

Investigating the Effect of Different Nanoparticles on the Interfacial Tension Reduction

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Research Article

Volume 2 Issue 7

Received Date: October 16, 2018

Published Date: November 26, 2018

DOI: 10.23880/ppej-16000176

Abstract

Nanoparticles gained respectful attention in the oil industry due to their ability to enhance physical properties for the injected fluid, and reservoir fluid. Many kinds of literature have demonstrated nanoparticles ability to decrease the interfacial tension, consequently, reduce residual oil saturation, and increase the oil recovery factor. This research aims to study the effect of nanoparticles on reducing interfacial tension between crude oil and nanofluids through applying different nanoparticles including Aluminum oxide, Nickel oxide, Zeolite, Silica, Ferric oxide, Tungsten trioxide and montmorillonite with the size of 5 nm. Different nanofluids concentrations were displaced through sand pack model, where interfacial tension between crude oil and ejected brine was estimated. Interfacial tension between crude oil/brine was measured to be 47.9 dyne/cm, finally, the interfacial tension was reduced to 30.5009 dyne/cm by using nano montmorillonite.

Keywords: Nanoparticles; Enhanced Oil Recovery; Interfacial Tension Reduction; Sandpack model

Introduction

The probability of exploring new huge hydrocarbon fields is not as enormous as before. On the other hand, exploring new oil fields is uneconomical due to their highly expensive costs [1,2]. Therefore, the most economical solution is to produce the trapped oil inside the previously developed wells. Surfactant flooding and

nanoparticles displacement are implemented on a high scale to produce this trapped oil and increase the oil recovery [3]. The use of nanotechnology was commonly needed in the downstream industry [4]. However, there are researches that have approved the great impact of using nanoparticles inside the reservoirs, where an enhancement of viscosity, interfacial tension, and wettability alteration occur [5]. Zhi- Yong, et al. [6] stated

that TiO₂ nanofluid increases the water viscosity so, providing favorable mobility ratios, which in turn improve macroscopic displacement proficiency [7], and also improve pore-scale microscopic displacement [8]. Bayat, et al. [9] settled that the use of water-based Al₂O₃, TiO₂, and SiO₂ nanofluids meaningfully reduce the interfacial tension between crude oil /water, and consequently increased the additional oil recovery from a limestone reservoir. Adsorption of lipophobic and hydrophilic polysilicon nanoparticles (~ 10 to 500 nm), were generated to explore the efficiency of wettability alteration with regard to a sandstone surface. The experiments revealed that the nanoparticles effectively change the wettability of the sandstone surface, which improves the oil recovery factor [10]. Moreover, Ehtesabi, et al. [11] have developed inexpensive and environmental friendly TiO₂ nanofluids by mixing titanium tetraisopropoxide, H₂O₂, and water for heavy oil recovery from sandstone reservoirs. Al-Anssari, et al. [12] stated that silica nanofluids can alter the wettability of oil-wet calcite surfaces to strongly water-wet. Sedaghat, et al. [13] used a micro model to generate several flooding displacements to monitor the effect of SiO₂ & TiO₂ nanoparticles on wettability alteration in the presence of partially hydrolyzed polyacrylamide and sodium dodecylsulfate. The literature reported by El-hoshoudy, et al., stated that silica nanoparticles can alter rock wettability from oil-wet to water wet [14-18]. For the optimum nanofluid displacement, the concentration of nanoparticles should exceed the critical micelle concentration, to decrease the interfacial tension and to increase the oil recovery [19]. Therefore, this research aims to investigate the effect of nanoparticles flooding on the interfacial tension and the oil recovery. These nanoparticles including; Zeolite, tungsten trioxide (WO₃), Montmorillonite, Ferric oxide (Fe₂O₃), Silica oxide (SiO₂) and Potash Aluminum Sulfate. Each nanoparticle type was used in four different concentration (0.005, 0.01, 0.1 & 1 wt %). Finally, the interfacial tension between crude oil and brine was estimated after the conventional brine flooding.

Experimental Work

Preparation of Brine

Sodium chloride (NaCl) was used for preparing brine with a concentration of 35,000 ppm. Then sand pack was initially saturated with this brine and then crude oil displaced this brine to have the initial conditions like the reservoir conditions. Moreover, nanofluids with different

nanoparticles concentrations subjected to sonication for 15 minutes in brine solution [20].

