
Polyphosphazene-based gas separation membranes: Pushing the boundaries

254th ACS National Meeting in Washington, DC, August
20-24, 2017

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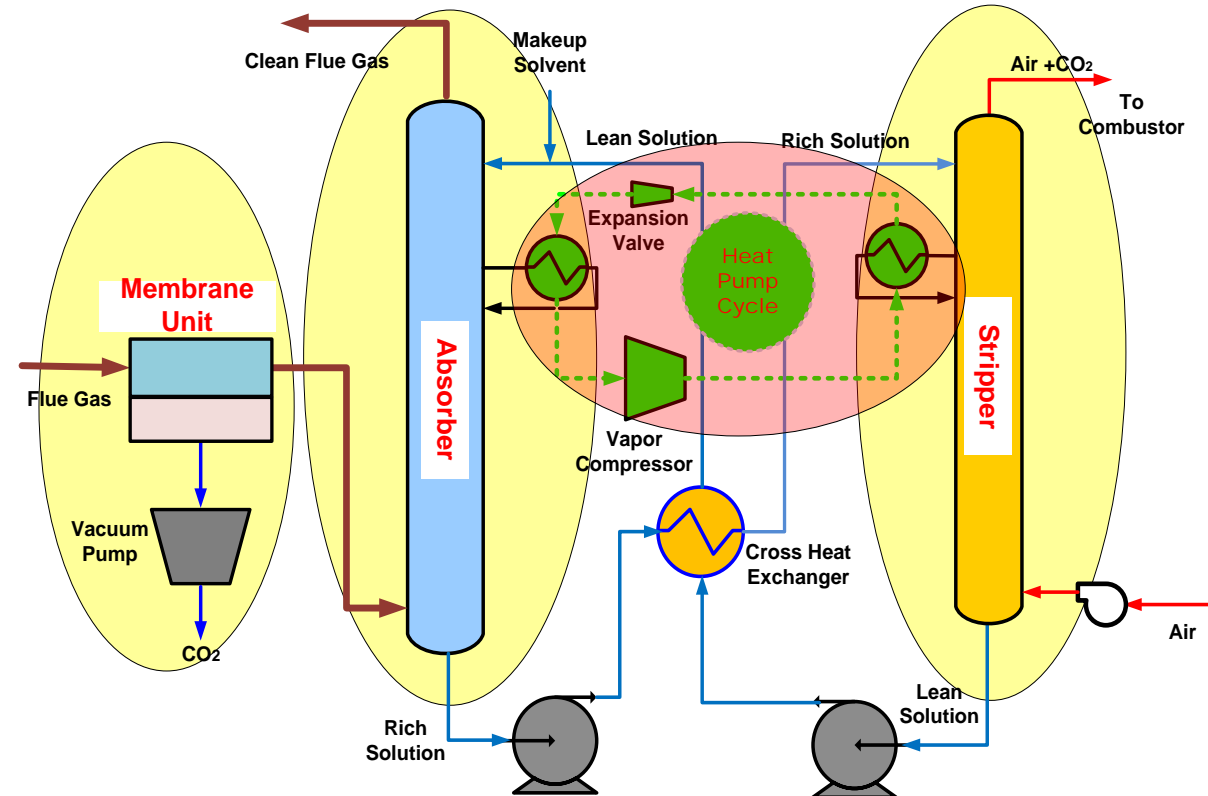
Membrane/Solvent Integrated Process

Advantages

- Tail-end technology which is easily used in retrofits
- No steam extraction is required
- Heat pump is seamlessly integrated into the cooling and heating of absorption/stripping process
- Operating pressure of the stripper will be very flexible depending on the low quality heat

Disadvantage

- Capital cost could be intensive



Synthetic Membranes

- Used in variety of industrial, medical, and environmental applications.
 - desalination, dialysis, sterile filtration, food processing, dehydration
- Low energy requirements
- Compact design
- No moving parts and modular

Permeability/Selectivity Material Property

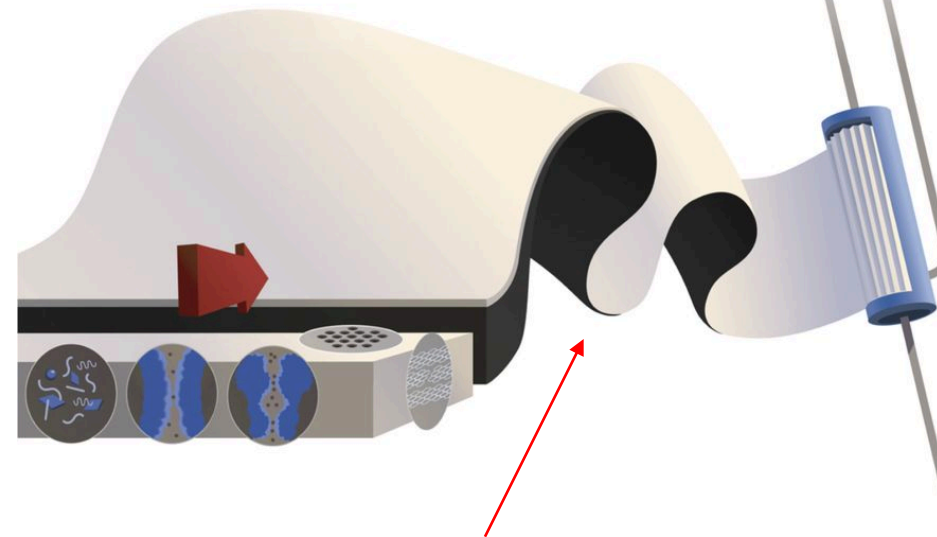
Materials
design
Permeability

Material Processing

Membrane
Permeance

Membrane
device
Module type

Membrane
process
Optimal process
Permeate quality
yield



Accessing thin membranes

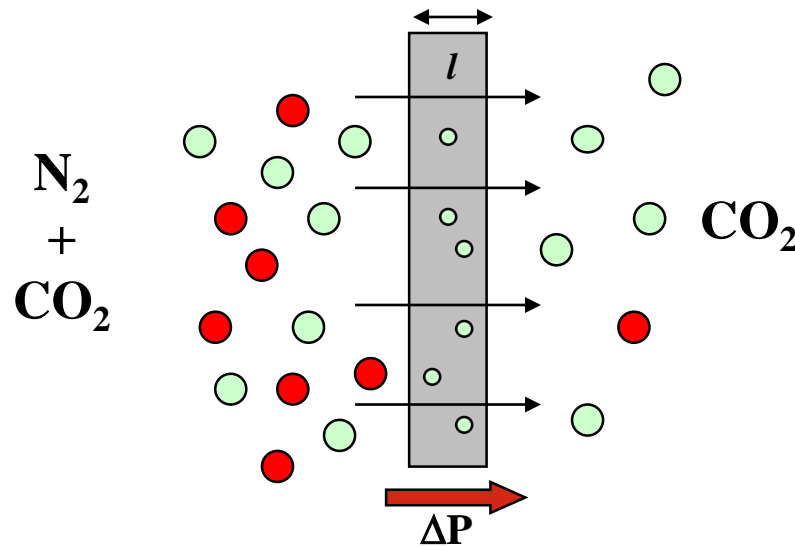
Stages

Membrane Terms

- **Permeability** is a *material* property: describes rate of permeation of a solute through a material, normalized by its thickness and the pressure driving force
- **Permeance** is a *membrane* property: calculated as solute flux through the membrane normalized by the pressure driving force (but not thickness)
- **Ideal selectivity** describes the ratio of the permeabilities (or permeances) of two different permeating species through a membrane, and is a *material* property
- High membrane **permeance** is achieved by both material selection (high **permeability**) and membrane design (low **thickness**)

CO₂ Separation Using Membranes

- Mechanism of separation: **diffusion through a non-porous membrane**
- A pressure driven process - the **driving force is the partial pressure difference** of each gas in the feed and permeate.



