	1.02006	1.02005	1.02003	1.02002	1.02000	1.01998	1.01997	53.7
53.8	1.01977	1.01975	1.01974	1.01972	1.01971	1.01969	1.01967	1.01966	53.8

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53.9	1.01946	1.01944	1.01943	1.01941	1.01940	1.01938	1.01937	1.01935	53.9
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TABLE 53E - FOR NGL ~~AND~~ LPG LIQUIDS
DENSITY REDUCTION TO 15°C

TEMP. (°C)	OBSERVED DENSITY										TEMP. (°C)
	CORRESPONDING DENSITY AT 15°C										
31.0	352.6	352.6	352.7	352.9	353.2	353.5	353.9	354.5	355.2	355.2	31.0
32.0	356.8	356.8	356.9	357.0	357.2	357.5	357.8	358.1	358.5	358.5	32.0
33.0	359.6	359.6	359.7	359.7	359.9	360.1	360.3	360.7	361.1	361.1	33.0
34.0	362.1	362.2	362.2	362.3	362.4	362.6	362.9	363.3	363.7	363.7	34.0
35.0	364.7	364.7	364.7	364.8	365.0	365.2	365.5	365.9	366.3	366.3	35.0
36.0	367.2	367.2	367.3	367.4	367.5	367.8	368.1	368.4	368.9	368.9	36.0
37.0	369.7	369.8	369.8	369.9	370.1	370.3	370.6	371.0	371.5	371.5	37.0
38.0	372.3	372.3	372.4	372.5	372.7	372.9	373.2	373.6	374.1	374.1	38.0
39.0	374.8	374.9	374.9	375.1	375.2	375.5	375.8	376.2	376.7	376.7	39.0
40.0	377.4	377.4	377.5	377.6	377.8	378.0	378.4	378.8	379.3	379.3	40.0
41.0	379.9	380.0	380.1	380.2	380.4	380.6	380.9	381.4	381.9	381.9	41.0
42.0	382.5	382.5	382.6	382.7	382.9	383.2	383.5	383.9	384.5	384.5	42.0
43.0	385.1	385.1	385.2	385.3	385.5	385.8	386.1	386.5	387.0	387.0	43.0
44.0	387.6	387.7	387.7	387.9	388.1	388.3	388.7	389.1	389.6	389.6	44.0
45.0	390.2	390.2	390.3	390.4	390.6	390.9	391.2	391.7	392.2	392.2	45.0
46.0	392.7	392.8	392.9	393.0	393.2	393.5	393.8	394.3	394.8	394.8	46.0
47.0	395.3	395.4	395.4	395.6	395.8	396.0	396.4	396.8	397.4	397.4	47.0
48.0	397.9	397.9	398.0	398.1	398.4	398.6	399.0	399.4	399.9	399.9	48.0
49.0	400.4	400.5	400.6	400.7	400.9	401.2	401.5	402.0	402.5	402.5	49.0
50.0	403.0	403.1	403.1	403.3	403.5	403.8	404.1	404.6	405.1	405.1	50.0
51.0	405.6	405.6	405.7	405.9	406.1	406.3	406.7	407.1	407.7	407.7	51.0
52.0	408.1	408.2	408.3	408.4	408.6	408.9	409.3	409.7	410.2	410.2	52.0
53.0	410.7	410.8	410.9	411.0	411.2	411.5	411.8	412.3	412.8	412.8	53.0
54.0	413.3	413.3	413.4	413.6	413.8	414.1	414.4	414.9	415.4	415.4	54.0
55.0	415.8	415.9	416.0	416.1	416.4	416.6	417.0	417.4	418.0	418.0	55.0
56.0	418.4	418.5	418.6	418.7	418.9	419.2	419.6	420.0	420.5	420.5	56.0
57.0	421.0	421.0	421.1	421.3	421.5	421.8	422.1	422.6	423.1	423.1	57.0
58.0	423.6	423.6	423.7	423.9	424.1	424.4	424.7	425.1	425.7	425.7	58.0
59.0	426.1	426.2	426.3	426.4	426.7	426.9	427.3	427.7	428.2	428.2	59.0
60.0	428.7	428.8	428.9	429.0	429.2	429.5	429.9	430.2	430.7	430.7	60.0
61.0	431.1	431.1	431.2	431.3	431.5	431.7	432.0	432.4	432.8	432.8	61.0
62.0	433.2	433.3	433.4	433.5	433.7	433.9	434.2	434.6	435.0	435.0	62.0
63.0	435.4	435.5	435.5	435.7	435.8	436.1	436.4	436.7	437.1	437.1	63.0
64.0	437.6	437.6	437.7	437.8	438.0	438.2	438.5	438.9	439.3	439.3	64.0
65.0	439.8	439.8	439.9	440.0	440.2	440.4	440.7	441.0	441.4	441.4	65.0
66.0	441.9	442.0	442.1	442.2	442.3	442.6	442.8	443.2	443.6	443.6	66.0
67.0	444.1	444.1	444.2	444.3	444.5	444.7	445.0	445.3	445.8	445.8	67.0
68.0	446.3	446.3	446.4	446.5	446.7	446.9	447.2	447.5	447.9	447.9	68.0
69.0	448.4	448.5	448.6	448.7	448.8	449.0	449.3	449.7	450.1	450.1	69.0

