

Science and Technology of Separation Membranes

# **Science and Technology of Separation Membranes**

Tadashi Uragami Functional Separation Membrane Research Center, Japan



This edition first published 2017 © 2017 by John Wiley & Sons Ltd

Registered Office

John Wiley & Sons Ltd, The Atrium, Southern Gate, Chichester, West Sussex, PO19 8SQ, UK

For details of our global editorial offices, for customer services and for information about how to apply for permission to reuse the copyright material in this book please see our website at www.wiley.com.

The right of the author to be identified as the author of this work has been asserted in accordance with the UK Copyright, Designs and Patents Act 1988.

All rights reserved. No part of this publication may be reproduced, stored in a retrieval system, or transmitted, in any form or by any means, electronic, mechanical, photocopying, recording or otherwise, except as permitted by the UK Copyright, Designs and Patents Act 1988, without the prior permission of the publisher.

Designations used by companies to distinguish their products are often claimed as trademarks. All brand names and product names used in this book are trade names, service marks, trademarks or registered trademarks of their respective owners. The publisher is not associated with any product or vendor mentioned in this book.

Limit of Liability/Disclaimer of Warranty: While the publisher and author(s) have used their best efforts in preparing this book, they make no representations or warranties with respect to the accuracy or completeness of the contents of this book and specifically disclaim any implied warranties of merchantability or fitness for a particular purpose. It is sold on the understanding that the publisher is not engaged in rendering professional services and neither the publisher nor the author shall be liable for damages arising herefrom. If professional advice or other expert assistance is required, the services of a competent professional should be sought.

Library of Congress Cataloging-in-Publication data applied for

ISBN: 9781118932544

A catalogue record for this book is available from the British Library.

Cover image: Background: mariannehope/Gettyimages Illustration: Courtesy of the author

Set in 10/12pt Warnock by SPi Global, Pondicherry, India

10 9 8 7 6 5 4 3 2 1

# Contents

Preface xix
Acknowledgements xxiii

### Volume I

1	Introduction to Membrane Science and Technology 1
1.1	History of Membrane Science and Technology 1
1.2	Membrane Module 6
1.2.1	Plate-and-Frame Modules 6
1.2.2	Tubular Modules 6
1.2.3	Spiral-Wound Modules 6
1.2.4	Hollow-Fibre Modules 6
1.3	Necessity of Membrane Science and Technology 7
	References 8
2	Membrane Structure 13
2.1	Structural Design of Membranes 13
2.1.1	Chemical Design of Membrane Materials 13
2.1.2	Physical Construction of Separation Membranes 13
2.2	Symmetric Non-porous and Porous Membranes 14
2.3	Asymmetric and Composite Membranes 15
2.4	Relation between Structure and Preparation Condition of Membrane 16
2.4.1	Preparation of Casting Solution 17
2.4.1.1	Kind of Polymer Material 17
2.4.1.2	Polymer Concentration in Casting Solution 17
2.4.1.3	Casting Solvent 19
2.4.1.4	Combination of Casting Solvent 23
2.4.1.5	Addition of Additive in Casting Solution 25
2.4.1.6	Temperature of Casting Solution 27
2.4.2	Casting Condition 29
2.4.2.1	Temperature and Humidity during Casting 29
2.4.2.2	Evaporation Period 29
2.4.3	Gelation Condition 31
2.4.3.1	Gelation Period and Temperature 31
2.4.3.2	The Kind of Gelation Medium 32
2.4.4	Post-treatment 35

vi	Contents	
	2.4.4.1	Method of Heat Treatment 35
	2.4.4.2	Temperature and Period of Heat Treatment 35
	2.4.4.3	Pressure Treatment 42
	2.4.4.4	Elongation Treatment 43
	2.4.4.5	Post-reaction 43
	2.4.4.6	Post-solvent Treatment 47
	2.5	Structure of Liquid Membranes 50
	2.5.1	Bulk Liquid Membrane 50
	2.5.2	Emulsion Liquid Membrane 51
	2.5.3	Supported Liquid Membrane 52
	2.5.3.1	Thin-Porous-Film-Supported Liquid Membrane
	2.5.3.2	Hollow-Fibre-Supported Liquid Membrane 52
	2.6	Structure of Inorganic Membranes 53
		References 53
	3	Preparation Methods of Membranes 59
	3.1	Polymer Membranes 59
	3.1.1	Solution-Casting Method 59
	3.1.1.1	Thermally Induced Phase Separation 60
	3.1.1.2	Diffusionally Induced Phase Separation 64
	3.1.1.3	Drying-Induced Phase Separation 67
	3.1.1.4	Vapour-Induced Phase Separation 69
	3.1.2	Composite Method 72
	3.1.3	Casting–Reaction Method 73
	3.1.4	Polyion Complex Method 73
	3.1.5	Freeze-Dry Method 73
	3.1.6	Chemical Modification 73
	3.1.7	Filling Polymerization Method 73
	3.1.8	Expansion Method 74
	3.2	Inorganic Membranes 74
	3.2.1	Process for Preparation 75
	3.3	Organic-Inorganic Hybrid Membranes 75
	3.4	Liquid Membranes 76
	3.4.1	Carrier 76
	3.4.2	Solvent 76
	3.4.3	Emulsion 79
	3.4.4	Support 79
		References 80
	4	Membrane Shapes and Modules 87

52

# 4.1 Membrane Shapes and Modules 8. 4.1 Membrane Shapes 87 4.1.1 Flat-Sheet Membranes 87 4.1.2 Spiral Membranes 89 4.1.3 Tubular Membranes 89 4.1.4 Capillary Membrane 91 4.1.5 Hollow-Fibre Membrane 93

4.2 4.2.1 4.2.2 4.2.3 4.2.4 4.2.5 4.2.6 4.2.7 4.2.8	Membrane Module 94 Plate-Frame Module 95 Spiral Module 96 Tubular Module 97 Hollow-Fibre Module 98 Types of Membrane Filtration Modules 99 Durability of Membrane Modules 100 Degradation of Membrane Module Materials 100 Decline of Membrane Performance 101 References 102	
5	Characterization of Membrane 105	
5.1	Methods and Subjects of Evaluation 105	
5.1.1	Bubble-Point Method 105	
5.1.2	Mercury Intrusion Porosimetry 107	
5.1.3	Adsorption–Desorption Method (BET Method) 110	
5.1.4	Scanning Electron Microscope 111	
5.1.4.1	Sample Preparation 111	
5.1.5	Transmission Electron Microscopy 111	
5.1.5.1	Sample Preparation 112	
5.1.5.2	Tissue Sectioning 112	
5.1.5.3	Sample Staining 112	
5.1.6	Environmental Scanning Electron Microscope 113	
5.1.7	Atomic Force Microscopy 114	
5.1.8	Infrared Spectroscopy 116	
5.1.9	Fourier-Transform Infrared Spectroscopy 117	110
5.1.10	X-Ray Photoelectron Spectroscopy or Electron Spectroscopy for Chemical Analysis	119
5.1.11	Wide-Angle X-Ray Scattering or Wide-Angle X-Ray Diffraction 122	
5.1.12 5.1.13	Small-Angle Neutron Scattering 125 Positron Annihilation Spectroscopy or Positron Annihilation Lifetime Spectroscopy	125
5.1.14	Contact Angle 127	123
5.1.15	Zeta Potential 129	
5.1.16	Differential Scanning Calorimetry 131	
5.1.17	Thermogravimetry 133	
	Characteristics and Applications of Thermogravimetric Analysis 134	
5.1.18	Membrane Density 135	
5.1.19	Cross-link Density 136	
5.1.20	Degree of Membrane Swelling 137	
5.1.21	Sorption Selectivity 139	
5.1.22	Burst and Tensile Strength of Membrane 141	
	References 142	
6	Fundamentals of Membrane Transport Phenomena 147	
6.1	Thermodynamical Fundamentals for Membrane Transport 147	
6.1.1	Thermodynamics of Membrane Transport 147  Thermodynamics of Membrane Transport 147	
6.1.2	Volume Flow and Diffusion Flow 150	