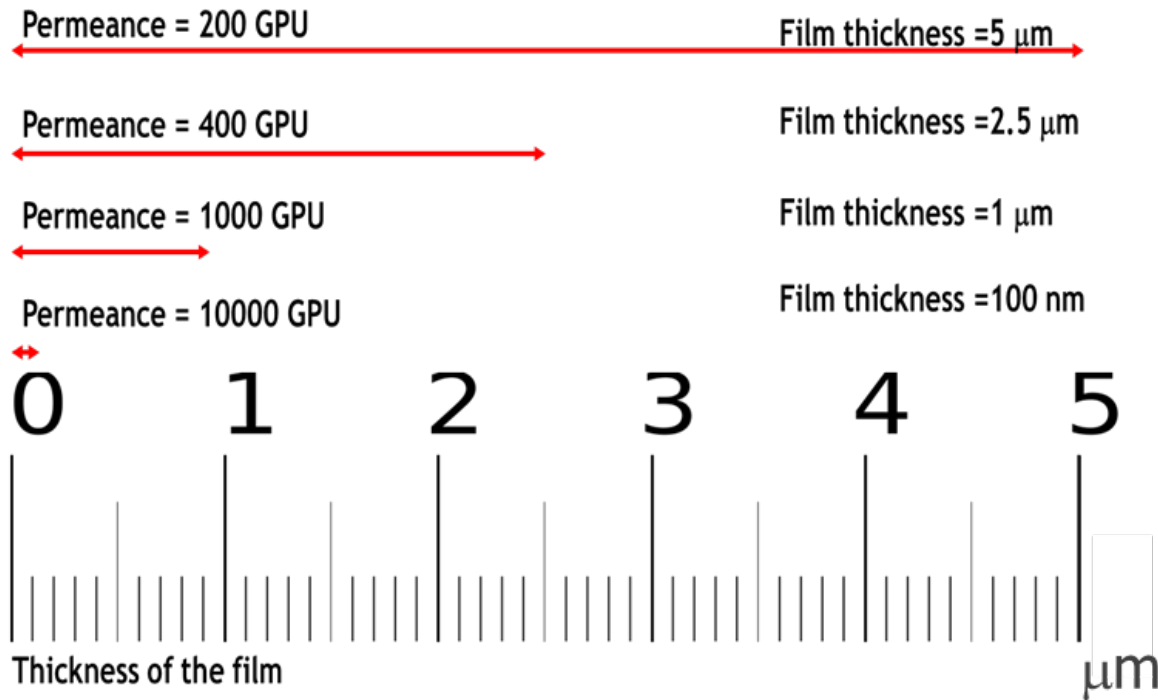
- **Selective removal of fast permeating gases from slow permeating gases.**
- **The solution-diffusion process can be approximated by Fick's law:**

$$J = \frac{P(p_1 - p_2)}{l}$$

$$P = D * S$$

- **Selectivity** - separation factor, α (typical selectivity for CO₂/N₂ is 20-45)
- **Permeability** = solubility (k) x diffusivity (D) (normalized over thickness)
- **Either high selectivity or high permeability - Trade-off.**

Permeance Vs. Permeability



- Current state-of-the-art fully commercialized membrane materials for CO₂/N₂ separations: 250 permeability with selectivity of 35-50.
- These are cast @ 100nm thickness, giving permeance of 2500 GPU.

The scale bar is in microns to illustrate permeability and permeance for a membrane material which has permeability of 1000 Barrers.

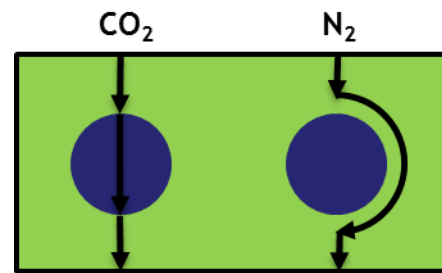
Mechanical Properties, Film Forming Ability

Membrane Material Advances

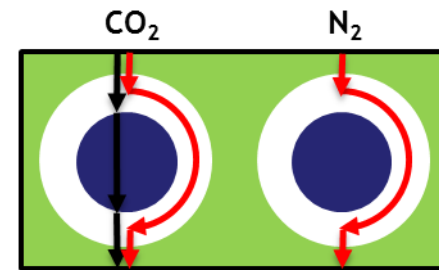
Needs

- More stable and robust membranes
 - Mechanically
 - Chemically
 - Thermally
- Higher permeability and selectivity
- Fundamental structure-property-processing relations needs to be incorporated.
- Various approaches to exceed the upper bound and access better performing membranes.
 - Surface modification
 - Phase separated polymer blends
 - Mixed-matrix membranes (MMMs)
 - Inorganic membranes (superior in performance but are difficult to make large thin films)
 - Supported ionic liquids
 - Facilitated transport

Mixed Matrix Membranes



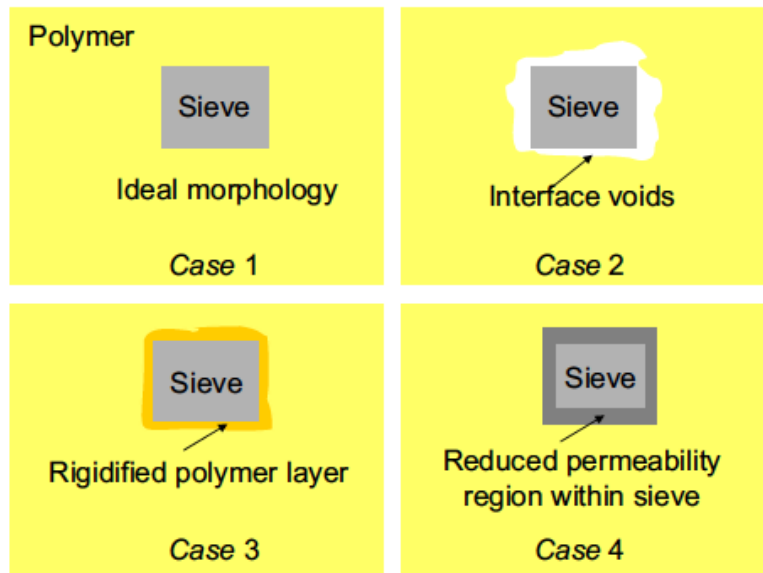
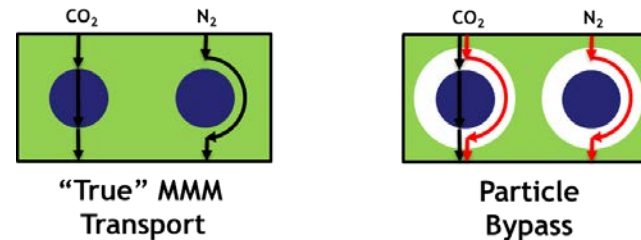
"True" MMM
Transport