Equipment used for Fluids Characterization

Fluids density measured through density meter DMA 4100M, while Chandler rolling ball viscometer was used to measure the viscosity of the fluid. Finally, interfacial tension between displaced crude oil and effluent brine were determined from surface tension measurements by Du Noüy Ring Tensiometer [14,21]. Table 1 summarizes the measure physical properties of the crude oil and brine solution.

Fluid type	Physical property	Value
Crude Oil	Density, g/cc	0.8010
	API	37
	IFT, dyne/cm	47.9
	Viscosity, cp	6.0
Brine solution	Density, g/cc	1.3
	Viscosity, cp	1.584

Table 1: Measured properties of the brine and crude oil.

Nanofluids Preparation

Nanofluids are kinetically stable diffusions of nanoparticles in various base fluids, such as water, polymeric solutions, glycols, or alcohols. Such nanofluids can be applied in various applications, including high-temperature operations [22], asphaltene inhibition [23], wettability alteration [24] and in oil recovery displacement operations [12]. Other benefits involve stable rheological properties of the base fluids, IFT reduction of the crude oil/water system, and alteration the of the reservoir rock wettability [12,25,26]. In this study, nanofluids were prepared by the required concentrations in the previously prepared brine. Then this solution undergoes sonication for 2-3 hours to make all nanoparticles suspended inside the solution or nanofluid.

Sand Pack Handling and Flooding Experiments

Flooding experiments carried out through linear sandstone model as depicted in Figure 1, through two-main stages;

Brine Flooding (Saturation)

The sandstone was evacuated and then saturated with brine solution for about 12 hours to establish ionic equilibrium. Brine solution flooded at a constant flow rate of 60 cc/h through the sand packed model, where the

differential pressures between the inlet and the outlet were monitored. After saturation was achieved, brine permeability (K_w) determined by measuring the pressure drop across the model and the flow rate using Darcy's law [27].

Crude Oil Flooding

The stock tank oil was injected at a rate of 60 cc/h by displacement pump until the water production ceased (i.e. water cut <1%). Crude oil permeability at initial water saturation (S_{wi}) was also measured [2]. After oil injection (API= 30.749, supplied from the western desert in Egypt), the sand pack was brine flooded until the oil production became negligible (oil cut <1%). At this stage recovered oil by primary and secondary methods is exhausted. After

brine injection, about 3.0 pore volume of nanofluids slug was flooded, where the oil production was determined on a volume basis to calculate recovery percentage. The viscosity and interfacial tension of the displaced oil was measured. Relative permeability curve was constructed to determine the wettability alteration. This case was considered as a reference case for each following case, where the results of each nanofluid case were compared by the first case of the conventional water flooding. Porosity, permeability, initial oil, and water saturation as well as residual oil saturation determined through Equations 1-6. The bulk volume, porosity, and permeability of the used model found to be 425cc, 28.2%, and 0.632darcy respectively.

$$\text{Porosity}(\Phi) = \left(\frac{\text{Pore volume}}{\text{Bulk volume}} \right) \quad (1)$$

$$\text{Pore Volume} = \frac{(\text{Wet Weight} - \text{Dry Weight})}{\text{Formation Brine Density}} \quad (2)$$

$$K = \frac{q\mu L}{A\Delta P} \quad (3)$$

$$S_{wi} = \frac{\text{Volume of Water Remain (@ water cut <1\%)}}{\text{Pore Volume}} \quad (4)$$

$$S_{oi} = \frac{\text{Volume of Oil Injected}}{\text{Pore Volume}} = 1 - S_{wi} \quad (5)$$

$$S_{or} = \frac{\text{Volume of Oil Remain @ oil cut <1\%}}{\text{Pore Volume}} \quad (6)$$



Figure 1: Linear sandpack model.

Injection of Nanofluids

After constructing the conventional water flooding as a reference case, each nanofluid was injected at different concentrations (0.005, 0.01, 0.1 & 1 wt %) after applying sonication for 15 minutes. The oil recovery of each case was determined along with measuring the viscosity,

interfacial tension, and wettability alteration. Accordingly, the reason behind the change (whether an enhancement or reduction) in oil recovery for each case, was identified (due to the change in oil viscosity, interfacial tension, and wettability).

Results and Discussion

Reduction of IFT

Figure 2 represents the percentage of IFT reduction for each conducted case, compared to the conventional waterflooding case. It is so clear that nanoparticles especially montmorillonite, silica nanoparticles, and ferric oxide has shown a great performance in reducing the IFT between crude oil and displaced fluid [28]. This behavior may resort to aggregation of nanoparticles in a micelle-like form at certain concentrations which adsorbed at the oil/ water boundary surface and consequently decrease the interfacial tension (IFT).