viii	Contents	
	6.1.3	N

6.1.3	Mobility and Diffusion Coefficient 153
6.1.4	Surface Potential and Membrane Potential 157
6.1.5	Distribution Coefficient and Membrane Permeability Coefficient 162
6.2	Solution-Diffusion Model 166
6.2.1	Fundamentals of Solution-Diffusion 166
6.2.2	Solution-Diffusion Model 168
6.3	Pore Flow 171
6.3.1	Pore-Flow Model 171
6.3.2	Knudsen Diffusion 173
6.3.3	Surface Diffusion 174
6.3.3.1	
6.3.3.2	Microporous Membrane and Surface Transport 175
0.5.5.2	References 177
	References 177
7	Phenomena during Membrane Permeation and Separation 181
7.1	Concentration Polarization 181
7.1.1	State of Boundary Layer on Membrane Surface 183
7.1.2	Concentration Polarization in Gas Separation 184
7.1.3	Concentration Polarization in Pervaporation 185
7.1.4	Concentration Polarization in Reverse Osmosis 186
7.1.5	Concentration Polarization in Nanofiltration 188
7.1.6	Concentration Polarization in Ultrafiltration 190
7.1.7	Concentration Polarization in Microfiltration 191
7.1.8	Concentration Polarization in Membrane Distillation 193
7.1.9	Concentration Polarization in Dialysis 194
7.1.10	Concentration Polarization in Electrodialysis 195
7.1.10	Membrane Fouling 197
7.2.1	Cause of Membrane Fouling 197
7.2.2	Control of Membrane Fouling 199
, .2.2	References 199
	Notice in the second se
8	Dialysis 205
8.1	Diffusion Dialysis 205
8.1.1	Principle of Diffusion Dialysis 206
8.1.2	Fundamental Analysis of Diffusion Dialysis 206
8.1.2.1	Diffusion and Diffusion Dialysis 207
8.1.2.2	Diffusion Dialysis with Crossflow 209
8.1.3	Membranes for Diffusion Dialysis 211
8.1.4	Technologies 213
8.1.4.1	Diffusion Dialysis 213
8.1.4.2	Haemodialysis 220
8.2	Donnan Dialysis 224
8.2.1	Principle of Donnan Dialysis 224
8.2.2	Membranes and Technology of Donnan Dialysis 225
8.3	Neutralization Dialysis 226
8.3.1	Principle of Neutralization Dialysis 226
0.0.1	Timelphe of recutalization Diarysis 220

8.3.2	Membranes and Technologies of Neutralization Dialysis 227
8.4	Piezodialysis 228
8.4.1	Membranes for Piezodialysis 228
8.4.2	Principle and Fundamental Analysis of Piezodialysis 230
8.4.3	Technologies of Piezodialysis 231
8.5	Electrodialysis 233
8.5.1	Principle of Electrodialysis 233
8.5.2	Fundamental Analysis of Electrodialysis 233
8.5.3	Membranes of Electrodialysis 235
8.5.3.1	Fundamental Characteristics 235
8.6	Technologies of Electrodialysis 237
8.6.1	Salt Production 237
8.6.2	Recovery 240
8.6.3	Water Desalination 241
8.6.4	Production of Organic Acid 243
8.7	Electrodialysis with Bipolar Membranes 244
8.7.1	Principle and Fundamental of Bipolar Membrane Electrodialysis 244
8.7.2	Technologies of Bipolar Membrane Electrodialysis 246
	References 251
9	Reverse Osmosis 259
9.1	Principle of Reverse Osmosis 259
9.2	Fundamental Analysis of Reverse Osmosis 259
9.2.1	Nonequilibrium Thermodynamics Model 261
9.2.2	Friction Model 262
9.2.3	Solution-Diffusion Model 263
9.2.4	Micropore Model 263
9.2.5	Preferential Sorption-Capillary Flow Model 264
9.3	Materials and Structures of Reverse Osmosis Membranes 266
9.4	Concentration Polarization and Fouling 270
9.4.1	Concentration Polarization 270
9.4.2	Fouling of Reverse Osmois 272
9.5	Technologies and Applications of Reverse Osmosis 274
9.5.1	Polymer Membranes 274
9.5.1.1	Cellulose Acetate Membranes 274
9.5.1.2	Composite Polyamide Membranes 274
9.5.2	Inorganic Membranes 278
9.5.3	Mixed Matrix Membranes 281
9.5.3.1	Composite Membranes of Nanoparticle–Polymer 282
9.5.3.2	Composite Membranes of Carbon Nanotube–Polymer 283
9.5.4	Organic–Inorganic Hybrid Membranes 284
9.5.5	Boron Separation in Reverse Osmosis 285
9.5.6	Removal of Radioactive Materials by Reverse Osmosis Membrane 288
9.6	Membrane Module of Reverse Osmosis 289
9.6.1	Spiral-Wound Membrane Module 289
9.6.2	Hollow-Fibre Membrane Module 290

x Contents	
------------	--

9.7	Membrane Cleaning 291
	References 292
10	Nanofiltration 297
10.1	Principle of Nanofiltration 297
10.2	Fundamental Analysis of Nanofiltration 297
10.2.1	Permeation Characteristics of Nanofiltration 297
10.2.2	Concentration Characteristics of Nanofiltration 299
10.3	Membranes and Modules for Nanofiltration 300
10.3.1	Membranes for Nanofiltration 300
10.3.1.1	Surface Modification 301
10.3.1.2	Interfacial Polymerization 301
10.3.1.3	Composite 303
10.3.1.4	Hollow Fibre 305
	Hybrid Membrane 306
10.3.1.6	Solvent-Resistant Membranes 307
10.3.2	
	Spiral-Wound Module 308
	Tubular Module 308
10.4	Concentration Polarization and Membrane Fouling in Nanofiltration 308
10.4.1	Concentration Polarization in Nanofiltration 308
10.4.2	Membrane Fouling in Nanofiltration 309
10.4.3	Antifouling in Nanofiltration 309
10.5	Technology 311
10.5.1	Treatment of Fresh, Process and Waste Waters 311
10.5.2	Food, Dairy and Beverage 313
10.5.3	Chemical Processing 314
10.5.4	Pulp, Paper and Textile Industry 316
10.5.5	Nanofiltration in Organic Solvents 318 References 318
	References 516
11	Ultrafiltration 325
11.1	Principle of Ultrafiltration 325
11.2	Fundamental Analysis of Ultrafiltration 325
11.2.1	Phenomenological Treatment of Membrane Permeation 325
11.2.2	Pore Model 327
11.2.3	Rejection Rate and Concentration Polarization 327
11.2.4	Concentration Magnification and Rejection Rate 328
11.2.5	Molecular Weight Cut-off 331
11.2.6	Batch-Style Concentration 332
11.3	Membranes for Ultrafiltration 333
11.3.1	Organic Membranes 333
11.3.2	Inorganic Membrane 333
11.4	Ultrafiltration Modes 333
11.4.1	Batch Concentration 333
11.4.2	Multistage Continuous Concentration 334
11.4.3	Batch Diafiltration 334

