

# SEPARATOR: PRINCIPLES AND DESIGN

*MAB 4633/ EMB 5443*

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# SEPARATOR?

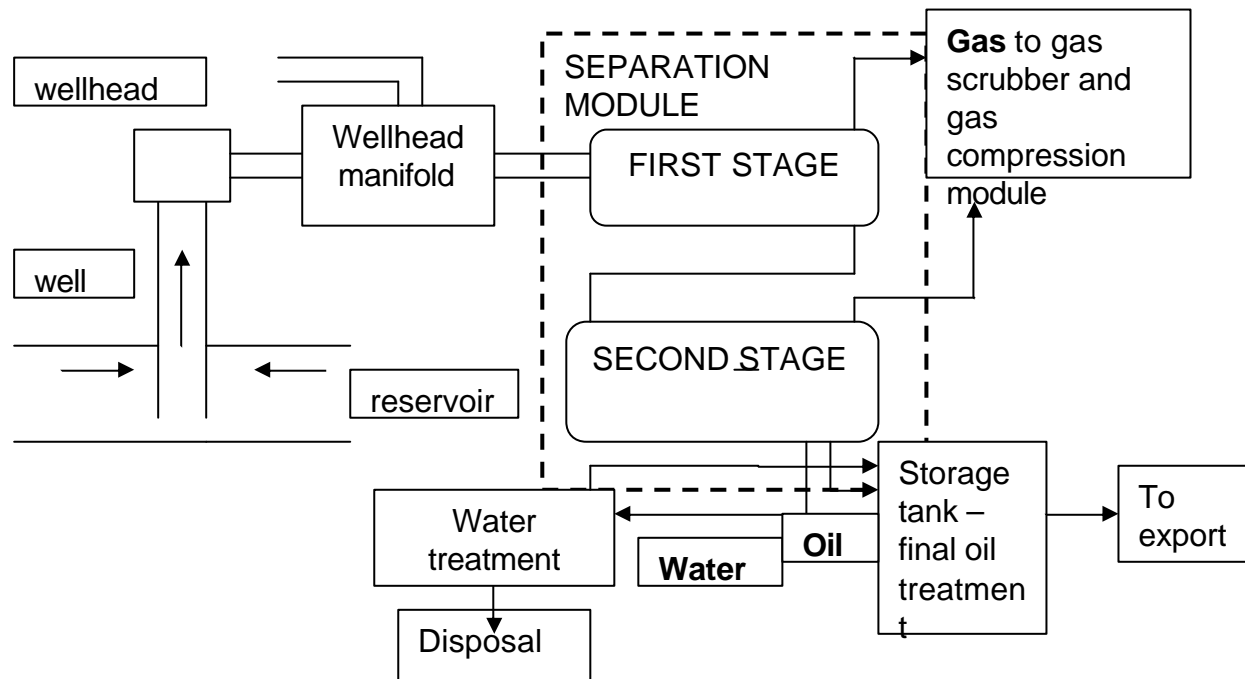


# SEPARATOR...



# The production process...

*“SEPARATORS form the HEART of the production process”*





# FUNDAMENTALS



# What is a separator?

- A SEPARATOR is a pressure VESSEL designed to DIVIDE a combined liquid-gas system into individual COMPONENTS that are relatively free of each other for SUBSEQUENT PROCESSING or disposition



# Why separator is needed?

- Downstream equipment cannot handle gas-liquid mixtures
  - Pumps require gas-free liquid
  - Compressor/ dehydration equipment require liquid-free gas
  
- Product specifications has limits on impurities
  - Oil should not contain  $> 1\%$  BS&W
  - Gas sales contract  $\rightarrow$  no free liquids in gas
  
- Measurement devices (metering) for gases/liquids highly inaccurate when the other phase is present



# How separation happens?

## Principles of separation!

### ■ Momentum

- Fluid phases at different densities have different momentum
- Changes in fluid direction will separate fluids at different momentum

### ■ Gravity

- Liquid phase separated from gas due to difference in weight of droplets

### ■ Coalescence

- Small droplets coalesced when “combined” together
- Coalescing devices force small droplets flowing through it to collide, form larger droplets and then settling out of the gas phase by gravity





# What properties affect separation?

- Gas and liquid flow rates
  - Operating & design pressures and temperatures
  - Surging or slugging tendencies of the feed streams
  - Fluid physical properties – density, compressibility
  - Desired phase separation - gas-liquid or liquid-liquid
  - Desired degree of separation - e.g. remove 100% particles >10 micron in size
  - Presence of impurities – paraffin, sand, scale
  - Foaming tendencies
  - Corrosive tendencies
- Must know and understand the characteristics of the flow stream in order to design separators!**