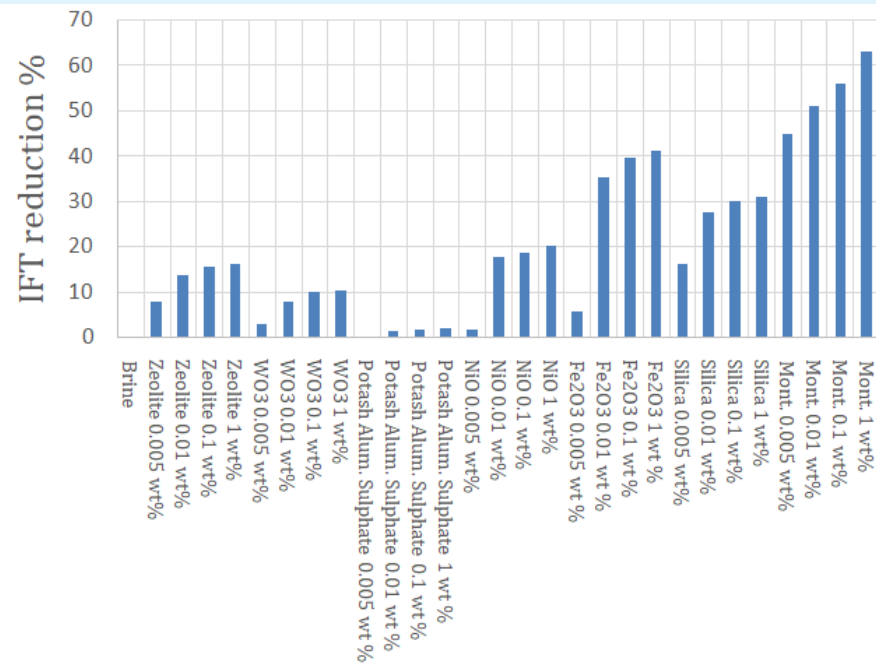


Figure 2: IFT reduction % relative to nanofluids type and concentration.

Oil Recovery Factor

Figure 3 represents the percentage of the change in oil recovery factor for each conducted case, compared to the conventional waterflooding case. It is so clear that montmorillonite and silica both gave the highest improvement to the oil recovery factor. This may be ascertained to nanofluids ability to adsorb onto rock

surface, so change rock wettability from oil-wet to water-wet, which in turn enhance oil recovery. Moreover, by nanoparticles adsorption onto rock surface, they displace some of the oil by wedge-like mechanism, in which nanoparticles act as a knife dislodge the oil from the rock surface, so increase the recovery factor [29].

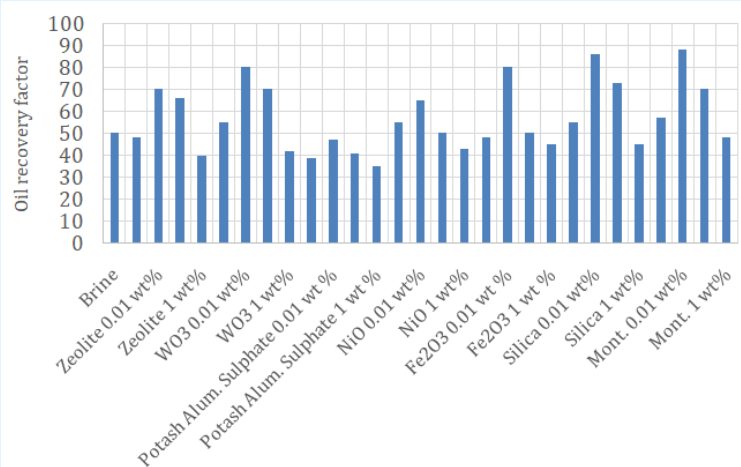


Figure 3: percentage of oil recovery factor related to nanoparticles type and concentration.

Economical Profile

To find whether the need for this recovery mechanism is applicable or not. The net present value for the total project has to be estimated. First, the initial oil in place for a field is assumed to be 100 MM STB and the field will produce from 4 production wells with the same decline rate. Also, the number of years for production is assumed to be 10 years. Moreover, drilling and production operational cost is assumed to be 25 million dollars

considering the cost of flooding operations. More and more, a discount factor of 10% is also assumed. All the previous assumptions were applied to all the cases. However, the only variable now is the nano cost that differs from each nano type and its concentration. Therefore, by considering the PV injected to reach the optimum oil recovery using this mechanism, now the cumulative net present value for the total project can be calculated as shown in Figure 4.