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70.0	450.6	450.7	450.7	450.8	451.0	451.2	451.5	451.8	452.2	70.0
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TABLE 54E - FOR NGL ~~&AND~~ LPG LIQUIDS
TEMPERATURE VOLUME CORRECTION TO 15°C

TEMP. (°C)	DENSITY AT 15 DEGREES °C									TEMP. (°C)
	400.00	405.00	410.00	415.00	420.00	425.00	430.00	435.00	FACTOR FOR CORRECTING VOLUME TO 15°C	
10.0	1.02824	1.02719	1.02623	1.02535	1.02453	1.02377	1.02306	1.02220	10.0	10.0
10.5	1.02551	1.02456	1.02368	1.02288	1.02214	1.02145	1.02081	1.02003	10.5	10.5
11.0	1.02276	1.02190	1.02112	1.02040	1.01974	1.01912	1.01855	1.01785	11.0	11.0
11.5	1.01999	1.01923	1.01854	1.01791	1.01732	1.01678	1.01628	1.01566	11.5	11.5
12.0	1.01720	1.01654	1.01595	1.01540	1.01489	1.01443	1.01399	1.01346	12.0	12.0
12.5	1.01438	1.01384	1.01333	1.01287	1.01245	1.01206	1.01169	1.01125	12.5	12.5
13.0	1.01155	1.01111	1.01070	1.01033	1.00999	1.00967	1.00938	1.00902	13.0	13.0
13.5	1.00870	1.00836	1.00806	1.00777	1.00752	1.00728	1.00706	1.00679	13.5	13.5
14.0	1.00582	1.00559	1.00539	1.00520	1.00503	1.00487	1.00472	1.00454	14.0	14.0
14.5	1.00292	1.00281	1.00270	1.00261	1.00252	1.00244	1.00237	1.00227	14.5	14.5
15.0	1.00000	1.00000	1.00000	1.00000	1.00000	1.00000	1.00000	1.00000	15.0	15.0
15.5	0.99705	0.99717	0.99728	0.99737	0.99746	0.99754	0.99762	0.99771	15.5	15.5
16.0	0.99409	0.99432	0.99453	0.99473	0.99491	0.99507	0.99523	0.99541	16.0	16.0
16.5	0.99109	0.99145	0.99177	0.99207	0.99234	0.99259	0.99282	0.99310	16.5	16.5
17.0	0.98807	0.98855	0.98899	0.98938	0.98975	0.99008	0.99040	0.99077	17.0	17.0
17.5	0.98503	0.98563	0.98618	0.98668	0.98714	0.98757	0.98796	0.98843	17.5	17.5
18.0	0.98196	0.98269	0.98335	0.98396	0.98452	0.98503	0.98551	0.98608	18.0	18.0