# Separator classification and types

## ■ Classification

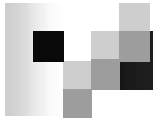
- Two-phase separation (gas-liquid)
- Three-phase separation (liquid-liquid i.e. water/oil/gas separation)

## ■ Types

- Gravity separators
  - Horizontal
  - Vertical
  - Spherical
- Centrifugal separators

(effect of gravity is enhanced by spinning the fluids at a high velocity)

**Selection of separators is based on obtaining the desired results at the lowest cost**



# BASIC SEPARATOR CONSTRUCTION

Source: International Training &  
Development, M. Stewart



# We focus on *gravity* separators...

- Working principle: Depends on density difference between the phases to be separated
- They are large cylindrical pressure vessels (up to 5 m diameter and 20 m long)
- Used in either 2-phase or 3-phase separation
- Mounted in a series of 2, 3 or even 4 separators
- Mounted either vertically or horizontally



# 4 main sections...

## 1. INLET DIVERTER

- Primary section

**Must remember these!**

## 2. GRAVITY SETTLING

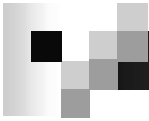
- Secondary section

## 3. MIST EXTRACTOR

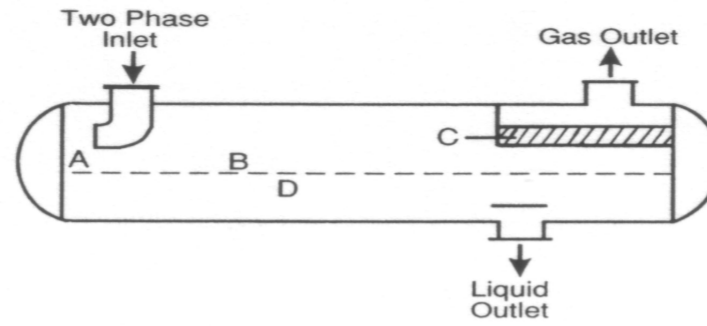
- Coalescing section
- Gas outlet

## 4. LIQUID COLLECTION

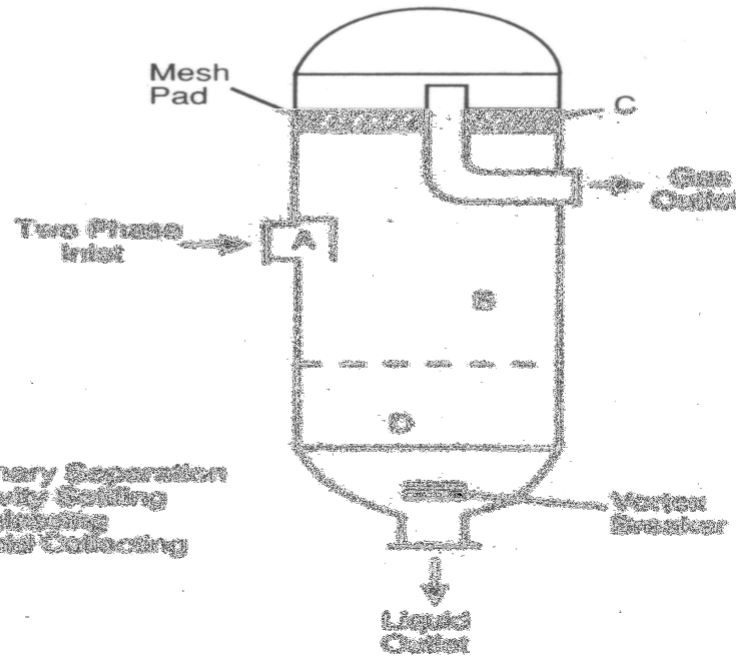
- Sump section
- Liquid outlet under level control to evacuate liquid



### HORIZONTAL



### VERTICAL



- A - Primary Separation
- B - Gravity Settling
- C - Gaslifting
- D - Liquid Collecting



# 4 main principles...

## 1. MOMENTUM

- Occurs at inlet diverter
- Initial separation of gas phase from the free liquid phase → gross separation
- Fluid stream hits diverter, changes its flow direction, fluids at different momentum are separated



## 2. GRAVITY

- Occurs at gravity settling section
- As gas flows through the section, gravitational force causes small liquid droplets to fall out from the gas stream
- Droplets then fall to the gas-liquid interface below → droplet settling section
- 100 to 400 micron droplet removal





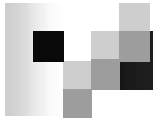
### 3. COALESCING

- Occurs at mist extractor
- Before gas leaves vessel, it flows through mist extractor → 99% droplets >10 micron removed
- Refine gross separation by removing the remaining entrained mist (very small liquid droplets) from gas phase
- Mist extractor uses vanes, wire mesh or plates