Particle
Bypass

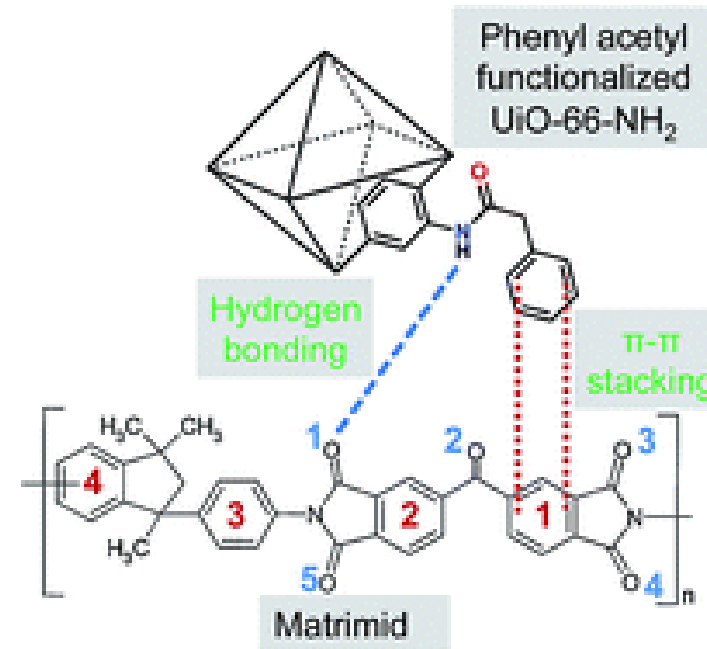
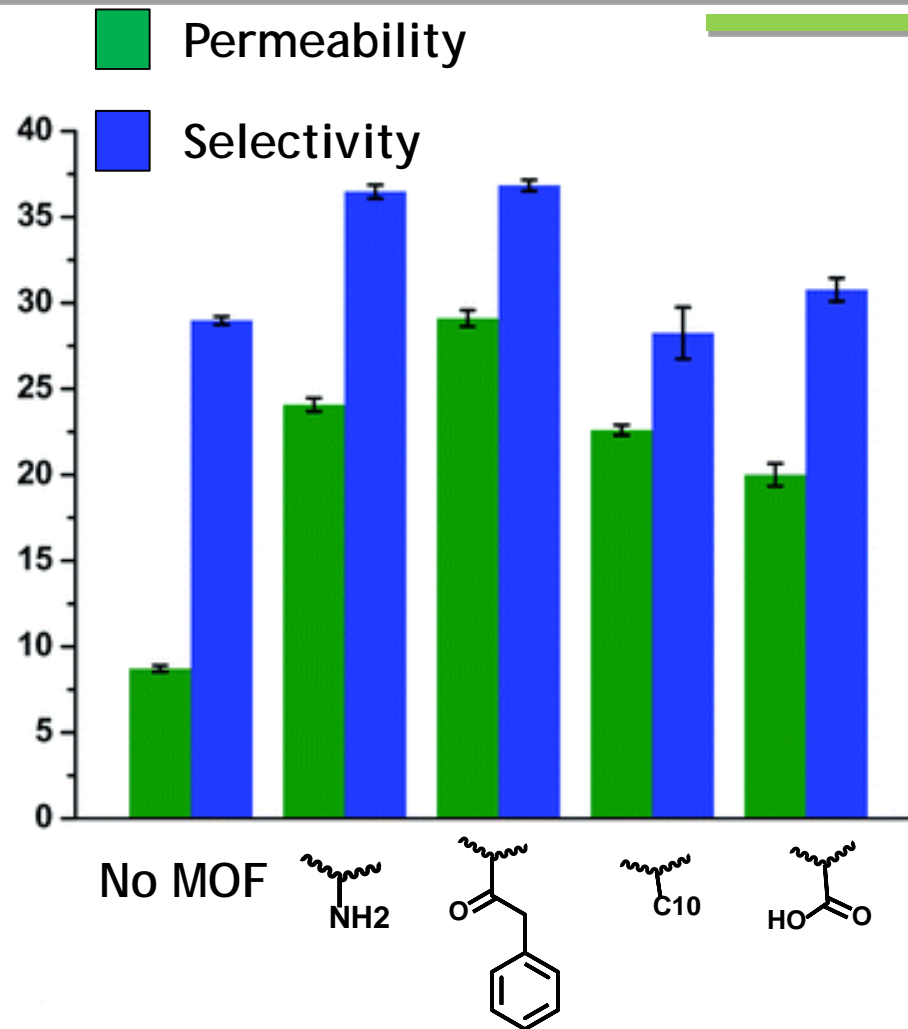
The Trouble with Mixed Matrix Membranes

- Poor compatibility of the polymer and inorganic particles that leads to poor adhesion at the organic-inorganic interface.
- General trade-off between selectivity and permeability



- Solutions:
 - Addition of interfacial agents
 - Surface modification of inorganic particles
 - Chemical modification of polymers
 - Use of flexible polymers

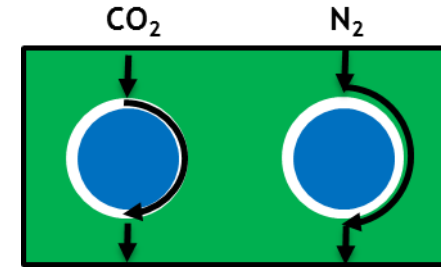
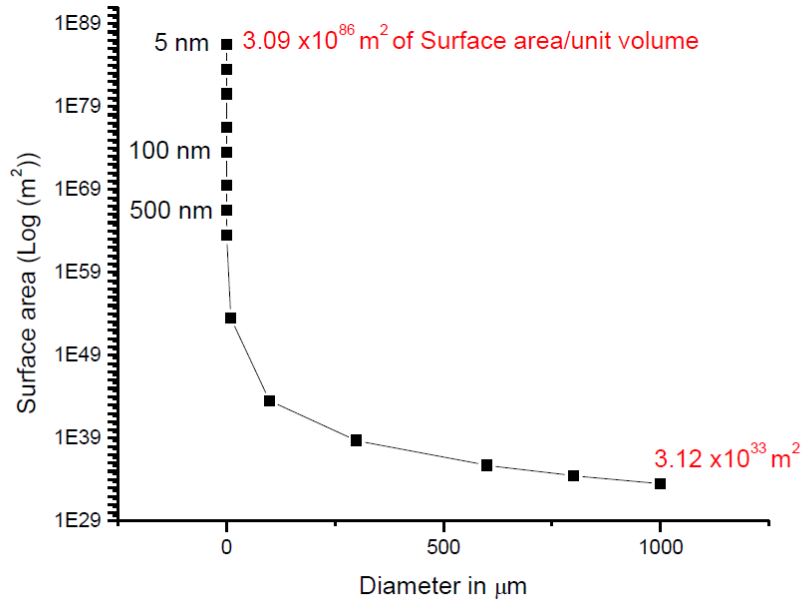
Insight



J. Mater. Chem. A, 2015, 3, 5014-5022
U.S. Patent Application number: 14/519,743

Interface

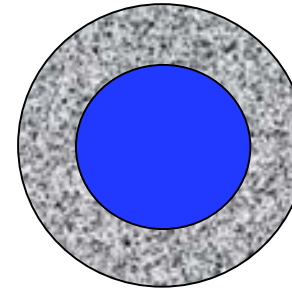
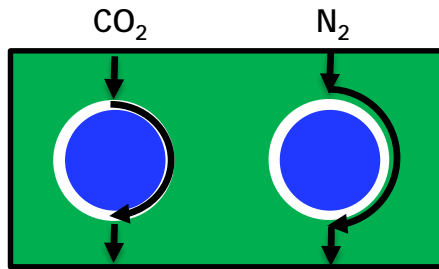
If you can't beat 'em, join 'em!