18.5	0.97886	0.97972	0.98050	0.98122	0.98187	0.98248	0.98304	0.98371	18.5	18.5
19.0	0.97573	0.97673	0.97763	0.97846	0.97921	0.97991	0.98055	0.98133	19.0	19.0
19.5	0.97257	0.97371	0.97474	0.97567	0.97653	0.97732	0.97805	0.97893	19.5	19.5
20.0	0.96939	0.97066	0.97182	0.97287	0.97383	0.97472	0.97553	0.97652	20.0	20.0
20.5	0.96617	0.96759	0.96887	0.97004	0.97111	0.97209	0.97300	0.97409	20.5	20.5
21.0	0.96293	0.96449	0.96590	0.96719	0.96837	0.96945	0.97045	0.97165	21.0	21.0
21.5	0.95965	0.96136	0.96291	0.96432	0.96561	0.96679	0.96788	0.96919	21.5	21.5
22.0	0.95633	0.95820	0.95989	0.96142	0.96282	0.96411	0.96529	0.96671	22.0	22.0
22.5	0.95299	0.95501	0.95684	0.95850	0.96002	0.96141	0.96269	0.96422	22.5	22.5
23.0	0.94960	0.95179	0.95376	0.95556	0.95719	0.95868	0.96006	0.96171	23.0	23.0
23.5	0.94618	0.94854	0.95066	0.95258	0.95434	0.95594	0.95742	0.95919	23.5	23.5
24.0	0.94273	0.94525	0.94753	0.94959	0.95146	0.95318	0.95476	0.95665	24.0	24.0
24.5	0.93923	0.94193	0.94436	0.94656	0.94856	0.95039	0.95207	0.95408	24.5	24.5
25.0	0.93570	0.93858	0.94117	0.94351	0.94564	0.94758	0.94937	0.95150	25.0	25.0
25.5	0.93212	0.93519	0.93794	0.94043	0.94269	0.94475	0.94665	0.94891	25.5	25.5
26.0	0.92850	0.93176	0.93468	0.93732	0.93971	0.94190	0.94390	0.94629	26.0	26.0
26.5	0.92483	0.92829	0.93138	0.93417	0.93671	0.93902	0.94113	0.94365	26.5	26.5
27.0	0.92112	0.92478	0.92805	0.93100	0.93367	0.93611	0.93834	0.94100	27.0	27.0
27.5	0.91736	0.92123	0.92469	0.92780	0.93062	0.93318	0.93553	0.93832	27.5	27.5
28.0	0.91355	0.91764	0.92128	0.92456	0.92753	0.93022	0.93269	0.93562	28.0	28.0
28.5	0.90969	0.91400	0.91784	0.92129	0.92441	0.92724	0.92983	0.93290	28.5	28.5
29.0	0.90577	0.91032	0.91436	0.91798	0.92126	0.92423	0.92695	0.93016	29.0	29.0