11.4.4	Continuous Diafiltration 334
11.5	Concentration Polarization and Fouling in
	Ultrafiltration 335
11.5.1	Concentration Polarization in Ultrafiltration 335
11.5.2	Fouling in Ultrafiltration 338
11.6	771. C1
11.6.1	
	Plate-and-Frame Module 342
	Spiral-Wound Module 343
11.6.1.3	<u>-</u>
11.6.1.4	
11.7	Ultrafiltration Applications 343
11.7.1	Drinking Water 343
11.7.2	Protein Concentration 344
11.7.3	Enzyme Recovery 345
11.7.4	
11.7.5	
11.7.6	
11.7.7	
11.7.8	
11.7.9	
11.7.10	
11.7.11	
	Wine Production 352
11.7.13	
11.7.10	References 355
	References 555
12	Microfiltration 359
12.1	Principle of Microfiltration 359
12.2	Fundamental Analysis of Microfiltration 360
12.2.1	and the second s
12.2.2	
12.3	Membranes for Microfiltration 363
12.3.1	
	Polymer Membranes 363
12.3.1.2	Inorganic Membranes 364
12.4	Fouling in Microfiltration 365
12.5	Module of Microfiltration 368
12.5.1	Plate-and-Frame Module 368
12.5.2	Spiral-Wound Module 368
12.6	Microfiltration Technology 368
12.6.1	Water Treatment 368
12.6.2	Dairy Industry 370
12.6.3	Sterilization 371
12.6.4	Virus Removal 373
12.6.5	Oil Refining 374
	References 375

13.1 13.2	Comparison of Pressure-Driven Membrane Separation Processes 379 Pressure-Driven Membrane Separation Technologies 379 Problems of Reverse Osmosis and Nanofiltration 382 References 383
Volume	П
14	Forward Osmosis 385
14.1	Principle of Forward Osmosis 385
14.2	Advantages and Problems of Forward Osmosis 385
14.3	Fundamental Analysis of Forward Osmosis 387
14.4	Membranes and Modules for Forward Osmosis 387
14.4.1	Membranes for Forward Osmosis 387
14.4.2	Modules for Forward Osmosis 390
14.5	Technology 391
14.6	Application Area of Forward Osmosis Process 391
14.6.1	Seawater Desalination 391
14.6.2	Wastewater Treatment and Water Purification 394
14.6.3	Pharmaceutical Applications 396
14.6.4	Food Processing 396
14.6.5	Power Generation 399
14.7	Improvement of Forward Osmosis Membrane Performance 401
14.7.1	Improvement of Forward Osmosis Membrane 401
14.7.2	Improvement of Draw Solution 403
14.7.3	Reproduction of Draw Solution 405
14.8	Fouling in Forward Osmosis 406
	References 408
15	Pervaporation 413
15.1	Principle of Pervaporation 413
15.2	Fundamental Analysis of Pervaporation 414
15.2.1	Fundamental Permeation Equation 414
15.2.2	Solution-Diffusion Model 415
15.2.3	Separation Factor 416
15.2.4	Quantitative Treatment of Separation Factor 416
15.3	Membranes for Pervaporation 417
15.3.1	Materials of Pervaporation Membrane 417
15.3.1.1	Hydrophilic Membrane Materials 417
15.3.1.2	Hydrophobic Membrane Materials 418
15.3.2	Membrane Structure 420
15.3.2.1	Symmetric Membranes 420
15.3.2.2	Asymmetric Membranes 421
15.3.2.3	Composite Membranes 422
15.3.2.4	Hybrid Membranes 424
15.3.2.5	Inorganic Membranes 427
15.4	Technologies 428
1541	Dehydration 429

15.4.1.1	Water–Alcohol Dehydration 429				
15.4.1.2	Water–Organic Dehydration 433				
15.4.2	Organic Separation from Water 436				
15.4.2.1	Alcohol-Selective Concentration 436				
15.4.2.2					
15.4.3	Organic Mixture Separation 448				
15.4.3.1	Benzene–Cyclohexane Separation 448				
15.4.3.2	•				
15.4.3.3					
	Ether–Ethanol Mixtures 453				
15.4.3.4	Separation of Xylene Isomers 455				
15.4.3.5	•				
15.4.3.6	<del>-</del>				
15.4.3.7	-				
15.4.4	Desalination by Pervaporation 459				
	References 461				
16	Evapomeation 471				
16.1	Principle of Evapomeation 471				
16.2	Membranes of Evapomeation 472				
16.3	Technology of Evapomeation 475				
16.3.1	Comparison of Membrane Performance in Pervaporation and Evapomeation 475				
16.3.1.1					
16.3.1.2	·				
16.3.1.3	Permselectivity of Isomers 483				
16.3.2	Effect of Cyclodextrin Content on Permeation and Separation Characteristics of				
	Xylene Isomers 486				
16.3.3	Dehydration of Organic Liquid in Evapomeation 489				
16.3.4	Concentration of Organic Liquid by Evapomeation 500				
16.3.5	Separation of Optical Enantiomers by Evapomeation 501				
16.3.6	Acceleration of Chemical Reaction by Evapomeation Technique 502				
	References 502				
17	Temperature-Difference Controlled Evapomeation 509				
17.1	Principle of Temperature-Difference Controlled Evapomeation 509				
17.2	Membranes of Temperature-Difference Controlled Evapomeation 509				
17.3	Technology of Temperature-Difference Controlled Evapomeation 510				
17.3.1	Comparison of Membrane Performance in Evapomeation and Temperature-Difference				
	Controlled Evapomeation 510				
17.3.2	Preparation of Porous Poly(dimethylsiloxane) Membranes 524				
	References 533				
10	Manufacture Distillation 525				
18	Membrane Distillation 535				
18.1	Principle of Membrane Distillation 535				
18.1.1	Direct Contact Membrane Distillation 535				
18.1.2	Vacuum Membrane Distillation 535				
18.1.3	Air Gap Membrane Distillation 536				