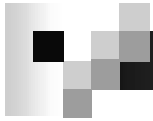


#### 4. “EQUILIBRIUM”

- Occurs at liquid collection
- Provide *retention time* required to allow entrained gas to evolve out from the liquid phase and rise to the vapour space
- After a certain period of retention time, phases become equilibrium with each other and separated ‘naturally’ due to density differences



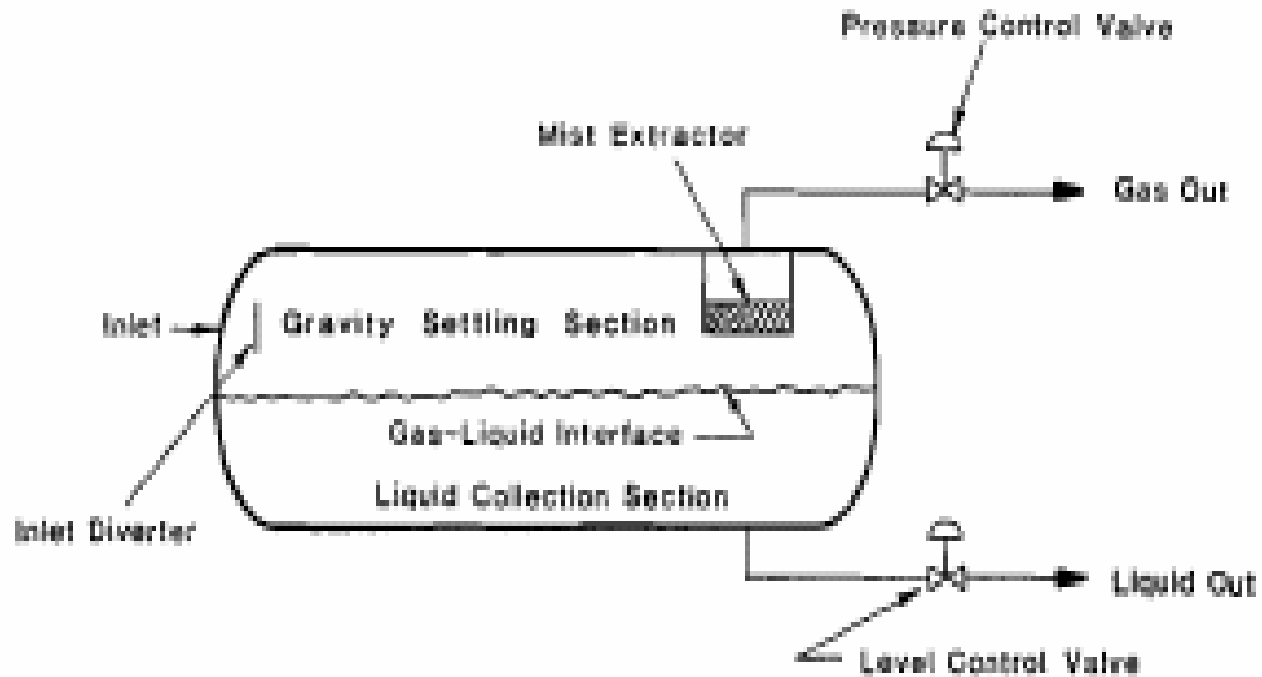
# TWO-PHASE (GAS-LIQUID) SEPARATION



# Main types

- HORIZONTAL separator
- VERTICAL separator
- SCRUBBERS

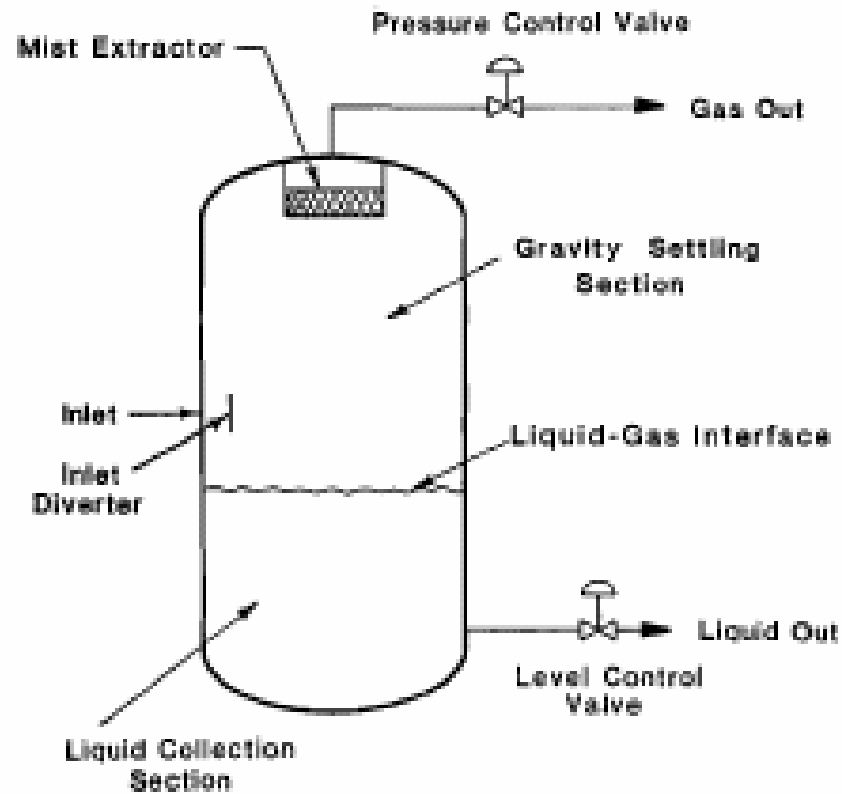
# *Horizontal (2-P) separator*



**Operation ?**

Source: International Training &  
Development, M. Stewart

# *Vertical 2-P separator*



Source: International Training & Development, M. Stewart



## *Horizontal - advantages...*

- Horizontal separators smaller and less expensive than vertical for given gas capacity
  - In gravity settling section, liquid droplets fall perpendicular to the gas flow
  - So more easily separated out of gas continuous phase
  - Interface area also larger so easier for gas bubbles that come out of the liquid phase to reach vapour space



## *Cont.*

- Horizontal separators offer greater liquid capacity
  - Well suited for liquid-liquid separation
  - And foaming crude





## *Vertical - advantages...*

- Good in handling solids
  - Liquid dump can be placed at bottom centre so that solids don't build up inside
    - Continue to next vessel
    - or install drain that allows solid to be disposed periodically
  
- Less plan area for same separation
  - Very important in offshore platforms



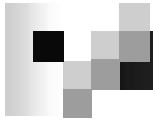
## *Cont.*

- Larger liquid SURGE capacity for same flow rate
  - For same liquid surface elevation, vertical has smaller increase in liquid volume than horizontal
  - High level (shutdown) controller could be placed much higher than normal operating level – so level controller and dump valve have more time to react to surge

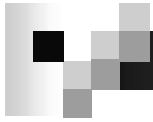


# *Scrubbers*

- Designed to recover liquids carried over from production separators or condensers after initial separation
- Liquid loading level much lower than separator
- Applications
  - Upstream of compressors
  - Downstream of coolers (liquids can condense)
  - Upstream of dehydration equipment
  - Upstream of a vent or flare outlet