Interfacially-Controlled Envelope (ICE) Membranes

- Makes use of envelopment effects which have plagued mixed matrix membranes
- Diffusion phenomena determined by interactions with the particle and polymer surface
- Possibility of using simple nanoparticle fillers
- Advanced polymers allow an excellent starting point

Plan of Attack for Mixed Matrix Membranes

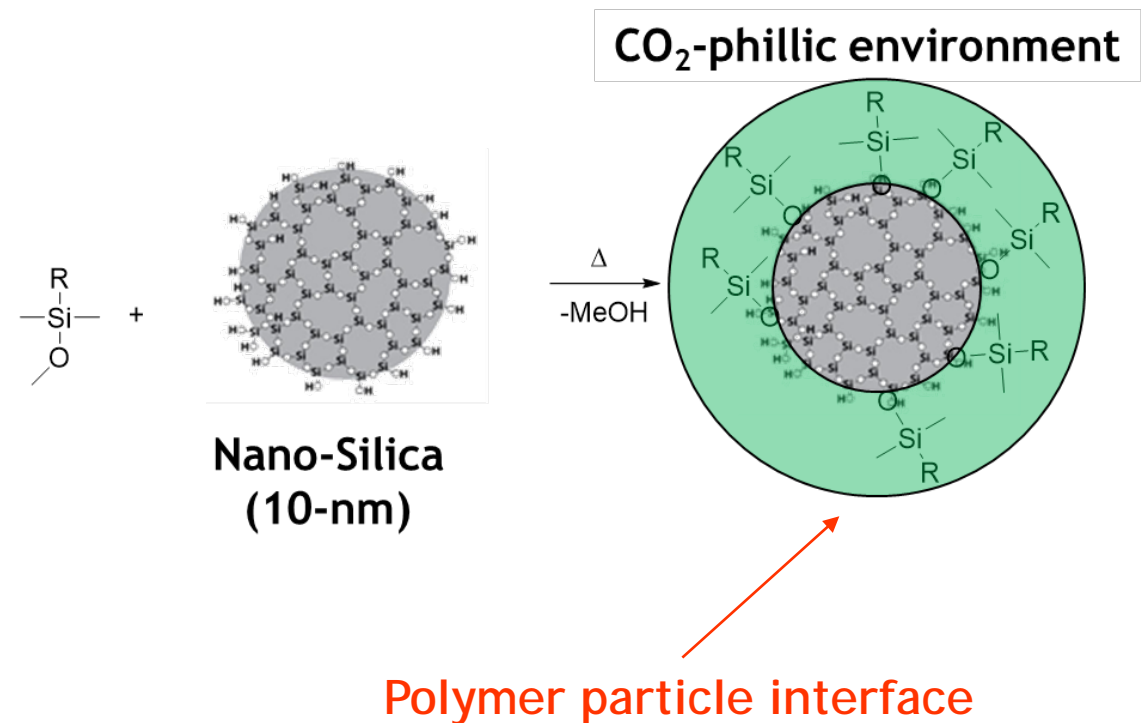


5-10 nm

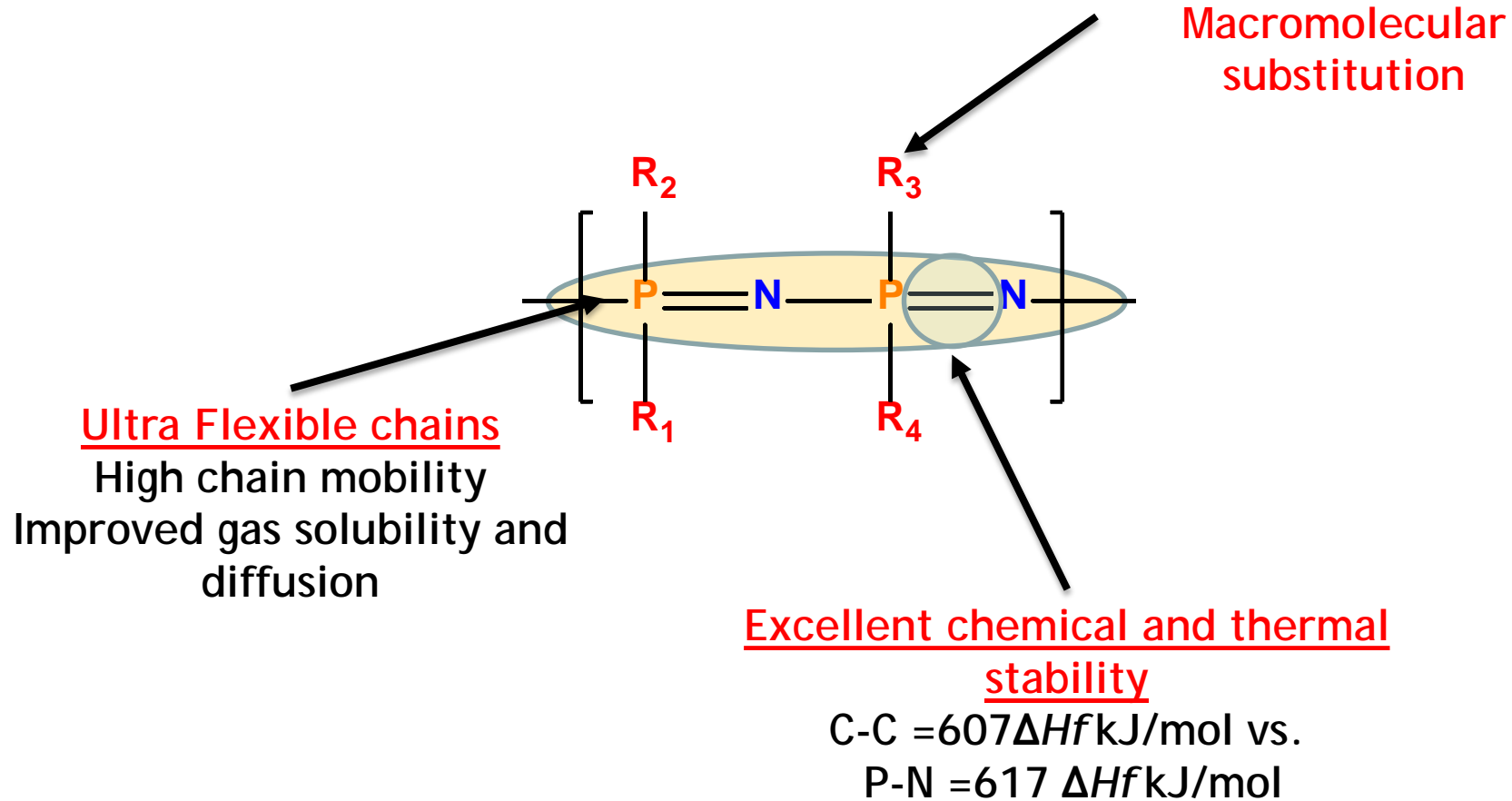
- Use simple nanoparticle fillers
- Surface modify the particles to tune optimal interactions with CO_2 and the polymer
- Employ an advanced polymer with good compatibility and CO_2 transport properties
- Create a membrane in which diffusion phenomena are determined by interactions with the particle and polymer surface

Surface Functionalized Nanoparticles

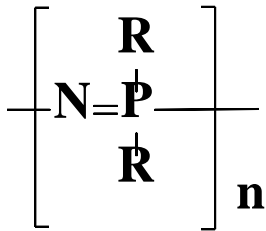
- Careful and detailed screening of the surface modifier was carried out.
- Nanoparticles have been synthesized @ 200g levels for 3 different loadings