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29.5	0.90180	0.90659	0.91084	0.91464	0.91807	0.92119	0.92404	0.92740	29.5
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TABLE 59E - FOR NGL ~~AND~~ LPG LIQUIDS
DENSITY REDUCTION TO 20°C

TEMP. (°C)	OBSERVED DENSITY										TEMP. (°C)
	210.0	215.0	220.0	225.0	230.0	235.0	240.0	245.0	250.0	CORRESPONDING DENSITY AT 20°C	
31.0	332.9	332.9	333.1	333.3	333.6	334.0	334.5	335.2	336.1	31.0	
32.0	338.0	338.1	338.1	338.3	338.5	338.9	339.2	339.7	340.2	32.0	
33.0	341.6	341.6	341.7	341.8	341.9	342.2	342.5	343.0	343.5	33.0	
34.0	344.8	344.8	344.9	345.0	345.1	345.4	345.7	346.2	346.7	34.0	
35.0	347.9	347.9	348.0	348.1	348.3	348.5	348.9	349.3	349.9	35.0	
36.0	351.0	351.0	351.1	351.2	351.4	351.6	352.0	352.4	353.0	36.0	
37.0	354.0	354.0	354.1	354.2	354.4	354.7	355.0	355.5	356.0	37.0	
38.0	357.0	357.0	357.1	357.2	357.4	357.7	358.0	358.5	359.1	38.0	
39.0	359.9	359.9	360.0	360.1	360.3	360.6	361.0	361.5	362.0	39.0	
40.0	362.8	362.9	362.9	363.1	363.3	363.6	363.9	364.4	365.0	40.0	
41.0	365.7	365.8	365.8	366.0	366.2	366.5	366.8	367.3	367.9	41.0	
42.0	368.6	368.6	368.7	368.9	369.1	369.3	369.7	370.2	370.8	42.0	
43.0	371.4	371.5	371.6	371.7	371.9	372.2	372.6	373.1	373.6	43.0	
44.0	374.3	374.3	374.4	374.6	374.8	375.1	375.4	375.9	376.5	44.0	
45.0	377.1	377.1	377.2	377.4	377.6	377.9	378.3	378.7	379.3	45.0	
46.0	379.9	379.9	380.0	380.2	380.4	380.7	381.1	381.5	382.1	46.0	
47.0	382.7	382.7	382.8	383.0	383.2	383.5	383.9	384.3	384.9	47.0	
48.0	385.5	385.5	385.6	385.8	386.0	386.3	386.6	387.1	387.7	48.0	
49.0	388.2	388.3	388.4	388.5	388.7	389.0	389.4	389.9	390.5	49.0	
50.0	391.0	391.0	391.1	391.3	391.5	391.8	392.2	392.6	393.2	50.0	
51.0	393.7	393.8	393.9	394.0	394.3	394.6	394.9	395.4	396.0	51.0	
52.0	396.5	396.5	396.6	396.8	397.0	397.3	397.7	398.1	398.7	52.0	
53.0	399.2	399.2	399.4	399.5	399.7	400.0	400.4	400.9	401.4	53.0	
54.0	401.9	402.0	402.1	402.2	402.5	402.7	403.1	403.6	404.1	54.0	
55.0	404.6	404.7	404.8	405.0	405.2	405.5	405.8	406.3	406.9	55.0	
56.0	407.3	407.4	407.5	407.7	407.9	408.2	408.5	409.0	409.6	56.0	
57.0	410.0	410.1	410.2	410.4	410.6	410.9	411.2	411.7	412.3	57.0	
58.0	412.7	412.8	412.9	413.1	413.3	413.6	413.9	414.4	414.9	58.0	
59.0	415.4	415.5	415.6	415.8	416.0	416.3	416.6	417.1	417.6	59.0	
60.0	418.1	418.2	418.3	418.5	418.7	419.0	419.3	419.7	420.2	60.0	
61.0	420.6	420.7	420.8	420.9	421.1	421.3	421.6	422.0	422.5	61.0	
62.0	422.9	423.0	423.1	423.2	423.4	423.6	423.9	424.3	424.8	62.0	
63.0	425.2	425.3	425.4	425.5	425.7	425.9	426.2	426.6	427.0	63.0	
64.0	427.5	427.6	427.7	427.8	428.0	428.2	428.5	428.9	429.3	64.0	
65.0	429.8	429.9	429.9	430.1	430.2	430.5	430.8	431.1	431.6	65.0	
66.0	432.1	432.1	432.2	432.4	432.5	432.8	433.1	433.4	433.9	66.0	
67.0	434.4	434.4	434.5	434.6	434.8	435.0	435.3	435.7	436.1	67.0	
68.0	436.7	436.7	436.8	436.9	437.1	437.3	437.6	437.9	438.4	68.0	
69.0	438.9	439.0	439.1	439.2	439.3	439.6	439.8	440.2	440.6	69.0	

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70.0	441.2	441.3	441.3	441.4	441.6	441.8	442.1	442.4	442.9	70.0
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TABLE 60E - FOR NGL ~~&AND~~ LPG LIQUIDS
TEMPERATURE VOLUME CORRECTION TO 20°C