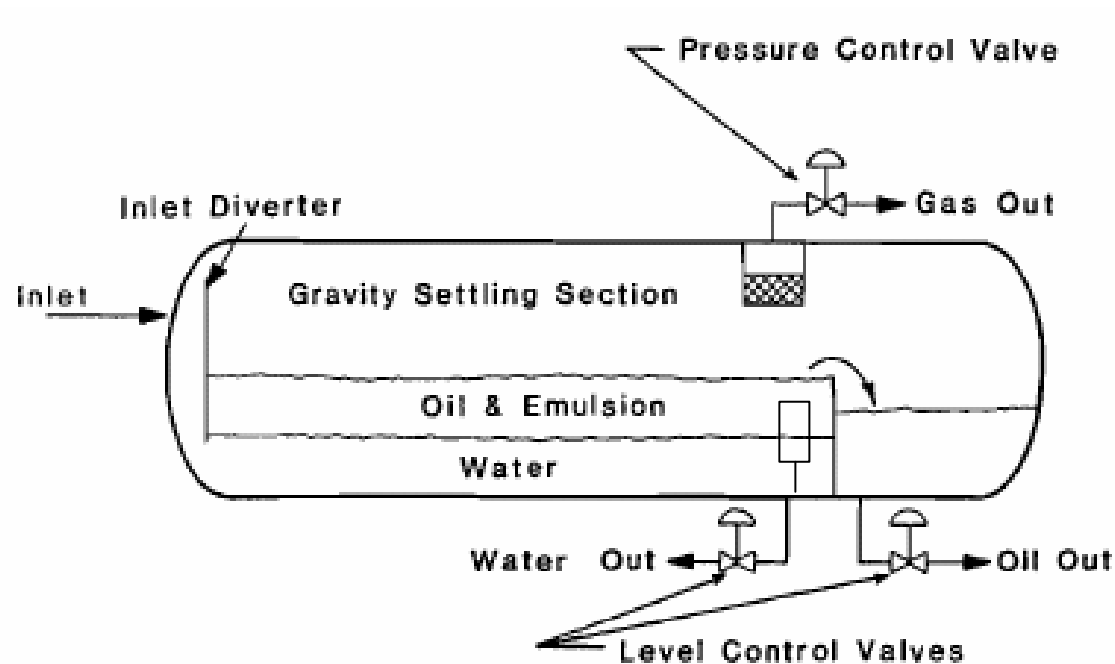
# THREE-PHASE (OIL-WATER) SEPARATION



# Types (Horizontal and/or Vertical)

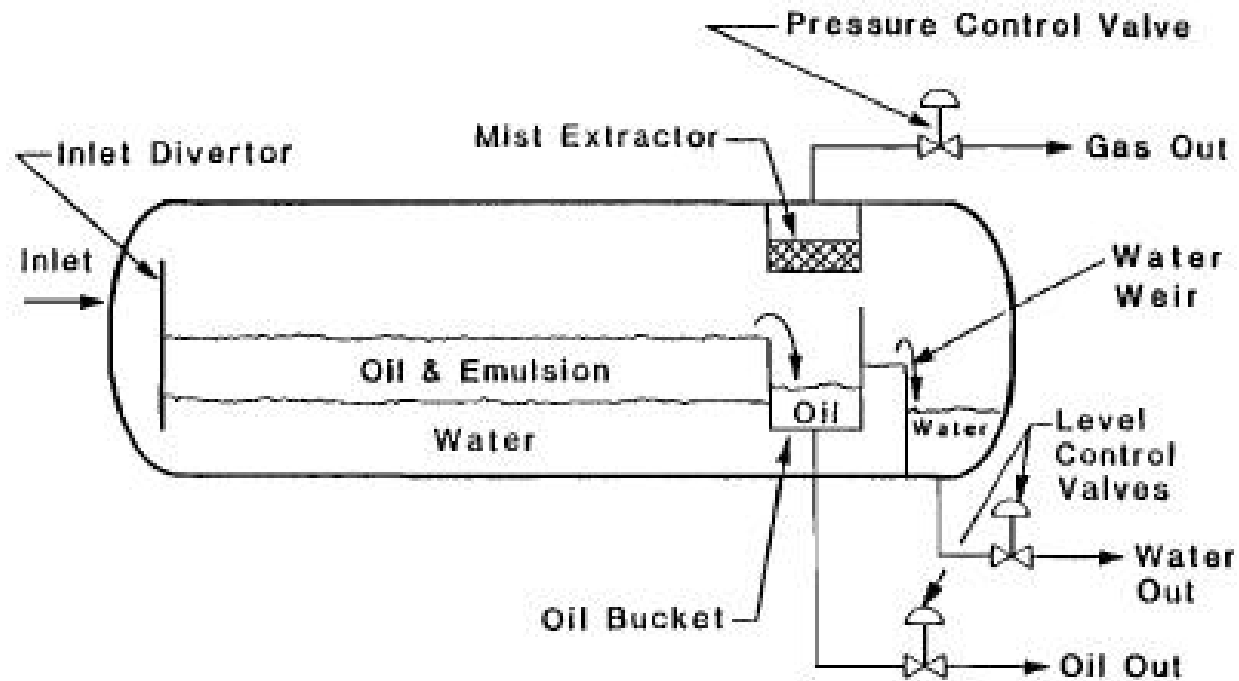
- Interface level control design
- Bucket-and-weir design

# Horizontal (3-P) Separator – Interface level controller design



Source: International Training &  
Development, M. Stewart

# Horizontal (3-P) Separator – “Bucket-and-Weir” design



Source: International Training &  
Development, M. Stewart



# Operation of 3-P separation...


- Inlet diverter → gross separation
- **Downcomer** → directs liquid flow below oil-water interface
- Liquid collection
  - Oil/water mixture then mixes with water continuous phase → “**Water-washing**”
  - By “water-washing”, water droplets entrained in oil continuous phase will **coalesce**
  - Oil and emulsion has sufficient time to form layer of “oil pad” & Free water settles to bottom





# *Interface level control*

- Located at the oil-water-interface
- Senses the height of the interface → sends signal to water dump valve
- If level reach “high level” then fully open water valve
- If level “low level” then fully close valve
- Advantage
  - Easily adjustable to handle unexpected changes in oil/water specific gravity or flow rates
- Disadvantage
  - Heavy oil/large amount of emulsions, paraffin → difficult to sense interface level