Polymer of Choice

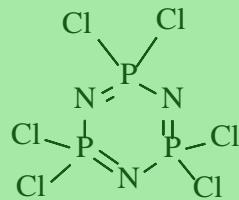


Polyphosphazenes

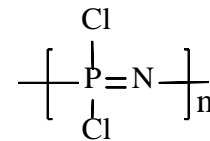


Organic-Inorganic Hybrid Polymeric System

Ring Opening Polymerization

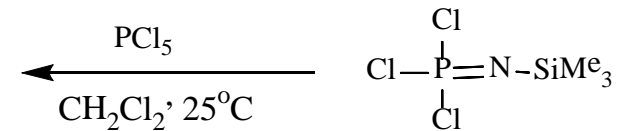


250°C



Poly(dichlorophosphazene)
Reactive Intermediate

Living Cationic Polymerization

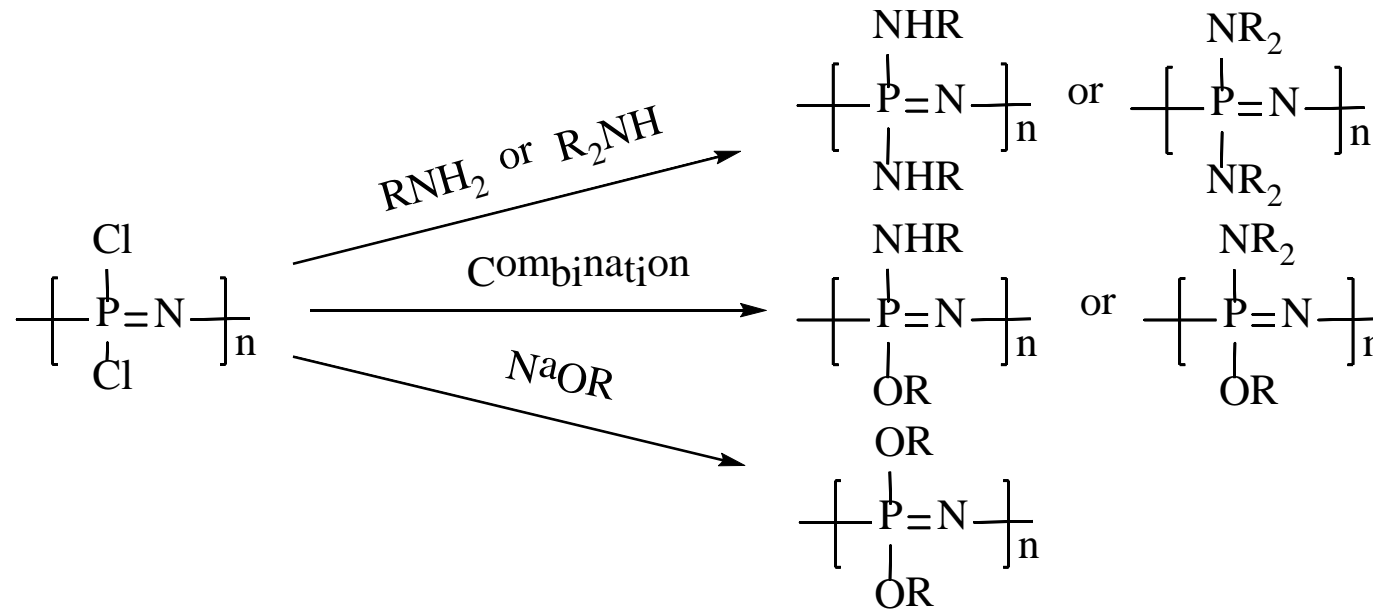


- High Molecular Weight (MW)
- Relatively Large Scale Preparation
- Poor Molecular Weight Control
- Broad Poly-disperity (PD)
- No End-chain Modifications

- Relatively Lower MW
- Well-controlled MW and PD
- Room Temperature
- Small Scale Preparation
- End-chain Modifications

Polyphosphazenes

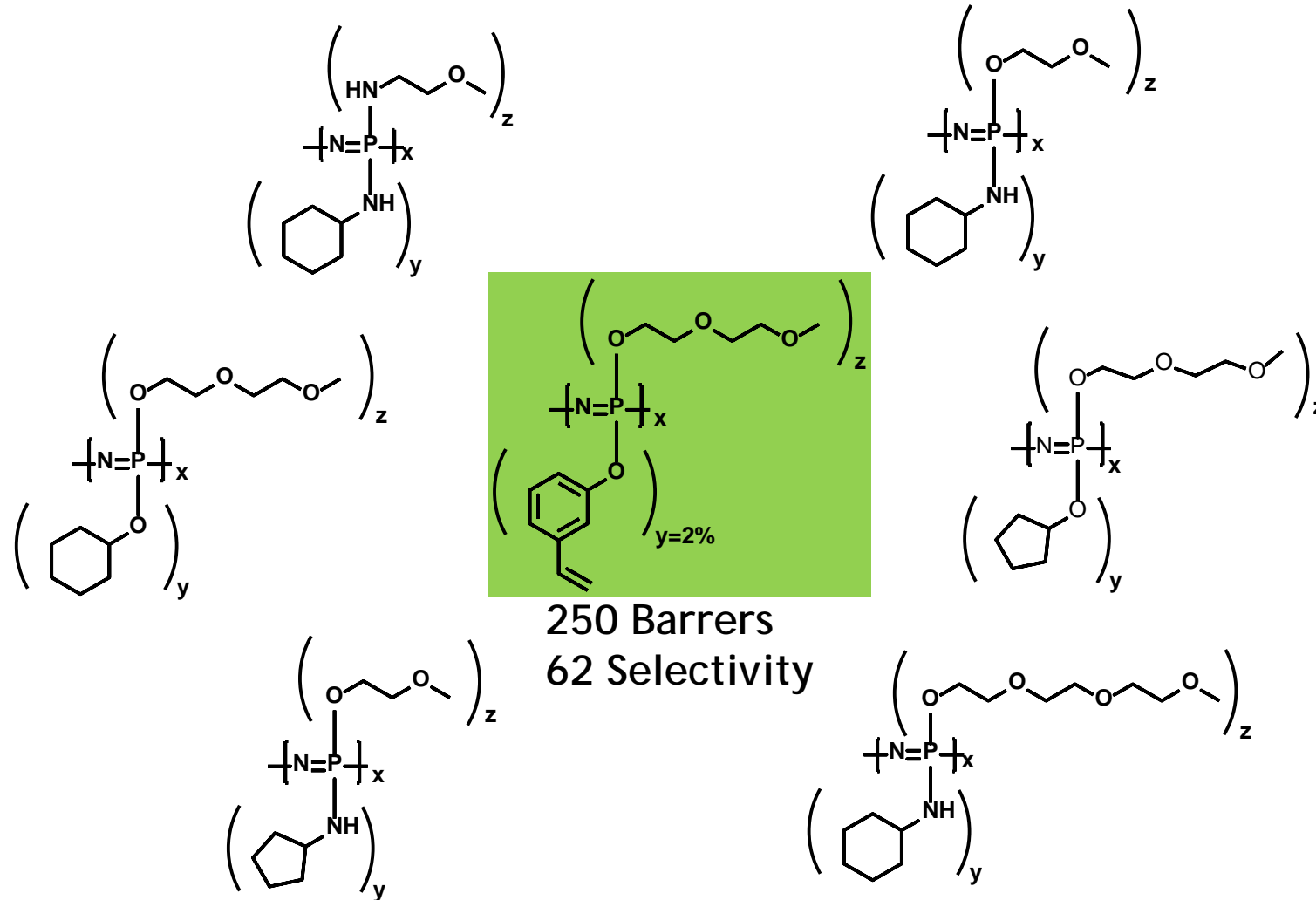
Macromolecular Substitution



Library of Over 700
Different
Polyphosphazenes

- **Synthetic Simplicity:** Nucleophilic Substitutions
- **Synthetic Tunability:** Homo-substitutions OR Mix-substitutions
- **Property Tunability:** Glass Transition Temperature, Solubility, Degradability, Hydrophobicity