18.1.4	Sweep Gas Membrane Distillation 537
18.2	Fundamental Analysis of Membrane Distillation 537
18.2.1	Mass Transfer in Membrane Distillation 537
	Direct Contact Membrane Distillation 538
	Vacuum Membrane Distillation 540
	Air Gap Membrane Distillation 540
	<u>=</u>
18.3	Sweep Gas Membrane Distillation 541 Membranes of Membrane Distillation 541
18.3.1	
	Membranes of Membrane Distillation 542
	Membrane Structure 542
	Electrospun Membranes in Membrane Distillation 544
18.3.3	
	Plate-and-Frame Module 545 Tubular and Hollow-Fibre Module 545
18.3.4	
18.4	Technologies of Membrane Distillation 546
18.4.1	1
	Desalination and Removal of Salt 547
	Desalination 547
	Removal of Salt 548
18.4.3	
	Wastewater 549 Food 550
	Concentration and Removal of Organics 551 Concentration 551
	Removal 552
10.4.0.2	References 553
	References 333
19	Gas Permeation 559
19.1	Beginning of Gas Permeation 559
19.2	Fundamentals of Gas Permeation 560
19.2.1	Permeation and Separation of Gas through a Rubbery Membrane 560
	Permeability Coefficient 560
	Diffusion Coefficient 562
	Separation Factor 562
19.2.2	Membrane Permeation of Gas through a Glassy Membrane 563
19.2.2.1	Dual Sorption Model Theory 563
19.2.2.2	Partial Immobilization Model 564
19.2.3	Application to Gas Separation 566
19.3	Membranes for Gas Permeation 567
19.3.1	Membranes from Natural Polymers 568
19.3.2	Membranes from Synthetic Polymers 569
19.3.2.1	Polyamides, Polyimides, Poly(phenylene oxide) and Fluoropolymers 569
19.3.2.2	Polysulfone 571
19.3.2.3	Silicon Polymers 571
_,	

19.3.3	Blend, Composite and Hybrid Membranes 572
19.3.4	Membranes from Organic–Inorganic Hybridization 574
19.4	Membranes from Inorganic Materials 575
19.4.1	Metal Membranes 575
19.4.2	Ceramic Membranes 575
19.4.3	Zeolite Membranes 576
19.4.4	Carbon Membranes 577
19.5	Modules of Gas Separation Membrane 577
19.6	Technology of Gas Permeation Membrane 577
19.6.1	Hydrogen Separation 577
19.6.2	Oxygen Production 578
19.6.3	Carbon Dioxide Separation 579
19.6.4	Helium Separation 580
19.6.5	Methane Production 580
19.6.6	Separation of Some Gases 581
19.6.7	Olefin–Paraffin Separation 581
	References 583
20	Carrier Transport 587
20.1	Fundamental Principle of Carrier Transport through Artificial Membranes 587
20.1.1	Passive Transport 587
20.1.2	Facilitated Transport 588
20.1.3	Active Transport 590
20.2	Carriers in Membrane Transport 591
20.2.1	Role of Carrier 591
20.2.2	Membranes for Carrier Transport 592
20.3	Technology of Carrier Transport Membranes 596
20.3.1	Mobile Carrier Membranes 596
20.3.1.1	Transport and Separation of Inorganic Cations 596
20.3.1.2	Transport and Separation of Inorganic Anions 599
20.3.1.3	Transportation and Separation of Organic Compounds 600
20.3.1.4	Transport and Separation of Gas 602
20.3.1.5	Transport of Radioactive Ions 603
20.3.2	Fixed Carrier Membranes 605
20.3.2.1	Transport and Separation of Inorganic Cations 605
20.3.2.2	Transport and Separation of Inorganic Anions 613
20.3.2.3	Transport and Separation of Organic Compounds 616
20.3.2.4	Transport and Separation of Gas 622
20.3.2.5	Transport of Radioactive Ions 626
20.3.3	Improvement of Transport Efficiency in Carrier Transport 627
	References 629
21	Membrane Reactor 635
21.1	Concept of Membrane Reactors 635
21.2	Membranes for Membrane Reactors 635
21.2.1	Inorganic Membranes 635