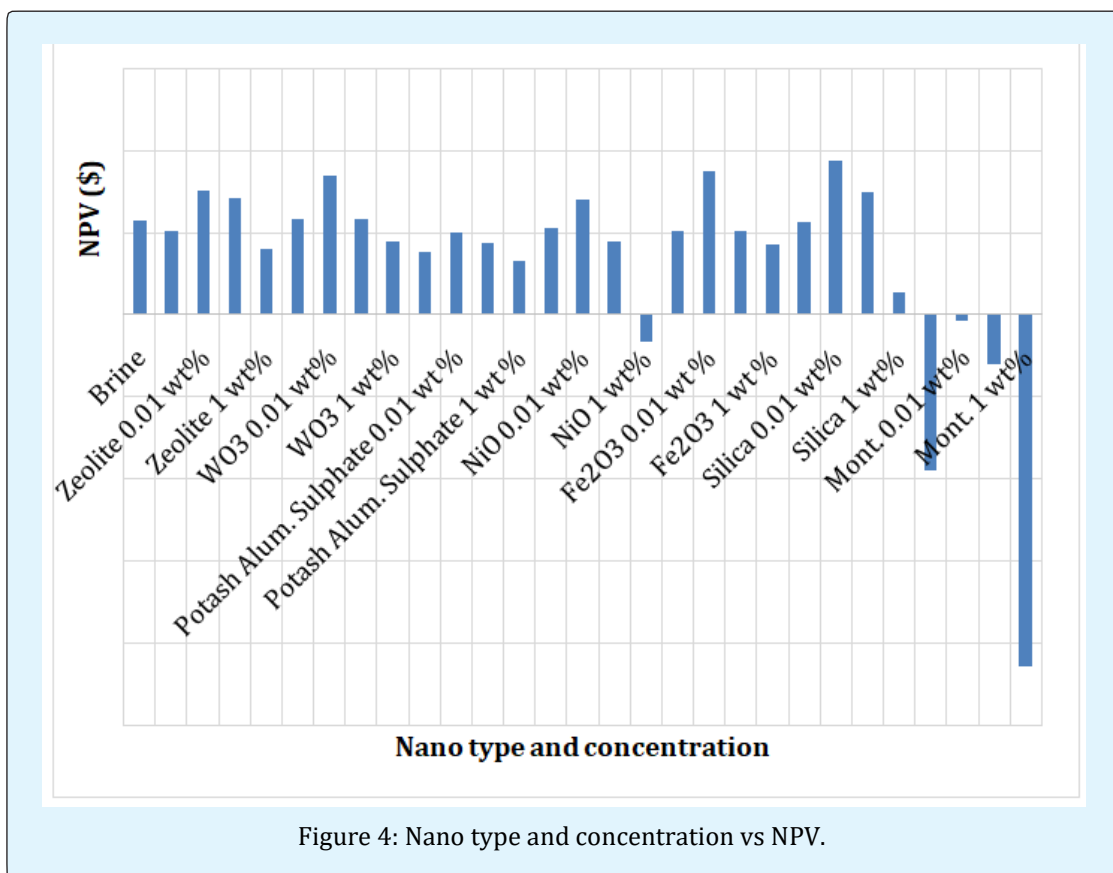


Figure 4: Nano type and concentration vs NPV.

Conclusion

Nanoparticles have a great ability to reduce interfacial tension. Nano montmorillonite flooding has shown its great performance in decreasing the interfacial tension, where 0.005 wt% of Montmorillonite reduce interfacial tension by 40%, 0.01 wt% reduce interfacial tension by 50% and both concentrations of 0.1 wt% and 1 wt% has reduced interfacial tension to 60%. Accordingly, it is proved that increasing nano concentration from 0.005 wt % to 0.01 or 0.1 wt % lead to a noticeable enhancement in interfacial tension for all nanoparticles. Continuous

increasing of nanoparticles concentration till 1 wt % will continue enhancing interfacial tension but slight improvement will occur for this concentration. However, this does not guarantee to increase the oil recovery as the relatively high nano concentration will plug the pore spaces leading the oil to be difficult production that will decrease the oil recovery. The best oil recovery came from nano montmorillonite flooding. However, it was economically proven that Montmorillonite is too expensive to be used as it gives a net present value of negative value. The best nanofluid that gave highest oil recovery, with applicable reduction of interfacial tension

and can be economically applied is Nano Fe₂O₃, that gave about 40% reduction in the interfacial tension and the highest oil recovery of 80% and it was proven that it economically applicable to be used.

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