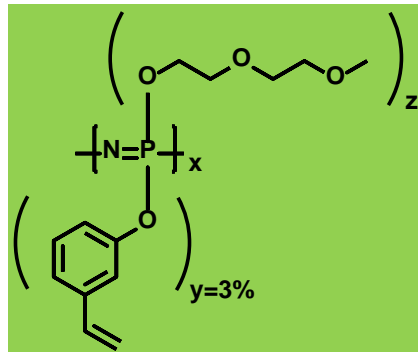
Polymer Screening



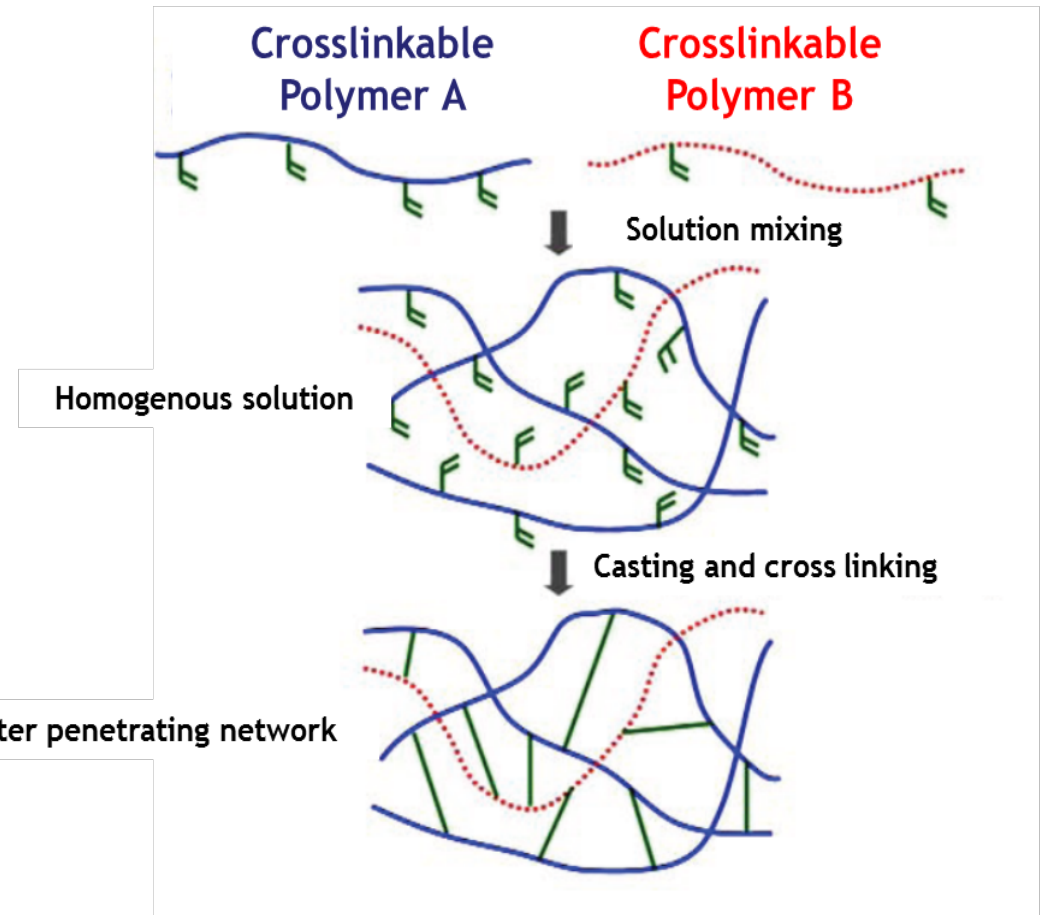
Material Optimization

Challenges

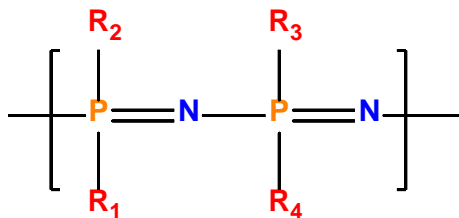
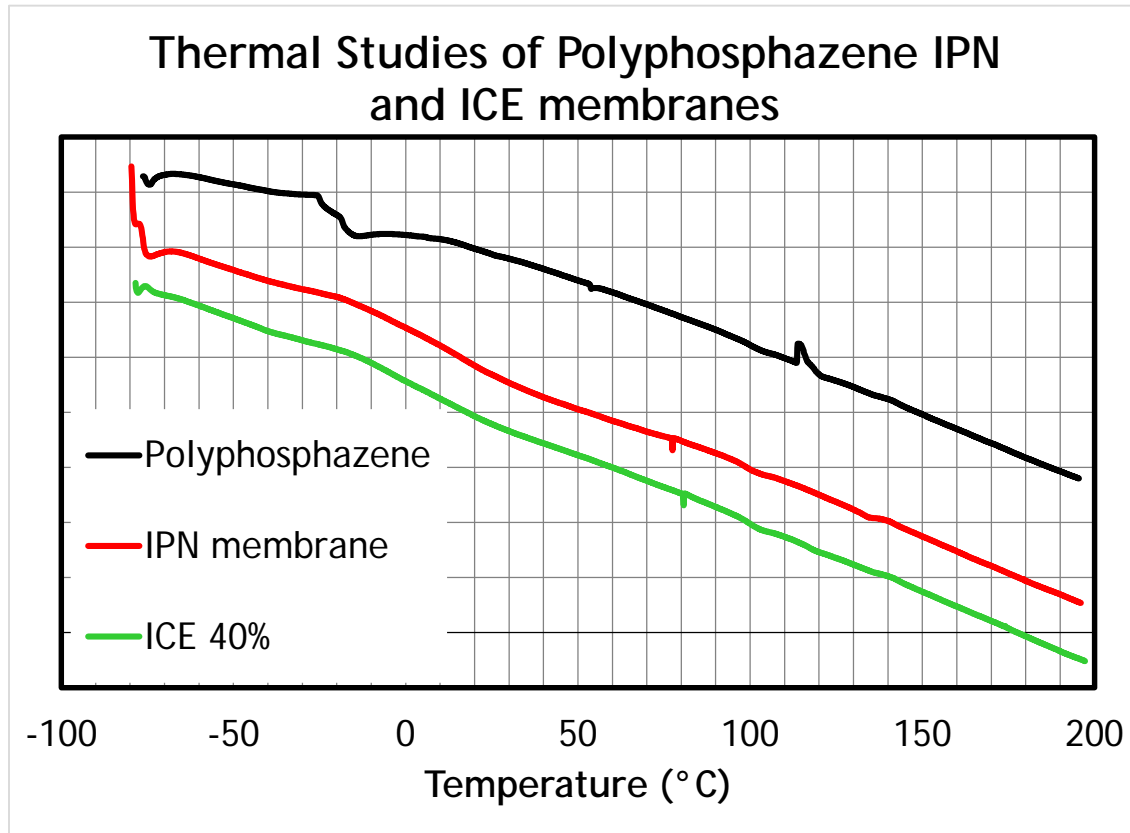
- Not a film former
- Sticky
- Does not have required mechanical properties



Solution = Inter Penetrating Networks (IPN)



Glass Transition Studies

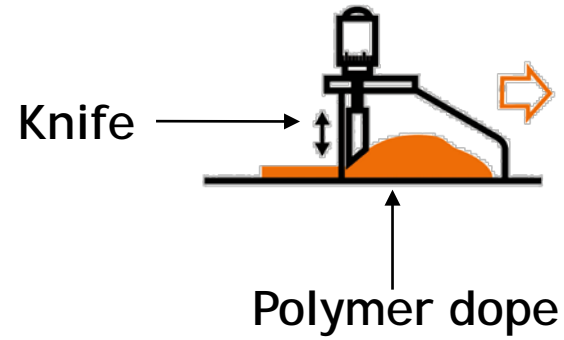


- Difference T_g of uncrosslinked Polyphosphazene vs. IPN is observed
- Minor difference is observed between IPN vs. ICE membranes in T_g studies.
 - Effect of extremely chain mobility
- 30 compositions of ICE membranes have been evaluated for their thermal properties.
 - Long-term stability test are on going.