## *Bucket-and-Weir design*

- Alternative of not using *interface* level controller
- Has oil bucket and weir, and water weir
- Level controller for both oil and water uses displacer float → both connected to dump valve
- But design decrease liquid capacity
- **Critical → height of water weir sufficiently below oil weir height**
  - To provide **sufficient oil retention time**, so that oil will not be swept under oil box and out of water outlet
  - Why? Because oil/water **specific gravity** or **flow rates** changes

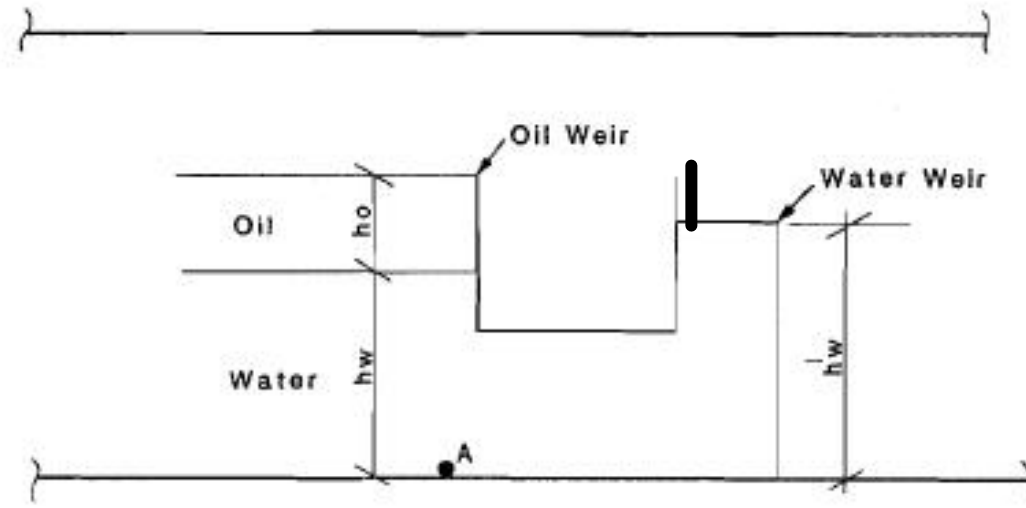
**“Balancing” effect**



# Cont.

- **Height of oil weir** controls **liquid level** in vessel
- **Difference** in height of oil weir and water weir controls the **thickness of oil pad**
  - Oil pad thickness changes as specific gravity or flow rate changes
  - HOW?
  - So, either oil or water weir is adjusted so that these changes can be accommodated

# Determination of oil pad thickness



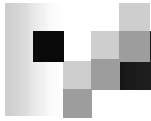
$$\Delta h = h_o \left[ 1 - \frac{r_o}{r_w} \right]$$

**Remember  
the derivation  
of the equation!**

$\Delta h$  = distance below oil weir (in)

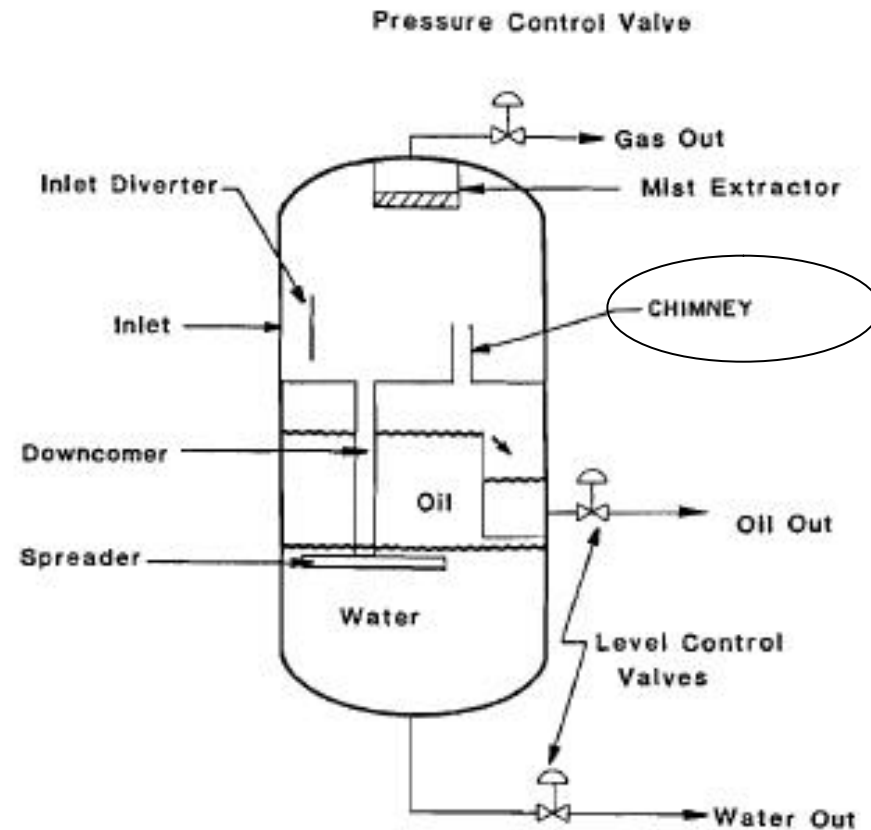
$h_o$  = desired oil pad height (in)