|--|

21.2.1.1	Metal Membranes 637				
	Ceramic Membranes 638				
	Zeolite Membranes 639				
	Carbon Membranes 639				
	Polymer Membranes 639				
21.3	·				
21.3.1	· ·				
	Biocatalyst-Immobilized Polymer Membranes 640				
	Technology of Biocatalyst-Immobilized Polymer Membranes in Membrane Reactors 640				
	Polymer–Metal Complex Membranes 646				
	Polymer—Metal Complex Membranes 646 Polymer Catalysis Membranes 649				
	Ion-Exchange Resins and Ion-Exchange Membranes in Membrane Reactor 650				
	Metal Membranes 651				
	Ceramic Membranes 654				
	Polymer–Metal Composite Membranes 655				
21.3.2	•				
	Membrane Reactor with Pervaporation 655				
	Membrane Reactor with Evapomeation 661				
	Combination of Fermentation Tank and Temperature-Difference Controlled				
21,0,2,0	Evapomeation 661				
	References 661				
22	Membrane Contactors 667				
22.1	Principle and Fundamentals of Membrane Contactors 667				
22.1 22.2	Principle and Fundamentals of Membrane Contactors 667  Membranes for Membrane Contactors 669				
	Membranes for Membrane Contactors 669				
22.2	Membranes for Membrane Contactors 669 Inorganic Membranes 669				
22.2 22.2.1	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670				
22.2 22.2.1 22.2.2	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic–Inorganic Hybrid Membranes 670				
22.2 22.2.1 22.2.2 22.2.3	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic-Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672				
22.2 22.2.1 22.2.2 22.2.3 22.3	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic–Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672 Liquid–Liquid Membrane Contactors 672				
22.2 22.2.1 22.2.2 22.2.3 22.3 22.3.1	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic-Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672				
22.2 22.2.1 22.2.2 22.2.3 22.3 22.3.1 22.3.2	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic-Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672 Liquid-Liquid Membrane Contactors 672 Gas-Liquid Membrane Contactors 673 Gas-Gas Membrane Contactors 675				
22.2 22.2.1 22.2.2 22.2.3 22.3 22.3.1 22.3.2 22.3.3	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic–Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672 Liquid–Liquid Membrane Contactors 672 Gas–Liquid Membrane Contactors 673				
22.2 22.2.1 22.2.2 22.2.3 22.3 22.3.1 22.3.2 22.3.3	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic-Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672 Liquid-Liquid Membrane Contactors 672 Gas-Liquid Membrane Contactors 673 Gas-Gas Membrane Contactors 675 Membrane Contactors Promoting Chemical Reaction 676				
22.2 22.2.1 22.2.2 22.2.3 22.3 22.3.1 22.3.2 22.3.3	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic-Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672 Liquid-Liquid Membrane Contactors 672 Gas-Liquid Membrane Contactors 673 Gas-Gas Membrane Contactors 675 Membrane Contactors Promoting Chemical Reaction 676				
22.2 22.2.1 22.2.2 22.2.3 22.3 22.3.1 22.3.2 22.3.3 22.3.4	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic-Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672 Liquid-Liquid Membrane Contactors 672 Gas-Liquid Membrane Contactors 673 Gas-Gas Membrane Contactors 675 Membrane Contactors Promoting Chemical Reaction 676 References 676				
22.2 22.2.1 22.2.2 22.2.3 22.3.1 22.3.2 22.3.3 22.3.4	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic-Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672 Liquid-Liquid Membrane Contactors 672 Gas-Liquid Membrane Contactors 673 Gas-Gas Membrane Contactors 675 Membrane Contactors Promoting Chemical Reaction 676 References 676  Fuel Cell Membranes 679				
22.2 22.2.1 22.2.2 22.2.3 22.3.1 22.3.2 22.3.3 22.3.4 23.3	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic-Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672 Liquid-Liquid Membrane Contactors 672 Gas-Liquid Membrane Contactors 673 Gas-Gas Membrane Contactors 675 Membrane Contactors Promoting Chemical Reaction 676 References 676  Fuel Cell Membranes 679 Principles of the Fuel Cell 679				
22.2 22.2.1 22.2.2 22.2.3 22.3.1 22.3.2 22.3.3 22.3.4 23.1 23.2	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic-Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672 Liquid-Liquid Membrane Contactors 672 Gas-Liquid Membrane Contactors 673 Gas-Gas Membrane Contactors 675 Membrane Contactors Promoting Chemical Reaction 676 References 676  Fuel Cell Membranes 679 Principles of the Fuel Cell 679 Good Points of Fuel Cells 680				
22.2 22.2.1 22.2.2 22.2.3 22.3.1 22.3.2 22.3.3 22.3.4 23.1 23.2 23.1 23.2 23.3	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic-Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672 Liquid-Liquid Membrane Contactors 672 Gas-Liquid Membrane Contactors 673 Gas-Gas Membrane Contactors 675 Membrane Contactors Promoting Chemical Reaction 676 References 676  Fuel Cell Membranes 679 Principles of the Fuel Cell 679 Good Points of Fuel Cells 680 Membranes for Fuel Cells 681				
22.2 22.2.1 22.2.2 22.2.3 22.3.1 22.3.2 22.3.3 22.3.4 23.1 23.2 23.1 23.2 23.3 23.3	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic-Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672 Liquid-Liquid Membrane Contactors 672 Gas-Liquid Membrane Contactors 673 Gas-Gas Membrane Contactors 675 Membrane Contactors Promoting Chemical Reaction 676 References 676  Fuel Cell Membranes 679 Principles of the Fuel Cell 679 Good Points of Fuel Cells 680 Membranes for Fuel Cells 681 Polymer Membranes 681				
22.2 22.2.1 22.2.2 22.2.3 22.3.1 22.3.2 22.3.3 22.3.4 23.1 23.2 23.3 23.3 23.3.1 23.3.2	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic-Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672 Liquid-Liquid Membrane Contactors 672 Gas-Liquid Membrane Contactors 673 Gas-Gas Membrane Contactors 675 Membrane Contactors Promoting Chemical Reaction 676 References 676  Fuel Cell Membranes 679 Principles of the Fuel Cell 679 Good Points of Fuel Cells 680 Membranes for Fuel Cells 681 Polymer Membranes 681 Ceramic Membranes 681				
22.2 22.2.1 22.2.2 22.2.3 22.3.1 22.3.2 22.3.3 22.3.4 23.1 23.2 23.3 23.3.1 23.3.2 23.4	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic-Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672 Liquid-Liquid Membrane Contactors 672 Gas-Liquid Membrane Contactors 673 Gas-Gas Membrane Contactors 675 Membrane Contactors Promoting Chemical Reaction 676 References 676  Fuel Cell Membranes 679 Principles of the Fuel Cell 679 Good Points of Fuel Cells 680 Membranes for Fuel Cells 681 Polymer Membranes 681 Ceramic Membranes 681 Technology of Fuel Cells 682				
22.2 22.2.1 22.2.2 22.2.3 22.3.1 22.3.2 22.3.3 22.3.4 23.1 23.2 23.3 23.3.1 23.3.2 23.4 23.4.1	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic-Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672 Liquid-Liquid Membrane Contactors 672 Gas-Liquid Membrane Contactors 673 Gas-Gas Membrane Contactors 675 Membrane Contactors Promoting Chemical Reaction 676 References 676  Fuel Cell Membranes 679 Principles of the Fuel Cell 679 Good Points of Fuel Cells 680 Membranes for Fuel Cells 681 Polymer Membranes 681 Technology of Fuel Cells 682 Technology of Fuel Cells with Polymer Electrolyte Membranes 682				
22.2 22.2.1 22.2.2 22.2.3 22.3.1 22.3.2 22.3.3 22.3.4 23.1 23.2 23.3 23.3.1 23.3.2 23.4 23.4.1 23.4.2	Membranes for Membrane Contactors 669 Inorganic Membranes 669 Organic Membranes 670 Organic-Inorganic Hybrid Membranes 670 Technology of Membrane Contactors 672 Liquid-Liquid Membrane Contactors 672 Gas-Liquid Membrane Contactors 673 Gas-Gas Membrane Contactors 675 Membrane Contactors Promoting Chemical Reaction 676 References 676  Fuel Cell Membranes 679 Principles of the Fuel Cell 679 Good Points of Fuel Cells 680 Membranes for Fuel Cells 681 Polymer Membranes 681 Ceramic Membranes 681 Technology of Fuel Cells 682 Technology of Fuel Cells with Polymer Electrolyte Membranes 682 Technology of Fuel Cells with Inorganic Electrolyte Membranes 685				

24	Hybrid Systems of the Membrane Separation Process 695					
24.1	Hybrid Systems of Membrane Technology and Reactive Production Step, Other Separation					
	Technology 695					
24.2	Hybrid Systems with Plural Membrane Technology 705					
24.2.1	Haemodialysis–Dialysis Hybrid 705					
24.2.2	Dialysis–Reverse Osmosis Hybrid 706					
24.2.3	Nanofiltration–Reverse Osmosis Hybrid 706					
24.2.4	Ultrafiltration–Reverse Osmosis Hybrid 707					
24.2.5	·					
24.2.6	Microfiltration—Reverse Osmosis Hybrid 708					
24.2.7	Ultrafiltration–Nanofiltration Hybrid 709					
	Ultrafiltration—Membrane Distillation Hybrid 709					
24.2.8	Membrane Distillation–Forward Osmosis Hybrid 709					
24.2.9	Electrodialysis–Forward Osmosis Hybrid 710					
24.2.10	Forward Osmosis–Reverse Osmosis Hybrid 711					
24.2.11	Forward Osmosis–Nanofiltration Hybrid 711					
24.2.12	Forward Osmosis–Electrokinetic Hybrid 711					
24.2.13	Nanofiltration–Forward Osmosis–Reverse Osmosis Hybrid 712					
24.2.14	Ultrafiltration–Reverse Osmosis–Electrodialysis Reversal Hybrid 713					
	References 713					
25	Optical Resolution by Membranes 717					
25.1	Present Conditions and Problem of Optical Resolution with Membranes 717					
25.2	Membranes for Optical Resolution 718					
25.2.1	Liquid Membranes 718					
25.2.1.1	Emulsion Liquid Membrane 720					
25.2.1.2						
25.2.1.3						
25.2.2	Polymer Membranes 720					
25.3	Technology of Optical Resolution Membranes 721					
25.3.1	Liquid Membranes in Optical Resolution 721					
25.3.2	Solid Membranes in Optical Resolution 723					
	References 730					
26	Material Separations by Other Membrane Processes 735					
26.1	Carbon Nanotube Membranes 735					
26.1.1	Fabrication of Carbon Nanotubes 735					
26.1.2	Chemical Modification of Carbon Nanotubes 735					
26.2	Graphene Membranes 736					
26.3	<u> </u>					
26.3.1	Technologies of Carbon Nanotube and Graphene Membranes 738  Technology of Carbon Nanotube Membranes 738					
26.3.1.1	<del></del>					
26.3.1.2	·					
	Reverse Osmosis 741					
	Nanofiltration 742					
	Ultrafiltration 744					
	Microfiltration 744					
26.3.1.7	Gas Permeation 745					