Membrane Casting



Screening is done using films cast by hand

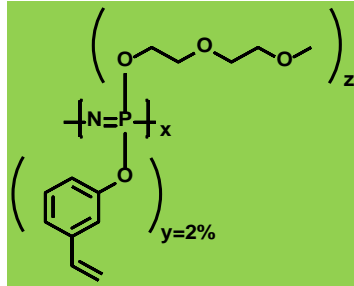


10-12 microns

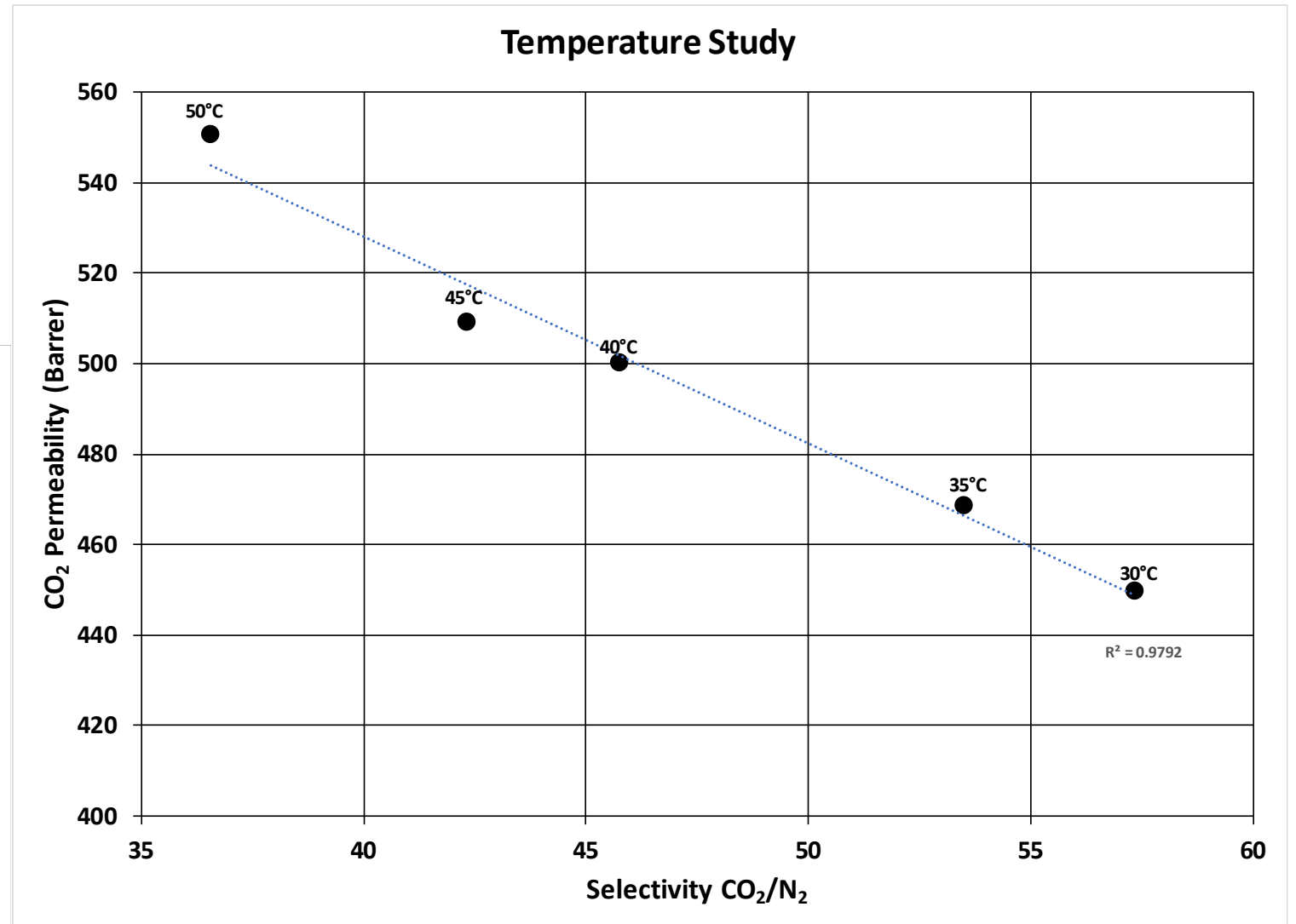
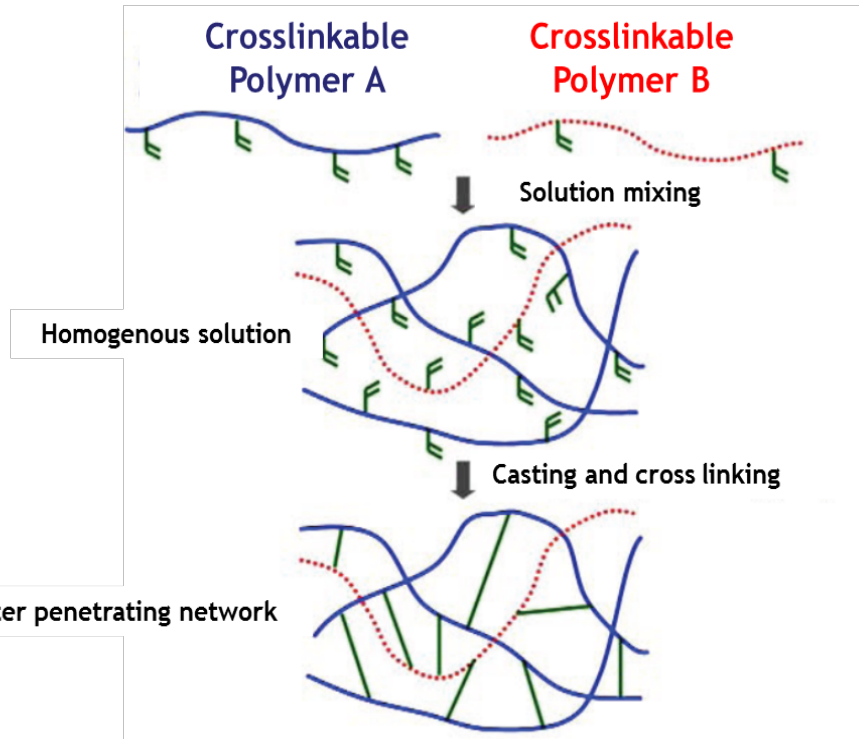
HV	Mag	WD	Spot	Sig	HFW
20.0 kV	500x	9.6 mm	5.0	BSE	0.60 mm