Source: International Training &  
Development, M. Stewart



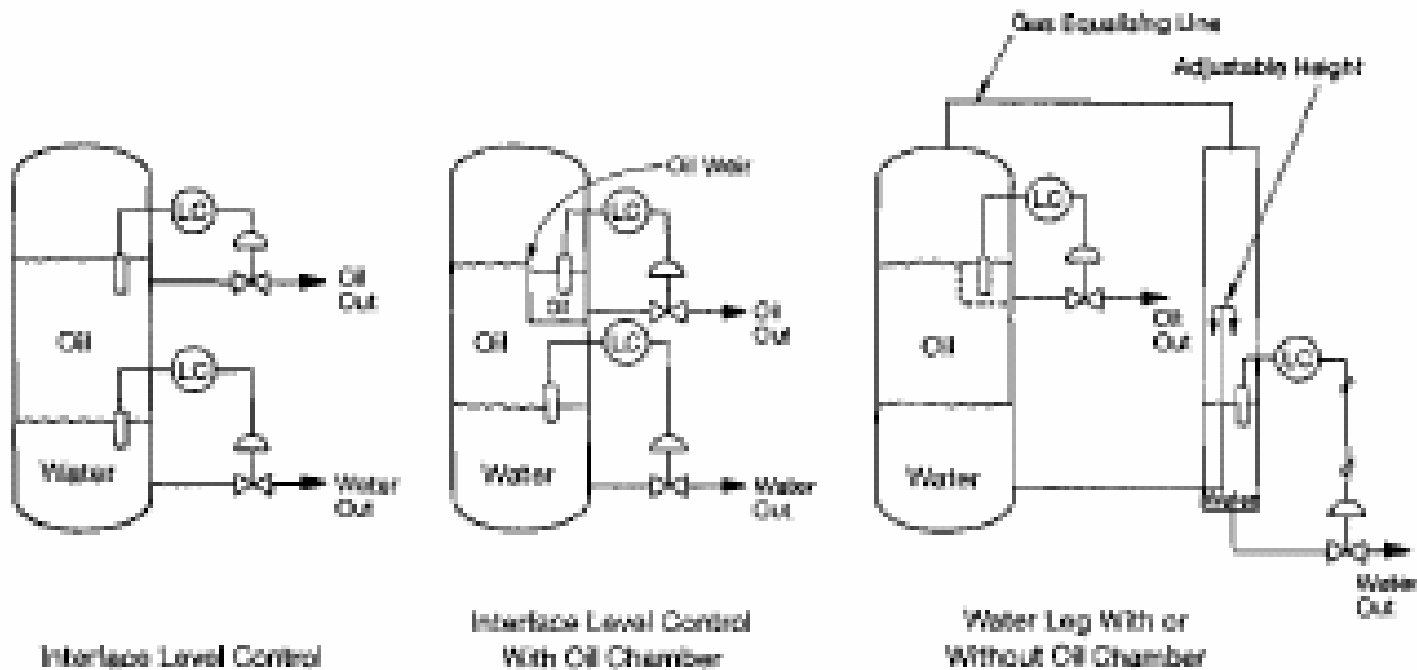
- But, this equation assumes NO inflow
- If there is inflow, then problem
  - Large oil inflow
    - Top oil rise, oil pad thicker
    - Oil pad thick could make oil swept below oil bucket
    - To accommodate this, make oil bucket deeper
  - Large water inflow
    - Water flow over water weir rises
    - At same time, pushes oil pad up and oil flows into oil weir rises
    - So what to do? Make weirs as long as possible