xviii	Contents	
-------	----------	--

26.3.1.8	Pervaporation 746
26.3.1.9	Forward Osmosis 747
26.3.1.10	Membrane Distillation 748
26.3.1.11	Membrane Reactor and Membrane Contactor 749
26.3.2	Technologies of Graphene Membranes 750
26.3.2.1	Dialysis 750
26.3.2.2	Reverse Osmosis 750
26.3.2.3	Nanofiltration 751
26.3.2.4	Ultrafiltration 752
26.3.2.5	Microfiltration 753
26.3.2.6	Gas Permeation 754
26.3.2.7	Pervaporation 755
26.3.2.8	Forward Osmosis 756
26.3.2.9	Membrane Distillation 757
26.3.3	Comparison of Carbon Nanotubes and Graphene Membranes 757
26.3.4	Hybrids of Carbon Nanotubes and Graphene Membranes 759
	References 760

# 27 Conclusions and Prospects for the Future 769

Reference 771

Index *773* 

#### **Preface**

After reading this book, and having understood its contents, its biggest aim is to be able to contribute to new technical ideas more than existing membrane separation technologies.

At first it is essential to learn the history of the development of the separation membrane; the equilibrium phenomena of the solubility of the material and the electrochemical properties as the basic phenomena of the membrane properties of matter in the field of application, nonequilibrium phenomena such as the mass transfer, the quantitative understanding of various underlying phenomena, the problems of membrane separation technology and the solution methods for existing separation membranes are the same in all fields.

With that in mind, it is strongly wished that each researcher can suggest a new technique beyond the existing membrane separation technology with courage.

There is a membrane at all boundaries. A membrane of the thickness of the order of molecules exists even on a bare surface. Probably the only surface on which there is no membrane at all will be a solid surface newly cut under a high vacuum.

It was known for a long time that the surface of the plant cell had a cell wall. Also there is a membrane called a plasma membrane on the surface of an animal cell, and it came to be known that there is a great variety of filmy structure in the inside of the cell. It came to be recognized widely that it is the most important when the elucidation of the function pursues a life phenomenon.

In particular, from the viewpoint of saving resources, saving energy and environmental conservation, new techniques with membranes have attracted attention. For example, the development of water processing technology using an ion-exchange membrane and the reverse osmotic membrane was propelled by such a strong request. In addition, haemodialysis with a membrane, based on the artificial kidney, is at the forefront of medical technology, and has been used for the treatment of many patients. These technologies are fine examples that indicate the importance of the applied study of artificial membranes.

The principle of reverse osmosis was proposed as a new method for the desalination of seawater by Professor Breton at the University of Florida [1,2]. Today's prosperity of science and the technique of the polymer membrane are due to Professor Loeb and Sourirajan, who developed excellent semipermeable cellulose acetate membranes using their original membrane preparation method [3], and their membranes went into practical use [4]. And then Dr Kesting evaluated the remarkable developments in his book as being the 'golden age of membranology' [5]. Along with such developments has come a large number of books; commentary books have been published about the formation, structure, physical properties, function and application of polymer membranes in many countries from about 1970. Of these, a certain book establishes an important point of fundamental principle, a certain thing is main by the design of the module, and in addition, a certain one puts an important point for the function developed in as a general effect; a characteristic is devised with each book.

I engaged in the fundamentals and development study of polymer membranes and membranes that include polymers and have deepened my understanding about the basic matter that was indispensable in the study of membranes for 40-odd years.

Because the membrane exists as a partition of phases, the barrier characteristics, material permeability or separability, are the most important physical properties. The driving force of the material transportation through such membranes can involve a difference in chemical potential, a difference in electrical potential, a difference in pressure and a difference in temperature; and depending on the particular membrane, the naming of the material transportation is different, too. At first it is an important thing that we unify these and can look. Furthermore, these properties of matter may be modified in response to external stimulation, in this case not only the simple physical properties, but also the function of the membranes.

When a membrane caught some kind of outside stimulation, a fact to produce replies to support is defined as the function of the membrane. The permeability and separability are polymer responses that are brought about by a concentration gradient or a pressure gradient due to an external stimulation, but because they may not bring about a structural change of the polymer itself, a membrane function and way of speaking that it is said are usually done, but are the place where it is difficult whether it may be said that it is a polymer function.

However, in the biomembrane, membrane structure changes, for example, by outbreak of the specific material transmission and electric potential depending on stimulation like excitement phenomena and develops a chemical reaction. It may be said that this is a function enough. There is a thing indicating the behavior very similar to a reaction to participate in the function in the biomembrane with the heterogeneity structure of the artificial membrane as the inanimate object.

These permeability, separability and membrane functions are expressed by an index for the membrane as a whole, but they actually consist of a combination of some basic phenomena. To develop and improve a membrane it is necessary to understand these basic phenomena exactly. Furthermore, for an accurate understanding, quantification of the phenomenon must be accomplished.

In this book, we first describe the history and necessity for membrane science and technology. Thereafter, the structural design of the membrane, the relationship between the membrane formation conditions and the membrane structure are discussed in detail. Furthermore, various membrane preparation methods, shapes of membranes and membrane modules are introduced. And then the analyses of membrane characteristics by various methods are described. The thermodynamic basics of membrane transport phenomena and various transport models are discussed, and then the phenomena during membrane permeation in various kinds of membrane transport method and their solution methods are discussed. After the description of these basic matters, the principles of the various membrane permeation separation methods, fundamental analyses and applied technology are described from different angles. In addition, hybrid systems of membrane separation processes are discussed with interest.

#### References

- 1 Breton, E.J. Jr. (1957) Water and ion flow through imperfect osmotic membrane. Office of Saline Water, US Department of the Interior, Research & Development Progress Report, No. 16.
- 2 Reid, C.E., Breton, E.J. Jr. (1959) Water and ion flow across cellulosic membranes. Journal of Applied Polymer Science, 1, 133-143.