TEMP. (°C)	DENSITY AT 20 DEGREES °C									TEMP. (°C)
	400.00	405.00	410.00	415.00	420.00	425.00	430.00	435.00	FACTOR FOR CORRECTING VOLUME TO 20°C	
10.0	1.05537	1.05348	1.05172	1.05009	1.04852	1.04671	1.04502	1.04346	10.0	
10.5	1.05278	1.05096	1.04928	1.04772	1.04623	1.04449	1.04288	1.04138	10.5	
11.0	1.05017	1.04844	1.04683	1.04534	1.04392	1.04226	1.04073	1.03930	11.0	
11.5	1.04754	1.04589	1.04437	1.04295	1.04159	1.04002	1.03856	1.03721	11.5	
12.0	1.04490	1.04333	1.04189	1.04055	1.03926	1.03777	1.03639	1.03511	12.0	
12.5	1.04224	1.04076	1.03939	1.03813	1.03691	1.03551	1.03420	1.03300	12.5	
13.0	1.03956	1.03817	1.03688	1.03569	1.03455	1.03323	1.03201	1.03087	13.0	
13.5	1.03686	1.03556	1.03436	1.03324	1.03218	1.03094	1.02980	1.02874	13.5	
14.0	1.03415	1.03294	1.03182	1.03078	1.02979	1.02864	1.02758	1.02660	14.0	
14.5	1.03142	1.03030	1.02926	1.02830	1.02739	1.02633	1.02535	1.02445	14.5	
15.0	1.02866	1.02764	1.02669	1.02581	1.02497	1.02401	1.02311	1.02228	15.0	
15.5	1.02589	1.02496	1.02410	1.02331	1.02254	1.02167	1.02086	1.02011	15.5	
16.0	1.02310	1.02227	1.02150	1.02078	1.02010	1.01932	1.01859	1.01792	16.0	
16.5	1.02029	1.01955	1.01887	1.01824	1.01764	1.01695	1.01631	1.01572	16.5	
17.0	1.01746	1.01682	1.01623	1.01569	1.01517	1.01457	1.01402	1.01351	17.0	
17.5	1.01460	1.01407	1.01357	1.01312	1.01268	1.01218	1.01172	1.01129	17.5	
18.0	1.01173	1.01130	1.01090	1.01053	1.01018	1.00977	1.00940	1.00906	18.0	
18.5	1.00883	1.00850	1.00820	1.00792	1.00766	1.00735	1.00707	1.00681	18.5	
19.0	1.00591	1.00569	1.00549	1.00530	1.00512	1.00492	1.00473	1.00455	19.0	
19.5	1.00297	1.00286	1.00275	1.00266	1.00257	1.00247	1.00237	1.00228	19.5	
20.0	1.00000	1.00000	1.00000	1.00000	1.00000	1.00000	1.00000	1.00000	20.0	
20.5	0.99701	0.99712	0.99723	0.99732	0.99741	0.99752	0.99761	0.99770	20.5	
21.0	0.99399	0.99422	0.99443	0.99463	0.99481	0.99502	0.99522	0.99539	21.0	
21.5	0.99095	0.99130	0.99162	0.99191	0.99219	0.99251	0.99280	0.99307	21.5	
22.0	0.98788	0.98835	0.98878	0.98917	0.98955	0.98998	0.99037	0.99073	22.0	
22.5	0.98478	0.98538	0.98592	0.98642	0.98689	0.98743	0.98793	0.98838	22.5	
23.0	0.98166	0.98238	0.98304	0.98364	0.98421	0.98487	0.98547	0.98602	23.0	
23.5	0.97851	0.97936	0.98013	0.98084	0.98152	0.98228	0.98299	0.98364	23.5	
24.0	0.97533	0.97631	0.97720	0.97802	0.97880	0.97968	0.98050	0.98125	24.0	
24.5	0.97212	0.97323	0.97425	0.97518	0.97606	0.97707	0.97799	0.97884	24.5	
25.0	0.96887	0.97012	0.97127	0.97231	0.97330	0.97443	0.97546	0.97641	25.0	
25.5	0.96560	0.96699	0.96826	0.96942	0.97052	0.97177	0.97292	0.97397	25.5	
26.0	0.96229	0.96383	0.96523	0.96651	0.96772	0.96910	0.97036	0.97152	26.0	
26.5	0.95895	0.96064	0.96217	0.96357	0.96490	0.96640	0.96778	0.96904	26.5	
27.0	0.95558	0.95741	0.95908	0.96061	0.96206	0.96369	0.96518	0.96656	27.0	
27.5	0.95217	0.95416	0.95597	0.95762	0.95919	0.96095	0.96257	0.96405	27.5	
28.0	0.94872	0.95087	0.95282	0.95461	0.95629	0.95820	0.95993	0.96153	28.0	
28.5	0.94523	0.94755	0.94965	0.95157	0.95338	0.95542	0.95728	0.95899	28.5	
29.0	0.94170	0.94419	0.94644	0.94850	0.95043	0.95261	0.95460	0.95643	29.0	

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29.5	0.93814	0.94080	0.94321	0.94540	0.94746	0.94979	0.95191	0.95385	29.5
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