# Vertical 3-P separator – “Bucket-and-weir” design



Source: International Training &  
Development, M. Stewart

# Vertical 3-P separator – Interface Level Controller design



**Know the advantages and disadvantages of each method**

Source: International Training &  
Development, M. Stewart



# VESSEL INTERNALS





# Main Vessel internals

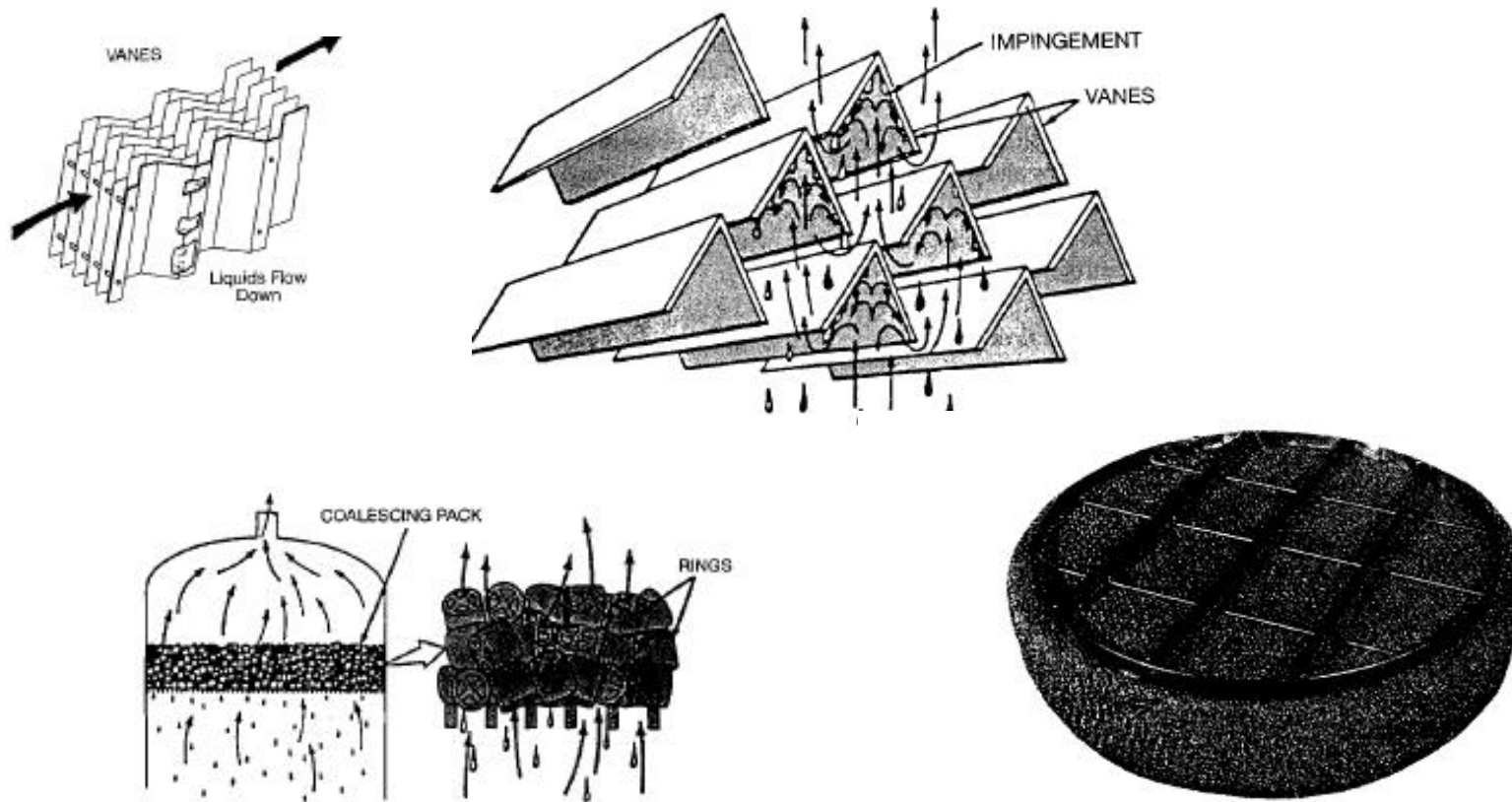
- Inlet diverter

- Baffle plates or centrifugal diverters
- Baffle plates → spherical dish, flat plate, cone etc

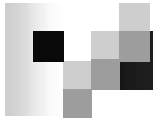
- Mist extractor

- As gas flows through the vanes / wire mesh, it makes numerous directional changes
  - Due to greater mass, liquid droplets cannot follow the rapid change in flow direction
  - These droplets impinge and collect on vanes / mesh

# *Types of mist extractor...*



Source: International Training & Development, M. Stewart



# Production Problems

Source: International Training &  
Development, M. Stewart



# Operational Production Problems

- Foaming
- Solids
  - Scale
  - Wax
  - Asphaltenes
  - Sand
- Emulsion
- Surging flow → high, instantaneous feed rates which cause level to rise above normal operating values
- Liquid carry over and Gas blowby



**END.**  
**THE REST YOU READ YOURSELF, OK...**