- 3 Loeb, S., Sourirajan, S. (1959) Sea water demineralization by surface skimming process. University of California, Los Angeles, Department of Chemical Engineering, Sea Water Research, Quarterly Progress Reports, No. 59-28.
- 4 Loeb, S., Sourirajan, S. (1963) Sea water demineralization by means of an osmotic membrane. In Saline Water Conversion – II. Advances in Chemistry Series, ACS 38. American Chemical Society, pp. 117–132.
- 5 Kesting, R.E. (1971) Synthetic Polymeric Membranes. McGraw Hill, New York.

# Acknowledgements

I studied the kinetics of the formation mechanism of thermosetting resins and the theory of their gelation from 1964 to 1970 and acquired the degree of the doctor of engineering in 1970. I began the study of polymer separation membranes when I became a teacher in Kansai University in 1970. I seemed to engage in the totally different study field at first, but I noticed that it was not so different a field when I looked from the point of view of handling molecules, and so decided that I would make separation membrane study a lifetime friend, and that has been the case for 40-odd years now and has culminated in the opportunity to write this book.

First, I express great gratitude in having got much encouragement and support from many friends during the writing of this book.

In particular, on the occasion of writing this book, I had great aid from Professor Takashi Miyata and Dr Akifumi Kawamura, co-workers in Kansai University. In the true work, the great help from Chisa Norioka (PhD postgraduate) and Kazuki Ueda, Kazuki Matsuo, Masaya Yamada, Yusuke Masuda, Toshiki Shimai, Yuki Tanaka, Saya Yamafuji and Shingo Yamashita (Masters postgraduates) in the preparation of figures, tables, schemes and so on will never be forgotten. Without their help, I think that this book would never have been completed. That is why I want express my great thanks to them. I also appreciate the help given by the associated members of John Wiley & Sons. Finally, I thank my wife, Tamiko Uragami, who always supplies mental support and great encouragement.

1

# Introduction to Membrane Science and Technology

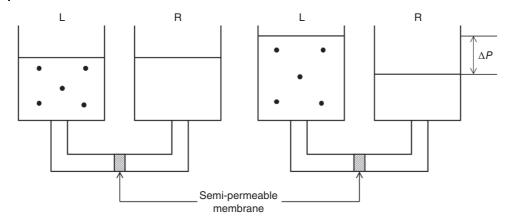
# 1.1 History of Membrane Science and Technology

The word 'osmosis' is used to describe the permeation of water through a diaphragm in contact on one side with a water–ethanol mixture and on the other side with pure water, as shown in Figure 1.1, a process discovered by Nollet in 1748 [1]. Probably, the relation between a semipermeable membrane and the osmotic pressure was recognized first by Nollet.

Graham carried out more systematic studies on mass transport in semipermeable membranes, studied the diffusion of gases through different media and, furthermore, discovered that rubber exhibits different permeabilities to different gases [2]. Membranes in the nineteenth and early twentieth centuries were not applied to industrial or commercial fields, but were used to analyse physical/chemical theories. As a good example, van't Hoff used the measurements of osmotic pressure of solutions with membranes to develop his limit law, to explain the behaviour of ideal dilute solutions, in 1887; this work led directly to the van't Hoff equation.

Most of the early studies on membrane permeation were carried out with natural membranes, such as bladders of pig, cattle, fish and sausage casings made of animal gut or gum elastics. Traube was the first to introduce an artificially prepared semipermeable membrane by precipitating cupric ferrocyanide in a thin layer of porous porcelain [3]. This type of membrane was used by Pfeffer in his fundamental studies on osmosis [4]. The theoretical treatment and much of the interpretation of osmotic phenomena and mass transport through membranes is based on the studies of Fick, who interpreted diffusion in liquids as a function of concentration gradients, and van't Hoff, who gave a thermodynamic explanation for the osmotic pressure of dilute solutions [5,6]. A little later, Nernst and Planck introduced the flux equation for electrolytes under the driving force of a concentration or electrical potential gradient [7,8]. With the classical publications of Donnan describing the theory of membrane equilibria and membrane potentials in the presence of electrolytes, the early history of membrane science ends with most of the basic phenomena satisfactorily described and theoretically interpreted [9].

Until about 1960, interest in membrane technology was mainly in the academic field. Cellulose nitrate, the first synthetic (or semisynthetic) polymer was studied by Schoenbein [10] in 1846. In 1855 Fick [11] used cellulose nitrate membranes in his classic study 'Über Diffusion'. In the same year, the concept of *solution*, that is, membrane–permeant interaction, to membrane permeation theory was proposed by L'hermite [12]. Thus, at the very outset, the cast of characters for the ongoing solution–diffusion drama was complete. In 1860, Schumacher dipped test tubes into cellulose nitrate (collodion) solutions and prepared the first tubular membranes [13]. Baranetzky [14] prepared the first



**Figure 1.1** Osmosis across the semi-permeable membrane.  $\Delta P$  is the hydrostatic pressure difference.

flat membranes in 1872. Bechhold [15] prepared the first series of microfiltration membranes of graded pore size in 1907 and was also the first to define the relationship between bubble point, surface tension and pore radius, and developed a method of making the first synthetic membranes by impregnating a filter paper with a solution of nitrocellulose in glacial acetic acid [16]. These membranes could be prepared and accurately reproduced with different permeabilities by varying the ratio of acetic acid to nitrocellulose. Nitrocellulose membranes were also used in the studies of Zsigmondy and Bachmann as ultrafilters to separate macromolecules and fine particles from an aqueous solution [17]. Based on a patent of Zsigmondy, Sartorius GmbH began in 1927 the production of a series of nitrocellulose membranes with various pore sizes. These membranes were used in microbiological laboratories in analytical applications.

Early attempts to control and vary porosity were largely empirical. Bechhold observed that permeability varied inversely with the concentration of polymer in the sol. Bigelow and Gemberling [18] studied the effects of drying time on the membrane preparation process. Zsigismondy *et al.* [19] and Elford [20] developed two series of graded pore-size membranes of cellulose nitrate. The former were the basis for the first commercial microfiltration membranes, which appeared in 1927 in Germany.

The concept of pore-size distribution was developed by Karplus, cited by Erbe [21], who combined bubble point and permeability measurements. The development of the first successfully functioning haemodialyser [22] was the key to the large-scale application of membranes in the biomedical area.

Industrial interest of the membrane separation technology suddenly increased from about 1950. On the other hand, with the progress in high polymer chemistry, a large number of synthetic polymers which are excellent for the preparation of new membranes with specific transport properties, excellent mechanical and thermal stability were provided. In addition, a comprehensive theory based on the thermodynamics of irreversible processes for membrane transport properties was proposed by Staverman [23] and Kedem and Katchalsky [24]. Merten described membrane processes based on postulating certain membrane transport models, such as the model of a diffusion—solution membrane [25].

In 1960 the important paper by Maier and Scheuermann [26] provided the basic mechanism which has since been utilized by Kesting to accommodate every (wet, dry and thermal) class of *phase inversion* membranes within its general framework. The two editions of *Synthetic Polymeric Membranes* [27,28] provide comprehensive coverage of phase inversion, which is by far the most versatile and important membrane fabrication process.