300.0μm

Polymer Membrane Results

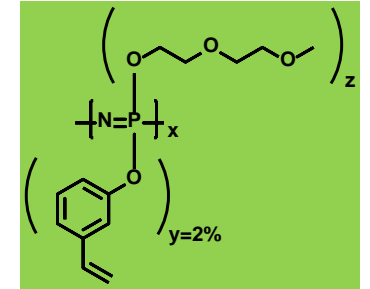


250 Barrers
62 Selectivity



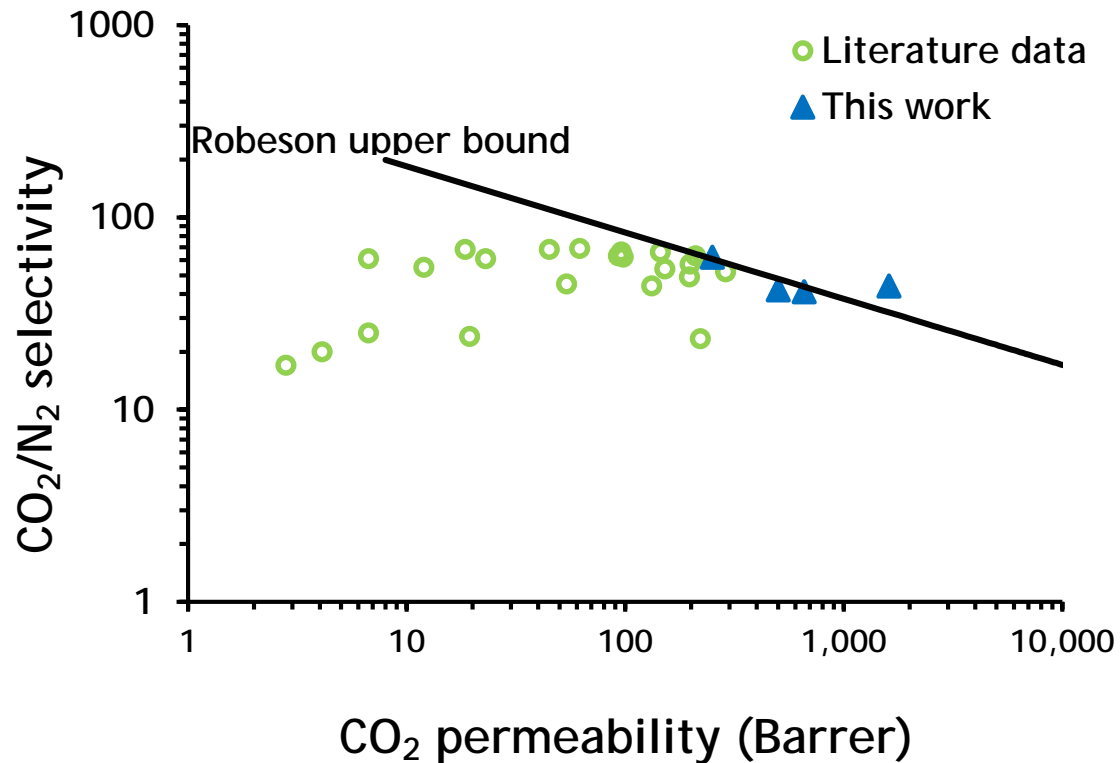
Membrane Performance

%wt. Loading of Nanoparticles	Cast number	Characterization	Membrane results	
			Permeability	Selectivity
30% unmodified particles	LS-01-45A	Turned into a gel with white precipitates (not useable)	N/A	N/A
10% surface modified 10 nm particles	LIS-01-41 A	SEM, TGA, DSC, Membrane testing	659	41
20% surface modified 10 nm particles	LS-01-51 B*	Membrane testing	675-1025	20-33
40% surface modified 10 nm particles	LIS-01-41 B, LIS-01-43	SEM, TGA, DSC, membrane testing	1609	44
60% surface modified 10 nm particles	LIS-01-51A*	TGA, DSC, Membrane testing	250-400	25-30



60% loading

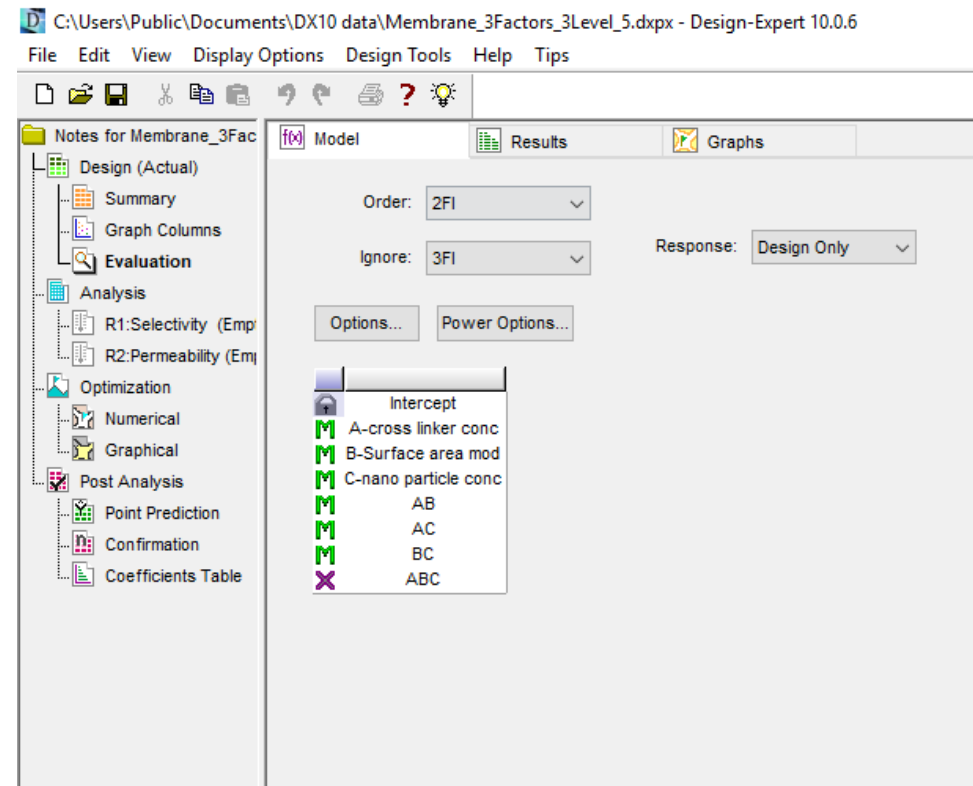
Membrane Performance



- Membrane of half a micron would yield permeance of 3200 GPU with a selectivity of 44 for CO₂/N₂ separation.
- Work is being performed to convert these materials properties into membranes – Open for collaborations
- Module design– Open for collaborations and joint research.

Design of Experiments Matrix

- Further optimization of membrane composition Design of Experiments
 - Optimized surface modification of the nanoparticles
 - Optimized concentration of nanoparticles
 - Optimized level of crosslinking
- 30 composition done
- DSC studies complete
 - Minor differences in T_g
 - Structure-property relationship is being carried out
- Performance testing in Progress.



Using statistical analytical tools to optimize membrane composition

Acknowledgement

Liquid Ion Solutions, Carbon Capture Scientific and Penn State University gratefully acknowledge the support of the United States Department of Energy's National Energy Technology Laboratory under agreement DE-FE0026464, which is responsible for funding the work presented.

- Dr. Scott Chen
- Dr. Zijiang Pan
- Dr. Zhiwei Li

- Prof. Harry Allcock
- Dr. Zhongjing Li
- Dr. Yi Ren

- Dr. David Luebke
- Krystal Koe
- Dr. Xu Zhou