The beginning of the golden age of membrane science and technology depended significantly upon both the invention of reverse osmosis by Professor Reid [29] and the development of the asymmetric cellulose acetate membrane by Loeb and Sourirajan [30,31]. The development of a reverse osmosis membrane from cellulose acetate which gave high salt rejection and high fluxes at moderate operating pressures by Loeb and Sourirajan was a major advance toward the application of reverse osmosis membranes as an effective technology for the production of potable water from sea water.

The membrane developed by them was an asymmetric structure consisting of a dense skin layer, which determines the selectivity of salt and flux of desalinated water, and a porous layer that holds the mechanical strength of the whole membrane. The preparation of asymmetric cellulose acetate membranes is based on a phase inversion process in which a homogeneous polymer solution is converted into a two-phase system, such as a solid polymer-rich phase forming the solid polymer structure and a polymer lean phase making the liquid-filled membrane pores [27,28,32]. Soon, other synthetic polymers - such as polyamides, polyacrylonitrile, polysulfone and polyethylene - were used as basic material for the preparation of synthetic membranes in reverse osmosis desalination. These polymers often showed better mechanical strength, chemical stability, thermal stability and tolerance for bacteria than the cellulose esters as semi-natural material. However, cellulose acetate remained the dominant material for the preparation of reverse osmosis membranes until the development of the interfacial-polymerized composite membrane [33,34]. These membranes showed significantly higher fluxes, higher rejection, and better chemical stability, mechanical strength, tolerance for bacteria and chlorine sterility than the cellulose acetate membranes.

Microfiltration was developed in 1918 by Richard Zsigmondy, who is a Nobel Prize in Chemistry winner, and then he developed the ultrafiltration membrane in 1922 and established the basics of membrane separation technology as one of founders of Sartorius. In medicine, dialysis (from Greek dialusis, 'διάλυσις', meaning dissolution, dia, meaning through, and lysis, meaning loosening or splitting) is a process for removing waste and excess water from the blood and is used primarily as an artificial replacement for lost kidney function in people with kidney failure (https://en.wikipedia.org/wiki/Dialysis). Electrodialysis (ED) is used to transport salt ions from one solution through ion-exchange membranes to another solution under the influence of an applied electric potential difference. This is done in a configuration called an electrodialysis cell. The cell consists of a feed (dilute) compartment and a concentrate (brine) compartment formed by an anion exchange membrane and a cation exchange membrane placed between two electrodes. (https://en.wikipedia.org/wiki/Electrodialysis). This method was proposed for the first time in 1890 by Maigrot and Sabates [35]. Reverse osmosis was proposed by Reid and Breton [29] and developed by Loeb and Sourirajan [30] for the desalination of sea water.

Nanofiltration is a relatively recent membrane filtration process used most often with low total dissolved solids water, such as surface water and fresh groundwater, with the purpose of softening (polyvalent cation removal) and removal of disinfection by-product precursors, such as natural organic matter and synthetic organic matter. Nanofiltration is also becoming more widely used in food processing applications, such as dairy, for simultaneous concentration and partial (monovalent ion) demineralization (https://en.wikipedia.org/wiki/Nanofiltration). Nanofiltration was known as lowpressure reverse osmosis and came to gradually attract attention from the second half of 1980, and the first applications were reported by Eriksson [36], Colonlon and McClellan [37].

Sir Thomas Graham carried out the first membrane gas separation and obtained oxygen-enriched air containing 46.6% oxygen. He proposed that increasing the pressure of a gas mixture to be separated should be beneficial for obtaining higher fluxes. He observed that changes in the thickness of films affect the flux but not the composition of permeated gas. He noted the effect of temperature on permeation rates [38].

Pervaporation is one of the most popular areas of current membrane research, but the concept of pervaporation separation is not new. As early as 1906, Kahlenberg reported a qualitative study on the separation of a mixture of a hydrocarbon and an alcohol through a rubber membrane [39]. As early as 1917, it was recorded that water permeated through collodion films selectively, and the term pervaporation was first introduced by Kober [40]. Schwob [41] demonstrated dehydration of alcohols by using 20  $\mu$ m thin membranes. However, an analysis of pervaporation literature and patents showed that most of the work in the field was done in more recent times [42]. In 1955, Hagerbaumer conducted the first quantitative investigation with a microporous Vycor glass membrane with a high-pressure drop across it, to allow for the separation of liquid–liquid mixtures [43]. It was the work by Binning and co-workers [44,45] from 1958 to 1961 that established the principles and highlighted the potential of pervaporation separation.

Later, in 1965, Binning and co-workers utilized this operation of separating a liquid—liquid mixture into a vapour mixture using a nonporous polymeric film. This research yielded a high degree of separation along with high permeation rates. The process did not come into commercial use until 1982 when Gesellchaft für Trenntechnik mbH (GFT) of Germany installed a pervaporation plant to separate water from concentrated alcohol solutions. Since then, more than 100 plants have been installed. Recently, Exxon has used pervaporation in its refineries to separate hydrocarbon mixtures containing aromatics and aliphatics. Another commercial use for pervaporation is the removal of methylene chloride from small waste streams [46].

Membrane distillation was developed more than 50 years ago. It is a thermally driven separational programme in which separation is enabled due to phase change. A hydrophobic membrane displays a barrier for the liquid phase, allowing the vapour phase (e.g. water vapour) to pass through the membrane's pores. The driving force of the process is given by a partial vapour pressure difference commonly triggered by a temperature difference (https://en.wikipedia.org/wiki/Membrane\_distillation).

A membrane reactor is a physical device that combines a chemical conversion process with a membrane separation process to add reactants or remove products of the reaction. Chemical reactors making use of membranes are usually referred to as membrane reactors. The membrane can be used for different tasks, such as separation – selective extraction of reactants and retention of the catalyst, distribution/dosing of a reactant and catalyst support (often combined with distribution of reactants). Membrane reactors are an example for the combination of two unit operations in one step; for example, membrane filtration with a chemical reaction.

Uragami *et al.* [47] proposed 'evapomeation (EV)' as a new membrane separation technique method to improve a fault of pervaporation in 1988. This EV has some advantages, such as an improvement of membrane performance with the repression of swelling or shrinking of the membrane due to the feed liquids [48–53] (see detail in Chapter 16) and gives excellent dehydration, organic permselectivity of aqueous organic mixtures and separation of organic–organic liquid mixtures.

Uragami and co-workers also proposed temperature-difference controlled evapomeation (TDEV), further developing the EV method. In this TDEV method, the temperature of membrane surroundings is set less than that of the feed liquid (see detail in Chapter 17) [48–51,54–65].

The first carrier transport experiment was carried out by Osterhout, who investigated the transport of ammonia through algae cell walls [66]. Gliozzi explained biologically the couple transport mechanism in liquid membranes, as shown in Figure 1.2 [67].

About the middle of 1960s a number of couple transport systems were studied by Shean and Sollner [68]. Bloch *et al.* published the first paper on coupled transport [69], and the separation of uranium using phosphate ester carriers was later reported [70,71].

Table 1.1 summarizes the history of membrane processes and materials.